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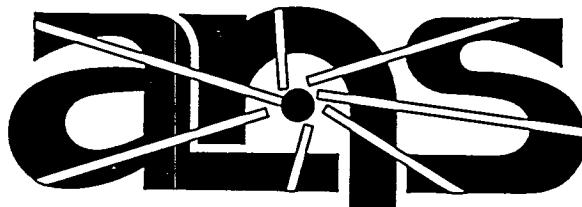
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**RELAP5 Model for
Advanced Neutron Source Reactor
Thermal-Hydraulic Transients,
Two-Element-Core Design**

N. C. J. Chen
M. W. Wendel
G. L. Yoder

November 1995

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Advanced Neutron Source

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Engineering Technology Division

RELAP5 Model for Advanced Neutron Source Reactor Thermal-Hydraulic Transients, Two-Element-Core Design

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February 1996

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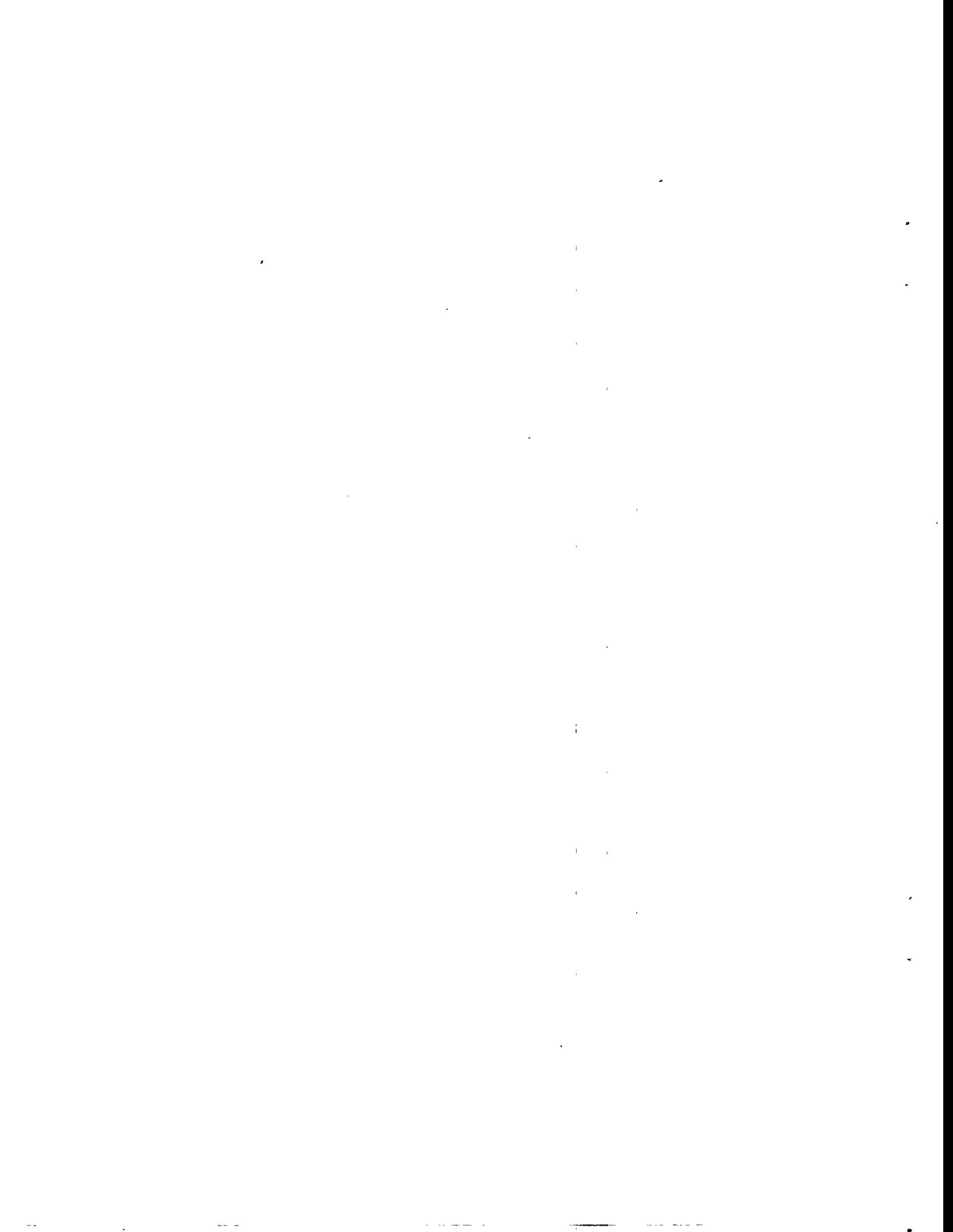
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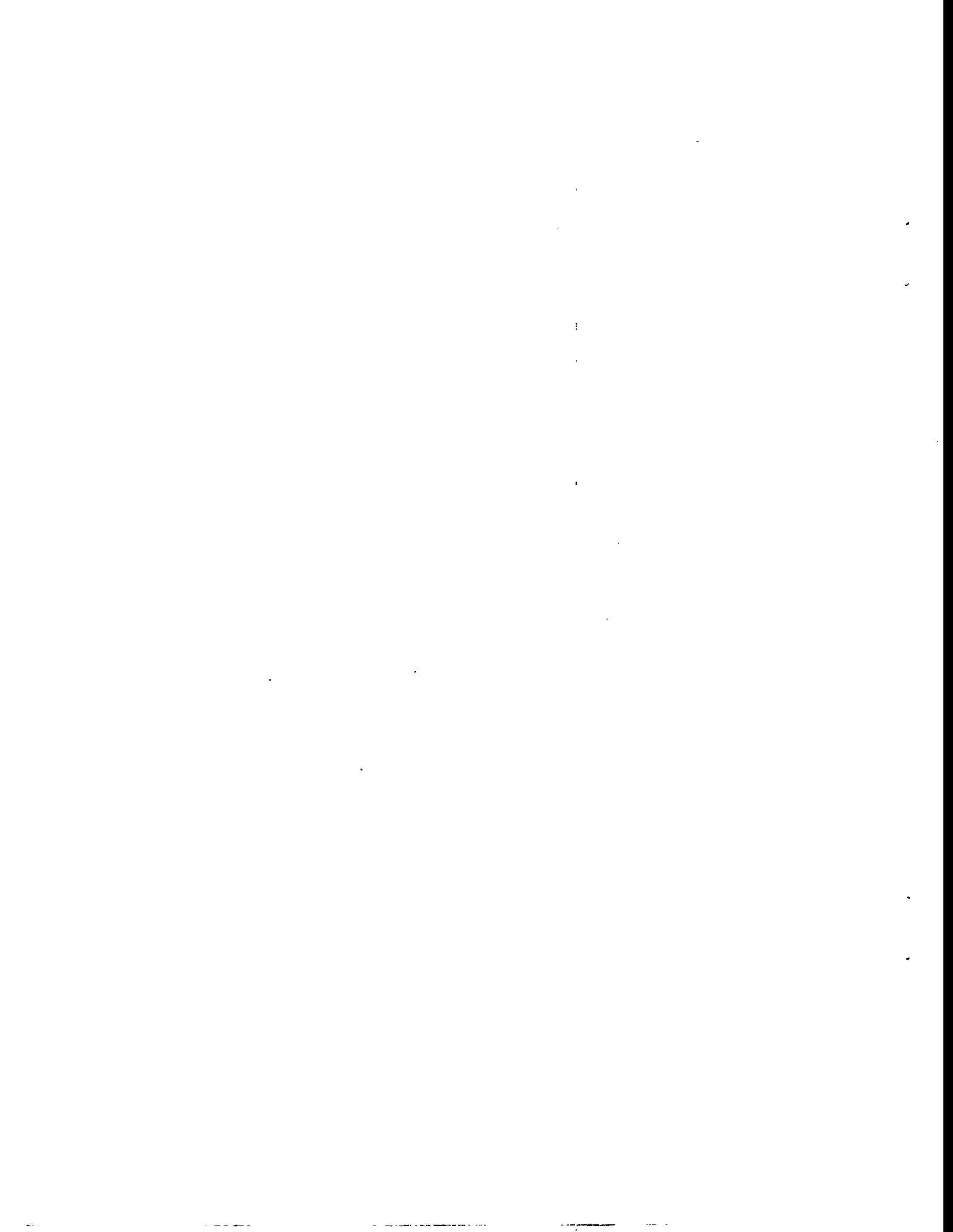
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LIST OF ACRONYMS

ANSR	Advanced Neutron Source Reactor
BOC	beginning-of-cycle
CCFL	counter current flow limit
CHF	critical heat flux
CPBT	core pressure boundary tube
CPU	central processing unit
CR	control rod
CSAR	conceptual safety analysis report
CV	control variable
EHX	emergency heat exchanger
FE	flow excursion
HFIR	High Flux Isotope Reactor
HS	hot spot
HTC	heat transfer coefficient
IB	incipient boiling
INEL	Idaho National Engineering Laboratory
LOSP	loss-of-offsite power
MHX	main heat exchanger
NEPL	nonexceedance probability level
NPSH	net positive suction head
OSV	onset of significant void
PID	Proportional Integral Derivative
PSVAW	primary supply vessel adapter weldment
PVM	Parallel Virtual Machine
RDA	rapid depressurization accident
SF	scaling factor
SZ	Saha-Zuber
TDJ	time dependent junction
TDV	time dependent volume



NOMENCLATURE

Symbol	Definition	Units
A	Cross-sectional area	m ²
C_d	Discharge coefficient	-
dh	Volume hydraulic diameter	m
dZ	Volume elevation rise	m
e	Surface roughness	m ²
f	Friction coefficient	-
g	Coolant gap dimension	m
HAN	Dimensionless homologous pump parameter	-
HVN	Dimensionless homologous pump parameter	-
K_f	Forward loss coefficient	-
K_r	Reverse loss coefficient	-
L	Volume length	m
r	Radial dimension	m
Re	Reynolds number	-
q_{COSTA}	Costa limiting heat flux	MW/m ²
s	Fuel plate span	m
SF	Control variable scaling factor	varies
t_{oxide}	Oxide thickness	m
T_{bulk}	Fluid bulk temperature	K
T_{sat}	Saturation temperature	K
T_w	Wall temperature	K
v	Pump flow ratio	-
v_j	Liquid velocity at a junction	m/s
α	Pump speed ratio	-
α_j	Liquid void fraction at a junction	-
ΔP	Pressure drop	Pa
Δx	Clean fuel plate thickness	m
ρ_j	Liquid density at a junction	kg/m ³



RELAP5 Model for Advanced Neutron Source Reactor Thermal-Hydraulic Transients, Two-Element-Core Design

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ABSTRACT

In support of the conceptual safety analysis report (CSAR) for the Advanced Neutron Source Reactor (ANSR), a RELAP5 thermal-hydraulic input model has been developed. The purpose of the model is to quantify the ANS thermal safety margin during a rapid depressurization accident (RDA) and during a loss-of-offsite power (LOSP).

This report contains a detailed description of the input for each RELAP5 component, or a reference where a description for that input may be found. Justification for the assumptions made in developing the RELAP5 model is provided wherever possible. In addition to the RELAP5 component input, the control variables used for various system actions and for auxiliary output are described.

1. INTRODUCTION

In support of the conceptual safety analysis report (CSAR), a RELAP5/MOD3 Version 8K0 thermal hydraulic input model for the primary cooling system of the Advanced Neutron Source Reactor two-element-core G693 design has been developed. This model has been used for simulating postulated transients (Chap. 15 of the CSAR) involving the primary coolant system. This report describes in detail the RELAP5 input model.

The input model consists of thermal-hydraulic components, heat structures, neutronics model, material property data, and control logic. Thermal hydraulic components are used to define the geometry, connectivity, and boundary conditions of the primary coolant contained within the primary coolant pressure boundary. Heat structures are used to define the geometry and configuration of conducting solids (e.g., piping and fuel plates) important to the thermal behavior of the primary coolant system. The neutronics model is a one-dimensional (point kinetics) model that is used to define the transient behavior of the distributed neutronic heat source in the ANSR. Material property data are supplied to define the thermal conductivity and specific heat for each of the materials comprising the heat structures. The control logic is used to define the dynamic behavior of the reactor control systems (control variables, trips, and general tables), to facilitate post-simulation analysis (minor edit and control variables), and to control directly the numerical simulation (RELAP5 time-step control cards). Appendix A contains a complete listing of the input model.

Special ANSR updates to the RELAP5/MOD3 program are invoked in the core heat structures to use the Petukhov¹ correlation for heat transfer and Gambill-Weatherhead^{2,3} critical heat flux (CHF) correlation and in the fuel channels to use the Griffith⁴ drift flux correlation. As part of the post-processing, the following other thermal limits besides CHF are examined:

1. Costa⁵ onset of significant void (OSV) correlation, used to predict the point of flow excursion (FE),
2. Bergles/Rohsenow⁶ incipient boiling correlation,
3. Saha/Zuber⁷ OSV correlation, and
4. A local modification⁸ of the Saha/Zuber correlation.

No modifications have been made to the RELAP5 code to examine these other limits.

The nodalization diagram for the RELAP5 model is given in Fig. 1 (core region) and Fig. 2 (loop region).

Some of the assumptions that have been made in developing the model are:

1. The choking option has been disabled at all junctions, unless indicated otherwise. Previous problems have been observed with the choking model giving unrealistic results at internal junctions and causing the code to bomb.
2. The reactor pool temperature is assumed constant at 38°C (311.15 K).
3. The secondary coolant supply temperature is assumed constant at 29.4°C (302.55 K).

For all transient simulations, the initial conditions are at a perturbed state from nominal, in the conservative direction, by the amount necessary to account for measurement error and routine control variations:

1. reactor power: +4.2% (ref. 9)
2. primary pressure: -5% (ref. 8)
3. core inlet temperature: +0.6°C (ref. 8)
4. primary flow: maintained at the nominal flow rate being constrained such that the upper core inlet velocity is 25 m/s inside the fuel channel.

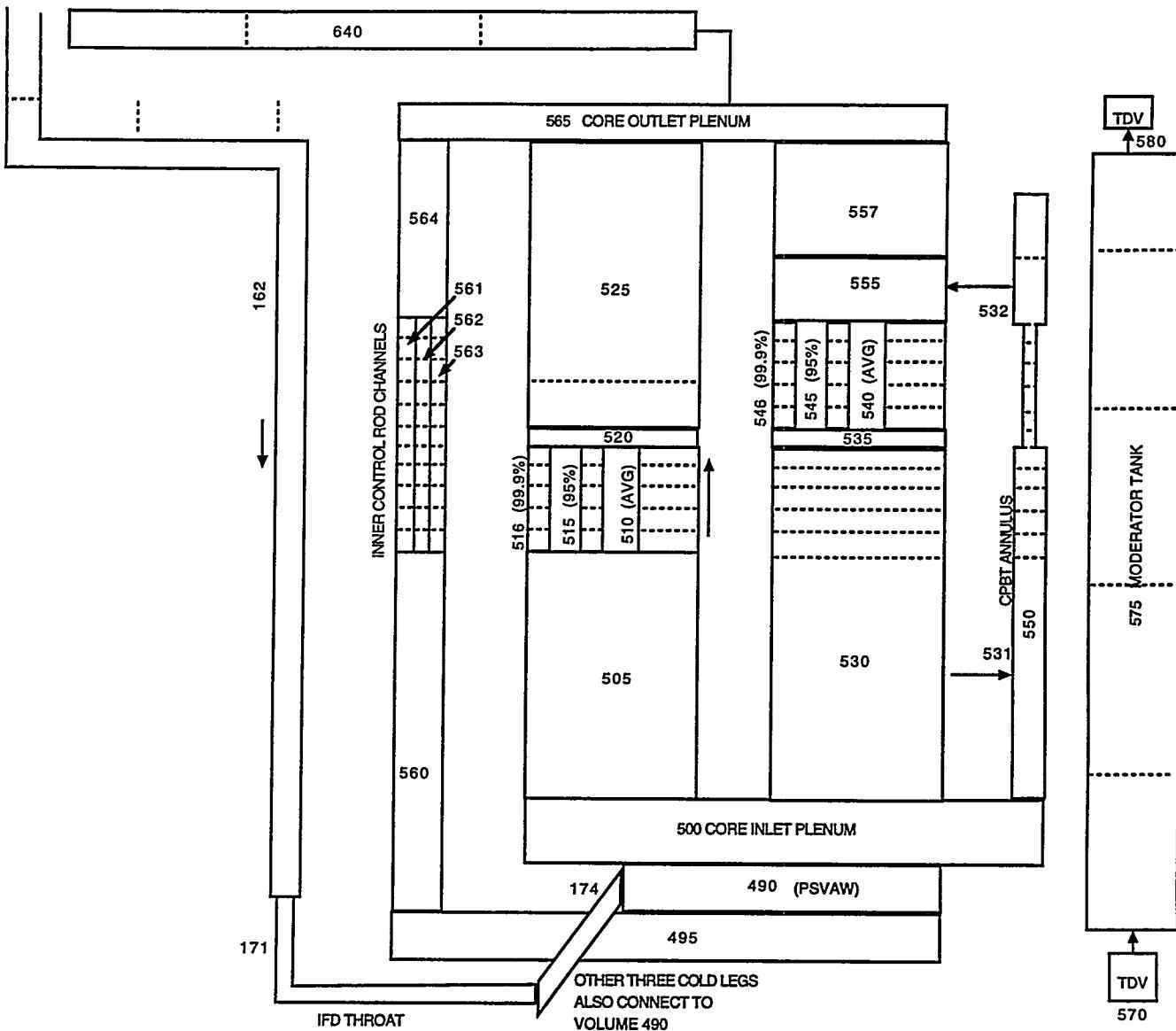


Fig 1. ANS two-element-core RELAP5 nodalization diagram: core region.

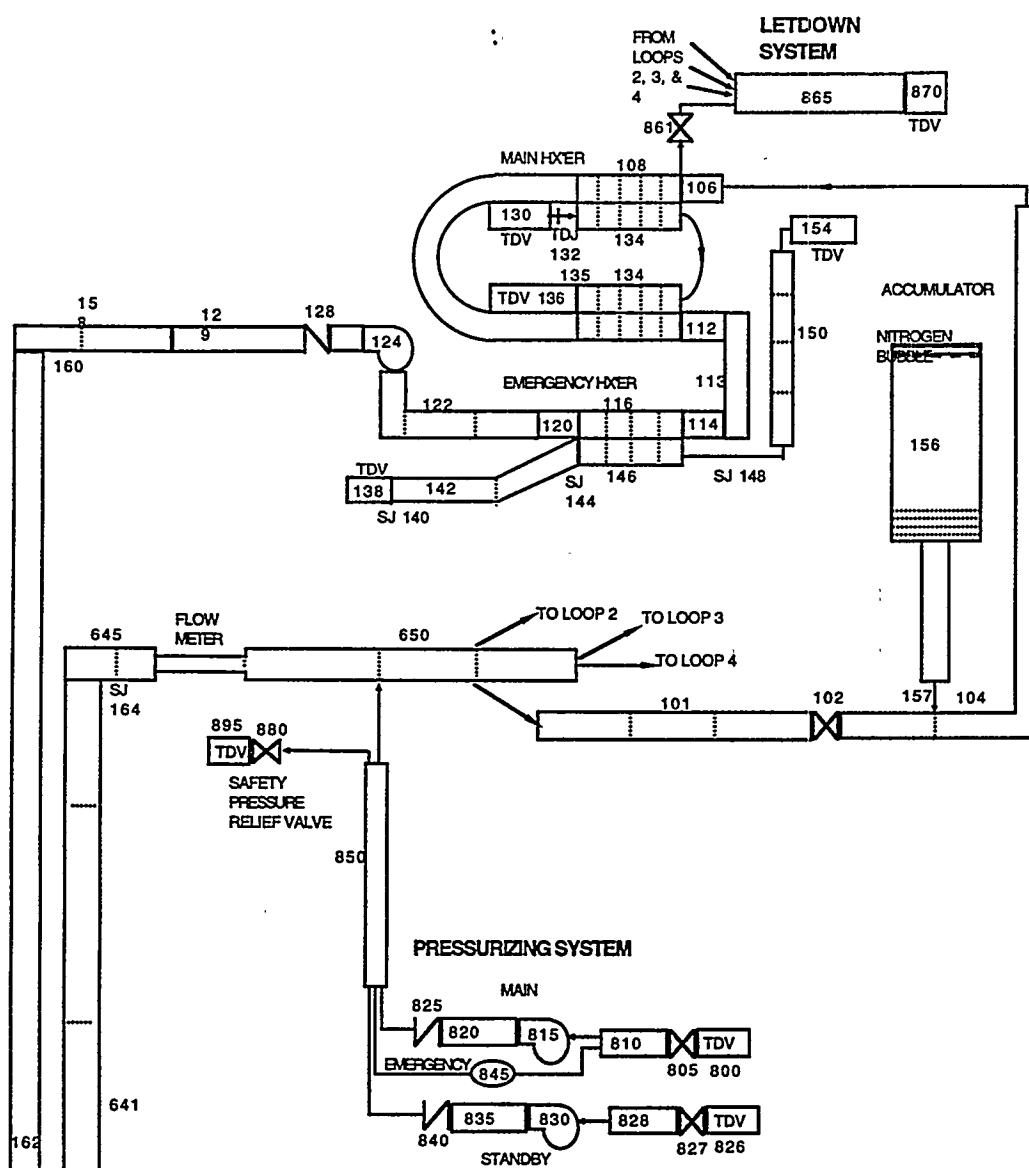


Fig. 2. ANS two-element-core RELAP5 nodalization diagram: loop region.

2. PRELIMINARY INPUT

Card 0000001 - Updates

Updates 8, 10, and 22 (for code version 8K0 only) are invoked.

Update 8 invokes the following functions:

1. limits the time step to the Courant limit (shortest time for fluid to flow through a single control volume) of the most limiting volume in the problem,
2. limits the time step based on void fraction, and
3. makes corrections to the standard CHF calculation.

Update 10 invokes a time-step limit based on the change in pressure within a hydrodynamic volume,

Update 22 invokes an update to improve the RELAP5 use of the Colebrook¹⁰ single-phase pressure correlation. This update should not be used with RELAP5 MOD3.1.1.1 because it serves to *disable* the improvement for that version of the code.

Card 0000100 - Problem Type and Option

The option "new" specifies that this is a new simulation as opposed to a "restart" from a previous simulation. For some transients (e.g., pipe break events) a second input file is used that uses the "restart" option to continue from a run that used the Appendix A input file. This second input file also contains any changes to the normal configuration of the primary system (e.g., the addition of a pipe break junction between the primary system and the pool) that are necessary to represent the transient.

The option "transnt" specifies that a transient simulation is requested. The transient option is always used, even in establishing a new steady-state condition for the primary system.

Card 0000101 - Input Check or Run Option

The option "run" instructs RELAP5 to run the simulation as opposed to simply checking the input for errors.

Card 0000102 - Units Selection

The SI option is selected for both input and output units. This card is not required, but it is included for clarity. Pressures are in Pascals (Pa) and temperatures are in Kelvin (K).

Card 0000105 - CPU Time Remaining

The first two words on this card are central processing unit (CPU) margins that will cause RELAP5 to start wrapping up the job if the CPU time remaining is approaching the value specified in the third word. The allotted CPU time for the job (word 3) is used to smoothly terminate a simulation in case the simulation gets bogged down, and RELAP5 unexpectedly begins using a very small time step. Otherwise, enough CPU time should be allotted to cause the simulation to be terminated based on the time-step control cards (0000201-0000299).

Card 0000110 - Noncondensable gas

The noncondensable gas assumed for the accumulator bubbles is nitrogen. This gas is the only noncondensable used in the ANSR simulations.

Cards 0000120 thru 0000126 - Hydrodynamic Systems

Separate hydrodynamic systems are defined here by specifying one reference volume for each system. Seven systems are identified: the primary heavy-water system and six secondary light-water systems (two for each active loop).

Cards 0000201-0000299 Time-Step Control Cards

These cards are used to request time steps for the simulation. If the requested time step is too high, RELAP5 will halve it until a successful time-step advance can be made with a converged solution. A minimum time step of 0.1 μ s is specified. Also, on this card, the frequencies for minor edits, major edits (printed snapshots of the entire system), and restart dumps are specified in integer multiples of the requested time step.

The time-step control cards will nearly always change from simulation to simulation, as the necessary temporal discretization will be a strong function of the simulated transient.

Cards 20800001-20800999 Expanded Edit/Plot Variables

These cards are included to request additional dependent variables to be made available in the restart plot file and in the current run. These variables are not ordinarily provided as such by RELAP5. The heat structure temperatures requested here are internal to the heat structures; whereas RELAP5 normally only provides the heat structure boundary temperatures. The variables with the alpha designator "fwalf" request wall friction terms useful in interpolating pressures at control volume boundaries. The remainder of the extended edit variables request thermal properties (specific heat, thermal conductivity, and dynamic viscosity) in the fuel channels useful in calculating the core thermal limits.

Cards 0000301-0000399 Minor Edit Requests

These variables are requested as output in the RELAP5 standard output file at the frequency specified in the time-step control cards. These cards do not impact the content of the restart/plot file.

3. TRIPS

Trips are logical switches that assume a value of true or false depending on the conditions specified on the trip definition card. For the ANSR thermal-hydraulic model, the trip logic is used for pump, valve, and control variable input. Some trips are dependent upon the state of other trips. The conditions for which each trip is true are given below:

- 501 - True if cntrlvar 940 (flux-to-flow ratio) exceeds the reactor trip setpoint of 1.2.
- 502 - True if trip 501 has been true for at least 0.2 s, representing a flow sensor delay.
- 503 - True if the temperature at the CPBT inlet (volume 500-01) exceeds the high-temperature setpoint of 328.05 K.
- 504 - True if trip 503 has been true for at least 2 s, representing a temperature sensor delay.
- 506 - True if cntrlvar 839 (pressure at sensor location, 645-01, with a 0.03 s first-order pressure sensor lag applied) is less than the low-pressure setpoint.
- 508 - True if time is greater than a predetermined value (normally not used), allowing for a manual reactor trip.
- 510 - True if trip 603 (reactor scram indicator) has been true for at least 0.03 s, representing the pressure switch unlatch time it takes to start the control rod insertion stroke.
- 515 - True if time is greater than some predetermined value for loop 1 isolation (normally not used).
- 516 - True if time is greater than some predetermined value for loop 2 isolation (normally not used).
- 517 - True if time is greater than some predetermined value for loop 3 isolation (normally not used).
- 525 - True if time is greater than some predetermined value for loop 1 secondary coolant flow coastdown.
- 526 - True if time is greater than some predetermined value for loop 2 secondary coolant flow coastdown.
- 527 - True if time is greater than some predetermined value for loop 3 secondary coolant flow coastdown.
- 528 - True if time is greater than some predetermined value. When the pump cavitation model is being used, this trip determines when to turn off the steady-state pump speed controller and begin holding the speed constant for a forth-coming transient.
- 536 - True if cntrlvar 65 (loop 1 homologous pump quantity v/α) is greater than 1. Used in determining which portion of the homologous pump curve to reference.
- 537 - True if cntrlvar 115 (loop 2 homologous pump quantity v/α) is greater than 1. Used in determining which portion of the homologous pump curve to reference.
- 538 - True if cntrlvar 165 (loop 3 homologous pump quantity v/α) is greater than 1. Used in determining which portion of the homologous pump curve to reference.
- 540 - True if time is greater than some predetermined value, representing the time at which to trip the main pressurizer pump motor.
- 541 - True if time is greater than some predetermined value, representing the time at which to trip the standby pressurizer pump motor.

- 542 - True if time is greater than some predetermined value, representing the time at which to start the emergency pressurizer pump speed table (turn the pump on).
- 550 - True if time is greater than some predetermined value, representing the time at which to start the standby pressurizer pump speed table (turn the pump on).
- 551 - True if cntrlvar 804 is greater than a predetermined constant, representing the mass inventory in the make-up tank that leads to a pressurizer pump trip. This constant is currently assumed to be 8358.4 kg.
- 552 - True if trip 551 has been true for 11 s, resulting in a pressurizer pump trip due to low make-up tank inventory.
- 555 - True if time is greater than some predetermined value. When this trip turns true, power is disconnected from the primary coolant pump shafts, and the velocity table is not used (i.e., a torque balance based on the pump shaft is used to determine shaft speed). This trip will not override the pump cavitation model, should it be invoked on the pump velocity table cards (1246100, 2246100, 3246100).
- 560 - True if pressure in 850-01 is greater than a predetermined low-high pressure setpoint for opening the safety valve.
- 561 - True if pressure in 850-01 is greater than a predetermined high-high pressure setpoint for opening the safety valve.
- 599 - True if time is greater than a predetermined time to terminate the simulation.
- 600 - True if trip 599 is true, terminate the simulation.
- 601 - True if trip 502 or 504 is true, representing the first flag for reactor trip.
- 602 - True if trip 601 or 506 is true, representing the second flag for reactor trip.
- 603 - True if trip 602 or 508 is true, representing the third and final flag for reactor trip.
- 610 - True if trips 560 and 611 are true. This is the first half of the safety valve logic.
- 611 - True if trips 561 and 610 are true. This is the second half of the safety valve logic.
- 615 - True if trip 552 is false. This trip is used to isolate the pressurizing system if a low level in the make-up tank occurs.
- 619 - True if trip 555 is false. This flag is used to disable the pump velocity table, when the user desires to invoke a no-motor primary coolant pump coastdown based on a RELAP5 torque balance.
- 620 - True if trip 540 is false. This flag is used to disable the pump velocity table for the main pressurizer pump should a trip occur.
- 621 - True if trip 541 is false. This flag is used to disable the pump velocity table for the standby pressurizer pump should a trip occur.

4. CORE REGION

The core region is very complicated, as shown in Fig. 2. The core model consists of two fuel annuli, core bypass channels, and central control rod region. The core is surrounded by the core pressure boundary tube (CPBT), which separates the high-pressure primary system from the low-pressure moderator tank.

4.1 FUEL ELEMENTS

Three fuel element channels are included for each of the upper and lower fuel elements: an average channel, and two hot channels corresponding to the 95% and 99.9% nonexceedance probability uncertainty levels in the power distribution. In each hot channel, two hot stripes are used to represent both the critical heat flux (CHF) and the Costa onset-of-significant-void (OSV), used in the ANSR analysis as a flow excursion (FE) correlation, peaking factors. The G693 power distribution was used with peaking factors and power densities obtained for end-of-cycle (EOC) conditions with the exception of the lower-core hot stripes which were taken at beginning-of-cycle (BOC) conditions. These conditions correspond to the highest (most conservative) heat flux levels. Appendix B contains a listing of the FORTRAN computer program (power.f) that was used to insert the source terms directly into the RELAP5 input file. The source terms that represent heating in the CPBT and control rod region are not modified by power.f. The power densities and peaking factors that were used as input to power.f are supplied in this section. For the power distribution within the fuel plate, uniform heating in the fuel meat and clad is assumed, and a $1/r$ profile in the side plates, control rods, central hole wall, and CPBT walls is used.

4.1.1 Average Fuel Channels

The core contains two fuel annuli. The core geometry is described in ref. 11. The lower fuel annulus consists of 252 fuel plates with thickness of 1.27 mm and span of 87.35 mm. The upper fuel annulus consists of 432 fuel plates with thickness of 1.27 mm and span of 70.29 mm. One average channel is used in the lower fuel region to represent (as a lumped volume) all but two of the fuel channels. The same method is used for the upper fuel region. The two fuel channels excluded from the lumped volume serve as the 95% and 99.9% hot fuel channels where the channel thickness is narrowed to account for uncertainties in the fuel plate manufacture. The fuel plate surface roughness was calibrated such that the pressure drop predicted by the ANSR steady-state code¹² was obtained at an upper-core inlet velocity of 25 m/s.

Pipe 510

Lower core average channel,

L =	0.1014 m for each of 5 nodes, giving 0.507 m total length
A =	0.027675 m ² (total flow area in lower core except two hot channels)
=	(250/252) × [π(0.168 ² – 0.102 ²) – (252)(1.276 × 10 ⁻³)(87.35 × 10 ⁻³)]
dZ =	0.1014 m, assumes vertical orientation of the core
e =	1.772 × 10 ⁻⁶ m, calibrated to get correct pressure drop over the core
dh =	0.002498 m = 4(87.35)(1.2672) / 2(87.35 + 1.2672)

The ANS rectangular-channel geometry updates are invoked on card 5101001, and the pitch and span are specified to be 0.00127 m and 0.08735 m, respectively, on card 5101501.

Three sets of heat structures are attached to the average channel. The first set represents the average fuel plate. The second set represents the inner side plate, and the third represents the outer side plate. The same method applies for the upper fuel region.

Pipe 540

Upper-core average channel,

$$\begin{aligned}
 L &= 0.1014 \text{ m for each of 5 nodes, giving } 0.507 \text{ m total length} \\
 A &= 0.038359 \text{ m}^2 \text{ (total flow area in upper core except two hot channels)} \\
 &= (430/432) \times [\pi(0.2352 - 0.175^2) - (432)(1.276 \times 10^{-3})(70.25 \times 10^{-3})] \\
 dZ &= 0.1014 \text{ m (elevation)} \\
 e &= 1.772 \times 10^{-6} \text{ m, calibrated roughness to get correct pressure drop over the core} \\
 dh &= 0.002494 \text{ m} = 4(70.29)(1.269) / 2(70.29 + 1.269)
 \end{aligned}$$

The ANS rectangular-channel geometry updates are invoked on card 5401001 and the pitch and span are specified to be 0.00127 m and 0.07029 m, respectively, on card 5401501.

4.1.2 Hot Fuel Channels

Two hot channels are used in the lower fuel region to include uncertainties combined to produce the worst-case thermal-hydraulic conditions. Each hot channel is assumed to have a minimum channel gap of 1.14 mm (equal to 90% of nominal 1.27-mm gap).¹³ One of the hot channels is used to produce conditions at a 95% nonexceedance probability level (NEPL) for analysis of unlikely events, and the other at 99.9% nonexceedance probability level for analysis of anticipated events. The same method is used for the upper fuel region.

Pipes 515 and 516

Lower core 95% and 99.9% NEPL hot channel,

$$\begin{aligned}
 L &= 0.1014 \text{ m for each of 5 nodes, giving } 0.507 \text{ m total length} \\
 A &= 0.000110698 \text{ m}^2 \text{ (flow area for the single channel)} \\
 &= (1/252) \times [\pi(0.168^2 - 0.102^2) - (252)(1.276 \times 10^{-3})(87.35 \times 10^{-3})] \\
 dZ &= 0.1014 \text{ m (elevation)} \\
 e &= 1.772 \times 10^{-6} \text{ m, calibrated roughness to get correct pressure drop} \\
 dh &= 0.002498 \text{ m} = 4 \times 1.10698 \times 10^{-4} / [2(87.35 + 1.2672) \times 10^{-3}]
 \end{aligned}$$

The ANS rectangular-channel geometry updates are invoked on cards 5151001 and 5161001, and the pitch and span are specified to be 0.0011433 m and 0.08735 m, respectively, on cards 5151501 and 5161501.

Pipe 545 and 546

Upper core 95% and 99.9% NEPL hot channel,

$$L = 0.1014 \text{ m for each of 5 nodes, giving } 0.507 \text{ m total length}$$

$$\begin{aligned}
 A &= 8.9206 \times 10^{-5} \text{ m}^2 \text{ (flow area for the single channel)} \\
 &= (1/432) \times [\pi(0.235^2 - 0.175^2) - (432)(1.276 \times 10^{-3})(70.29 \times 10^{-3})] \\
 dZ &= 0.1014 \text{ m (elevation)} \\
 e &= 1.772 \times 10^{-6} \text{ m, calibrated roughness to get correct pressure drop} \\
 dh &= 0.002493 \text{ m} = 4 \times 8.9206 \times 10^{-5} / [2(70.29 + 1.276) \times 10^{-3}]
 \end{aligned}$$

The ANS rectangular-channel geometry updates are invoked on cards 5451001 and 5461001 and the pitch and span are specified to be 0.0011433 m and 0.08735 m, respectively, on cards 5451501 and 5461501.

4.1.3 Unheated Annular Channels

Several control volumes are defined to represent the annular channels upstream and downstream of each fuel element. Volumes 520 and 535 are defined to represent the short (0.05-m) midcore volumes.

Pipe 505

Lower (inner) core inlet annulus

$$\begin{aligned}
 L &= 1.545 \text{ m (ref. 14)} \\
 A &= 0.05598 \text{ m}^2 = \pi(0.168^2 - 0.102^2) \\
 dZ &= 1.545 \text{ (vertical orientation)} \\
 e &= 1.52 \times 10^{-6} \text{ m} \\
 dh &= 0.034 \text{ m (ERROR IN MODEL, should be } 0.132 = 4 \times 0.05598 / [2\pi(0.168 + 0.102)])
 \end{aligned}$$

Pipe 520

Lower (inner) core mid-core volume

$$\begin{aligned}
 L &= 0.05 \text{ m (ref. 14)} \\
 A &= 0.055983 \text{ m}^2 = \pi(0.168^2 - 0.102^2) \\
 dZ &= 0.05 \text{ m (vertical orientation)} \\
 e &= 1.52 \times 10^{-6} \text{ m} \\
 dh &= 0.132 \text{ m} = 4 \times 0.05598 / [2\pi(0.168 + 0.102)]
 \end{aligned}$$

Pipe 525

Lower (inner)-core exit annulus (upper-core bypass)

Segment 1

$$\begin{aligned}
 L &= 0.2028 \text{ m, exit of volume aligned with exit of 2nd volume in upper-core fuel channels}^{14} \\
 A &= 0.055983 \text{ m}^2 = \pi(0.168^2 - 0.102^2) \\
 dZ &= 0.2028 \text{ m (vertical orientation)} \\
 e &= 1.52 \times 10^{-6} \text{ m} \\
 dh &= 0.132 \text{ m} = 4 \times 0.05598 / [2\pi(0.168 + 0.102)]
 \end{aligned}$$

Segment 2

L =	2.3610 m, entrance of volume aligned with exit of 2nd volume in upper core fuel channels. ¹⁴
A =	$0.055983 \text{ m}^2 = \pi(0.168^2 - 0.102^2)$
dZ =	0.2028 m (vertical orientation)
e =	$1.52 \times 10^{-6} \text{ m}$
dh =	$0.132 \text{ m} = 4 \times 0.05598 / [2\pi(0.168 + 0.102)]$

Pipe 530

Upper (outer)-core inlet annulus

Segment 1

L =	1.545 m, aligned with lower-core inlet annulus ¹⁴
A =	$0.07728 \text{ m}^2 = \pi(0.235^2 - 0.175^2)$
dZ =	1.545 m (vertical orientation)
e =	$1.52 \times 10^{-6} \text{ m}$
dh =	0.044 m (ERROR IN MODEL, should be 0.120 m = $4 \times 0.07728 / [2\pi(0.235 + 0.175)]$)

Segments 2-6

L =	0.1014 m, aligned with lower-core fuel channel volumes
A =	$0.07728 \text{ m}^2 = \pi(0.235^2 - 0.175^2)$
dZ =	0.1014 m (vertical orientation)
e =	$1.52 \times 10^{-6} \text{ m}$
dh =	0.044 m (ERROR IN MODEL, should be 0.120 m = $4 \times 0.07728 / [2\pi(0.235 + 0.175)]$)

Pipe 535

Upper (outer)-core mid-core volume

L =	0.05 m (ref. 14)
A =	$0.07728 \text{ m}^2 = \pi(0.235^2 - 0.175^2)$
dZ =	0.05 m (vertical orientation)
e =	$1.52 \times 10^{-6} \text{ m}$
dh =	0.044 m (ERROR IN MODEL, should be 0.120 m = $4 \times 0.07728 / [2\pi(0.235 + 0.175)]$)

Pipe 555

Upper (outer)-core exit annulus

L =	0.7715 m, aligned to receive cross-flow from CPBT annulus ¹⁴
A =	$0.07728 \text{ m}^2 = \pi(0.235^2 - 0.175^2)$
dZ =	0.7715 m (vertical orientation)
e =	$1.52 \times 10^{-6} \text{ m}$
dh =	0.120 m = $4 \times 0.07728 / [2\pi(0.235 + 0.175)]$

Pipe 557

Upper (outer)-core exit annulus

$$\begin{aligned}
 L &= 1.2853 \text{ m (ref. 14)} \\
 A &= 0.07728 \text{ m}^2 = \pi(0.235^2 - 0.175^2) \\
 dZ &= 1.2853 \text{ m (vertical orientation)} \\
 e &= 1.52 \times 10^{-6} \text{ m} \\
 dh &= 0.120 \text{ m} = 4 \times 0.07728 / [2\pi(0.235 + 0.175)]
 \end{aligned}$$

Core Flow Separation Shroud Heat StructuresHeat Structure 5052 (Separation shroud between core annuli in entrance region)

Number of Heat Structure (NHS) = 1

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.168-m inner radius of core flow separation shroud¹⁴Right-boundary coordinate = 0.175-m outer radius of core flow separation shroud¹⁴

Composition is No. 2 - Al 6061

Left Boundary is Pipe 505

Right Boundary is Pipe 530

Heat Structure 5202 (Separation shroud between core annuli in mid-core region)

Number of Heat Structure (NHS) = 1

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.168-m inner radius of core flow separation shroud¹⁴Right-boundary coordinate = 0.175-m outer radius of core flow separation shroud¹⁴

Composition is No. 2 - Al 6061

Left Boundary is Pipe 520

Right Boundary is Pipe 535

Heat Structure 5551 (Separation shroud between middle and outer cores in core outlet region)

Number of Heat Structure (NHS) = 2

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.168-m inner radius of core flow separation shroud¹⁴Right-boundary coordinate = 0.175-m outer radius of core flow separation shroud¹⁴

Composition is No. 2 - Al 6061

Left-Boundary is Pipe 525

Right-Boundary is Pipe 555

4.1.4 Fuel Channel Interconnecting Junctions

Multiple Junction 507

Junction 1

Connects pipe 500 (core inlet plenum) to pipe 505 (lower-core inlet annulus)

A = 0.05598 m² (defaulted to area of 505)

Kf = 0.0

Kr = 0.0

Use abrupt area change model to represent sudden area contraction

dh = 0.132 m (same as the correct dh for 505)

Junction 2

Connects pipe 505 (lower-core inlet annulus) to pipe 510 (lower-core average channel)

A = 0.027675 m² (defaulted to area of 510)

Kf = 0.1079 = 0.04 (taken from HFIR value¹⁵) + 0.0679 (fL/d, for smooth pipe, Re = 1.5 × 10⁵, L = 0.010 m unheated length)

Kr = 0.1079

Use smooth area change model

dh = 0.0024831 m, ERROR: should be 0.002498 m, same as the dh for 510

NOTE: The errors on the junction hydraulic diameters are on the CCFL cards and are not used in calculating normal unidirectional flow pressure drops.

Junction 3

Connects pipe 505 (lower-core inlet annulus) to pipe 515 (lower-core 95% NEPL hot channel)

A = 0.000110698 m² (defaulted to area of 515)

Kf = 0.1079 = 0.04 (taken from HFIR value¹⁵) 0.0679 (fL/d, for smooth pipe, Re = 1.5 × 10⁵, L = 0.010 m unheated length)

Kr = 0.1079

Use smooth area change model

dh = 0.0024831 m, ERROR: should be 0.002498 m, same as the dh for 515

Junction 4

Connects pipe 505 (lower-core inlet annulus) to pipe 516 (lower-core 99.9% NEPL hot channel)

A = 0.000110698 m² (defaulted to area of 516)

Kf = 0.1079 = 0.04 (taken from HFIR value¹⁵) + 0.0679 (fL/d, for smooth pipe, Re = 1.5 × 10⁵, L = 0.01 m unheated length)

Kr = 0.1079

Use smooth area change model

dh = 0.0024831 m, ERROR: should be 0.002498 m, same as the dh for 516

Multiple Junction 522

Junction 1

Connects pipe 510 (lower-core average channel) to pipe 520 (lower-core exit annulus)

A = 0.027675 m² (defaulted to area of 510)

Kf = 0.0679 = (fL/d for smooth pipe, Re = 1.5×10^5 , L = 0.010 m unheated length)
 Kr = 0.1079, ERROR: for reverse flow, 4% loss has inadvertently been included
 Use abrupt area change model to represent sudden expansion at core exit
 dh = 0.0024982 m, same as the dh for 510

Junction 2

Connects pipe 515 (lower-core 95% NEPL hot channel) to pipe 520 (lower-core exit annulus)
 A = 0.000110698 m² (defaulted to area of 515)
 Kf = 0.0679 = (fL/d for smooth pipe, Re = 1.5×10^5 , L = 0.010 m unheated length)
 Kr = 0.1079, ERROR: for reverse flow, 4% loss has inadvertently been included
 Use abrupt area change model to represent sudden expansion at core exit
 dh = 0.0024982 m, same as the dh for 515

Junction 3

Connects pipe 520 (lower-core mid-core volume) to pipe 525 (lower-core exit annulus)
 A = 0.055983 m² (defaulted to area of 520)
 Kf = 0.0679, ERROR: unheated length loss coefficient inadvertently included
 Kr = 0.1079, ERROR: core exit loss coefficient inadvertently included
 Abrupt area change model invoked, although no area change exists, so it could be smooth
 dh = 0.132 m (same as the correct dh for 520)

Junction 4

Connects pipe 516 (lower-core 99.9% NEPL hot channel) to pipe 520 (lower-core exit annulus)
 A = 0.000110698 m² (defaulted to area of 516)
 Kf = 0.0679 = (fL/d for smooth pipe, Re = 1.5×10^5 , L = 0.010 m unheated length)
 Kr = 0.1079, ERROR: for reverse flow, 4% loss has inadvertently been included
 Use abrupt area change model to represent sudden expansion at core exit
 dh = 0.0024982 m, same as the dh for 515

Single Junction 529

Connects pipe 500 (core inlet plenum) to pipe 530 (lower-core bypass annulus)
 A = 0.07728 m² (defaulted to area of 530)
 Kf = 0.0
 Kr = 0.0
 Use abrupt area change model to represent sudden area contraction
 dh = 0.120 m (same as the correct dh for 530)

Multiple Junction 537

Junction 1

Connects pipe 530 (lower-core bypass annulus) to pipe 535 (upper-core midcore volume)
 A = 0.07728 m² (defaulted to area of 530)
 Kf = 0.0
 Kr = 0.0

Use abrupt area change model although there is no area change
 $dh = 0.120 \text{ m}$ (same as the dh for 530)

Junction 2

Connects pipe 535 (upper-core midcore volume) to pipe 540 (upper-core average channel)

$$A = 0.038359 \text{ m}^2 \text{ (defaulted to area of 540)}$$

$$Kf = 0.1079 = 0.04 \text{ (taken from HFIR value¹⁵)} + 0.0679 \text{ (fL/d, for smooth pipe, Re} = 1.5 \times 10^5, L = 0.010 \text{ m unheated length)}$$

$$Kr = 0.1079$$

Use smooth area change model

$$dh = 0.0024787 \text{ m, ERROR: should be } 0.002494 \text{ m, same as the dh for 540}$$

Junction 3

Connects pipe 535 (upper-core midcore volume) to pipe 545 (upper-core 95% NEPL hot channel)

$$A = 0.000089206 \text{ m}^2 \text{ (defaulted to area of 545)}$$

$$Kf = 0.1079 = 0.04 \text{ (taken from HFIR value¹⁵)} + 0.0679 \text{ (fL/d, for smooth pipe, Re} = 1.5 \times 10^5, L = 0.010 \text{ m unheated length)}$$

$$Kr = 0.1079$$

Use smooth area change model

$$dh = 0.0024787 \text{ m, ERROR: should be } 0.002494 \text{ m, same as the dh for 515}$$

Junction 4

Connects pipe 535 (upper-core midcore volume) to pipe 546 (upper-core 99.9% NEPL hot channel)

$$A = 0.000110698 \text{ m}^2 \text{ (defaulted to area of 546)}$$

$$Kf = 0.1079 = 0.04 \text{ (taken from HFIR value¹⁵)} + 0.0679 \text{ (fL/d, for smooth pipe, Re} = 1.5 \times 10^5, L = 0.01 \text{ m unheated length)}$$

$$Kr = 0.1079$$

Use smooth area change model

$$dh = 0.0024787 \text{ m, ERROR: should be } 0.002494 \text{ m, same as the dh for 546}$$

Multiple Junction 556

Junction 1

Connects pipe 540 (upper-core average channel) to pipe 555 (upper-core exit annulus)

$$A = 0.038359 \text{ m}^2 \text{ (defaulted to area of 540)}$$

$$Kf = 0.0679 = (\text{fL/d for smooth pipe, Re} = 1.5 \times 10^5, L = 0.010 \text{ m unheated length})$$

$$Kr = 0.0$$

Use abrupt area change model to represent sudden expansion at core exit

$$dh = 0.0024935 \text{ m, same as the dh for 540}$$

Junction 2

Connects pipe 545 (upper-core 95% NEPL hot channel) to pipe 555 (upper-core exit annulus)

$$A = 0.000089206 \text{ m}^2 \text{ (defaulted to area of 545)}$$

$$Kf = 0.0679 = (\text{fL/d for smooth pipe, Re} = 1.5 \times 10^5, L = 0.010 \text{ m unheated length})$$

$$Kr = 0.0$$

Use abrupt area change model to represent sudden expansion at core exit

$$dh = 0.0024787 \text{ m, ERROR should be } 0.002494, \text{ same as the dh for 545}$$

Junction 3

Connects pipe 546 (upper-core 99.9% NEPL hot channel) to pipe 555 (upper-core exit annulus)

$A = 0.000089206 \text{ m}^2$ (defaulted to area of 545)

$K_f = 0.0679 = (fL/d \text{ for smooth pipe, } Re = 1.5 \times 10^5, L = 0.010 \text{ m unheated length})$

$K_r = 0.0$

Use abrupt area change model to represent sudden expansion at core exit

$dh = 0.0024787 \text{ m}$, ERROR: should be 0.002494, same as the dh for 545

Junction 4

Connects pipe 555 (upper-core bottom exit annulus) to pipe 557 (upper-core top exit annulus)

$A = 0.07728 \text{ m}^2$ (defaulted to area of 555)

$K_f = 0.0$

$K_r = 0.0$

Use abrupt area change model (unnecessarily)

$dh = 0.0024787 \text{ m}$, ERROR: should be 0.120, same as 557

4.1.5 Average Channel Heat Structures

The fuel plates and side plates are modeled with slab (rectangular geometry) heat structures. Source terms are included within each heat structure based on neutronics calculations for the distribution of thermal power in the core. For illustration, a calculational procedure for the lower-core average fuel plates is here described. The same procedure applies to the upper-core fuel region.

(A) Average Fuel Plates

Fuel plate geometry and response is symmetrical with respect to the plate centerline. Taking advantage of symmetry, the fuel plates are modeled as single-sided plates of half thickness with a convective boundary on one side and an adiabatic (symmetry) boundary on the other side.

The clean fuel plates are 1.27 mm (50 mils) thick with a 0.762 mm (30 mils) thick fuel meat and a 0.254 mm (10 mils) aluminum 6061 clad on each side. During oxide formation, cladding is consumed such that the total plate thickness is increased by only 28.6% of the oxide thickness. For the G693 fuel grading, the maximum oxide thickness was $10.2 \times 10^{-6} \text{ m}$. Therefore, the corroded plates consists of 0.762-mm fuel meat, 0.2468-mm clad on each side, and 0.0102-mm oxide on each side, for a total thickness of 1.276 mm.

Fuel meat thickness (half plate)= 0.381 mm

Clad thickness= 0.2468 mm

Oxide thickness= 0.0102 mm

Heat Structure Group Number 5101

Number of Heat Structure (NHS) = 5

Number of Mesh Point (NMP) = 11

2 intervals from the left boundary through right coordinate (RCOORD) = $1.02 \times 10^{-5} \text{ m}$ (oxide)

2 intervals through RCOORD= $2.57 \times 10^{-4} \text{ m}$ (cladding)

6 intervals through RCOORD= $6.38 \times 10^{-4} \text{ m}$ (fuel meat)

Composition No. 4 (Oxide) through interval 2
 Composition No. 2 (Al 6061) through interval 4
 Composition No. 5 (Fuel Meat) through interval 10

Power Distribution through the fuel plate thickness

Constant uniform values for heat generation are specified for the fuel meat and cladding. At EOC, the power split between the lower and upper cores is 0.281 - lower, and 0.717 - upper.¹⁶ The constant heat source terms are calculated as follows:

$$\begin{aligned} \text{lower-core fuel meat source term} &= 0.281 \times 0.9106 \times 50.75 / (50.75 + 0.3) = 0.25440, \\ \text{lower-core fuel clad source term} &= 0.281 \times 0.9106 \times 0.3 / (50.75 + 0.3) = 0.00150, \\ \text{upper-core fuel meat source term} &= 0.717 \times 0.9106 \times 39.74 / (39.74 + 0.27) = 0.6485, \\ \text{upper-core fuel clad source term} &= 0.717 \times 0.9106 \times 0.27 / (39.74 + 0.27) = 0.00441, \end{aligned}$$

where 0.9106 is the total power fraction deposited in the fuel meat and cladding,¹⁷ and the fraction of power to fuel meat and cladding is based on the L7 fuel grading.

The heat transfer area to coolant per cell is calculated as follows:

axial heated length per cell × effective span × number of plates × 2 sides,

where the effective span is the total span length less 1.143 mm (45 mils) both ends for the non-fuel regions. Although only half of the average fuel plate is modeled (taking advantage of symmetry), both sides of the fuel plate are included in the area calculation because the total power is used to generate the source term. The following calculations are done for the fuel plate heat structures to determine the total heat transfer area.

HS 5101	$0.507/5 \times (0.08735 - 2 \times 0.001143) \times (252 - 2) \times 2 = 4.31 \text{ m}^2$
HS 5151	$0.507/5 \times (0.08735 - 2 \times 0.001143) \times 1 \times 2 = 0.01724 \text{ m}^2$
HS 5161	$0.507/5 \times (0.08735 - 2 \times 0.001143) \times 1 \times 2 = 0.01724 \text{ m}^2$
HS 5401	$0.507/5 \times (0.07029 - 2 \times 0.001143) \times (432 - 2) \times 2 = 5.93 \text{ m}^2$
HS 5451	$0.507/5 \times (0.07029 - 2 \times 0.001143) \times 1 \times 2 = 0.01379 \text{ m}^2$
HS 5461	$0.507/5 \times (0.07029 - 2 \times 0.001143) \times 1 \times 2 = 0.01379 \text{ m}^2$

A FORTRAN program (Appendix B: power.f) has been written to calculate source terms in heat structures according to RELAP5 input requirements. The procedure to calculate source terms requires the use of power allocation (Table 1), relative power density as derived from neutronic calculations (Tables 2 and 3), and peaking factors (Tables 4 and 5).

Table 1. Distribution of steady-state heat load in the ANSR RELAP5 system model.^a

Model region	Core power (%)
Fuel meat	89.74
Fuel-plate cladding	0.57
Core coolant	1.74
Fuel side plates	0.71
Central control rods	0.52
CPBT	0.23
Inner wall	
Outer wall	0.36
Moderator tank coolant	5.1
Control rod coolant	0.8
Others (e.g., pool, shielding, neutrinos)	0.26

^aNormalized to reactor total power.

Table 2. G693 power density in upper core.

Zone ^a	Avg Chan ^b	Hot Chan ^c .	CHF HS ^d	FE HS
1	1.157	1.480	1.700	1.671
2	1.315	1.624	1.700	1.544
3	1.287	1.497	1.539	1.428
4	1.238	1.392	1.444	1.315
5	1.151	1.257	1.316	1.246

^aAxial Zones: Zones 1 and 5 represent entry and exit volumes in any channels, respectively.

^bAverage Channel: Radially and zone averaged over multiple channels using neutronic data, it provides average bulk temperature rise.

^cHot Channel: Zone averaged over the single hottest channel for each core, it provides the maximum bulk temperature rise.

^dHot Spot: No averaging, used local maximum relative power density as the worst case in each zone.

Table 3. G693 power density in lower core

Zone	Average channel	Hot channel	CHF Hot stripe	FE Hot stripe
1	0.800	1.630	1.709	1.541
2	0.727	1.495	1.573	1.388
3	0.637	1.357	1.428	1.303
4	0.588	1.225	1.305	1.150
5	0.587	1.042	1.146	0.765

Table 4. Peaking factors used for hot channels and hot stripes at 95% nonexceedance probability

Zone	Hot channel	CHF	FE	IB	SZ	SZ (Modified)	$T_w = T_{sat}$	$T_w = T_{sat}$
1	1.074	1.631	1.305	1.30	1.521	2.08	1.14	1.16
2	1.074	1.554	1.305	1.30	1.521	2.08	1.14	1.16
3	1.074	1.554	1.305	1.30	1.521	2.08	1.14	1.16
4	1.074	1.554	1.305	1.30	1.521	2.08	1.14	1.16
5	1.074	1.631	1.305	1.30	1.521	2.08	1.14	1.16

Table 5. Peaking factors used for hot channels and hot stripes at 99.9% nonexceedance probability

Zone	Hot Chan	CHF	FE	IB	SZ	$T_w = T_{sat}$	$T_w = T_{sat}$	$T_w = T_{sat}$
1	1.113	1.995	1.592	1.59	2.3	1.23	1.23	1.25
2	1.113	1.899	1.592	1.59	2.3	1.23	1.23	1.25
3	1.113	1.899	1.592	1.59	2.3	1.23	1.23	1.25
4	1.113	1.899	1.592	1.59	2.3	1.23	1.23	1.25
5	1.113	1.995	1.592	1.59	2.3	1.23	1.23	1.25

Sample Calculation: Lower-core average and hot channel fuel plate source terms

1. Determine power fractions

In the lower fuel element, the model contains 250 plates for the average channels, one plate for the 95% hot channel, and one plate for the 99.9% hot channel. The power to the lower core is apportioned to the average and hot channels by applying the conservation of energy.

$$250/252 \times p + \frac{\text{averaged hot channel power density}}{\text{channel power density}} \times \frac{(1.252 \text{ peaking factor for the } 95\% \text{ hot channel} + 1/252 \text{ peaking factor for the } 99.9\% \text{ hot channel})}{1.252 \text{ peaking factor for the } 95\% \text{ hot channel}} = 1.$$

The above equation expressed using the FORTRAN variables is:

$$\text{mavgl} + \text{ml95} + \text{ml99} = 1,$$

where

$$\begin{aligned} \text{mavgl} &= 250 \times P/252 = \text{average channel power fraction}, \\ \text{ml95} &= 1 \times \text{averaged hot channel power desity} / \text{averaged channel power density} \times \text{peaking factor of the } 95\% \text{ hot channel} / 252 = 95\% \text{ hot channel power fraction}, \\ \text{ml99} &= 1 \times \text{averaged hot channel power desity} / \text{averaged channel power density} \times \text{peaking factor of the } 99.9\% \text{ hot channel} / 252 = 99.9\% \text{ hot channel power fraction}. \end{aligned}$$

2. Derive source terms for average fuel heat structures.

In power.f, the source multiplier (defined as W2) for the averaged fuel heat structure in the first cell of the lower core is expressed by:

$$W2 = 0.05118 \times \text{mavgl} \times \text{pdlcac}(n)/\text{avpdla},$$

where, in addition:

$\text{pdlcac}(n)$ = the n th-cell power density, lower core, average channel heat structure

avpdla = average power density in lower core average fuel heat structure

and the leading constant is calculated as follows:

Lower-core power fraction \times total fuel meat and clad power fraction / 5 cells

$$0.28 \times 0.9106/5 = 0.05118,$$

where the lower-core power fraction (0.28), along with the upper-core power fraction, was calculated from neutronic data.¹⁶

$$W_3 = 2.56 \times 10^{-4} \times m_{avg} \times p_{dlcac}(n) / a_{vpdla}$$

wherein the leading constant is computed as $0.00128/5 = 2.56 \times 10^{-4}$ (0.00128 from¹⁷ is the power fraction deposited in the coolant immediately next to the fuel element). Repeat the same procedure for the inner and outer side plates.

3. Load the calculated source terms into the RELAP5 input file.

As the source terms are inserted into the RELAP5 input, a summation of the itemized heat sources is performed as a check on total power conservation. The G693 core output for the lower-core average fuel plates is shown in Table 6. For the lower core average fuel plate (heat structure 5101), the right heat is inputed zero because it is an adiabatic (symmetry) boundary at the fuel plate centerline.

(B) Average Channel Side Plates

Heat Structure 5102 (Lower-Core Average Channel Inner Side Plate)

The lower-core average channel inner side plate is modeled with a two-sided structure that can pass heat from coolant between the average fuel plates (Pipe 510) to coolant in the control rod channel (Pipe 562). RELAP5 does not allow conduction heat transfer between two heat structures. Therefore, fuel plate heat transfer can not be modeled to flow spanwise to the side plates. In the model, heat must pass from the fuel plate to the coolant and then to the side plates. As a result, the side plate temperatures calculated will be low. The same procedure that was used above was used to compute source terms.

Left-boundary radius is 0.095 m

Right-boundary radius is 0.102 m

Composition is No. 2 - Al6061

Heat transfer length = 0.10098 m , ERROR neglected to divide the available heat transfer area by 2,
should be $0.5 \times 250/252 \times 0.507/5 = 0.05030$ m

Heat Structure 5103 (Lower-Core Average Channel Outer-Side Plate)

The lower-core average channel outer-side plate is modeled with a two-sided structure that can pass heat from coolant between the average fuel plates (Pipe 510) to coolant in the lower fuel bypass annulus (Pipe 530). The method used for heat structure 5102 was also used here to calculate source terms. The same procedure that was used above was used to compute source terms.

Left-boundary radius is 0.095 m

Right-boundary radius is 0.102 m

Composition is No. 2 - Al6061

Heat transfer length = 0.10098 m , ERROR neglected to divide the available heat transfer area by 2, should be $0.5 \times 250/252 \times 0.507/5 = 0.05030$ m

Heat Structure 5103 (Lower-Core Average Channel Outer-Side Plate)

The lower-core average channel outer-side plate is modeled with a two-sided structure that can pass heat from coolant between the average fuel plates (Pipe 510) to coolant in the lower fuel bypass annulus (Pipe 530). The method used for heat structure 5102 was also used here to calculate source terms. The same procedure that was used above was used to compute source terms.

Left-boundary radius is 0.095 m

Right-boundary radius is 0.102 m

Composition is No. 2 - Al6061

Heat transfer length = 0.10098 m , ERROR neglected to divide the available heat transfer area by 2, should be $0.5 \times 250/252 \times 0.507/5 = 0.05030$ m

Heat Structure 5402 (Upper-Core Average Channel Inner-Side Plate)

The upper-core average channel inner-side plate is modeled with a two-sided structure that can pass heat from coolant between the average fuel plates (Pipe 540) to coolant in the lower-core exit annulus (pipe 525). The same procedure that was used above was used to compute source terms.

Left-boundary radius is 0.168 m

Right-boundary radius is 0.175 m

Composition is No. 2 - Al6061

Heat transfer length = 0.1012 m , ERROR neglected to divide the available heat transfer area by 2, should be $0.5 \times 430/432 \times 0.507/5 = 0.05047$ m

The upper-core outer-side plate is the same as heat structure 5503, corresponding to the inner CPBT wall.

4.1.6 Hot Channel Heat Structures

(A) Main Fuel Heat Structure

The peaking factors presented in Tables 4 and 5 are used to calculate the 95% and 99.9% non-exceedance probability hot channel power density distributions. Similar to the lower-core average channel, the lower- core hot channel contains heat structures 5151, 5152, 5153, 5161, 5162, and 5163 for the fuel plate, inner side plate, and outer side plate, respectively. The upper-core hot channel heat structures, 5451, 5452, 5461, and 5462 are similar to those for the upper-core average heat structures. The same procedure for calculating source terms applies.

Heat Structures 5151 and 5161 (Lower-Core 95% and 99.9% Hot Channel Main Fuel Plates)

The lower-core hot channel fuel plate has the same dimensions as the average fuel plate. The heat transfer area

The lower-core hot channel fuel plate has the same dimensions as the average fuel plate. The heat transfer area is different because only one fuel plate is modeled.

Left-boundary radius is 0.0 m

Right-boundary radii for each component are same as described for average fuel plate

Composition is the same as described for average channel fuel

$$\text{Heat transfer area} = 0.017102 \text{ m} = 0.507/5 \times (0.08735 - 2 \times 0.001143) \times 1 \times 2 = 0.01724 \text{ m}^2$$

Heat Structures 5451 and 5461 (Upper-Core 95% and 99.9% Hot Channel Main Fuel Plates)

The upper-core hot channel fuel plate has the same dimensions as the average fuel plate. The heat transfer area is different because only one fuel plate is modeled.

Left-boundary radius is 0.0 m

Right-boundary radii for each component are same as described for average fuel plate

Composition is the same as described for average channel fuel

$$\text{Heat transfer area} = 0.013711 \text{ m} = 0.507/5 \times (0.07029 - 2 \times 0.001143) \times 1 \times 2 = 0.01379 \text{ m}^2$$

(B) Hot Channel Side Plate Heat Structures

Heat Structure 5152 and 5162 (Lower-Core 95% and 99.9% Hot Channel Inner-Side Plate)s

The lower-core hot channel inner-side plate is modeled with a two-sided structure that can pass heat from coolant between the 95% hot channel (Pipes 515 and 516) to coolant in the control rod channel (Pipe 562). The same procedure that was used above was used to compute source terms.

Left-boundary radius is 0.095 m

Right-boundary radius is 0.102 m

Composition is No. 2 - Al6061

$$\begin{aligned} \text{Heat transfer length} &= 0.0004024 \text{ m}, \text{ERROR neglected to divide the available heat transfer area by 2, should} \\ &\text{be } 0.5 \times 1/252 \times 0.507/5 = 0.00020119 \text{ m} \end{aligned}$$

Heat Structures 5153 and 5163 (Lower-Core 95% and 99.9% Hot Channel Outer-Side Plates)

The lower-core hot channel outer-side plate is modeled with a two-sided structure that can pass heat from coolant between the hot fuel channel (Pipes 515 and 516) to coolant in the lower fuel bypass annulus (Pipe 530). The method used for heat structure 5102 was also used here to calculate source terms. The same procedure that was used above was used to compute source terms.

Left-boundary radius is 0.095 m

Right-boundary radius is 0.102 m

Composition is No. 2 - Al6061

$$\begin{aligned} \text{Heat transfer length} &= 0.0004024 \text{ m}, \text{ERROR neglected to divide the available heat transfer area by 2, should} \\ &\text{be } 0.5 \times 1/252 \times 0.507/5 = 0.00020119 \text{ m} \end{aligned}$$

Heat Structure 5452 and 5462 (U-per-Core 95% and 99.9% Hot Channel Inner-Side Plate)s

The upper-core hot channel inner side plate is modeled with a two-sided structure that can pass heat from coolant between the 95% hot channel (Pipes 545 and 546) to coolant in the lower-core exit annulus (Pipe 525). The same procedure that was used above was used to compute source terms.

Left-boundary radius is 0.168 m

Right-boundary radius is 0.175 m

Composition is No. 2 - Al6061

Heat transfer length = 0.000235 m, ERROR neglected to divide the available heat transfer area by 2, should be $0.5 \times 1/432 \times 0.507/5 = 0.00011736$ m

(C) Hot Stripe Heat Structures

Two separate hot spot factors are incorporated in each of the hot channels, one for CHF (heat structures 5154, 5164, 5454 and 5464) and one for Costa OSV (FE) (heat structure 5155, 5165, 5455 and 5465).¹ These hot spots are modeled as extremely small heat structures (heat transfer area is 1/100th of that for the main hot channel fuel plate) at each axial node. The areas of these heat structures are small enough that they do not affect the hot-channel bulk coolant temperature; however, the peaking factors (Tables 4 and 5) are applied to elevate the local heat flux appropriately.

Heat Structures 5154, 5155, 5164, 5165 (Lower-Core 95% and 99.9% CHF and FE Hot Stripes)

The lower-core hot stripes have the same dimensions as the average fuel plate. The heat transfer area is only 1/100th of that for a single fuel plate.

Left-boundary radius is 0.0 m

Right-boundary radii for each component are same as described for average fuel plate

Composition is the same as described for average channel fuel

Heat transfer area = $0.00017102 \text{ m}^2 = 0.01724/100. \text{ m}^2$

ERROR on card 15155303 for lower-core 95% FE hot stripe, relative source term should be 0.25440 instaed of 0.5075.

Heat Structures 5454, 5455, 5464, 5465 (Upper-Core 95% and 99.9% CHF and FE Hot Stripes)

The upper-core hot stripes have the same dimensions as the average fuel plate. The heat transfer area is only 1/100th of that for a single fuel plate.

Left-boundary radius is 0.0 m

¹ Additionally, in the postprocessor, three thermal limit heat fluxes are calculated based on the Costa OSV hot spot fluxes for the $T_w = T_{sat}$, the incipient boiling (IB), and the modified Saha-Zuber OSV at the 95% and 99.9% non-exceedance probability levels.

Right-boundary radii for each component are same as described for average fuel plate
 Composition is the same as described for average channel fuel
 Heat transfer area = $0.00013711 \text{ m}^2 = 0.01379/100. \text{ m}^2$

**Table 6. Source terms in the lower-core average fuel plates
 (Heat Structure 5101) as coded in the RELAP5 ANSR
 system input model**

Source type	Multiplier ($\times 100$)	Left heat ($\times 10^4$)	Right heat	Heat structure No.
1000	6.02362	3.01298	0	1
1000	5.47397	2.73805	0	2
1000	4.79631	2.39909	0	3
1000	4.42736	2.21454	0	4
1000	4.41983	2.21078	0	5

4.2 CONTROL ROD CHANNELS

This region is contained within the control rod shroud (IR = 95 mm, OR = 102 mm) (ref. 14). The elevation span is from the flow split elevation to the top of the CPBT. Three control rods are enclosed by the shroud. Each rod consists of an aluminum inner cylinder (IR = 22 mm, OR = 31.25 mm) and a hafnium outer cylinder (IR = 31.5 mm, OR = 35.5 mm) with coolant gaps in between. The control rod channel model incorporates the region of coolant flow surrounding the control rods, the coolant passages between the hafnium and the aluminum carrier, and the central coolant channel within the control rods themselves. All three rods are modeled with a 6-m/s coolant velocity in each coolant channel at steady-state conditions. This is accomplished by outlet orifice loss coefficients at junctions 566-01, 566-02, and 566-03. In the model, pipes 561, 562, and 563 with elevation spanning from the lower-core bottom to the upper-core top represent paths inside rods, paths outside rods, and internal rod gaps, respectively. The remaining branches 560 and 564 represent the inlet and outlet of the channel.

Because of gamma heating, the fraction of core power deposited within structures external to the fueled region (such as the control rods and the CPBT) increases after the reactor scram, although the absolute value decreases. When using the normal RELAP5 reactor point kinetics model for calculating total core power, it is necessary to assume that the distribution of the core power among the various core regions does not vary with time. To improve the simulation of both the control rods and the CPBT after reactor scram, the RELAP5 ANSR model was modified by (a) decoupling the CPBT and control rod heating rates from the reactor point kinetics calculation and (b) implementing realistic functions for CPBT and control rod heating following a reactor trip. The associated heat structures are modeled as a two-sided aluminum wall (heat structure 5611), aluminum-hafnium (heat structure 5621), and hafnium wall (heat structure 5631). In addition, heat structures 5612 and 5622 represent the inside and outside D₂O heating, respectively.

Pipe 560

Control rod inlet

L =	2.419 m (ref. 14)
A =	0.03018 m ² , ERROR IN MODEL, $0.03485 \text{ m}^2 = \pi(0.130^2 - 3 \times 0.044^2)$
dZ =	2.419 m (vertical orientation)
e =	1.52×10^{-6} m
dh =	$0.0207 \text{ m, ERROR IN MODEL, } 0.08468 \text{ m} = 4 \times 0.03485 / 2\pi / (3 \times 0.044 + 0.130)$

Pipe 561

Coolant in control rod tube

Segments 1-11, except 6

L =	0.1014 m (ref. 14), corresponds to upper and lower fuel axial regions
A =	$0.00456159 \text{ m}^2 = 3 \times \pi \times 0.022^2$
dZ =	0.1014 m (vertical orientation)
e =	1.52×10^{-6} m
dh =	$0.044 \text{ m} = 2 \times 0.022$

Segment 6

L =	0.050 m (ref. 14), corresponds to midcore volume
A =	$0.00456159 \text{ m}^2 = 3 \times \pi \times 0.022^2$
dZ =	0.050 m (vertical orientation)
e =	1.52×10^{-6} m
dh =	$0.044 \text{ m} = 2 \times 0.022$

Pipe 562

Coolant around control rod tube

Segments 1-11, except 6

L =	0.1014 m (ref. 14), corresponds to upper and lower fuel axial regions
A =	$0.0164753 \text{ m}^2 = \pi(0.095^2 - 3 \times 0.0355^2)$
dZ =	0.1014 m (vertical orientation)
e =	1.52×10^{-6} m
dh =	$0.0520521 \text{ m} = 4 \times 0.0164753 / 2\pi / (0.095 + 3 \times 0.0355)$

Segment 6

L =	0.050 m (ref. 14), corresponds to midcore volume
A =	$0.0164753 \text{ m}^2 = \pi(0.095^2 - 3 \times 0.0355^2)$
dZ =	0.050 m (vertical orientation)
e =	1.52×10^{-6} m
dh =	$0.0520521 \text{ m} = 4 \times 0.0164753 / 2\pi / (0.095 + 3 \times 0.0355)$

Pipe 563

Coolant in control rod gap

Segments 1-11, except 6

$L = 0.1014 \text{ m}$ (ref. 14), corresponds to upper and lower fuel axial regions
 $A = 0.0013195 \text{ m}^2 = \pi(0.0315^2 - 0.0285^2) \times 8 \times 35^\circ / 360^\circ \times 3$
 $dZ = 0.1014 \text{ m}$ (vertical orientation)
 $e = 1.52 \times 10^{-6} \text{ m}$
 $dh = 0.006 \text{ m} = 4 \times 0.0013195 / [2\pi \times 8 \times 35^\circ / 360^\circ \times 3(0.0315 + 0.0285)]$

Segment 6

$L = 0.050 \text{ m}$ (ref. 14), corresponds to midcore volume
 $A = 0.0013195 \text{ m}^2 = \pi(0.0315^2 - 0.0285^2) \times 8 \times 35^\circ / 360^\circ \times 3$
 $dZ = 0.050 \text{ m}$ (vertical orientation)
 $e = 1.52 \times 10^{-6} \text{ m}$
 $dh = 0.006 \text{ m} = 4 \times 0.0013195 / [2\pi \times 8 \times 35^\circ / 360^\circ \times 3(0.0315 + 0.0285)]$

Pipe 564

Control rod outlet

$L = 2.0568 \text{ m}$ (ref. 14)
 $A = 0.03018 \text{ m}^2$, ERROR IN MODEL, $0.03485 \text{ m}^2 = \pi(0.130^2 - 3 \times 0.044^2)$
 $dZ = 2.0568 \text{ m}$ (vertical orientation)
 $e = 1.52 \times 10^{-6} \text{ m}$
 $dh = 0.0207 \text{ m}$, ERROR IN MODEL, $0.08468 \text{ m} = 4 \times 0.03485 / 2\pi / (3 \times 0.044 + 0.130)$

Multiple Junction 559

Junction 1

Connects pipe 560 (control rod inlet plenum) to pipe 561 (control rod tube channel)

$A = 0.00456159 \text{ m}^2$ (defaulted to area of 561)
 $Kf = 0.0$
 $Kr = 0.0$

Use smooth area change model

$dh = 0.044 \text{ m}$, same as the dh for 540

Junction 2

Connects pipe 560 (control rod inlet plenum) to pipe 562 (control rod tube external channel)

$A = 0.0164753 \text{ m}^2$ (defaulted to area of 562)
 $Kf = 0.0$
 $Kr = 0.0$

Use smooth area change model

$dh = 0.0520521 \text{ m}$, same as the dh for 562

Junction 3

Connects pipe 560 (control rod inlet plenum) to pipe 563 (control rod gap flow)

$A = 0.0013195 \text{ m}^2$ (defaulted to area of 563)
 $Kf = 0.0$
 $Kr = 0.0$

Use smooth area change model

$dh = 0.006 \text{ m}$, same as the dh for 563

Multiple Junction 566

Junction 1

Connects pipe 561 (control rod tube channel) to pipe 564 (control rod exit plenum)

$A = 0.00456159 \text{ m}^2$ (defaulted to area of 561)

$Kf = 55.82$ (calibrated to get 6 m/s in control rod channel)

$Kr = 55.82$

Use smooth area change model

$dh = 0.044 \text{ m}$, same as the dh for 540

Junction 2

Connects pipe 562 (control rod tube external channel) to pipe 564 (control rod exit plenum)

$A = 0.0164753 \text{ m}^2$ (defaulted to area of 562)

$Kf = 55.70$ (calibrated to get 6 m/s in control rod channel)

$Kr = 55.70$

Use smooth area change model

$dh = 0.0520521 \text{ m}$, same as the dh for 562

Junction 3

Connects pipe 563 (control rod gap flow) to pipe 564 (control rod exit plenum)

$A = 0.0013195 \text{ m}^2$ (defaulted to area of 563)

$Kf = 52.13$ (calibrated to get 6 m/s in control rod channel)

$Kr = 52.13$

Use smooth area change model

$dh = 0.006 \text{ m}$, same as the dh for 563

Heat Structure 5051 (control rod shroud in the inlet region)

Number of Heat Structure (NHS) = 1

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.095 m ERROR: should be 0.130 m inner radius of control rod shroud¹⁴

Right-boundary coordinate = 0.102 m ERROR: should be 0.1365 m outer radius of control rod shroud¹⁴

Composition is No. 2 - Al 6061

Left-Boundary is Pipe 560

Right-Boundary is Pipe 505

Heat Structure 5201 (Control rod shroud in mid-core region)

Number of Heat Structure (NHS) = 1

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.095 m (ref. 14)

Right-boundary coordinate = 0.102 m (ref. 14)

Composition is No. 2 - Al 6061

Left-Boundary is Volume 562-06

Right-Boundary is Volume 520-01

Heat Structure 5251 (Control rod shroud in upper-core region)

Number of Heat Structure (NHS) = 5

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.095 m (ref. 14)

Right-boundary coordinate = 0.102 m (ref. 14)

Composition is No. 2 - Al 6061

Left boundary is Volume 562-07 thru 562-11

Right boundary is Volume 525-01 and 525-02

Heat transfer length = 0.1014 m = 0.507/5

4.3 CORE PRESSURE BOUNDARY TUBE (CPBT)

The CPBT is a double-walled containment for the fuel assemblies. Coolant flows between the inner and outer walls in the CPBT annulus (pipe 550) to keep the exterior of the inner wall pressurized. This is accomplished by sizing the inner wall orifices at the bottom (inlet) and top (outlet) appropriately. The CPBT annulus is modeled as an annular flow channel with a 3-mm gap in the axial region defined by the upper core and a 5-mm gap at all other axial locations. The steady-state design coolant velocity in the 3-mm gap region is 7 m/s. Previous RELAP5 studies have shown that if the outer wall completely disappears, that an inlet orifice diameter of 0.076 m (3 in.) and an outlet orifice diameter of 0.0508 m (2 in.) is an acceptable combination to prevent fuel damage. These orifices are represented by single junctions 531 and 532.

The outer wall has an inside radius of 245 mm and an outside radius of 253 mm. The inner wall has an inside radius of 235 mm and an outside radius of either 240 or 242 mm, depending on the axial location.

4.3.1 CPBT Thermal-Hydraulic Volumes and Junctions

Junction 531

Connects center (via crossflow junction) of 530-01 to center of 550-01

A = 0.00454 m² (0.076-m-diam circular orifices)

Kf = 2.79 (orifice with C_D = 0.6)

Kr = 2.79 (orifice with C_D = 0.6)

Use smooth area change model

Invoke crossflow option for both volumes

dh = 0.01 m (assume 1-cm-hole diameters)

Junction 532

Connects center (via crossflow junction) of 530-01 to center of 550-01

A = 0.00204 m² (0.051-m-diam circular orifices)

Kf = 2.78 (orifice with C_D = 0.6)

Kr = 2.78 (orifice with C_D = 0.6)

Use smooth area change model

Invoke crossflow option for both volumes

$$dh = 0.0024787 \text{ m}$$

Pipe 550 (CPBT annulus)

Segment 1

$$\begin{aligned} L &= 1.545 \text{ m, aligned with lower-core inlet annulus} \\ A &= 0.007618 \text{ m}^2 = \pi(0.245^2 - 0.240^2) \\ dZ &= 1.545 \text{ m} \\ e &= 1.52 \times 10^{-6} \text{ m} \\ dh &= 0.01 \text{ m} = 2 \times \text{gap} \end{aligned}$$

Segments 2-6

$$\begin{aligned} L &= 0.1014 \text{ m, aligned with lower-core fuel channel volumes} \\ A &= 0.007618 \text{ m}^2 = \pi(0.245^2 - 0.240^2) \\ dZ &= 0.1014 \text{ m} \\ e &= 1.52 \times 10^{-6} \text{ m} \\ dh &= 0.01 \text{ m} = 4 \times 0.007618 / 2\pi(0.245 + 0.240) \end{aligned}$$

Segment 7

$$\begin{aligned} L &= 0.05 \text{ m, aligned with mid-core volumes} \\ A &= 0.004590 \text{ m}^2 = \pi(0.245^2 - 0.242^2) \\ dZ &= 0.05 \text{ m (vertical orientation)} \\ e &= 1.52 \times 10^{-6} \text{ m} \\ dh &= 0.006 \text{ m} = 2 \times \text{gap} \end{aligned}$$

Segments 8-12

$$\begin{aligned} L &= 0.1014 \text{ m, aligned with upper-core fuel channel volumes} \\ A &= 0.004590 \text{ m}^2 = \pi(0.245^2 - 0.242^2) \\ dZ &= 0.05 \text{ m (vertical orientation)} \\ e &= 1.52 \times 10^{-6} \text{ m} \\ dh &= 0.006 \text{ m} = 2 \times \text{gap} \end{aligned}$$

Segments 13-14

$$\begin{aligned} L &= 0.7715 \text{ m, volume 13 aligned with upper-core exit volume for cross-flow}\sup{14} \\ A &= 0.007618 \text{ m}^2 = \pi(0.245^2 - 0.240^2) \\ dZ &= 0.7715 \text{ m (vertical orientation)} \\ e &= 1.52 \times 10^{-6} \text{ m} \\ dh &= 0.01 \text{ m} = 2 \times \text{gap} \end{aligned}$$

All junctions have default areas with smooth area change option. Only junction 550-12 connecting volumes 550-12 and 550-13 (corresponding to the expanding area change) has a loss coefficient. This value was selected to be 95.40 from trial and error to obtain the correct CPBT flow rate.

4.3.2 CPBT Heat Structures

Heat Structure 5001 (Reactor vessel wall at vessel inlet)

Note: This heat structure is not part of the Al CPBT wall.

Number of Heat Structure (NHS) = 1

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.2265 m (inner radius of pipe leading to CPBT)

Right-boundary coordinate = 0.2465 m (outer radius of pipe leading to CPBT)

Composition is No. 1 - SS304

Left boundary is Pipe 500

Right boundary is natural circulation to pool, htc given by general table 581

Heat Structure 5351 (CPBT inner wall in mid-core region)

Number of Heat Structure (NHS) = 1

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.247 m, IR = 0.235 m

Right-boundary coordinate = 0.2595 m, OR = 0.242 m

Composition is No. 2 - Al 6061

Left boundary is Volume 535-01

Right boundary is Volume 550-01

Heat transfer length = 0.050 m, includes unheated fuel length

Heat Structure 5501 (CPBT outer wall in fueled axial regions)

Number of Heat Structure (NHS) = 10

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.245 m

Right-boundary coordinate = 0.253 m

Composition is No. 2 - Al 6061

Left boundary is Pipe 550 (Volumes 2-6, 8-12)

Right boundary is Pipe 575

Heat transfer length = 0.1014 m = 0.507/5

Heat sources are calculated separate from the point kinetics model and involve a complicated calculation using control variables and general tables.¹⁸

Heat Structure 5502 (CPBT inner wall in lower core region)

Number of Heat Structure (NHS) = 5

Number of Mesh Point (NMP) = 4

Left-boundary coordinate = 0.235 m (ref. 14)

Right-boundary coordinate = 0.240 m

Composition is No. 2 - Al 6061

Left boundary is Pipe 530 (Volumes 2-6)

Right boundary is Pipe 550
Heat transfer length = 0.1014 m = 0.507/5

Heat Structure 5503 (CPBT inner wall in upper-core region)

Number of Heat Structure (NHS) = 5
Number of Mesh Point (NMP) = 4
Left-boundary coordinate = 0.235 m
Right-boundary coordinate = 0.242 m
Composition is No. 2 - Al 6061
Left boundary is Pipe 540 (Volumes 1-5)
Right boundary is Pipe 550 (Volumes 8-12)
Heat transfer length = 0.1014 m = 0.507/5

Heat Structure 5552 (CPBT inner wall in core outlet region)

Number of Heat Structure (NHS) = 2
Number of Mesh Point (NMP) = 4
Left-boundary coordinate = 0.235 m
Right-boundary coordinate = 0.240 m
Composition is No. Al 6061
Left boundary is Pipe 555
Right boundary is Pipe 550
Heat transfer length = 0.7715 m

5. PRIMARY COOLANT PIPING

The primary coolant piping described in this section extends from the exit of the CPBT through each of the heat exchanger/pump loops, and back to the primary supply vessel adapter weldment (PSVAW). Three complete active loops are modeled, and the fourth inactive loop is included upstream of the isolation valve and downstream of the check valve. Heat structures are also included for each piece of pipe. The description of RELAP5 components in the input model proceeds from the CPBT exit back to the PSVAW. Since some components are the same for all three loops, they are described together. The primary coolant pump and heat exchanger models are not discussed in this section.

Pipe 565 (core outlet plenum)

Exit volume into the hot leg

24-in. pipe, ID = 0.56037 m, A = 0.24663 m²

ID	=	0.56037 m (ref. 19)
L	=	0.918 m (ref. 19)
A	=	0.24663 m ²
dZ	=	0.54 m
e	=	4.57 × 10 ⁻⁵ m (ref. 20)
dh	=	0.56037 m (default)

Multiple Junction 567

Junction 1

Connects exit of 557-01 to entrance of 565-01

A = 0.07728 m² (default = area of Volume 557-01)

Kf = 0.

Kr = 0.

Invoke abrupt area change model

dh = 0.120 m (= dh of Volume 557-01)

Junction 2

Connects exit of 525-01 to entrance of 565-01

A = 0.055983 m² (default = area of Volume 525-01)

Kf = 0.

Kr = 0.

Invoke abrupt area change model

dh = 0.132 m (= dh of Volume 525-01)

Junction 3

Connects exit of 564-01 to entrance of 565-01

A = 0.0250354 m²

Kf = 22.8

Kr = 22.8

Invoke smooth area change model

dh = 0.120 m (= dh of Volume 557-01)

Junction 4

Connects exit of 557-01 to entrance of 565-01

A = 0.07728 m² (default = area of Volume 557-01)

Kf = 0.

Kr = 0.

Invoke abrupt area change model

dh = 0.120 m (= dh of Volume 557-01)

Pipe 64024-in. pipe, ID = 0.56037 m, A = 0.24663 m²

L = 1.88 m (ref. 21)

dZ = 0.0 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.56037 m (default)

Pipe 64124-in. pipe, ID = 0.56037 m, A = 0.24663 m²

L = 7.01 m (ref. 21)

dZ = 7.01 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.56037 m (default)

Pipe 64524-in. pipe, ID = 0.56037 m, A = 0.24663 m²

L = 8.23 m (ref. 21)

dZ = 0.0 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.56037 m (default)

Junction 647-01

Connects exit of 641 to entrance of 645

A = 0.24663 m² (default)

Kf = 0.24 [90° bend (ref. 20)]

Kr = 0.24 [90° bend (ref. 20)]

Invoke smooth area change model

dh = 0.56037 m (default)

Junction 647-02

Connects exit of 645 to entrance of 650

A = 0.24663 m² (default)

Kf = 0.

Kr = 0.

Invoke smooth area change model

dh = 0.56037 m (default)

Pipe 650

Segment 1 (Flow.Nozzle)

ID = 0.3362 m, A = 0.08879 m²

L = 1.68 m (ref. 21)

dZ = 0.0 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.3362 m (default)

Segment 2

24-in. pipe, ID = 0.56037 m, A = 0.24663 m²

L = 3.51 m (ref. 21)

dZ = 0.0 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.56037 m (default)

Segment 3

24-in. pipe, ID = 0.56037 m, A = 0.24663 m²

L = 1.22 m (ref. 21)

dZ = 0.0 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.56037 m (default)

Segment 4

24-in. pipe, ID = 0.56037 m, A = 0.24663 m²

L = 1.83 m (ref. 21)

dZ = 0.0 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.56037 m (default)

Junction between Segment 1 and Segment 2

A = 0.24663 m² (default)

$K_f = 0.$ (will change when flow-meter losses are considered)
 $K_r = 0.$ (will change when flow-meter losses are considered)
 Use smooth area change
 $dh = \text{default}$

Junction between Segment 2 and Segment 3

This junction is to facilitate pressurizer flow injection.

$A = 0.24663 \text{ m}^2$ (default)

$K_f = 0.$

$K_r = 0.$

Use smooth area change

$dh = \text{default}$

Junction between Segment 3 and Segment 4

$A = 0.24663 \text{ m}^2$ (default)

$K_f = 0.2$ [flow thru a main passage of a cross with 2/3 loss (ref. 22)]

$K_r = 0.2$ [flow thru a main passage of a cross with 2/3 loss (ref. 22)]

Use smooth area change

$dh = \text{default}$

Pipe 101 and Pipe 201

Segment 1

Assume 14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 1.07 \text{ m}$ (ref. 21)

$dZ = 0.0 \text{ m}$

$e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)

$dh = 0.3255 \text{ m}$ (default)

Segment 2

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 3.66 \text{ m}$ (ref. 21)

$dZ = 0.0 \text{ m}$

$e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)

$dh = 0.3255 \text{ m}$ (default)

Segment 3

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 2.21 \text{ m}$ (ref. 21)

$dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $dh = 0.3255 \text{ m}$ (default)

Junction between Segment 1 and Segment 2

$A = 0.08322 \text{ m}^2$ (default)
 $Kf = 0.182$ (90° bend) (ref. 20)
 $Kr = 0.182$ (90° bend) (ref. 20)
 Use smooth area change
 $dh = \text{default}$

Junction between Segment 2 and Segment 3

$A = 0.08322 \text{ m}^2$ (default)
 $Kf = 0.182$ (90° bend) (ref. 20)
 $Kr = 0.182$ (90° bend) (ref. 20)
 Use smooth area change
 $dh = \text{default}$

Pipe 301

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 3.28 \text{ m}$ (ref. 21)
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $dh = 0.3255 \text{ m}$ (default)

Pipe 401

Hot leg stub pipe.

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 3.28 \text{ m}$ (ref. 21)
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $dh = 0.3255 \text{ m}$ (default)

Junction 103, and 203

Connects exit of 650-03 to entrances of 101-01 and 201-01

$A = 0.24663 \text{ m}^2$ (area of main pipe)
 $Kf = 1.2$ (based on main pipe area, ref. 22)
 $Kr = 1.2$ (based on main pipe area, ref. 22)

Invoke smooth area change model

$dh = 0.56037 \text{ m}$

Junction 303

Connects exit of 650-04 to entrance of 301-01

$A = 0.08322 \text{ m}^2$ (area of main pipe)

$K_f = 0.25$ (based on branched area, ref. 22)

$K_r = 0.25$ (based on branched area, ref. 22)

Invoke smooth area change model

$dh = 0.3255 \text{ m}$

Junction 102, 202 and 302

Isolation valve (trip valve component).

$A = 0.08322 \text{ m}^2$ (area of 14-in. pipe)

$K_f = 0.104 = 8f_r$, gate valve (ref. 20, p. A-27)

$K_r = 0.104$

Invoke smooth area change model

$dh = 0.3255 \text{ m}$

Pipe 104, 204 and 304

Segment 1

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 0.69 \text{ m}$ (ref. 21)

$dZ = 0.0 \text{ m}$

$e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)

$dh = 0.3255 \text{ m}$ (default)

Segment 2

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 12.95 \text{ m}$ (ref. 21)

$dZ = 0.0 \text{ m}$

$e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)

$dh = 0.3255 \text{ m}$ (default)

Segment 3

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 2.51 \text{ m}$ (ref. 21)

$dZ = 2.44 \text{ m}$

$e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)

$dh = 0.3255 \text{ m}$ (default)

Junction between Segment 1 and Segment 2

A = 0.08322 m² (default)

Kf = 0.0

Kr = 0.0

Use smooth area change

dh = default

Junction between Segment 2 and Segment 3

A = 0.08322 m² (default)

Kf = 0.182 (90° bend) (ref. 20)

Kr = 0.182 (90° bend) (ref. 20)

Use smooth area change

dh = default

Pipe 113, 213 and 313

Segment 1

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 1.98 m (ref. 21)

dZ = 0.762 m

theta = -tan⁻¹(762/1828.8) = -22.6°

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.3255 m (default)

Segment 2

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 1.23 m (ref. 21)

dZ = 0.6093 m

theta = -tan⁻¹(609.6/1067) = -29.7°

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.3255 m (default)

Segment 3

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 0.6096 m (ref. 21)

dZ = 0.6096 m

e = 4.57 × 10⁻⁵ m (ref. 20)

dh = 0.3255 m (default)

Junction between Segment 1 and Segment 2

$A = 0.08322 \text{ m}^2$ (default)
 $Kf = 0.182$ (90° bend) (ref. 20)
 $Kr = 0.182$ (90° bend) (ref. 20)
 Use smooth area change
 $dh = \text{default}$

Junction between Segment 2 and Segment 3

$A = 0.08322 \text{ m}^2$ (default)
 $Kf = 0.182$ (90° bend) (ref. 20)
 $Kr = 0.182$ (90° bend) (ref. 20)
 Use smooth area change
 $dh = \text{default}$

Pipe 122, 222 and 322

Segment 1

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 2.31 \text{ m}$ (ref. 21)
 $dZ = 0.305 \text{ m}$
 $\theta = -\tan^{-1}(305/2286) = -7.6^\circ$
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $dh = 0.3255 \text{ m}$ (default)

Segment 2

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 2.13 \text{ m}$ (ref. 21)
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $dh = 0.3255 \text{ m}$ (default)

Segment 3

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 0.762 \text{ m}$ (ref. 21)
 $dZ = 0.762 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $dh = 0.3255 \text{ m}$ (default)

Junction between Segment 1 and Segment 2

A = 0.08322 m² (default)
 Kf = 0.182 (90° bend) (ref. 20)
 Kr = 0.182 (90° bend) (ref. 20)
 Use smooth area change
 dh = default

Junction between Segment 2 and Segment 3

A = 0.08322 m² (default)
 Kf = 0.182 (90° bend) (ref. 20)
 Kr = 0.182 (90° bend) (ref. 20)
 Use smooth area change
 dh = default

Pipe 126, 226 and 326

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 0.9146 m (ref. 21)
 dZ = 0.0 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.3255 m (default)

Pipe 129, 229, 329 and 429

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 6.25 m (ref. 21)
 dZ = 0.0 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.3255 m (default)

Single Junction 131, 231, 331, and 431

Junction between pipe x29 and pipe x58 in cold leg

A = 0.08322 m² (default)
 Kf = 0.182 (90° bend) (ref. 20)
 Kr = 0.182 (90° bend) (ref. 20)
 Use smooth area change
 dh = default

Pipe 158 and 258

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 4.50 \text{ m (ref. 21)}$
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m (ref. 20)}$
 $dh = 0.3255 \text{ m (default)}$

2020

Pipe 358 and 458

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 7.24 \text{ m (ref. 21)}$
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m (ref. 20)}$
 $dh = 0.3255 \text{ m (default)}$

Single Junction 160 and 260

Junctions between pipes 158 and 162 and between pipes 258 and 262

$A = 0.08322 \text{ m}^2 \text{ (default)}$
 $K_f = 0.182 \text{ (90}^\circ \text{ bend) (ref. 20)}$
 $K_r = 0.182 \text{ (90}^\circ \text{ bend) (ref. 20)}$
 Use smooth area change
 $dh = \text{default}$

Pipe 162

Cold-leg downcomer up to the inertia flow diode (IFD)

Segment 1

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 1.83 \text{ m (ref. 21)}$
 $dZ = -1.83 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m (ref. 20)}$
 $dh = 0.3255 \text{ m (default)}$

Segment 2

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

$L = 1.57 \text{ m (ref. 21)}$
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m (ref. 20)}$
 $dh = 0.3255 \text{ m (default)}$

Segment 3

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 1.45 m (ref. 21)
dZ = 0.0 m
e = 4.57×10^{-5} m (ref. 20)
dh = 0.3255 m (default)

Segment 4

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 12.6 m - 0.49561 m = 12.10439 m, compromise refs. 21 and 19
dZ = -12.10439 m
e = 4.57×10^{-5} m (ref. 20)
dh = 0.3255 m (default)

Junction between Segment 1 and Segment 2

A = 0.08322 m² (default)
Kf = 0.182 (90° bend) (ref. 20)
Kr = 0.182 (90° bend) (ref. 20)
Use smooth area change
dh = default

Junction between Segment 2 and Segment 3

A = 0.08322 m² (default)
Kf = 0.13 (45° bend) (ref. 20)
Kr = 0.13 (45° bend) (ref. 20)
Use smooth area change
dh = default

Junction between Segment 3 and Segment 4

A = 0.08322 m² (default)
Kf = 0.182 (90° bend) (ref. 20)
Kr = 0.182 (90° bend) (ref. 20)
Use smooth area change
dh = default

Single Junction 172, 272, 372, and 472

Junction between pipe x62 and IFD (pipe x71)

Entrance to IFD throat

A = 0.03095 m² (default)
Kf = 0.2062 (ref. 20)
Kr = 0.4513 (ref. 20)
Use smooth area change

$dh = \text{default}$

Pipe 171

Inertial Flow Diode

8-in. throat from, ID = 0.1985 m, A = 0.03095 m²

Segment 1

$L = 0.3 \text{ m (ref. 19)}$
 $dZ = -0.3 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m (ref. 20)}$
 $dh = 0.1985 \text{ m (default)}$

Segment 2

$L = 2.0 \text{ m (ref. 19)}$
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m (ref. 20)}$
 $dh = 0.1985 \text{ m (default)}$

Segment 3

$L = 2.28 \text{ m (ref. 19)}$
 $dZ = 0.0 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m (ref. 20)}$
 $dh = 0.1985 \text{ m (default)}$

Junction between Segment 1 and Segment 2

$A = 0.03095 \text{ m}^2 \text{ (default)}$
 $Kf = 0.196 \text{ (90}^\circ \text{ bend in 8-in. pipe) (ref. 20)}$
 $Kr = 0.196 \text{ (90}^\circ \text{ bend in 8-in. pipe) (ref. 20)}$
 Use smooth area change
 $dh = \text{default}$

Junction between Segment 2 and Segment 3

$A = 0.03095 \text{ m}^2 \text{ (default)}$
 $Kf = 0.196 \text{ (90}^\circ \text{ bend in 8-in. pipe) (ref. 20)}$
 $Kr = 0.196 \text{ (90}^\circ \text{ bend in 8-in. pipe) (ref. 20)}$
 Use smooth area change
 $dh = \text{default}$

Single Junction 173, 273, 373, and 473

Junction between pipes 171 and 174

$A = 0.03095 \text{ m}^2 \text{ (default)}$

$K_f = 0.1028$ (ref. 20, p. A-26) entering flow with 22.5° half-angle
 $K_r = 0.04696$ (ref. 20, p. A-26) exiting flow with 5.0° half-angle
 Use smooth area change
 $d_h = \text{default}$

Pipe 174, 274, 374, 474

14-in. pipe, ID = 0.3255 m, $A = 0.08322 \text{ m}^2$
 $L = 0.50 \text{ m}$ (ref. 21)
 $dZ = 0.50 \text{ m}$ (includes some rise in IFD throat)
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $d_h = 0.3255 \text{ m}$ (default)

Pipe 490

CPBT annular volume that receives cold-leg flow

$ID = 0.273 \text{ m}$ (ref. 19)
 $OD = 0.573 \text{ m}$ (ref. 19)
 $L = 0.543 \text{ m}$ (ref. 19)
 $A = 0.1993 \text{ m}^2$
 $dZ = 0.543 \text{ m}$
 $e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)
 $d_h = (OD^2 - ID^2)/(OD + ID) = 0.3 \text{ m}$

Multiple Junction 492-01

Junction 1

Connects exit of pipe 174 to side of 490

$A = 0.08322 \text{ m}^2$ (default = area of Volume 174-01)
 $K_f = 0.$
 $K_r = 0.$

Invoke abrupt area change model

Invoke cross-flow junction on volume 490

$d_h = \text{default}$

Junction 2

Connects exit of pipe 274 to side of 490

$A = 0.08322 \text{ m}^2$ (default = area of Volume 274-01)
 $K_f = 0.$
 $K_r = 0.$

Invoke abrupt area change model

Invoke cross-flow junction on volume 490

$d_h = \text{default}$

Junction 3

Connects exit of pipe 374 to side of 490

A = 0.08322 m² (default = area of Volume 374-01)

Kf = 0.

Kr = 0.

Invoke abrupt area change model

Invoke cross-flow junction on volume 490

dh = default

Junction 4

Connects exit of pipe 490 to entrance of pipe 500

A = 0.1799 m² (default = area of Volume 500-01)

Kf = 0.

Kr = 0.

Invoke abrupt area change model

dh = default

Junction 5

Connects exit of pipe 495 to entrance of 560

A = 0.1134115 m² (default = area of Volume 560-01)

Kf = 152. (calibrated to get correct control rod channel flow)

Kr = 152. (calibrated to get correct control rod channel flow)

Use smooth area change

dh = default

Junction 6

Connects entrance of pipe 490 to entrance of 495

A = 0.1993 m² (default = area of Volume 490-01)

Kf = 0.

Kr = 0.

Invoke abrupt area change model

dh = default

Junction 7

Connects exit of pipe 474 to side of 490

A = 0.08322 m² (default = area of Volume 474-01)

Kf = 0.

Kr = 0.

Invoke abrupt area change model

Invoke cross-flow junction on volume 490

dh = default

Pipe 495

Bottom CPBT volume that surrounds the three control cylinders

3 cylinders ID = 0.087 m (ref. 19)

OD = 0.573 m (ref. 19)

L = 1.80 m (ref. 19)

A = 0.2400 m²

dZ = 1.80 m

e = 4.57×10^{-5} m (ref. 20)

dh = $(OD^2 - 3ID^2)/(OD + 3ID) = 0.3664$ m (default)

Pipe 500 (core-inlet plenum)

Entry Volume into the inner and outer fuel annuli

OD = 0.573 m (ref. 19)

L = 1.80 m (ref. 19)

A = 0.2400 m²

dZ = 1.80 m

e = 4.57×10^{-5} m (ref. 20)

dh = $(OD^2 - 3ID^2)/(OD + 3ID) = 0.3664$ m (default)

Pipe 557

L = 1.2853 m (ref. 19)

A = 0.07728 m²

dZ = 1.2853 m

e = 4.57×10^{-5} m (ref. 20)

dh = 0.120 m

Pipe 564

L = 2.0568 m (ref. 19)

A = 0.0318 m²

dZ = 2.0568 m

e = 4.57×10^{-5} m (ref. 20)

dh = 0.0207 m

Pipe 262

Cold-leg downcomer up to IFD

Segment 1

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²

L = 0.64538 m (ref. 21)

dZ = 0.00 m

e = 4.57×10^{-5} m (ref. 20)
 dh = 0.3255 m (default)

Segment 2

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²
 L = 14.7436 m - 0.3 m - 0.49561 m - 0.0136 m (to match RELAP5 elevations) = 13.93439 m
 (ref. 21 and 19. An elevation drop of 0.3 m is included in the IFD).
 dZ = -12.10439 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.3255 m (default)

Junction between Segment 1 and Segment 2

A = 0.08322 m² (default)
 Kf = 0.182 (90° bend) (ref. 20)
 Kr = 0.182 (90° bend) (ref. 20)
 Use smooth area change
 dh = default

Pipe 271

Inertial Flow Diode

8-in. throat, ID = 0.1985 m, A = 0.03095 m²

Segment 1

L = 0.3 m (ref. 19)
 dZ = -0.3 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.1985 m (default)

Segment 2

L = 0.29 m (ref. 19)
 dZ = 0.00 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.1985 m (default)

Segment 3

L = 0.94 m (ref. 19)
 dZ = 0.0 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.1985 m (default)

Junction between Segment 1 and Segment 2

A = 0.03095 m² (default)
 Kf = 0.196 (90° bend in 8-in. pipe), ref. 20

$K_r = 0.196$ (90° bend in 8-in. pipe), ref. 20

Use smooth area change

$d_h = \text{default}$

Junction between Segment 2 and Segment 3

$A = 0.03095 \text{ m}^2$ (default)

$K_f = 0.196$ (90° bend in 8-in. pipe), ref. 20

$K_r = 0.196$ (90° bend in 8-in. pipe), ref. 20

Use smooth area change

$d_h = \text{default}$

Pipe 362

Cold-leg downcomer up to Inertial Flow Diode

Segment 1

14-in. pipe, ID = 0.3255 m, $A = 0.08322 \text{ m}^2$

$L = 1.2166 \text{ m}$ (ref. 21)

$dZ = 0.00 \text{ m}$

$e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)

$d_h = 0.3255 \text{ m}$ (default)

Segment 2

14-in. pipe, ID = 0.3255 m, $A = 0.08322 \text{ m}^2$

$L = 14.7436 \text{ m} - 0.3 \text{ m} - 0.49561 \text{ m} - 0.0136 \text{ m}$ (to match RELAP5 elevations) = 13.93439 m
(ref. 21 and 19. An elevation drop of 0.3 m is included in the IFD).

$dZ = -12.10439 \text{ m}$

$e = 4.57 \times 10^{-5} \text{ m}$ (ref. 20)

$d_h = 0.3255 \text{ m}$ (default)

Junction between Segment 1 and Segment 2

$A = 0.08322 \text{ m}^2$ (default)

$K_f = 0.182$ (90° bend), ref. 20

$K_r = 0.182$ (90° bend), ref. 20

Use smooth area change

$d_h = \text{default}$

Pipe 371

Inertial Flow Diode

8-in. throat, ID = 0.1985 m, $A = 0.03095 \text{ m}^2$

Segment 1

$L = 0.3 \text{ m}$ (ref. 19)

dZ = -0.3 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.1985 m (default)

Segment 2

L = 0.51 m (ref. 19)
 dZ = 0.0 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.1985 m (default)

Segment 3

L = 0.98 m (ref. 19)
 dZ = 0.0 m
 e = 4.57×10^{-5} m (ref. 20)
 dh = 0.1985 m (default)

Junction between Segment 1 and Segment 2

A = 0.03095 m² (default)
 Kf = 0.196 (90° bend in 8-in. pipe), (ref. 20)
 Kr = 0.196 (90° bend in 8-in. pipe), (ref. 20)
 Use smooth area change
 dh = default

Junction between Segment 2 and Segment 3

A = 0.03095 m² (default)
 Kf = 0.196 (90° bend in 8-in. pipe), (ref. 20)
 Kr = 0.196 (90° bend in 8-in. pipe), (ref. 20)
 Use smooth area change
 dh = default

6. PIPING HEAT STRUCTURES

Heat structures are attached to the piping control volumes to represent the primary coolant pipe walls. These structures are included to account for heat transfer to the pool and thermal inertia of the piping itself. All of these heat structures are cylindrical type. The length of each heat structure (input as the surface area factor) corresponds exactly to the length of that piping segment specified in the thermal-hydraulic control volume input. The left-boundary condition is the thermal-hydraulic control volume, and the right-boundary condition is the light-water pool with temperature specified in general table 501. The heat transfer coefficient between the pipe wall and the thermal-hydraulic control volume is based on Dittus-Boelter for forced convection (heat transfer package No. 1). The heat transfer coefficient on the right side, to the pool, is a natural convection coefficient that depends on the outside pipe surface temperature, pipe orientation (horizontal or vertical), and outside pipe diameter. Table 7 gives each heat structure number and the corresponding geometry and boundary condition information for each piping heat structure. No neutronic heating is assumed in any of these heat structures.

Table 7. Primary coolant piping heat structure parameters (all dimensions in m)

HS No.	Pipe IR	Pipe OR	Length	T-H Vol	HTC Table	
1011-01	0.1627	0.1778	1.07	101-01	511	* lp1 hot leg
1011-02	0.1627	0.1778	3.66	101-02	511	* lp1 hot leg
1011-03	0.1627	0.1778	3.66	101-03	511	* lp1 hot leg
1041-01	0.1627	0.1778	0.69	104-01	511	* lp1 hot leg
1041-02	0.1627	0.1778	12.96	104-02	511	* lp1 hot leg
1041-03	0.1627	0.1778	2.51	104-03	581	* lp1 hot leg
1221-01	0.1627	0.1778	2.31	122-01	511	* lp1 pump suction
1221-02	0.1627	0.1778	2.13	122-02	511	* lp1 pump suction
1221-03	0.1627	0.1778	0.762	122-03	581	* lp1 pump suction
1261-01	0.1627	0.1778	0.9146	126-03	511	* lp1 pump discharge
1291-01	0.1627	0.1778	4.5	158-01	511	* lp1 cold-leg horizontal
1581-01	0.1627	0.1778	4.50	158-01	511	* lp1 cold-leg horizontal
1581-02	0.1627	0.1778	4.50	158-01	511	* lp1 cold-leg horizontal
1621-01	0.1627	0.1778	1.83	162-01	581	* lp1 cold-leg downcomer
1621-02	0.1627	0.1778	1.57	162-02	511	* lp1 cold-leg downcomer
1621-03	0.1627	0.1778	1.45	162-03	511	* lp1 cold-leg downcomer
1621-04	0.1627	0.1778	12.10439	162-04	581	* lp1 cold-leg downcomer
1711-01	0.09925	0.1016	0.300	171-01	581	* lp1 IFD throat
1711-02	0.09925	0.1016	2.000	171-02	531	* lp1 IFD throat
1711-03	0.09925	0.1016	2.280	171-03	531	* lp1 IFD throat
1741-01	0.1627	0.1778	0.50	174-01	511	* lp1 PSVAW join
2011-01	0.1627	0.1778	1.07	201-01	511	* lp2 hot leg
2011-02	0.1627	0.1778	3.66	201-02	511	* lp2 hot leg
2011-03	0.1627	0.1778	2.21	201-03	511	* lp2 hot leg
2041-01	0.1627	0.1778	6.098	204-01	511	* lp2 hot leg
2041-02	0.1627	0.1778	3.048	204-02	511	* lp2 hot leg
2041-03	0.1627	0.1778	2.51	204-03	581	* lp2 hot leg
2221-01	0.1627	0.1778	2.31	222-01	511	* lp2 pump suction

Table 7. (continued)

HS No.	Pipe IR	Pipe OR	Length	T-H Vol	HTC Table	
2221-02	0.1627	0.1778	2.13	222-02	511	* lp2 pump suction
2221-03	0.1627	0.1778	0.762	222-03	581	* lp2 pump suction
2261-01	0.1627	0.1778	0.9146	226-01	511	* lp2 pump discharge
2291-01	0.1627	0.1778	6.25	229-01	511	* lp2 cold-leg horizontal
2581-01	0.1627	0.1778	4.50	258-01	511	* lp2 cold-leg horizontal
2581-02	0.1627	0.1778	4.50	258-01	511	* lp2 cold-leg horizontal
2621-01	0.1627	0.1778	0.64538	262-01	511	* lp2 cold-leg downcomer
2621-02	0.1627	0.1778	13.93439	262-01	581	* lp2 cold-leg downcomer
2711-01	0.09925	0.1016	0.300	271-01	581	* lp2 IFD throat
2711-02	0.09925	0.1016	0.290	271-02	511	* lp2 IFD throat
2711-03	0.09925	0.1016	0.940	271-03	511	* lp2 IFD throat
2741-01	0.1627	0.1778	0.50	274-01	511	* lp2 PSVAW join
3011-01	0.1627	0.1778	3.28	301-01	511	* lp3 hot leg
3041-01	0.1627	0.1778	0.69	304-01	511	* lp3 hot leg
3041-02	0.1627	0.1778	12.96	304-02	511	* lp3 hot leg
3041-03	0.1627	0.1778	2.51	304-03	581	* lp3 hot leg
3221-01	0.1627	0.1778	2.31	322-01	511	* lp3 pump suction
3221-02	0.1627	0.1778	2.13	322-02	511	* lp3 pump suction
3221-03	0.1627	0.1778	0.762	322-03	581	* lp3 pump suction
3261-01	0.1627	0.1778	0.9146	326-01	511	* lp3 pump discharge
3291-01	0.1627	0.1778	6.25	329-01	511	* lp3 cold-leg horizontal
3581-01	0.1627	0.1778	7.24	358-01	511	* lp3 cold-leg horizontal
3581-02	0.1627	0.1778	7.24	358-02	511	* lp3 cold-leg horizontal
3621-01	0.1627	0.1778	1.2166	362-01	511	* lp3 cold-leg downcomer
3621-02	0.1627	0.1778	13.93439	362-02	581	* lp3 cold-leg downcomer
3711-01	0.09925	0.1016	0.300	371-01	581	* lp3 IFD throat
3711-02	0.09925	0.1016	0.510	371-02	511	* lp3 IFD throat
3711-03	0.09925	0.1016	0.980	371-03	511	* lp3 IFD throat
3741-01	0.1627	0.1778	0.50	374-01	511	* lp3 PSVAW join
4011-01	0.1627	0.1778	3.28	451-01	511	* lp4 hot leg
4291-01	0.1627	0.1778	6.25	429-01	511	* lp4 cold-leg horizontal
4581-01	0.1627	0.1778	7.24	458-01	511	* lp4 cold-leg horizontal
4581-02	0.1627	0.1778	7.24	458-02	511	* lp4 cold-leg horizontal
4621-01	0.1627	0.1778	1.2166	462-01	511	* lp4 cold-leg downcomer
4621-02	0.1627	0.1778	13.93439	462-02	581	* lp4 cold-leg downcomer
4711-01	0.09925	0.1016	0.300	471-01	581	* lp4 IFD throat
4711-02	0.09925	0.1016	0.510	471-02	511	* lp4 IFD throat
4711-03	0.09925	0.1016	0.980	471-03	511	* lp4 IFD throat
4741-01	0.1627	0.1778	0.50	474-01	511	* lp4 PSVAW join
4951-01	0.2865	0.3165	1.800	495-01	581	* bottom volume of CPBT
5001-01	0.2265	0.2465	0.331	500-01	581	* core inlet plenum
6401-01	0.28019	0.3048	0.91463	640-01	521	* main hot leg
6401-02	0.28019	0.3048	0.91463	640-02	521	* main hot leg

Table 7. (continued)

HS No.	Pipe IR	Pipe OR	Length	T-H Vol	HTC Table	
6401-03	0.28019	0.3048	0.91463	640-03	521	* main hot leg
6401-04	0.28019	0.3048	2.33667	641-01	581	* main hot-leg riser
6401-05	0.28019	0.3048	2.33667	641-02	581	* main hot-leg riser
6401-06	0.28019	0.3048	2.33667	641-03	581	* main hot-leg riser
6451-01	0.28019	0.3048	4.88	645-01	521	* hot-leg distribution header
6451-02	0.28019	0.3048	3.35	645-02	521	* hot-leg distribution header
6501-01	0.28019	0.3048	1.68	650-01	521	* hot-leg distribution header
6501-02	0.28019	0.3048	3.51	650-02	521	* hot-leg distribution header
6501-03	0.28019	0.3048	1.22	650-03	521	* hot-leg distribution header
6501-04	0.28019	0.3048	1.83	650-04	521	* hot-leg distribution header

7. PRIMARY COOLANT PUMPS

Flow through each of the four parallel reactor coolant loops is provided by a centrifugal pump with a rated speed of 188.5 rad/s (1800 rpm), rated flow of 643 L/s (10,200 gpm), and a rated head of 207.3 m (680 ft) (ref. 23). These pumps are modeled with RELAP5 pump components 124, 224, and 324.

In RELAP5, the pump speed is controlled either by specifying torques applied to the pump shaft (and allowing RELAP5 to solve for the speed), or by directly specifying the speed using the 6100 series cards as a function of time or some other parameters. The ANSR input model uses both types of control, however, the torque balance is used only when all motor power (including power supplied by both the main AC motors and the back-up pony motors) is assumed to be lost to the pumps. In all other cases (whenever either the main or pony motors or both are available) the 6100 series cards are used to point to a control variable that directly specifies the pump shaft rotational speed.

In establishing a steady state, the operating pump speed is adjusted until the desired steady-state coolant velocity is achieved. This is accomplished by specifying the pump speed with control variables 86, 136, and 186 for pumps 124, 224, and 324 (see Sect. 15.1). For most transients (when the pump cavitation model is not being used) the control variable used to specify the pump speed is changed to 195 for all three pumps. For all transient cases (even when the pump cavitation model is applied) the pump speed remains equal to the steady-state speed until a trip (either 506 or 540) of the main AC primary pump motors occurs. When control variable 195 is being used, this pump trip causes the pump speed to decline (as prescribed in general table 135) until it reaches 10% of the steady-state value (pony motor speed). The pump cavitation model is rarely used and is explained further in Sect. 15.1.

The specified length, area and volume of the pump control volumes are rather arbitrary, because the final pump specifications are not yet available.

L	=	0.5 m
A	=	defaulted to V/L
V	=	0.7739 m ³
dZ	=	0.0 m
e	=	4.57 × 10 ⁻⁵ m (ref. 20)
dh	=	0.1985 m (default)

Entrance Junction to pump - from pipe 122

A	=	0.08322 m ² (default)
Kf	=	0.
Kr	=	0.

Use smooth area change

dh	=	default
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Exit Junction from pump - strainer junction to pipe 126

Assume a loss coefficient of 2.0 (based on HFIR strainer design)²⁴

A	=	0.08322 m ² (default)
Kf	=	2.0
Kr	=	2.0

Use smooth area change

dh	=	default
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The pumps are modeled based on the data shown in Table 8 obtained from Westinghouse. The performance at 18,000 and 24,000 gpm was not included in the data, but is extrapolated. The rated conditions are speed, $N_r = 188.5 \text{ rad s}^{-1}$; flow, $Q_r = 0.643 \text{ m}^3/\text{s}$; head, $H_r = 207.3 \text{ m}$; and density, $\rho = 1098 \text{ kg/m}^3$.

Table 8. Pump head vs flow at 188.5 rad s⁻¹ (1800 rpm). Note that α is the ratio of pump speed to rated pump speed, HAN = h/α^2 , and HVN = h/v^2

Flow rate, Q (gpm)	Head, H (ft)	$v = Q/Q_r$	$h = H/H_r$	v/α	α/v	HAN	HVN
0.	766.	0.	1.126	0.		1.126	
2000.	780.	0.196	1.147	0.196		1.147	
4000.	791.	0.392	1.163	0.392		1.163	
6000.	775.	0.588	1.140	0.588		1.140	
8000.	742.	0.784	1.091	0.784		1.091	
10,000.	686.	0.980	1.009	0.980		1.009	
12,000.	605.	1.176	0.890		0.850		0.644
14,000.	502.	1.373	0.738		0.728		0.391
16,000.	400.	1.569	0.588		0.637		0.239
18,000.	300.	1.765	0.441		0.567		0.142
24,000.	0.	2.353	0.		0.425		0.

An additional point was added to the HVN curve to cover the full range of possible values. It was selected so that the transition to the negative flow/speed homologous curve segments would be smooth. The remaining six homologous head curve segments, which are required only for the case of backwards flow or reverse speed, were taken from ref. 25.

The rated torque, shaft friction coefficients, pony motor torque (as a function of speed) and moment of inertia are only important if the pump coastdown is to be calculated by RELAP5 based on a pump shaft torque balance (see discussion above). The assumed moment of inertia is 91.5 kg-m^2 (2171 lbm-ft^2). This inertia is much higher than the HFIR pumps (HFIR pumps are 468 lbm-ft^2) and was selected so that the torque-balance coastdown would be consistent with SDD-61, p. 203, that the pump speed would drop by a factor of 2, 2 s after pump trip. The hydraulic torque, τ_{hy} , imparted to the fluid at rated conditions is

$$\tau_{hy} = \frac{\rho_r g H_r Q_r}{N_r} = \frac{(1098)(9.81)(207.3)(0.643)}{188.5} = 7616.76 \text{ N-m.}$$

In order to specify the motor torque, $\tau = \tau_{hy}/\eta$ to RELAP5, the pump efficiency, η , as a function of speed must be known. Since the efficiency was not known, the torque data for a centrifugal pump²⁵ were nondimensionalized and used.

The two-phase head multipliers were taken from data for a Semiscale pump supplied in ref. 26.

8. MAIN HEAT EXCHANGER

The main heat exchangers (MHXs) are double-pass counterflow with the primary coolant on the shell side. Design data²⁷ were used to define the input and calibrate the heat exchanger model. The tube inner and outer diameters are 14.1 and 15.9 mm, respectively. There are 3920 tubes in each main heat exchanger with the tube bank length of 5.55 m. Because each of the 3920 tubes (with total length of 11.1 m) is bent in a U-shape, each cross-section of the exchanger contains 7840 tube cross-sections. The heat exchanger shell has a length of 7.01 m with an inner diameter of 2.03 m and wall thickness of 44.5 mm. The hemispherical cap has a radius of curvature of 0.7315 m (2.4 ft).

The model for the ANS secondary coolant system is limited to the secondary sides of the main heat exchangers. A specified mass flow rate is used as a boundary condition on the main heat exchanger secondary side. Also on each heat exchanger, a secondary mass source and sink (time-dependent volume) is used. The mass flow through the secondary (tube) side of the main heat exchangers is controlled during a steady-state run with a PID controller to reduce the error between the primary coolant core inlet temperature to the target inlet temperature. During a transient, the secondary flow rate is held constant as long as the secondary pumps are assumed to be active. If the secondary pumps are tripped, such as in a loss-of-offsite-power (LOSP) event, then the flow rate is reduced to 3.23% of steady-state flow. This assumed natural convection flow rate is based on the results obtained by E. A. Schneider²⁸ with a more detailed secondary system model.

Ten nodes were used to represent the coolant in the U-Tubes (secondary, pipe 134), and ten for the coolant on the shell side (primary, pipe 108). An additional control volume (108-06) was included on the primary (shell) side to represent coolant in the MHX hemispherical cap. Heat is lost from the shell (primary) side to the reactor pool from both the MHX cap (assumed to be a vertical surface) and the horizontal cylindrical exterior.

Because the flow pattern on the shell side is multidimensional, the one-dimensional heat transfer and pressure drop correlations in RELAP5 are insufficient. Therefore, the main heat exchanger model was calibrated (using the input shown in Appendix C) to match the supplied performance data. The design shell-side (primary) pressure drop was obtained by adjusting entrance and exit loss coefficients.

Pipes 108, 208 and 308

Segments 1-5 and 7-11

$$\begin{aligned} L &= 1.11 \text{ m} = (5.55 \text{ m})/5 \\ A &= 0.8258 \text{ m}^2 = 0.5 \times \pi/4(2.03^2 - 7840 \times 0.0159^2) \\ dZ &= 0.0 \text{ m} \\ e &= 4.57 \times 10^{-5} \text{ m, (ref. 20)} \\ dh &= 0.636 \text{ m} = 4A/P = 4 \times 0.8258/(\pi/2 + 1)/(2.03) \end{aligned}$$

Segment 6

$$\begin{aligned} L &= 2.03 \text{ m} = \text{inside shell diameter} \\ A &= 0.841 \text{ m}^2 = 0.5 \times \pi \times 0.7315^2 \\ dZ &= 0.0 \text{ m} \\ e &= 4.57 \times 10^{-5} \text{ m, (ref. 20)} \\ dh &= 0.636 \text{ m} = 4A/P = 4 \times 0.8258/(\pi/2 + 1)/(2.02) \end{aligned}$$

Time-Dependent Volume 130

Source boundary condition for secondary coolant

$$A = 1.e6 \text{ m}^2$$

$$V = 1.e6 \text{ m}^3$$

Pressure is 0.5 MPa (this value is not used on a source boundary condition)

Temperature is 302.55 K, assumed for secondary coolant supply temperature

Time-Dependent Junction 132, 232, 332

Specified mass flow rate for secondary side based on control variable 586

$$A = 0.7122 \text{ m}^2 \text{ (unimportant since mass flow is specified)}$$

The input table for this time-dependent junction is built so that the output value is always equal to the input value for a range of -1.e6 to 1.e6. Hence, the input value (control variable 586) is always taken as the specified mass flow rate for each main heat exchanger secondary.

Pipes 134, 234 and 334

Segments 1-10

$$L = 1.314 \text{ m} = (5.55 \text{ m})/5$$

$A = 0.612 \text{ m}^2 = \pi/4(0.01588^2) \times 3920$, the heat exchangers were calibrated using the outside tube diameter instead of the inside diameter on the secondary side. This mistake is not important to the results.

$$dZ = 0.0 \text{ m}$$

$$e = 4.57 \times 10^{-5} \text{ m, (ref. 20)}$$

$$dh = 0.01588 \text{ m (mistake: same comment as above)}$$

Junction 135, 235, 335

Exit junction for primary heat exchanger secondary flow

$$A = 0.776 \text{ m}^2 \text{ (defaulted)}$$

$$Kf = 0.$$

$$Kr = 0.$$

$$dh = 0.01588 \text{ m (mistake: see comment for pipe 134)}$$

Time-Dependent Volume 136, 236, 336

Sink boundary condition for secondary coolant

$$A = 1.e6 \text{ m}^2$$

$$V = 1.e6 \text{ m}^3$$

Pressure is 0.449 MPa (this assumption is unimportant for simplified secondary system)

Temperature is 319 K, unused for a sink boundary condition

The designed total heat transfer from shell to tube was obtained by adjusting the overall heat transfer area. The calculated total tube length, L_{ht} , is

$$L_{ht} = Nl = 7840 \times 5.55 = 43,512 \text{ m,}$$

here N is the number of tube cross-sections and l is the tube bank length. This value was approximately doubled to 87,004 m (8700.4 m per heat structure) to transfer the required 100 MW at the design conditions.

Cylindrical heat structures were used to represent the tubes themselves. The heat structure numbers, inner and outer radii, total heat transfer length, and left and right thermal-hydraulic control volume numbers are shown in Table 9. Table 10 shows the heat structure information for the cylindrical heat structures that thermally connect the main heat exchanger primary side to the light-water pool. Table 11 shows the heat structure information for the rectangular (slab) heat structures that thermally connect the main heat exchanger primary side plenum to the light-water pool.

Table 9. Main Heat exchanger tube heat structure information

HS No.	Inner radius (m)	Outer radius (m)	Length (m)	Left volume No.	Right volume No.
1083-01	0.007049	0.007938	8700.4	108-01	134-05
1083-02	0.007049	0.007938	8700.4	108-02	134-04
1083-03	0.007049	0.007938	8700.4	108-03	134-03
1083-04	0.007049	0.007938	8700.4	108-04	134-02
1083-05	0.007049	0.007938	8700.4	108-05	134-01
1083-06	0.007049	0.007938	8700.4	108-07	134-10
1083-07	0.007049	0.007938	8700.4	108-08	134-09
1083-08	0.007049	0.007938	8700.4	108-09	134-08
1083-09	0.007049	0.007938	8700.4	108-10	134-07
1083-10	0.007049	0.007938	8700.4	108-11	134-06
2083-01	0.007049	0.007938	8700.4	208-01	234-05
2083-02	0.007049	0.007938	8700.4	208-02	234-04
2083-03	0.007049	0.007938	8700.4	208-03	234-03
2083-04	0.007049	0.007938	8700.4	208-04	234-02
2083-05	0.007049	0.007938	8700.4	208-05	234-01
2083-06	0.007049	0.007938	8700.4	208-07	234-10
2083-07	0.007049	0.007938	8700.4	208-08	234-09
1083-08	0.007049	0.007938	8700.4	208-09	234-08
2083-09	0.007049	0.007938	8700.4	208-10	234-07
2083-10	0.007049	0.007938	8700.4	208-11	234-06
3083-01	0.007049	0.007938	8700.4	308-01	334-05
3083-02	0.007049	0.007938	8700.4	308-02	334-04
3083-03	0.007049	0.007938	8700.4	308-03	334-03
3083-04	0.007049	0.007938	8700.4	308-04	334-02
3083-05	0.007049	0.007938	8700.4	308-05	334-01
3083-06	0.007049	0.007938	8700.4	308-07	334-10
3083-07	0.007049	0.007938	8700.4	308-08	334-09
3083-08	0.007049	0.007938	8700.4	308-09	334-08
3083-09	0.007049	0.007938	8700.4	308-10	334-07
3083-10	0.007049	0.007938	8700.4	308-11	334-06

**Table 10. Cylindrical heat structures joining the shell side of
the main heat exchangers to the light-water pool**

HS #	Inner radius (m)	Outer radius (m)	Heat trans- fer length (m)	Left boundary volume No.	General table number for right Boundary HTC
1081-01	1.009	1.0540	0.555	108-01	599 * Main HX shell-to-pool
1081-02	1.009	1.0540	0.555	108-02	599 * Main HX shell-to-pool
1081-03	1.009	1.0540	0.555	108-03	599 * Main HX shell-to-pool
1081-04	1.009	1.0540	0.555	108-04	599 * Main HX shell-to-pool
1081-05	1.009	1.0540	0.555	108-05	599 * Main HX shell-to-pool
1081-06	1.009	1.0540	0.555	108-07	599 * Main HX shell-to-pool
1081-07	1.009	1.0540	0.555	108-08	599 * Main HX shell-to-pool
1081-08	1.009	1.0540	0.555	108-09	599 * Main HX shell-to-pool
1081-09	1.009	1.0540	0.555	108-10	599 * Main HX shell-to-pool
1081-10	1.009	1.0540	0.555	108-11	599 * Main HX shell-to-pool
2081-01	1.009	1.0540	0.555	208-01	599 * Main HX shell-to-pool
2081-02	1.009	1.0540	0.555	208-02	599 * Main HX shell-to-pool
2081-03	1.009	1.0540	0.555	208-03	599 * Main HX shell-to-pool
2081-04	1.009	1.0540	0.555	208-04	599 * Main HX shell-to-pool
2081-05	1.009	1.0540	0.555	208-05	599 * Main HX shell-to-pool
2081-06	1.009	1.0540	0.555	208-07	599 * Main HX shell-to-pool
2081-07	1.009	1.0540	0.555	208-08	599 * Main HX shell-to-pool
2081-08	1.009	1.0540	0.555	208-09	599 * Main HX shell-to-pool
2081-09	1.009	1.0540	0.555	208-10	599 * Main HX shell-to-pool
2081-10	1.009	1.0540	0.555	208-11	599 * Main HX shell-to-pool
3081-01	1.009	1.0540	0.555	308-01	599 * Main HX shell-to-pool
3081-02	1.009	1.0540	0.555	308-02	599 * Main HX shell-to-pool
3081-03	1.009	1.0540	0.555	308-03	599 * Main HX shell-to-pool
3081-04	1.009	1.0540	0.555	308-04	599 * Main HX shell-to-pool
3081-05	1.009	1.0540	0.555	308-05	599 * Main HX shell-to-pool
3081-06	1.009	1.0540	0.555	308-07	599 * Main HX shell-to-pool
3081-07	1.009	1.0540	0.555	308-08	599 * Main HX shell-to-pool
3081-08	1.009	1.0540	0.555	308-09	599 * Main HX shell-to-pool
3081-09	1.009	1.0540	0.555	308-10	599 * Main HX shell-to-pool
3081-10	1.009	1.0540	0.555	308-11	599 * Main HX shell-to-pool

Table 11. Slab heat structures connecting coolant in main heat exchanger hemispherical plenum to the light-water pool

HS No.	Left coord. (m)	Right Coord. (m)	Heat trans- fer area (m ²)	Left boundary volume No.	General table number for right Boundary HTC
1082-01	0.	0.0445	3.49	108-06	581 * Main HX shell-to-pool
2082-01	0.	0.0445	3.49	208-06	581 * Main HX shell-to-pool
3082-01	0.	0.0445	3.49	308-06	581 * Main HX shell-to-pool

9. EMERGENCY HEAT EXCHANGER

The emergency heat exchangers (EHXs) are single-pass counterflow heat exchangers with the primary coolant on the shell side. The secondary tubing (pipe 146 with 4 cells) has an OD of 19.05 mm (0.75 in.) and ID of 17.27 mm (0.68 in.) (ref. 27) and is connected to the pool (TDV 154) with a 3-m chimney (pipe 150) section rising just past the exit from the EHX. The tube bundle length is 6.40 m (21 ft) with 1670 tubes. The heat exchanger shell has an OD of 1.111 m (43.75 in.) and ID of 1.067 m (42.0 in.) and a length, assumed to be equal to the tube bundle length, of 6.4 m (21 ft).

No forced cooling is applied to the EHXs. The pressures in the secondary source and secondary sink time-dependent volumes are specified based on their hydrostatic pressures in the pool. The flow rates are then calculated by RELAP5 for natural circulation conditions. Calibration was performed at design conditions also supplied in ref.27. The hydraulic diameter on the shell side was calibrated to match the design pressure drop (0.048 MPa) at the design (primary) flow rate of 706 kg/s. When the pressure drop was matched, the total heat removed through the tubes was 1.60 MW which is very close to the 1.64 MW specified in the design data. The resulting tube (secondary) flow rate at this calibrated condition was matched (44 kg/s), even though the OD was inadvertently used to define the geometry on the tube-side control volumes instead of the ID. The RELAP5 input file used for the EHX calibration is shown in Appendix D. Table 12 gives the details for the heat structures that represent the tubing of the emergency heat exchangers. Table 13 shows the heat structures connecting the emergency heat exchanger to the light-water pool.

Pipes 116, 216 and 316

Segments 1-4

L	=	1.6 m = (6.4 m)/4
A	=	$0.894 \text{ m}^2 = \pi/4(1.067^2)$, incorrect because the tube cross-sectional area was not subtracted, this error was compensated by calibrating dh to design conditions.
dZ	=	0.0 m
e	=	$4.57 \times 10^{-5} \text{ m}$, (ref. 20)
dh	=	0.0017 m, calibrated to obtain correct pressure drop and heat transfer

Time-Dependent Volume 138, 238, 338

Source boundary condition for secondary coolant

A	=	1.e6 m ²
V	=	1.e6 m ³

Pressure is 180 kPa (the assumed pool pressure at the EHX secondary intake pipe). Only the pressure *difference* between inlet (these volumes) and outlet (volumes 154, 254, and 354) of tubes is important.

Temperature is 311.15 K, pool temperature

Junction 140, 240, 340

Entrance junction for emergency heat exchanger secondary flow
Abrupt area change model is invoked.

A	=	0.4264 m ² (defaulted to area of pipe 142)
Kf	=	0.
Kr	=	0.
dh	=	0.4573 m (assume 18.0-in. suction pipe)

Pipes 142, 242 and 342

Entrance pipe leading from pool to secondary side of emergency heat exchanger

Segments 1-2

L	=	0.7622 m = (1.5244 m)/2 (assume total suction pipe length of 5.0 ft)
A	=	0.4264 m ² = $\pi/4(0.4573^2)$
dZ	=	0.0 m
e	=	4.57 × 10 ⁻⁵ m, (ref. 20)
dh	=	0.4573 m (assum 18.0-in.-diam suction pipe)

Junction 144, 244, 344

Inlet junction for emergency heat exchanger secondary flow (tube entrance)

Abrupt area change model is invoked.

A	=	0.4264 m ² (defaulted)
Kf	=	0.
Kr	=	0.
dh	=	0.01905 m (same as tubes)

Pipes 146, 246 and 346

Emergency heat exchanger secondary coolant (in tubes).

Segments 1-4

L	=	1.6 m = 6.4 m/4
A	=	0.476 m ² = $\pi/4(0.01905^2) \times 1670$
dZ	=	0.0 m
e	=	4.57 × 10 ⁻⁵ m, (ref. 20)
dh	=	0.01905 m (incorrect, should have used ID instead of OD)

Junction 148, 248, 348

Exit junction for emergency heat exchanger secondary flow (tube exit)

Abrupt area change is invoked.

A	=	0.4264 m ² (defaulted)
Kf	=	0.
Kr	=	0.
dh	=	0.01905 m (same as tubes)

Pipes 150, 250 and 350

Emergency heat exchanger secondary coolant in chimney

Segments 1-4

L	=	$0.75 \text{ m} = 3 \text{ m} / 4$
A	=	$0.203 \text{ m}^2 = (\pi/4)(0.508^2)$
dZ	=	0.75 m
e	=	$4.57 \times 10^{-5} \text{ m}$, (ref. 20)
dh	=	0.508 m (assume a 20-in.-diam pipe for chimney)

Junction 152, 252, 352

Exit junction from emergency heat exchanger secondary chimney

Abrupt area change is invoked.

A	=	0.4264 m ² (defaulted)
Kf	=	0.
Kr	=	0.
dh	=	0.508 m (same as chimney)

Time-Dependent Volume 154, 254, 354

Sink boundary condition for secondary coolant

A	=	1.e6 m ²
V	=	1.e6 m ³

Pressure is $150773.6 \text{ Pa} = P_{138} - \rho gh = 180 \text{ kPa} - (993.08 \text{ kg/m}^3)(9.81 \text{ m/s}^2)(3 \text{ m})$

Temperature is 311.15 K, pool temperature

The pressure difference between TDV 138 (238 and 338) and TDV 154 (254 and 354) corresponds to a 3 m (9.8 ft) (ref. 29) difference in elevation within the light-water pool.

Table 12. Heat structure parameters representing emergency heat exchanger tubing

HS No.	Inside radius (m)	Outside radius (m)	Heat transfer area (m ²)	Left boundary volume No.	Right boundary volume No.
1163-01	0.008636	0.009525	2672.	116-01	146-04
1163-02	0.008636	0.009525	2672.	116-02	146-03
1163-03	0.008636	0.009525	2672.	116-03	146-02
1163-04	0.008636	0.009525	2672.	116-04	146-01
2163-01	0.008636	0.009525	2672.	216-01	246-04
2163-02	0.008636	0.009525	2672.	216-02	246-03
2163-03	0.008636	0.009525	2672.	216-03	246-02
2163-04	0.008636	0.009525	2672.	216-04	246-01
3163-01	0.008636	0.009525	2672.	316-01	346-04
3163-02	0.008636	0.009525	2672.	316-02	346-03
3163-03	0.008636	0.009525	2672.	316-03	346-02
3163-04	0.008636	0.009525	2672.	316-04	346-01

Table 13. Heat structures connecting emergency heat exchanger to the light-water pool

HS #	Left coord. (m)	Right Coord. (m)	Heat trans- fer area (m ²)	Left boundary volume No.	General table number for right Boundary HTC
1161-01	0.5334	0.5556	1.6	116-01	591 * Emergency HX shell-to-pool
1161-02	0.5334	0.5556	1.6	116-02	591 * Emergency HX shell-to-pool
1161-03	0.5334	0.5556	1.6	116-03	591 * Emergency HX shell-to-pool
1161-04	0.5334	0.5556	1.6	116-04	591 * Emergency HX shell-to-pool
1501-01	0.2287	0.2541	0.75	150-01	581 * Emergency HX chimney
1501-02	0.2287	0.2541	0.75	150-02	581 * Emergency HX chimney
1501-03	0.2287	0.2541	0.75	150-03	581 * Emergency HX chimney
1501-04	0.2287	0.2541	0.75	150-04	581 * Emergency HX chimney
2161-01	0.5334	0.5556	1.6	216-01	591 * Emergency HX shell-to-pool
2161-02	0.5334	0.5556	1.6	216-02	591 * Emergency HX shell-to-pool
2161-03	0.5334	0.5556	1.6	216-03	591 * Emergency HX shell-to-pool
2161-04	0.5334	0.5556	1.6	216-04	591 * Emergency HX shell-to-pool
2501-01	0.2287	0.2541	0.75	250-01	581 * Emergency HX chimney
2501-02	0.2287	0.2541	0.75	250-01	581 * Emergency HX chimney
2501-03	0.2287	0.2541	0.75	250-01	581 * Emergency HX chimney
2501-04	0.2287	0.2541	0.75	250-01	581 * Emergency HX chimney
3161-01	0.5334	0.5556	1.6	316-01	591 * Emergency HX shell-to-pool
3161-02	0.5334	0.5556	1.6	316-02	591 * Emergency HX shell-to-pool
3161-03	0.5334	0.5556	1.6	316-03	591 * Emergency HX shell-to-pool
3161-04	0.5334	0.5556	1.6	316-04	591 * Emergency HX shell-to-pool
3501-01	0.2287	0.2541	0.75	350-01	581 * Emergency HX chimney
3501-02	0.2287	0.2541	0.75	350-02	581 * Emergency HX chimney
3501-03	0.2287	0.2541	0.75	350-03	581 * Emergency HX chimney
3501-04	0.2287	0.2541	0.75	350-04	581 * Emergency HX chimney

10. ACCUMULATORS

The accumulators (total of 4) are vertical cylindrical pressure vessels located in the upper portion of each reactor primary coolant system valve limited volume cell. Each accumulator tank (ID = 1.52 m, height = 4.57 m) contains 0.52 m³ of nitrogen gas, 7.0 m³ of heavy water and sufficient heat sink material to avoid low gas temperatures on rapid gas expansion.²⁹

In the model, the accumulators are modeled with standard RELAP5 control volumes. Pipe components 156, 256, and 356 consisting of six control volumes are defined, the sixth volume of which represents the 0.3556-m (14-in.)-diam standpipe connecting the accumulator to the primary coolant system. The first (uppermost) volume represents 87.2% of the tank volume, and the remaining four volumes are used to discretize the bottom 12.8% of the accumulator tank. The nitrogen bubble (specified through the input noncondensable quality) is completely contained within the first (largest) control volume and remains that way until the system pressure reaches about 1 atm. The accumulators are attached to the hot legs using single junctions 157, 257 and 357. Table 14 shows the heat structures used for representing the tank walls.

The standard RELAP5 accumulator component is inadequate because it does not allow flow back into the accumulator. The present pipe model also has problems with numerical diffusion of the nitrogen gas into the system. RELAP5 assumes the bubbly flow regime in the bubble volume instead of the more physically correct stratified condition. Past experience has shown that when many volumes are used to more clearly define the interface between the bubble and the liquid, problems result during movement of the interface across cell boundaries. Each time nitrogen is convected into a previously liquid filled control volume, it is introduced at the saturation temperature of the control volume instead of the actual temperature of the convected gas.

A new accumulator model has been developed by INEL; however, the new model requires the use of Parallel Virtual Machine (PVM) software which complicates the process of running RELAP5. Hence, unless the rate of expansion of the nitrogen bubble within the accumulator is crucial to a particular transient, it is recommended that the default model be used.

Pipe 156, 256 and 356

Segment 1 (tank)

L	=	4.09 m (total tank height of 4.57, discretization chosen with one big volume)
A	=	(7.52 m ³)/(4.57 m) = 1.65 m ² (based on L and Volume)
dZ	=	4.09 m
e	=	4.57 × 10 ⁻⁵ m, (ref. 20)
dh	=	sqrt[(1.65 m ²)(4)/3.1459] = 1.449 m

Segments 2-5 (tank)

L	=	0.12 m = (4.57 - 4.09)/4 (remainder of tank height)
A	=	(7.52 m ³)/(4.57 m) = 1.65 m ² (based on L and Volume)
dZ	=	0.12 m
e	=	4.57 × 10 ⁻⁵ m, (ref. 20)
dh	=	sqrt[(1.65 m ²)(4)/3.1459] = 1.449 m

Segment 6 (surge-pipe)

14-in. pipe, ID = 0.3255 m, A = 0.08322 m²
 L = 4.88 m, (ref. 21)
 dZ = 4.88 m
 e = 4.57 × 10⁻⁵ m, (ref. 20)
 dh = 0.3255 m (default)

Junction 157 between surge pipe and hot-leg pipe

A = 0.08322 m² (default)
 Kf = 0.5, (ref. 20)
 Kr = 1.0, (ref. 20)
 Use smooth area change
 dh = default

Table 14. Heat structure parameters representing accumulator tank wall

HS No.	Inside radius (m)	Outside radius (m)	Heat transfer area (m ²)	Left boundary volume No.	Right boundary Volume No.
1561-01	0.7245	0.7396	4.09	156-01	Insulated
1561-02	0.7245	0.7396	0.12	156-02	Insulated
1561-03	0.7245	0.7396	0.12	156-03	Insulated
1561-04	0.7245	0.7396	0.12	156-04	Insulated
1561-05	0.7245	0.7396	0.12	156-05	Insulated
2561-01	0.7245	0.7396	4.09	256-01	Insulated
2561-02	0.7245	0.7396	0.12	256-02	Insulated
2561-03	0.7245	0.7396	0.12	256-03	Insulated
2561-04	0.7245	0.7396	0.12	256-04	Insulated
2561-05	0.7245	0.7396	0.12	256-05	Insulated
3561-01	0.7245	0.7396	4.09	356-01	Insulated
3561-02	0.7245	0.7396	0.12	356-02	Insulated
3561-03	0.7245	0.7396	0.12	356-03	Insulated
3561-04	0.7245	0.7396	0.12	356-04	Insulated
3561-05	0.7245	0.7396	0.12	356-05	Insulated

11. MODERATOR TANK

A simplified model for the moderator tank was used. In the model, the moderator tank was represented by a single pipe 575 with appropriate boundary conditions imposed. The coolant source and pressure boundary were represented by TDV components 570 and 580, respectively, while the desired mass flow was specified through a TDJ component 571.

The moderator tank, also referred to as the reflector tank, surrounds the core pressure boundary tube (CPBT) and contains 31.0 m³ of heavy water. The tank has four inlets at the bottom and a single outlet at the top. The nominal pressure at the bottom of the tank is 0.36 MPa. In the present RELAP5 model, a simple, 5-node representation of the reflector tank is used and the reflector tank cooling system is not modeled. Two time dependent volumes are used as source and sink boundary conditions at the inlet (bottom) and outlet (top) of the reflector tank. The reflector tank is important only in the event of a rupture of the CPBT, in which case a more detailed model (developed by E. Schneider) can be used.

12. LETDOWN VALVES

The total letdown flow rate is 14.6 kg/s at steady state.²⁹ The valves are assumed to have a full-open area 0.00028355 m² (corresponding to a 0.75-in. diam). This full-open area was obtained by calibration assuming an abrupt area change at the valve, so that when the valve is 50% open, the total flow rate is 14.6 kg/s thru all three valves. The valves are assumed to discharge to atmospheric pressure. Also all of the letdown line losses are lumped into the valve junction, so the actual valve area will be somewhat larger (drawings indicate that the line has a 2-in. diam).

Valves 861, 862, and 863

Connect inlet plenum of main heat exchangers (106, 206, and 306) to letdown lines (865) leading to the letdown head tank.

A = 0.00028355 m² (calibrated for 50% opening to yield total flow of 14.6 kg/s)
Kf = 0
Kr = 0
dh = default

Invoke the abrupt area change model

Ltdown valve area is controlled by control variable 860.

The letdown control system consists of CVs 840, 842, 844, 845, 847, and 860 which define the control action recommended by Jose March-Leuba:³⁰

$$d = K(P - P_s)$$
$$\frac{dx}{dt} = (d - x)/\tau_{au},$$

where

d = demanded valve position (normalized),
 K = proportional constant = 5/MPa,
 P = the measured sensor pressure (the upper-core exit pressure is controlled directly),
 P_s = the setpoint pressure,
 x = normalized valve position (-1 for fully closed, 1 for fully open, and 0 at normal position),
 t = time (s),
 τ_{au} = the valve time constant = 1 s.

13. PRESSURIZING SYSTEM

The letdown and pressurizing systems are coupled through the cleanup system which is not modeled but may be added later to update the model when the cleanup system design has been defined. The pressurizing system consists of a pressurizing centrifugal pump (component 815), a check valve (component 825), an isolation valve (component 827), and a source tank (time dependent volume 800). The source tank is assumed to be a constant pressure mass source at 300 K (80 F) and 0.165 MPa (24 psia). Heat structures representing the tank walls and the piping in the pressurizing system are not included in the model. The pressurizing line has an ID = 0.1016 m (4-in.) and is connected to the main hot leg header (component 650), located 13.4 m (44 ft) downstream of the hot leg riser. The normal make-up flow rate is 14.6 kg/s and is equal to total letdown flow during steady-state operation. The pump speed is controlled using control variable 815 when establishing an initial steady-state (See Sect. 16.7). The pump is tripped only in the event of a loss-of-offsite power (trip 540), in which case the pump speed is determined using a torque balance on the pump shaft.

ERROR: All piping in the pressurizing system is assumed to be of 0.1016-m (4-in.) diam. However, the drawings indicate that it should be 3-in. piping.

Time-Dependent Volume 800 and 826

Source boundary conditions representing make-up tank. TDV 800 is used for the main pressurizing pump and TDV 826 is used for the standby pressurizing pump.

$$\begin{aligned} A &= 1.e6 \text{ m}^2 \\ V &= 1.e6 \text{ m}^3 \end{aligned}$$

Pressure is 0.165 MPa, assumes atmospheric plus 6 m (18 ft) of head.

Temperature is 300 K.

Trip Valve 805 and 827

Isolation valves if make-up tank drains. Valve 805 is used for the main pressurizing pump and valve 827 is used for the standby pressurizing pump. These valves connect volumes 800-01 or 826-01 (make-up tank) to volume 810-01 or 828-01 (pressurizer pump suction line).

$$\begin{aligned} A &= 0.00811 \text{ m}^2 = \pi/4 \times (0.1016 \text{ m})^2 \\ Kf &= 0.48 = 3 \times 0.16, \text{ three } 90^\circ \text{ bends, (ref. 31)} \\ Kr &= 0.48 \end{aligned}$$

This valve closes if trip 615 turns true.

Branch 810 and 828

$$\begin{aligned} L &= 6.096 \text{ m (assumption of 20-ft length from tank to pump)} \\ A &= 0.00811 \text{ m}^2 = \pi/4 \times (0.1016 \text{ m})^2 \\ dZ &= 0.0 \text{ m} \\ e &= 4.57 \times 10^{-5} \text{ m, (ref. 20)} \\ dh &= 0.1016 \text{ m (4-in.)} \end{aligned}$$

Pumps 815 and 830

Main and Standby Pressurizer Pumps

A	=	$0.00811 \text{ m}^2 = \pi/4 \times (0.1016 \text{ m})^2$
V	=	0.0203 m ³ (assumed volume of water in pump)
dZ	=	0.0 m

Suction junction connecting 810-01 or 828-01 to 815-01 or 835-01

Kf	=	0.16, assume 90° bends at inlet and outlet, (ref. 20)
Kr	=	0.16

Discharge junction connecting 815-01 to 820-01

Kf	=	0.16
Kr	=	0.16

Control of the main pressurizer pump is accomplished using both the speed table and the pump motor trip leading to a torque balance on the pump shaft. During an initial steady-state run, the proportional-integral control using control variable 591 is used to achieve the make-up flow of 14.6 kg/s. During a transient, the pump speed is held constant unless a loss-of-offsite power (LOSP) occurs (i.e., trip 540 turns true). As soon as trip 540 (referred to on card 8150301) becomes true, trip 620 (referred to on card 8156100) turns false which de-activates the pump velocity table so that a torque-balance equation is used to perform a coastdown.

The rated flow is specified to be 1.080816 m³/s, the rated head is 106.39 m, the rated speed is 221.55 rad/s, and the rated torque is 217.82 N-m. The moment of inertia for this pump is assumed to be 2.381 kg ·m².

Single Volumes 820 and 835

A	=	$0.00811 \text{ m}^2 = \pi/4 \times (0.1016 \text{ m})^2$
L	=	30.48 m
e	=	$4.57 \times 10^{-5} \text{ m}$, (ref. 20)
dh	=	0.1016 m (4-in.)

Valves 825 and 840

Check valves preventing reverse flow through the pressurizing pumps. Connects volume 820-01 or 835-01 to 850-01 (main supply line to primary).

A	=	0.00811 m ² (same as line)
Kf	=	$1.28 = 75f_t = 75 \times 0.017$, (ref. 20, p. A-26, A-27) where f_t is the turbulent friction factor
Kr	=	1.28

Time-Dependent Junction 845

This specified flow condition represents the emergency pressurizing pump, connecting volumes 810-01 to 850-01 (main supply line to primary). If trip 542 turns true, then the flow rate will begin ramping up over a 10-s period from zero to 25 m/s.

$$A = 0.001 \text{ m}^2$$

Branch 810 and 828

Main supply line to primary.

$$\begin{aligned} L &= 12.2 \text{ m} \\ A &= 0.00811 \text{ m}^2 = \pi/4 \times (0.1016 \text{ m})^2 \\ dz &= 0.0 \text{ m} \\ e &= 4.57 \times 10^{-5} \text{ m, (ref. 20)} \\ dh &= 0.1016 \text{ m (4-in.)} \end{aligned}$$

14. MATERIAL PROPERTIES

Thermal material properties are supplied to the RELAP5 program through tables as described in this section.

14.1 COMPOSITION No. 1 304L STAINLESS STEEL

The thermal conductivity for stainless steel type 304L (ref. 32) is shown in Table 15. The volumetric heat capacity (product of specific heat and density) is given in Table 16 (ref. 33).

**Table 15. Thermal conductivity
for 304L stainless steel**

T (K)	k (W/m-K)
273.2	14.7
300.	15.2
400.	17.0
500.	18.4
600.	19.8
700.	21.2
800.	22.5
900.	23.9
1000.	25.3
1200.	28.1
1400.	30.9

Table 16. Thermal volumetric heat capacity for 304L stainless steel

T (K)	ρc_p (J/m ³ -K)
250.	2.97e6
478.	3.00e6
700.	3.13e6
811.	3.23e6
866.	3.33e6
922.	3.43e6
1033.	3.59e6
1200.	3.76e6
1311.	3.82e6

14.2 COMPOSITION No. 2 ALUMINUM 6061

The thermal conductivity for aluminum type 6061(ref. 34) is shown in Table 17. The volumetric heat capacity (product of specific heat and density) is given in Table 18 (ref. 34).

Table 17. Thermal conductivity for aluminum 6061

T (K)	k (W/m-K)
271.9	155.0
299.7	155.0
349.7	161.9
399.7	165.9
499.7	179.8
549.7	183.9
649.7	180.9
749.7	174.9
799.7	171.9
849.7	167.9
924.7	85.9
999.7	87.9

Table 18. Thermal volumetric heat capacity for aluminum 6061

T (K)	ρc_p (J/m ³ -K)
271.9	2.429e6
299.7	2.429e6
399.7	2.542e6
499.7	2.666e6
599.7	2.791e6
699.7	2.915e6
799.7	3.039e6
899.7	3.163e6
924.7	2.826e6
1060.8	2.826e6

14.3 COMPOSITION N₆. 3 HAFNIUM

The thermal conductivity for hafnium³² is given in Table 19. The volumetric heat capacity (product of specific heat,³² and density,³³) is given in Table 20.

**Table 19. Thermal conductivity
for hafnium**

T (K)	k (W/m-K)
250.	23.6
273.2	23.3
300.	23.0
400.	22.3
600.	21.3
800.	20.8
1200.	20.9
1600.	21.5
2000.	22.6

**Table 20. Thermal volumetric heat
capacity for hafnium**

T (K)	ρc_p (J/m ³ -K)
252.9	1.870e6
278.0	1.898e6
315.5	1.924e6
400.	1.975e6
500.	2.031e6
600.	2.087e6
800.	2.199e6
1000.	2.314e6
1350.	2.514e6

14.4 COMPOSITION No. 4 OXIDE

The thermal conductivity of boehmite is assumed constant at 2.25 W/m-K (ref. 35). Also from, the volumetric heat capacity (product of specific heat,³² and density,³³ is given in Table 21.

Table 21. Thermal volumetric heat capacity for boehmite

T (K)	ρc_p (J/m ³ -K)
273.	2.198e6
373.	2.739e6
473.	3.096e6
573.	3.316e6
673.	3.453e6
773.	3.554e6
873.	3.638e6
973.	3.707e6
1073.	3.759e6
1173.	3.803e6

14.5 COMPOSITION No. 5 FUEL MEAT

The properties³⁶ of the fuel meat are given here. The thermal conductivity fo the fuel meat is given in Table 22. The volumetric heat capacity is given in Table 23.

Table 22. Thermal conductivity for the fuel meat

T (K)	k (W/m-K)
273.	51.86
333.	59.0
1333.	178.0

Table 23. Thermal volumetric heat capacity for the fuel meat

T (K)	ρc_p (J/m ³ -K)
273.	2.176e6
373.	2.289e6
473.	2.402e6
673.	2.628e6
873.	2.854e6
1073.	3.080e6
1273.	3.306e6

15. CONTROL VARIABLES

The control variables (CVs) in the RELAP5 input are used for calculating important output values (such as thermal limits or pressure drops), controlling the pump speeds and secondary flow rate, and calculating changes in reactivity due to temperature changes or control rod movement. Because of the extensive use of control variable in the model this section is subdivided to describe each control system separately. A control system is a set of control variables that work together for a single purpose.

15.1 PRIMARY COOLANT PUMP SPEED CONTROL

Initial Steady State

Before reactor transients can be simulated, the initial conditions (temperatures, pressures and mass flows) in the model must be established at an appropriate steady state. Control systems have been developed that can be used during a RELAP5 preliminary run to establish those initial conditions (see Table 24). One of these systems represents a Proportional-Integral-Derivative (PID) controller (CVs 77-83) on the primary pump speed to establish the desired inlet velocity to the upper core. The pump velocity tables (cards 1246100, 2246100, and 3246100 cards) are used with CVs 86, 136, and 186. These control variables are equal to the output from the PID controller.

Table 24. Control variables used to define proportional-integral-derivative pump speed controller during initial steady state

Control variable No.	Variable type	Description
77	TRIPUNIT	Flag indicating if a transient calculation has begun and the pump cavitation model is being used (1 if true, 0 if false).
78	CONSTANT	Specified upper core average channel inlet velocity. This is the setpoint value for the control system.
79	SUM	Error signal supplied to controller. Deviation from setpoint velocity.
80	MULT	Modified error signal (error is zeroed to avoid change in pump speed if the pump cavitation model is being used during a transient simulation).
81	PROP-INT	Proportional Integral control. Control constants have been chosen by trial and error.
82	DIFFREND	Derivative control.
83	SUM	Output from PID controller.

Reactor Transients: Normal Mode

After the steady-state simulation is completed, the results are loaded back into the input deck (using PYGI, a companion program developed for RELAP5 at INEL). The pump velocity table controls (cards 1246100, 2246100, and 3246100) are then normally changed so that CV 195 is used to control the pump speed (see Table 25). This control variable is simply equal to the constant steady-state pump speed, until a pump trip occurs, after which time a specified pump velocity coastdown (general table 135) is applied. General table 135 provides a gradual transition from full speed down to 10% (pony motor speed). Also trip No. 619 is added to the pump velocity control cards as a switch between (1) using the pump velocity table to specify the velocity (trip 619 is true), or (2) using a RELAP5 torque balance calculation on the pump shaft to determine the pump speed (trip 619 is false). The torque balance is normally used only when the pony motors become unavailable, such as when the pony motor batteries expire late in the transient.

Table 25. Control variables used to define proportional-integral-derivative pump speed controller during reactor transients

Control variable No.	Variable type	Description
195	FUNCTION	Extracts function value between zero and 1.0 from general table 135 and multiplies by steady-state pump speed in rad/s.

Reactor Transients: Pump Cavitation Mode

A separate alternative for pump speed control, shown in Table 26, during simulation of a reactor transient has been developed, but is not normally used. To activate the pump cavitation model, the pump velocity table control remains the same as during the steady-state initialization phase. However, trip 528 must also be true. The pump cavitation model (CVs 39-76 for loop 1, 91-126 for loop 2, and 141-176 for loop 3) has largely been borrowed from a RELAP5 model of the High Flux Isotope Reactor.³⁷ It works by artificially modulating the input pump speed in order to degrade the developed pump head to be consistent with real pump performance when the NPSH is insufficient. The true pump speed is tracked separately by the control system. As long as the pumps have not been tripped (such as during a steady-state run), the pump cavitation model is not used to modulate the pump speed. The output from the cavitation model (CVs 76, 126, and 176) is simply equal to the output of the PID controller, which is the constant steady-state speed if trip 528 is true.

Table 26. Pump cavitation model control variables

Control variable No.	Variable Type	Description
39	TRIPUNIT	Flag indicating primary pumps have been tripped
40	TRIPUNIT	Flag indicating primary pumps have not been tripped
41	FUNCTION	Torque on pump 1 due to friction
42	FUNCTION	Motor torque applied to pump 1 shaft
43	MULT	Hydraulic power developed by primary pump 1
44	DIV	Hydraulic torque applied to shaft of pump 1
45	SUM	Sum of pump 1 torques divided by the pump inertia
46	MULT	Differential adjustment for rate of change of pump speed
47	INTEGRAL	Adjustment for pump speed (rad/s)
48	SUM	Actual (true) pump speed for pump 1
49	MULT	Velocity head at suction of pump 1
50	SUM	Temperature in °C of volume 122-03
51	FUNCTION	Saturation pressure at volume 122-03 based on general table 35
52	SUM	Available NPSH to pump 1 (Pressure in 122-03 + CV 49 - CV 51)
55	SUM	Step 1 for calculation of required NPSH
56	DIV	Step 2 for calculation of required NPSH
57	SUM	Step 3 for calculation of required NPSH

Table 26. (continued)

Control variable No.	Variable Type	Description
58	DIV	Step 4 for calculation of required NPSH
59	MULT	Required NPSH for pump 1
60	DIV	Ratio of available NPSH to critical NPSH
61	FUNCTION	Head degradation factor (less than 1, greater than zero) for pump 1
62	DIV	Flow rate in m ³ /s through pump 1
63	MULT	Nondimensional flow ratio for pump 1 (ν)
64	MULT	Nondimensional speed ratio for pump 1 (α)
65	DIV	Quantity ν/α used to correlate nondimensional pump head
66	DIV	Quantity α/ν used to correlate nondimensional pump head
67	FUNCTION	Quantity HVN = (nondimensional pump head)/ ν^2 , based on homologous pump curve in general Table 41
68	TRIPUNIT	Flag to indicate if pump 1 is operating in the second portion (HVN) of the homologous data
69	TRIPUNIT	Flag to indicate if pump 1 is operating in the first portion (HAN) of the homologous data
70	MULT	Quantity HVN for pump 1 after head degradation factor has been applied (if $\nu/\alpha < 1$)
71	MULT	Square of degraded pump speed (if $\nu/\alpha > 1$)
72	POWERR	Degraded pump speed (if $\nu/\alpha > 1$) for pump 1
73	FUNCTION	Quantity α/ν for pump 1 based on degraded pump head (CV 70)
74	MULT	Degraded pump speed (if $\nu/\alpha < 1$)
75	SUM	Degraded pump speed (less than actual pump speed only if pump is cavitating) for pump 1
76	LAG	Degraded pump speed for pump 1 after time lag has been applied
84	MULT	If pump hasn't tripped this value is steady speed, if it has, this value is zero
85	MULT	If pump has tripped, this value is CV76, if not, this value is zero
86	SUM	Sum of pre-trip (CV 84) and post-trip contributions (CV 85). These contributions are mutually exclusive
91-126		Same as 41-76 except applied to pump 2
134-136		Same as 84-86 except applied to pump 2
141-176		Same as 41-76 except applied to pump 3
184-186		Same as 84-86 except applied to pump 3

15.2 COSTA FLOW EXCURSION HEAT FLUX LIMITS

One of the thermal limits of interest in the ANSR safety analysis is the Costa Onset of Significant Void (OSV) correlation. The correlation is being used to represent the heat flux which, if exceeded, will lead to flow excursion (a phenomenon that will result in burnout). The correlation is only a function of the bulk conditions in the coolant:

$$q_{COSTA} = \frac{V^{1/2}(T_{sat} - T_{bulk})}{12.8},$$

where V is the coolant velocity in m/s, $(T_{sat} - T_{bulk})$ is the subcooling in K and q_{COSTA} is the limit in MW/m². This limit is calculated using control variables for each control volume in the four hot channels (two each for lower and upper cores corresponding to 95% and 99.9% nonexceedance probability levels). Control variables 200-279 are used to calculate the 20 limits (5 nodes per channel). Each limit calculation requires four CVs:

- (1) A POWER variable is used to calculate the square root of the coolant velocity at the location.
- (2) A SUM variable is used to extrapolate the saturation temperature to the exit of the control volume.
- (3) A SUM variable is used to calculate the coolant subcooling at the exit of the control volume.
- (4) A MULT variable is used to combine the first three variables into the COSTA limit.

This information is used by the postprocessor to determine when and where the Costa limit is violated.

15.3 WALL SUPERHEAT AT CHF HOT SPOTS

Control variables 280–299 are used to calculate the difference between the CHF hot spot fuel surface temperatures and the bulk saturation temperature in the adjacent channel. This information is read by the postprocessor and indicates if T_w exceeds T_{sat} on the CHF hot stripes.

15.4 PECLET NUMBERS FOR HOT CHANNELS

The Peclet number ($Re \times Pr$) is calculated for each control volume in the four hot channels using CVs 300-339 (4 channels × 5 control volumes × 2 variables per Peclet number). The Peclet numbers are used by the postprocessor in determining the level of uncertainty associated with the Saha-Zuber correlation.

15.5 PRANDTL NUMBERS FOR HOT CHANNELS

The Prandtl numbers ($\mu c_p/k$) for the hot channels are calculated using CVs 444–483 (two variables per Prandtl number). Prandtl number is used by the post-processor in calculating Saha-Zuber thermal limits.

15.6 PRIMARY COOLANT SYSTEM TEMPERATURE (MHX SECONDARY FLOW) CONTROL

The primary coolant inlet temperature is controlled by varying the secondary flow through the main heat exchangers. During a preliminary simulation to establish a steady-state with the model, the flow rate at the time-dependent junctions on the main heat exchanger secondary sides is specified to be the output from a PI controller (CV 581 commented out in standard deck). The error signal is the difference between the desired core inlet temperature (control setpoint specified on CV 580) and the current RELAP5-calculated temperature at the core inlet (volume 500-01).

During the simulation of a reactor transient, CV 581 is changed back to the CONSTANT value and assigned that value reached during the preliminary steady-state simulation. Control variable 582 is a trip unit (assumes a value of 1.0 if trip 540 is true, and 0.0 if 540 is false) to indicate whether or not a loss-of-offsite power is indicated. Then, and only then, the secondary flow rate will be ramped down to 3.23% of the steady state value. Control variable 583 calculates the difference between the current time and 10.0 seconds (currently hard-wired as the

secondary trip time for a LOSP). This difference is then used a ramp factor starting at 0 and increasing to a maximum of 0.9677 with CV 584. The complement to the ramp factor (1-CV584) is CV585 which then is used to decrement the secondary flow rate by direct multiplication in CV 586. Because CV584 cannot exceed 0.9677, CV 585 cannot be less than 0.0323, and CV 586 does not fall below 3.23% of the steady-state value specified by CV 581.

15.7 PRESSURIZER PUMP SPEED CONTROL

The pressurizer pump speed must also have a controller in order to obtain the correct make-up flow rate while establishing a steady-state in the RELAP5 ANSR model. Control variables 587–591 provide a simple PID controller with constants that have proven to be acceptable. The exact values of these constants are not important since they are used only in establishing a new steady state and not in simulating a reactor transient. The error in make-up flow (CV 588) is calculated as the difference between the current make-up flow and the desired make-up flow (CV 587). This error is then supplied to a PROP-INT control variable (CV 589) and a DIFFRED control variable (CV 590) to produce the output pump speed for the pump (CV 591).

Additional control (CVs 801–807) is specified to simulate the coastdown of the pressurizer pump in the event that the make-up tank empties. This control system has not yet been used for a transient, but is available nonetheless. Control variables 801–804 keep track of the inventory that has left the make-up tank. If that inventory exceeds 8358.4 kg, trip 551 turns true, and CVs 805–807 and 815 are used to decrement the pump speed from full speed to zero over a 1-s time period.

15.8 CONTROL ROD AND CPBT HEATING.

The transient heating behavior in the control rods (CRs) and core pressure boundary tube (CPBT) is different from that of the fuel. To prevent underprediction of core power deposited in the CR and CPBT regions it was necessary to model the heating in these regions separately. Control variables 600 to 775 were developed by C. D. Fletcher for this purpose.^{38,39} These modifications were performed based on neutronics calculations for the L7 core design and have not been updated to the present G693 design.⁴⁰

15.9 STANDBY PRESSURIZER PUMP SPEED CONTROL

The standby pressurizer pump has not yet been used for transients, but this logic exists so that it is possible to start up a second pressurizer pump in the event of a main pump failure. General table 820 is used to specify a linear ramped start-up from zero speed to full speed over a 5 s time period. In the event of an empty make-up tank, CV 807 is multiplied onto the standby pressurizer pump speed to force a coastdown identical to that of the main pressurizer pump.

15.10 CORE PRESSURE DROP CALCULATION

RELAP5 outputs pressures at the centers of the control volumes. CVs 831–838 are used to calculate the core pressure drop in the upper and lower core. The core pressure drop is the pressure drop through the fuel channels only including entrance and exit losses. The pressures immediately upstream and immediately downstream of

the core are calculated by subtracting (or adding) one half of the frictional loss in that volume from the control volume (center) pressure. Consider two control volumes with center locations K and L. The junction between the two control volumes is location J. Then,

$$\Delta P_{K-L} = FWALFJ \times \alpha_J \times \rho_J \times \frac{|\nu_J| \nu_J}{2} ,$$

where FWALFJ is available in the RELAP5 Major Edit, α_J is the liquid void fraction, ρ_J is the liquid density, and ν_J is the liquid velocity at the junction. Although this information is not in the RELAP5 documentation, Cliff Davis of INEL supplied the following relationship:

$$FWALFJ = \frac{1}{\alpha_J \rho_J |\nu_J|} (\Delta x_K \frac{A_J}{A_K} FWALF_K + \Delta x_L \frac{A_J}{A_L} FWALF_L) ,$$

where Δx_K and Δx_L are the lengths of control volumes K and L, and A_J, A_K, A_L are the areas at junction J, control volume K and control volume L. FWALF_K and FWALF_L are control volume quantities only available if requested using the extended minor edits. By substituting this last equation into the expression for ΔP , two contributions to the frictional pressure drop are obtained. Considering the pressure drop only in volume K, (i.e., the frictional pressure drop between locations K and J, excluding concentrated losses at J), we get

$$\Delta P_{K-J} = \frac{1}{2} \frac{A_J}{A_K} \Delta x_K FWALF_K \nu_J ,$$

which is calculated directly by control variables 831, 832, 833 and 834 for the volumes immediately outside both the lower and upper cores. Since the areas and control volume length are constant, they are included in the scaling factor. For CV 831, the frictional pressure drop between the center and exit of control volume 505-01 (lower core inlet) is calculated by multiplying the scaling factor, SF₈₃₁, times the product of FWALF₅₀₅₋₀₁ and ν_{507-02} (507-02 is the junction connecting lower core inlet volume to fuel channels), where

$$SF_{831} = \frac{1}{2} \frac{A_{507-02}}{A_{505-01}} \Delta x_{505-01} = \frac{1}{2} \left(\frac{0.027675 \text{ m}^2}{0.05598 \text{ m}^2} \right) (1.545 \text{ m}) = 0.381903 \text{ m} .$$

Similarly at the lower-core exit (CV 831), upper-core inlet (CV 832), and upper-core exit (CV 833), the scaling factors can be calculated as follows:

$$SF_{832} = \frac{1}{2} \frac{A_{522-01}}{A_{520-01}} \Delta x_{520-01} = \frac{1}{2} \left(\frac{0.027675 \text{ m}^2}{0.055983 \text{ m}^2} \right) (0.05 \text{ m}) = 0.0123587 \text{ m} ,$$

$$SF_{833} = \frac{1}{2} \frac{A_{537-02}}{A_{535-01}} \Delta x_{535-01} = \frac{1}{2} \left(\frac{0.038359 \text{ m}^2}{0.07728 \text{ m}^2} \right) (0.05 \text{ m}) = 0.012409 \text{ m} , \text{ and}$$

$$SF_{834} = \frac{1}{2} \frac{A_{556-01}}{A_{555-01}} \Delta x_{555-01} = \frac{1}{2} \left(\frac{0.038359 \text{ m}^2}{0.07728 \text{ m}^2} \right) (0.7715 \text{ m}) = 0.191472 \text{ m} .$$

The scaling factor for CV 833 is in error in the input deck, causing the steady-state pressure drop to be too high by only 28.6 Pa.

The core exit-plane pressures are then calculated (CVs 835 and 837 for the lower and upper cores) by adding these one-half cell frictional losses back onto the exit volume center pressures. Each core pressure drop (including losses at entrance and exit) is then calculated (CVs 836 and 838 for lower and upper cores) by subtracting the one-half cell frictional loss at the entrance volume and the exit-plane pressure from the entrance volume center pressure.

15.11 POINT KINETICS REACTIVITY FEEDBACK

CONTROL VARIABLES 900–905

CVs 900–905 monitor the change in RELAP5-calculated moderator density in the active fuel region. The average channels and 95% NEPL hot channels are monitored to provide feedback to the pointkinetics model via CV 972. Table 27 shows the total fluid volume for the upper and lower core average and 95% hot channels.

ERROR: The fuel channel volume factors applied here are not up to date with the present core design, and the 99.9% hot channels are completely excluded in the feedback calculation.

Table 27. Calculation of volume factors for average and 95% NEPL hot channels

Fuel channel	Cnrtl volumes	Volume per cell (m^3)	Volume factor
Lower average	Pipe 510 cells	$0.027675 \times 0.1014 = 0.002806$	0.0836
Lower 95% hot	Pipe 515 cells	$0.000110698 \times 0.1014 = 1.122 \times 10^{-5}$	0.000334
Upper average	Pipe 540 cells	$0.038359 \times 0.1014 = 0.003890$	0.1158
Upper 95% hot	Pipe 545 cells	$8.9206 \times 10^{-5} \times 0.1014 = 9.045 \times 10^{-6}$	0.000269
Total		$0.006716 \times 5 = 0.0336$	

Control Variable 900

For pipe 510 (lower-core average channel) the correct volume factor for density feedback is 0.0836, as indicated above; however, the input deck incorrectly weights the densities in pipe 510 with the factor 0.0769.

Control Variable 901

For pipe 515 (lower-core 95% hot channel) the correct volume factor for density feedback is 0.000334, as indicated above; however, the input deck incorrectly weights the densities in pipe 510 with the factor 0.000322.

Control Variable 902

For pipe 540 (upper-core average channel) the correct volume factor for density feedback is 0.1158, as indicated above; however, the input deck incorrectly weights the densities in pipe 510 with the factor 0.122.

Control Variable 903

For pipe 545 (upper-core 95% hot channel) the correct volume factor for density feedback is 0.000269, as indicated above; however, the input deck incorrectly weights the densities in pipe 510 with the factor 0.000294.

Control Variable 904

This control variable sums up all of the average and 95% hot channel coolant density contributions to give a weighted average for the coolant density. The initial average density is subtracted out so that this control variable represents the deviation in average density from the initial condition.

The multipliers on control variable 900 and 901 were changed⁴¹ from 1.0 to 0.7600 (0.057/0.075) to account for a change in the assumed lower-core region density feedback coefficient from -0.075 to -0.057. The multiplier on control variable 902 and 903 was changed from 1.0 to 0.2267 (0.017/0.075) to account for a change in the assumed upper core region density feedback coefficient from -0.075 to -0.017 (R. M. Harrington request of April 9, 1992). Whereas the same multiplier was originally applied to both the lower and upper core region density changes in the scaling factor of CV 905, now the lower and upper core regions have different reactivity

coefficients of -0.057 and -0.017 respectively. The division by 0.075 is compensated by the multiplication of 0.75 in CV 905. To initialize CV 904 to a zero value, the additive constant, A_0 , was changed to -467.766.

Control Variable 905

This control variable calculates the reactivity contribution due to moderator (coolant in the fuel channels) feedback:

$$REACTIVITY = \frac{\Delta\rho}{\rho_{initial}} \times 100 \times \text{reactivity coefficient} ,$$

where the *reactivity coefficient* is 0.075 \$/%change in ρ (ref. 42).

CONTROL VARIABLES 908-913

As the fuel plates change in temperature they will expand or contract leaving less or more room for coolant in the channels. This temperature change produces an apparent change in moderator density which is represented with these control variables. It is assumed that the increase or decrease in coolant volume is produced only to the extent that the fuel plate dimensional change differs from that of the side plates. Hence the temperature difference, ΔT , used in calculating the change in apparent moderator density is defined as

$$\Delta T = (T_{fuel} - T_{sideplate})_{NEW} - (T_{fuel} - T_{sideplate})_{OLD} .$$

where T_{fuel} and $T_{sideplate}$ are the average fuel and sideplate temperatures at a given time. The change in fuel plate volume is

$$V - V_0 = (1 + \alpha\Delta T)^3 V_0 - V_0 = (1 + 3\alpha\Delta T + H.O.T.) - V_0 = 3\alpha\Delta TV_0 .$$

where *H.O.T.* are terms of order ΔT^2 and higher which are assumed to be very small, and therefore, neglected. Also,

α = coefficient of linear expansion,

V_0 = initial volume of fuel,

V = current volume of fuel.

The change in moderator volume is equal and opposite to the change in metal volume, and for the ANS fuel, the initial moderator volume is equal to the initial fuel volume (plates and gaps have same thickness) so,

$$V_m - V_{m0} = -(V - V_0) = -3a\Delta T ,$$

Rearranging and dividing through by the moderator volume, $V_{m0} = V_0$, gives

$$\frac{V_{m0}}{V_m} = \frac{V_m + 3aV_0\Delta T}{V_m} = 1 + 3a\Delta T \frac{V_{m0}}{V_m} \approx 1 + 3a\Delta T ,$$

The reactivity insertion due to thermal expansion of the fuel plates is proportional to $\Delta\rho/\rho$, where $\Delta\rho$ is the apparent density change of the coolant:

$$\frac{\Delta\rho}{\rho} = \frac{\frac{M}{V_m} - \frac{M}{V_{m0}}}{\frac{M}{V_{m0}}} = \frac{\frac{1}{V_m} - \frac{1}{V_{m0}}}{\frac{1}{V_{m0}}} = \frac{V_{m0}}{V_m} - 1 = 3a\Delta T .$$

The temperature difference between the fuel plate and side plates is calculated by weighting the individual heat structures (using the same volume weighting factors). Again, the 99.9% hot channel is not included and the weighting factors are slightly off (see previous discussion).

Control Variable 908

The calculation for the temperature difference between the lower-core average channel fuel plates and side plates is performed here by summing the differences between each average fuel heat structure temperature and the average (of inner- and outer-) side-plate temperature. This summation is then weighted by the 0.0769 weighting factor, as was done for the liquid densities.

Control Variable 909

The calculation for the temperature difference between the lower-core hot channel fuel plates and side plates is performed here by summing the differences between each average fuel heat structure temperature and the average (of inner- and outer-) side-plate temperature. This summation is then weighted by the 0.000322 weighting factor, as was done for the liquid densities.

Control Variable 910

The calculation for the temperature difference between the upper-core average channel fuel plates and side plates is performed here by summing the differences between each average fuel heat structure temperature and the average (of inner- and outer-) side-plate temperature. This summation is then weighted by the 0.122 weighting factor, as was done for the liquid densities.

Control Variable 911

The calculation for the temperature difference between the upper-core hot channel fuel plates and side plates is performed here by summing the differences between each average fuel heat structure temperature and the average (of inner- and outer-) side-plate temperature. This summation is then weighted by the 0.000292 weighting factor, as was done for the liquid densities.

Control Variable 912

Sum of the contributions to the weighted average temperature difference between the fuel plates and the side plates.

The multiplier on control variables 908 and 909 were changed⁴¹ from 1.0 to 0.7600 (0.057/0.075) to account for a change in the assumed lower-core region density feedback coefficient from -0.075 to -0.057. The multipliers on control variable 910 and 911 were changed from 1.0 to 0.2267 (0.017/0.075) to account for a change in the assumed upper-core region density feedback coefficient from -0.075 to -0.017. Whereas the same multiplier was originally applied to both the lower- and upper-core region density changes in CV 913, now the lower- and upper-core regions have different reactivity coefficients of -0.057 and -0.017, respectively (R. M. Harrington request of April 9, 1992). The division by 0.075 is compensated by the multiplication of 0.75 in CV 913. To initialize CV 912 to a zero value, the additive constant, A_o , was changed to -89.1343.

Control Variable 913

$$CV913 = \frac{\Delta p}{\rho_{initial}} \times 100 \times R = -3 \times 27.5 \times 10^{-6} \Delta T \times 100 \times 0.075 = 0.000619 \Delta T .$$

This control variable calculates the reactivity contribution due to thermal expansion of the fuel channels. where the *reactivity coefficient*, R , is 0.075 \$%/change (from J. M. Ryskamp 12/06/89) in apparent density, and the thermal expansion coefficient is that for aluminum $27.5 \times 10^{-6} \text{ K}^{-1}$.

Control Variable 917

Density feedback for inlet and outlet plenums and bypass gap regions. Table 28 shows the volumes of each cell in the 9/16/94 version of the model. These volumes are different from those that are used in CV 917 because they have been modified since the input for CV 917 was generated. None of the weighting factors is correct in the input model; however, they are close to what they should be and probably within the accuracy of the modeling approximations.

Table 28. Calculation of correct volume factors for plenums and bypass gap regions

Region	Cnrtl volumes	Volume per cell (m ³)	Correct volume factor	Input volume factor
Core Inlet	500-01	0.1799 × 0.331 = 0.059546	0.07144	0.14586
Lower-Core In	505-01	0.05598 × 1.545 = 0.08649	0.10377	0.07207
Upper-Core In	530-01	0.07728 × 1.545 = 0.119398	0.14325	0.12983
Lower-Core Bypass	530-02 thru 530-06	0.07728 × 0.1014 = 0.007836	5 @ 0.0094013	Avg of 0.03863
Upper-Core Out 1	555-01	0.07728 × 0.7715 = 0.05962	0.071529	0.18451
Upper-Core Out 2	557-01	0.07728 × 1.2853 = 0.09933	0.119172	none
Upper-Core Bypass	525-01	0.055983 × 0.2028 = 0.01135	0.013617	0.01550
Lower-Core Out	525-02	0.055983 × 2.3610 = 0.13218	0.158584	0.12177
Core Outlet	565-01	0.24663 × 0.918 = 0.22641	0.271636	0.25263
Total		0.8335	1.00000	1.0

Control Variable 918

Control variable 918 is calculated as

$$CV918 = 0.0333 \text{ $/}%\text{densitychange} \times 100 \times \frac{\Delta\rho}{\rho}$$

The reactivity coefficient assumed for the annular inlet and outlet regions is 0.0333 \$/% change in density. This number is specified as the scaling factor for CV 918. The incremental change in density, $\Delta\rho$, is the result from CV 917, and the initial density divided into 100 is included in CV 918 as the multiplier on CV 917.

Control Variable 922

Mid-core density feedback. The two volumes 520-01 and 535-01 are short volumes that are located axially between the fuel elements. Table 29 shows the volume weighting factors.

Table 29. Calculation of volume factors for mid-core annular regions

Region	Control volumes	Volume per cell (m^3)	Correct volume factor	Input volume factor
Lower core annulus	520-01	$0.055983 \times 0.05 = 0.002799$	0.42008	0.34802
Upper core annulus	535-01	$0.07728 \times 0.05 = 0.003864$	0.57992	0.65198
Total		0.006663	1.00000	1.0

Control Variable 923

Control variable 923 is calculated as

$$CV923 = 0.0333 \text{ } \$/\% \text{ density change} \times 100 \times \frac{\Delta\rho}{\rho} .$$

The reactivity coefficient assumed for the annular midcore regions is 0.0333 \$/% change in density. This number is specified as the scaling factor for CV 923. The incremental change in density, $\Delta\rho$, is the result from CV 922, and the initial density divided into 100 is included in CV 923 as the multiplier on CV 922.

Control Variable 928

Control rod region moderator density feedback.

Originally (June 27, 1989, C. D. Fletcher calculation work sheets, p. 182), the model for the control rod region consisted of a single pipe 560. The four volumes in pipe 560 were weighted, as shown in Table 30. Each volume has a cross-sectional area of 0.0229678 m^2 , equal to the central hole area ($d = 0.095 \text{ m}$) less (originally) four control rod cylinders ($d = 0.041402 \text{ m}$). The total length spanned by pipe 560 in the original model is 3.0826 m.

Table 30. Original calculation of volume factors for control rod region

Cntrl volumes	Volume per cell (m ³)	Volume factor
560-02	$0.0229678 \times 0.3344 = 0.0076804$	0.108465
560-03	$0.0229678 \times 0.1896 = 0.00435469$	0.061499
560-01	$0.0229678 \times 1.0706 = 0.0245893$	0.347259
560-04	$0.0229678 \times 1.4884 = 0.0341853$	0.482777
Total	0.0708097	1.0

Method used by C. D. Fletcher² to calculate weighting factors

Since the original calculations were performed, the control rod region has been updated twice. The cross-sectional area has changed, but in the original calculation, the area was constant in the axial direction anyway, so the weighting was based on the lengths. The original weightings are applied to the most recent control rod region discretization by apportioning them to existing volumes based on lengths (and areas, for the three parallel pipes 561, 562, and 563). The pipe lengths of 1.0732 m, 0.2528 m, 0.2028 m, and 1.8472 m for volumes 560-01, -02, -03, and -04 are used to apportion the weighting factors. The old volume length for 560-01 is apportioned 0.769 to volume 560-01, and 0.1014 to each of the first three volumes in pipes 561, 562, and 563. The old volume length for 560-02 of 0.2528 is apportioned 0.1014 to each of cells 4 and 5 and 0.05 to cell 6 of pipes 561, 562, and 563. The old volume length for 560-03 of 0.2028 is apportioned 0.1014 to each of cells 7 and 8 of pipes 561, 562, and 563. Finally, the old volume length of 560-04 of 1.8472 m is apportioned 0.1014 to each of cells 9, 10 and 11 of pipes 561, 562, and 563, and 1.543 to volume 564-01.

Table 31 shows a direct calculation of the weighting factor based on the current input geometry (correct) compared against the input weighting factors based on C. D. Fletcher calculation (including area weighting between the parallel channels).

² C. D. Fletcher's calculational sheets for 3-CR Model dated 12-30-91 cite volume length numbers that are not the same as the lengths in the table which were taken from the original calculation work sheets (3-1-89). Since the original worksheets were written, the core length has changed from 0.474 m to 0.507 m. This discrepancy explains the difference in the lengths, but is inconsistent with the use of the weighting factors calculated with the 0.474-m core.

Table 31. Calculation of volume factors for central rod region

Cntrl volumes	Volume per cell (m ³)	Correct volume factor	Input volume factor
560-01	$0.03018 \times 2.419 = 0.0730054$	0.426603	0.24883
561-01	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.00669
561-02	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.00669
561-03	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.00669
562-01	$0.0165753 \times 0.1014 = 0.0016706$	0.00976205	0.02418
562-02	$0.0165753 \times 0.1014 = 0.0016706$	0.00976205	0.02418
562-03	$0.0165753 \times 0.1014 = 0.0016706$	0.00976205	0.02418
563-01	$0.0013196 \times 0.1014 = 0.000133797$	0.000781835	0.001936
563-02	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.001936
563-03	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.001936
561-04	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.00888
561-05	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.00888
561-06	$0.00456159 \times 0.05 = 0.00022808$	0.00133277	0.00438
562-04	$0.0164753 \times 0.1014 = 0.0016706$	0.00976205	0.03206
562-05	$0.0164753 \times 0.1014 = 0.0016706$	0.00976205	0.03206
562-06	$0.0164753 \times 0.05 = 0.0008234765$	0.00481194	0.01581
563-04	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.00257
563-05	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.00257
563-06	$0.24663 \times 0.05 = 0.0123315$	0.0720584	0.00127
561-07	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.006274
561-08	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.006274
562-07	$0.0164753 \times 0.1014 = 0.0016706$	0.00976205	0.02266
562-08	$0.0164753 \times 0.1014 = 0.0016706$	0.00976205	0.02266
563-07	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.001815
563-08	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.001815
561-09	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.005407
561-10	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.005407
561-11	$0.00456159 \times 0.1014 = 0.000462545$	0.00270285	0.005407
562-09	$0.0164753 \times 0.1014 = 0.0016706$	0.00976205	0.01953
562-10	$0.0164753 \times 0.1014 = 0.0016706$	0.00976205	0.01953
562-11	$0.0164753 \times 0.1014 = 0.0016706$	0.00976205	0.01953
563-09	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.001564
563-10	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.001564
563-11	$0.24663 \times 0.1014 = 0.000133797$	0.000781835	0.001564
564-01	$0.03018 \times 2.0568 = 0.0620742$	0.362727	0.403272
Total	0.171132	1.00000	1.0

Control Variable 929

Control variable 929 is calculated as

$$CV929 = 0.0910 \text{ \$}/\% \text{ density change} \times 100 \times \frac{\Delta\rho}{\rho}$$

The reactivity coefficient assumed for the control rod region is 0.00910 \\$/\% change in density (R. M. Harrington request 4/9/92). This number is specified as the scaling factor for CV 929. The incremental change in density, $\Delta\rho$, is the result from CV 928, and the initial density divided into 100 is included in CV 929 as the multiplier on CV 928.

Control Variable 934

Control variable 934 calculates the moderator tank feedback:

$$CV934 = -0.0174 \text{ \$/K} \times (T_{MT} - T_{MTinitial})$$

The reactivity coefficient assumed for the moderator tank region is -0.0174 \\$/K (per R. M. Harrington request, November 29, 1989).

15.12 CONTROL ROD REACTIVITY

The effect of control rod movement on the reactivity of the core is accounted for in the mode (Table 33). The shim speed control, to keep the reactor power constant is represented with control variables 943-961. Then the reactivity of the rods is determined with CVs 965, 967, 969, and 970. The control rods are assumed to move only during normal shim adjustment at a maximum rate⁴³ of 5.75 in./s or during reactor scram.

Table 33. Control rod reactivity control variables

Control Variable No.	Variable Type	Description
943	SUM	Time step calculation (current time less old time)
944	SUM	Old time (value is updated only after time step is calculated)
945	TRIPUNIT	Equal to 1.0 if a scram (Trip 510) has not yet occurred
946	TRIPUNIT	Equal to 1.0 if a scram (Trip 510) has occurred
949	SUM	Error in reactor power (current power less setpoint) in MW
950	LAG	Lag in reactor power (CV 949) arbitrarily selected to be 0.5 s

16. GENERAL TABLES

General tables are used for specifying tabular functions that are referenced by control systems and some RELAP5 thermal-hydraulic components, such as valves, pumps, heat structures, and time-dependent volumes and junctions. All the tables used in the RELAP5 ANSR input model are shown in Table 33.

Table 33. Summary of general tables used in RELAP5 input model

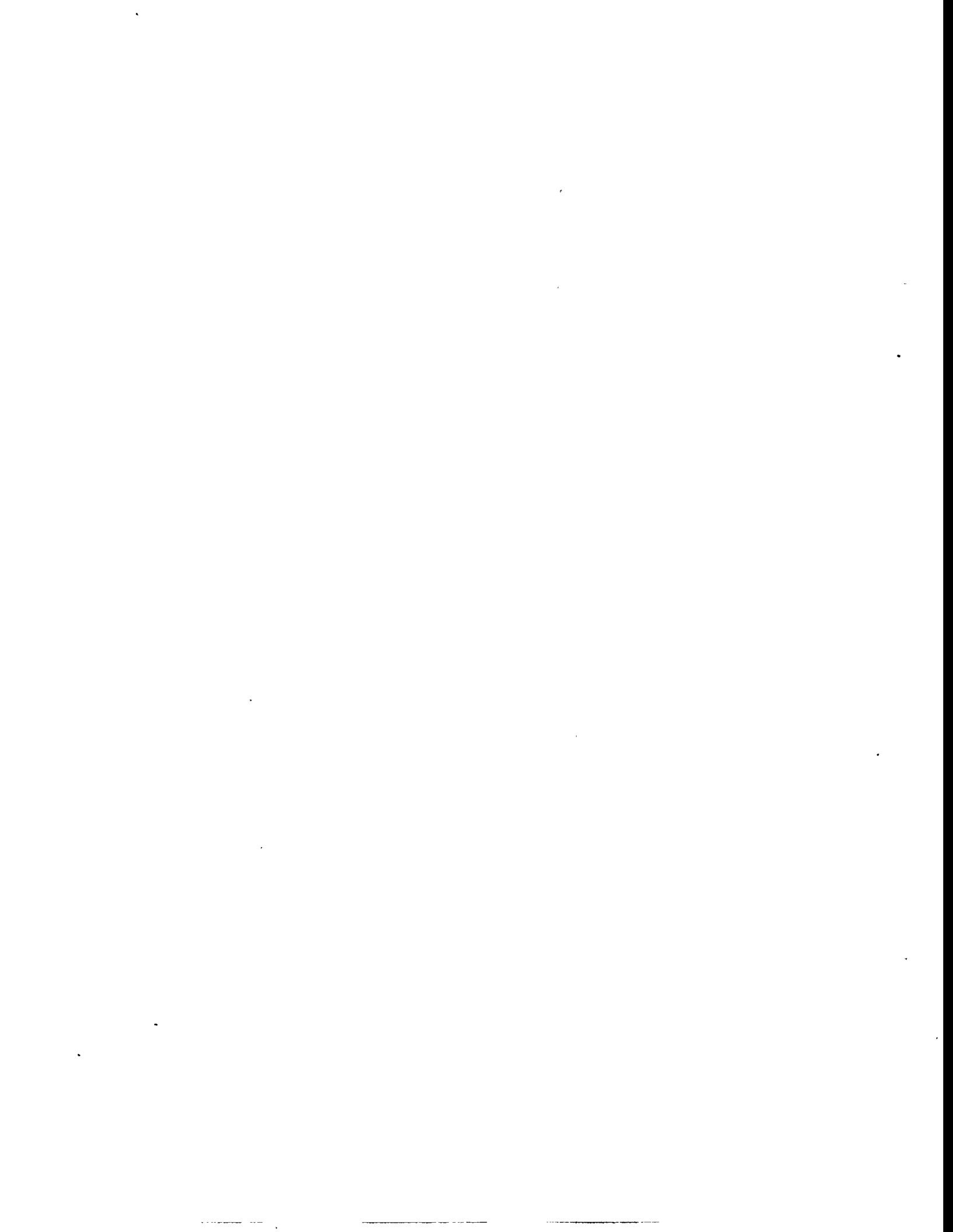
Table No.	Abcissa	Ordinate	Used by
35	Temperature	Saturation Pressure (Pa)	Pump cavitation model (CVs 51, 101, 151)
39	NPSH ratio	Head degradation factor	Pump cavitation model (CVs 61, 111, 161)
41	v/α	h/v^2	Pump cavitation model (CVs 67, 117, 167)
42	h/v^2	v/α	Pump cavitation model (CVs 73, 123, 173)
43	α	Pump Frictional Torque (N-m)	Pump cavitation model (CVs 41, 91, 141)
44	α	Pony-motor torque (N-m)	Pump cavitation model (CVs 44, 94 144)
135	Time (s)	α	Specified speed primary pump coastdown curve (CV 195)
235	Time (s)	α	Inactive
335	Time (s)	α	Inactive
500	Time (s)	Power (W)	Inactive
501	Time (s)	Temperature (K)	Pool temperature (constant at 311.15 K)
511	Temperature (K)	Heat transfer coefficient (W/m ² -K)	Film coefficient between 356-mm (14-in.)-diam horizontal pipe and pool
521	Temperature (K)	Heat transfer coefficient (W/m ² -K)	Film coefficient between 610-mm (24-in.)-diam horizontal pipe and pool
531	Temperature (K)	Heat transfer coefficient (W/m ² -K)	Film coefficient between 610-mm (24-in.)-diam horizontal pipe and pool
581	Temperature (K)	Heat transfer coefficient (W/m ² -K)	Film coefficient between vertical pipe and pool
591	Temperature (K)	Heat transfer coefficient (W/m ² -K)	Film coefficient between 1111-mm (43.75-in.)-diam horizontal cylinder and pool
599	Temperature (K)	Heat transfer coefficient (W/m ² -K)	Film coefficient between 2108-mm (83-in.)-diam horizontal cylinder and pool

Table 33. (continued)

Table No.	Abcissa	Ordinate	Used by
606	Time (s)	Normalized fission power	Control Rod and CPBT heating
607	Time (s)	Normalized decay power	Control Rod and CPBT heating
608	Time (s)	A1-28 decay power	Control Rod and CPBT heating
820	Time (s)	Pump speed (rad/s)	Standby pressurizer pump speed (CV 830)
956	Time (s)	Scram rod speed (m/s)	Scram rod insertion rate (CV 956)
970	Rod Position (in.)	Reactivity (\$)	Scram rod reactivity (CV 970)

17. POINT KINETICS

The heat generated in the fuel plates and coolant channels caused by neutronic heating is calculated by RELAP5 with a point (space-independent) kinetics model. The heating in the control rods and CPBT is calculated separately by the control system that has already been discussed. One source of information for the point kinetics input is ref. 42. As the design evolved, two key parameters, β (delayed neutron fraction), and λ (neutron generation lifetime), changed periodically. The ans91694in version of the model uses $\beta = 0.0074$, and $\lambda = 0.0013$ s (ref. 44). The total power for the reactor is 330 MW, and 344 MW with uncertainties included. The reactivity specified as input to the point kinetics model comes from control variable 972, which is a summation of several contributions, including control and safety rod worths and moderator density feedback.

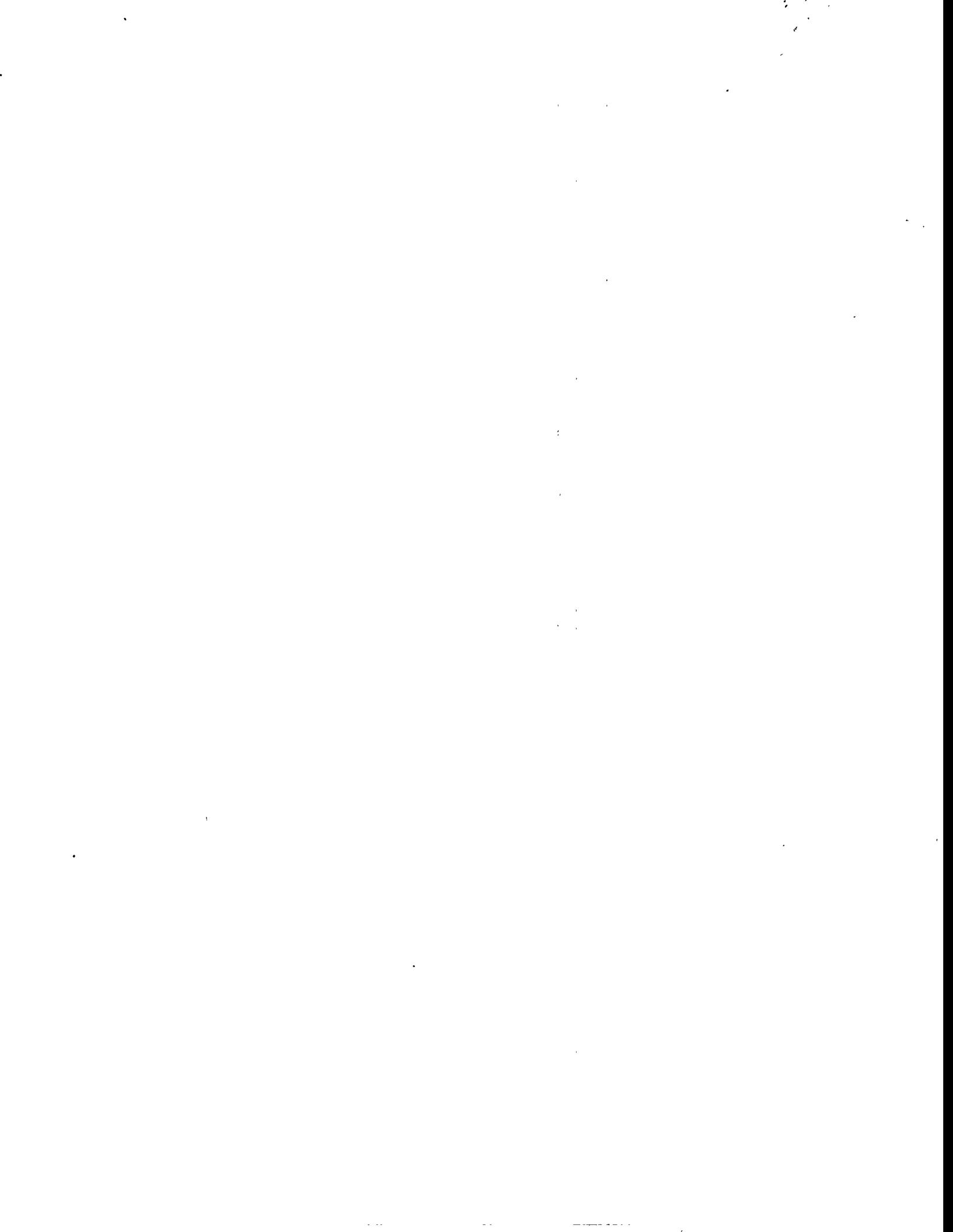


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APPENDIX A: RELAP5 INPUT FOR ANSR MODE (ans91694in)

*ANSR relaps system model - COARSE - ans5094in updated power densities

*CHANGES MADE SINCE 2.10-94 VERSION

- *Areas and DH's for 560 and 564 assuming annulus w/ 190mm ID & 273mm OD
- *Pressurizer line from 4" to 3"
- ===== PERTURBED CONDITIONS CASE TRANSIENT = FIRST 10 S =====
- 1. PRESSURE AT CORE EXIT
 - Control upper core average channel exit pressure so that the primary temp. should be 45.6 deg C (318.75 K).
 - exit pressure is at 94.9% (35% uncertainty) of the best-estimate case and the pressure drop is 1.54 MPa (9% uncertainty).
- Pexit = 1.78 * 0.949 = 1.69 MPa
- 2. TEMPERATURE AT CORE INLET
 - Hold secondary flow constant based on steady-state run
 - primary temp. should be 45.6 deg C (318.75 K).
- 3. VELOCITY AT CORE INLET
 - Primary coolant pump speed is held constant until tripped.
- 4. REACTOR POWER
 - Set total power in point kinetics model at 1.0424*330 = 344 MW
- 5. LEAKDOWN VALVE AREA
 - Calibrate leakdown valve area to 0.5 open at a pressurizing flow rate of 14.6 kg/s at nominal pressure.
- 6. PRESSURIZING FLOW
 - Pressurizer pump speed is held constant until tripped.
- 7. CORE ROUGHNESS
 - Core roughness is calibrated based on ANS steady-state code (assuming 25 m/s) core pressure drop at perturbed (95% uncert) conditions. This pressure drop is imposed on the upper core to get the calibrated nominal core roughness.
- 8. VELOCITY IN CONTROL RODS AND CPBT
 - Loss coefficients on functions 550-12, 564-01, 564-02, and 564-03 are calibrated to get velocities in the control rod channels to be 6.0 m/s and the entrance velocity in the CPBT annulus to be 4.3 m/s.
- 9. CONTROL ROD POSITION
 - The control rod position at steady-state is 7777777777777777
- 10. REACTOR TRIPS
 - Trips on FFR, High temperature and low pressure are enabled.
- 11. HEAT STRUCTURE HEAT CAPACITIES
 - Heat capacities are set to their true values.
- 12. LOSS-OF-OFFSITE POWER
 - Trips of the pressurizer pump and secondary coolant flow are set to occur at 10 s.

```

0000105 30. 40. 8.544
0000110 nitrogen
0000120 5700100000 0. d20 primary
0000121 1300100000 0. h20 mbx/sec
0000122 2300100000 0. h20 mbx2sec
0000123 3300100000 0. h20 mbx3sec
0000124 1338010000 0. h20 ebx/sec
0000125 2338010000 0. h20 ebx2sec
0000126 3338010000 0. h20 ebx3sec

time-step and output frequency information
0000201 50.00 1.e-7 0.0033 03 303 100000 100000
0000202 9000.0 1.e-7 0.0033 03 3000 100000 100000
expanded edit/plot variables
20800001 htimp 550100204 * Max CPBT Temp
20800002 htimp 562100306 * Max CR- Alt Temp
20800003 htimp 562100307 * Max CR- Hf Temp
20800004 fwaf 5205010000
20800005 fwaf 5205010000
20800006 fwaf 535010000
20800007 fwaf 535010000
20800008 fwaf 510010000
variables for modified sabra-zuber correlation
20800011 csuibf510010000
20800012 csuibf510020000
20800013 csuibf510030000
20800014 csuibf510040000
20800015 csuibf510050000
20800016 csuibf515010000
20800017 csuibf515020000
20800018 csuibf515030000
20800019 csuibf515040000
20800020 csuibf515050000
20800021 csuibf516010000
20800022 csuibf516020000
20800023 csuibf516030000
20800024 csuibf516040000
20800025 csuibf516050000
20800026 csuibf5240010000
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20800036 csuibf546010000
20800037 csuibf546020000
20800038 csuibf546030000
20800039 csuibf546040000
20800040 csuibf546050000
20800041 thcont 510010000
20800042 thcont 510020000
20800043 thcont 510030000
20800044 thcont 510040000
20800045 thcont 510050000
20800046 thcont 515010000
20800047 thcont 515020000
20800048 thcont 515030000

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0000318 thermf 515040000 tempf 490010000
 20800049 thermf 515050000 mflowf 136010000
 20800050 thermf 516010000 mflowf 256010000
 20800051 thermf 516020000 mflowf 356010000
 20800052 thermf 516030000 mflowf 515400500
 20800053 thermf 516040000 htrf 515400500
 20800054 thermf 516050000 htrf 515400500
 20800055 thermf 540010000 pmpvel 815
 20800056 thermf 540020000 cutivar 840
 20800057 thermf 540030000 cutivar 860
 20800058 thermf 540040000 cutivar 860
 20800059 thermf 540050000 cutivar 860
 20800060 thermf 540060000 cutivar 860
 20800061 thermf 545010000 cutivar 860
 20800062 thermf 545020000 cutivar 480
 20800063 thermf 545030000 cutivar 481
 20800064 thermf 545040000 cutivar 481
 20800065 thermf 545050000 trip input
 20800066 thermf 546010000 * high power-to-flow ratio trips
 20800067 thermf 546020000 0000501 cnthar 940 gt null 0 1.201.1.
 20800068 thermf 546030000 0000502 time 0 gt tuncd 301 0.2001.-1.
 20800069 thermf 546040000 * high temperature = 1.2245 deg C = 54.8 deg C
 20800070 thermf 546050000 0000503 tempf 5000100000 gt null 0 328.05 1.-1.
 20800071 vscf 510010000 0000504 time 0 gt timcd 503 2.01.-1. *high temp
 20800072 vscf 510020000 *Therefore, the setpoint pressure is 1.3399 MPa.
 20800073 vscf 510030000
 20800074 vscf 510040000
 20800075 vscf 510050000
 20800076 vscf 515010000
 20800077 vscf 515020000
 20800078 vscf 515030000
 20800079 vscf 515040000
 20800080 vscf 515050000
 20800081 vscf 516010000
 20800082 vscf 516020000
 20800083 vscf 516030000
 20800084 vscf 516040000
 20800085 vscf 516050000
 20800086 vscf 540010000
 20800087 vscf 540020000
 20800088 vscf 540030000
 20800089 vscf 540040000
 20800090 vscf 540050000
 20800091 vscf 545010000
 20800092 vscf 545020000
 20800093 vscf 545030000
 20800094 vscf 545040000
 20800095 vscf 545050000
 20800096 vscf 546010000
 20800097 vscf 546020000
 20800098 vscf 546030000
 20800099 vscf 546040000
 20800100 vscf 546050000
 0000311 cnthar 835 * minor edit requests
 0000312 cutivar 836
 0000313 cutivar 837
 0000314 cutivar 838
 0000317 rkpow 0

0000321 mflowf 567010400
 0000322 p 505010000
 0000323 vehf 507010200
 0000324 vehf 537010200
 0000325 p 550010000
 0000326 vehf 550070000
 0000328 vehf 559010100
 0000329 vehf 559010200
 0000330 vehf 559010300
 0000331 cnthar 835
 0000332 cutivar 836
 0000333 cutivar 837
 0000334 cutivar 838
 0000341 cnthar 860
 0000342 tempf 505010000
 0000343 cutivar 480
 0000344 cutivar 481

* Low-pressure trip is 80% of nominal at sensor location
 * Sensor location is in volume 645-01. 2.44 m downstream of hotleg riser
 * Nominal pressure taken from 645-01 in "nomis50193in" to be 1.674979 MPa.
 * Therefore, the setpoint pressure is 1.3399 MPa.
 0000506 cutivar 839 gt null 0 1.3399e-1.
 * 0000506 time 0 gt null 0 1.e61.-1.
 * reactor trip
 0000508 time 0 gt null 0 1.e61.-1. *manual trip
 0000510 time 0 gt timcd 603 0.0301.-1.
 0000515 time 0 1.e61 10. *loop1 isolation
 0000516 time 0 1.e61 10. *loop2 isolation
 0000517 time 0 1.e61 10. *loop3 isolation
 * pump cavitation model trips
 0000528 time 0 gt null 0 1.d61 - begin the transient if true
 0000536 cnthar 65 gt null 0 1. n * valpha range pump pu-1
 0000537 cnthar 115 gt null 0 1. n * valpha range pump pu-2
 0000538 cnthar 165 gt null 0 1. n *valpha range pump pu-3
 0000540 time 0 gt null 0 1.d61 - loss of offsite power
 * pressurizer pump trips
 0000541 time 0 & null 0 1.e6 1. *standby prrz pump
 0000542 time 0 & null 0 1.e6 1. *emergency prrz pump
 0000550 time 0 & null 0 1.e6 1. *standby spec'd table trip
 0000551 cnthar 804 gt null 0 8358.41.-1. fm tank empty
 0000552 time 0 st timcd 551 110 1.-1. *prrz sys isolate
 * loss power to primary coolant pumps (use torque balance)
 0000553 time 0 gt null 0 1.d61 .
 0000560 p 850010000 gt null 0 4.42856 n.-1. *safety valve
 0000561 p 850010000 gt null 0 4.600e-6 n.-1. *safety valve

0000569 time 0 gt null 0 1.e6 1.-1.
 0000570 599
 0000571 502 or 504 1 -1.
 0000572 601 or 506 1 -1.
 0000573 602 or 508 1 -1.
 0000574 603 or 510 1 -1.
 0000575 560 and 611 n 1.
 0000576 561 or 610 n -1.
 0000577 -552 or -552 n 0.
 0000578 -540 and -540 n 0.
 0000579 -541 and -541 n 0.

0000635 506 or 540 1 -1.0

4921031 9.37546 9.91641 4 * 1854.196

4921051 4.420535 4.7872 5 * 146.6658

4921061 .669406 .817959 6 * 146.6658

4921071 1.440176.5 1.440423.5 7 * 001320477

HYDRODYNAMIC COMPONENT INPUT

CORE REGION

* hydro component name "cryswe" component type pipe

4900001 1

* hydro volarea 0.1993

4900101 1

* hydro length 0.343

4900301 1

* hydro volume 0.0

4900401 1

* hydro vertangle 90.

4900601 1

* hydro delaz 0.543

4900701 1

* hydro roughness hyd diam 0.2599

4900801 1

* hydro fe 00

4901001 1

* hydro ch pressure tempc 176629.8 2419499. 0. 0.1

4901201 0 3381195. 176629.8 2419499. 0. 0.1

* hydro component name "cryswe" component type mfpmln

4920000 0

* hydro no. junks 7

4920001 0

* hydro from to area floss loss vecls

4920011 174010000 490010003 0. 0. 0. 0.0101

4920012 1.0 1.0 1.0 0 0 1

4920021 274010000 490010003 0. 0. 0. 0.0101

4920022 1.0 1.0 1.0 0 0 2

4920031 274010000 490010003 0. 0. 0. 0.0101

4920032 1.0 1.0 1.0 0 0 3

4920041 490010000 500000000 0. 0. 0. 0.0100

4920042 1.0 1.0 1.0 0 0 4

* Kentrance = 35 - constrained by flow through control rod channels

4920051 493010000 560000000 0. 35.0 35.0 0.0000

4920052 1.0 1.0 1.0 0 0 5

4920061 490010001 495010002 0. 0. 0. 0.0100

4920062 1.0 1.0 1.0 0 0 6

4920071 274010000 490010003 0. 0. 0. 0.0101

4920072 1.0 1.0 1.0 0 0 7

4921011 7.11934 7.668411 * 651.381

4921021 7.36089 7.9198 2 * 673.39

4921031 7.39046 7.95058 3 * 676.089

4922021 0.3255 0.0 1.0 1.0 1

4922031 0.3255 0.0 1.0 1.0 2

4922041 0.3255 0.0 1.0 1.0 3

4922051 0.1799 0.0 1.0 1.0 4

4922061 0.190 0.0 1.0 1.0 5

4922071 0.2989 0.0 1.0 1.0 6

4922081 0.3255 0.0 1.0 1.0 7

* hydro component name "cphiba" component type pipe

4930000 1

* hydro volarea 0.2400

4930101 1

* hydro length 1.80

4930301 1

* hydro volume 0.0

4930401 1

* hydro vert angle 90.

4930601 1

* hydro delta z 1.80

4930701 1

* hydro roughness 0.0000457

4930801 1

* hydro hyd diam 0.3664

4931001 1

* hydro fe 00

4931201 0 3392443. 176605.4 2419491. 0. 0.1

* hydro component name "Inlc" component type pipe

5000000 1

* hydro volarea 0.1799

5000101 1

* hydro length 0.331

5000301 1

* hydro volume 0.0

5000401 1

* hydro vert angle 90.

5000601 1

* hydro roughness 0.0000457

5000801 1

* hydro fe 00

5001001 1

* hydro vcahs jun 1
 * 5001101 01100
 * hydro cbt pressure tempe vol 0.1
 * 5001201 0 332311. 176630.2 2419540. 0.
 * hydro f velocity g velocity j velocity jun
 * 5001300 0
 * 5001301 7.26805 7.26805 0. 2
 * hydro component name component type
 * "icorein" pipe
 * 5030001 1
 * hydro vol area vol 1
 * 5030101 0.05598
 * hydro length vol 1
 * 5030201 1.545
 * hydro volume vol 1
 * 5030401 0.
 * hydro vert angle vol 1
 * 5030601 90.
 * hydro delta z vol 1
 * 5030701 1.545
 * hydro roughness hyd diam vol 1
 * 5030801 0.00000152 0.034
 * hydro fc vol 1
 * 5031001 00
 * hydro vcahs jun 1
 * 5031101 01100
 * hydro cbt pressure tempe vol 0.1
 * 5031201 0 3246074. 176575. 2419599. 0.
 * hydro f velocity g velocity j velocity jun
 * 5031300 0
 * 5031301 7.26805 7.26805 0. 2
 * hydro component name component type
 * "icorein" pipe
 * 5070001 4 0
 * inlet loss coefficients are:
 * 0.04 (from HFTR data) + 0.0679 (10 mm unheated length)
 * hydro from to vcahs floss vcahs
 * 5070011 500010000 50300000 0. 0. 0. 0.0100
 * 5070012 1.0 1.0 1.0 0. 0. 0. 1
 * 5070021 505010000 510000000 0. 0.079 0.1079 01000
 * 5070022 1.0 1.0 1.0 0. 0. 0. 2
 * 5070031 505010000 515000000 0. 0.079 0.1079 01000
 * 5070032 1.0 1.0 1.0 0. 0. 0. 3
 * 5070041 505010000 516000000 0. 0.079 0.1079 01000
 * 5070042 1.0 1.0 1.0 0. 0. 0. 4
 * hydro f velocity g velocity jun 4
 * 507011 12.32722 12.90393 1 * 758.611
 * 507021 24.7336 24.7336 2 * 752.454
 * 507031 25.29286 25.29286 3 * 3.07781
 * hydro component name component type
 * "icorein" pipe
 * 5100001 5
 * hydro vol area vol 5
 * 5100101 0.027675
 * hydro length vol 5
 * 5100301 0.1014
 * hydro volume vol 5
 * 5100401 0.
 * hydro vert angle vol 5
 * 5100601 90.
 * hydro delta z vol 5
 * 5100701 0.1014
 * hydro roughness hyd diam vol 5
 * 5100801 1.7720e-6 0.002498
 * hydro fc vol 5
 * hours**5101001 00
 * hydro fc vol 5
 * 5101001 200
 * hydro vcahs jun 4
 * 5101101 01000
 * hydro cbt pressure tempc vol 0.1
 * 5101201 0 2791262. 204874.2 2419427. 0.
 * 5101202 0 2.519e+6 230301.7 2418759. 0.
 * 5101203 0 2246044. 252986. 2417543. 0.
 * 5101234 0 1972517. 253740. 2415576. 0.
 * 5101205 0 1.699e+6 294448. 2412997. 0.
 * hydro f velocity g velocity jun
 * 5101300 0
 * 5101301 24.8089 32.1852 0.1 * 752.454
 * 5101302 24.8834 32.331575 0.2 * 752.454
 * 5101303 24.92473 32.47713 0.3 * 752.454
 * 5101304 25.02536 32.62555 0.4 * 752.454
 * hydro jun hyd diam
 * 5101401 0.002498 0.0 1.0 1.0
 * hydro pitch span vol
 * 5101501 1.27e-3 87.55e-3 5
 * hydro component name component type
 * "echoch1" pipe
 * 5150001 5
 * hydro vol area vol 5
 * 5150101 0.000110698
 * hydro length vol 5
 * 5150301 0.1014

*hydro	volume	vol	5				
5150401	0.						
*	hydro	vert angle	vol	5			
5150601	90.						
*	hydro	delta z	vol	5			
5150701	0.0104						
*	hydro	roughness	hyd diam	vol	5		
5150801	1.7720e-6	0.002498					
*	hydro	fc	vol	5			
5151001	00						
*	noans**5151001						
5151001	200			5			
*	hydro	veahs	vol	5			
5151101	01000						
*	hydro	ch pressure	tempc	vol	5		
5151201	0.2801631.	238228.3.2419446.0.		0.1			
5151202	0.2529383.	296007.2418793.0.		0.2			
5151203	0.2254116.	347128.2417388.0.		0.3			
5151204	0.1975945.	394597.2415706.0.		0.4			
5151205	0.1694758.	434306.2412947.0.		0.5			
*	hydro	vel/flu					
*	hydro	f velocity	g velocity	j velocity	jun		
5151300	0	33.040530.1 * 3.07781					
5151301	25.4685	33.040530.1 * 3.07781					
5151302	25.66407	33.3344.0.2 * 3.07781					
5151303	25.8696	33.664457.0.3 * 3.07781					
5151304	26.0773	33.9934.0.4 * 3.07781					
*	hydro	jun hyd diam		4			
5151401	0.002498	0.0 1.0 1.0					
*	hydro	pitch	span	vol			
5151501	1.14330e-3	87.35e-3					
*	component name	component type					
5160000	"echoch2"	pipe					
5160001	5						
*	hydro	volarea	vol	5			
5160101	0.000110698						
*	hydro	length	vol	5			
5160301	0.0104						
*	hydro	volume	vol	5			
5160401	0.						
*	hydro	vert angle	vol	5			
5160601	90.						
*	hydro	delta z	vol	5			
5160701	0.0104						
*	hydro	roughness	hyd diam	vol	5		
5160801	1.7720e-6	0.002498					
*	hydro	fc	vol	5			
5161001	00						
*	noans**5161001						
5161001	200			5			

* loss coefficient at fuel channel exit = 0.0879 (10 mm unheated length)

*hydro from to area floss rloss vecls
 5220011 510010000 520000000 0. 0.0579 0. 01100
 5220012 1.0 1.0 1.0 1.0 0 0 1 0.0579 0.079 0.01100
 5220021 510010000 520000000 0. 0.0579 0.079 0.01100
 5220022 1.0 1.0 1.0 1.0 0 0 2 0.0579 0.079 0.01100
 5220031 520000000 520000000 0. 0.0579 0.079 0.01100
 5220032 1.0 1.0 1.0 1.0 0 0 3 0.0579 0.079 0.01100
 5220041 516010000 520000000 0. 0.0579 0.079 0.01100
 5220042 1.0 1.0 1.0 1.0 0 0 4 0.0579 0.079 0.01100
 *hydro f velocity g velocity
 5221011 25.1006 32.5845 1 *752.454
 5221021 26.3705 34.0594 2 * 3.07781
 5221031 12.5166 13.1206 3 *756.611
 5221041 26.3394 34.14135 4 *3.07936
 *hydro component name component type
 5222001 0.0024982 0.0 1.0 1.1
 5222002 0.0024982 0.0 1.0 1.2
 5222003 0.132 0.0 1.0 1.3
 5222041 0.0024982 0.0 1.0 1.4
 *hydro "uinlet" pipe
 5223000 2
 *hydro volarea 0.055983
 5223001 2
 *hydro length 0.2028
 5223002 2.3610
 *hydro roughness 0.
 *hydro volume 0.
 *hydro vert angle 90.
 *hydro deliaz 0.
 52250401 0.2028
 52250701 2.3610
 *hydro roughness hyd diam 0.132
 0.00000152
 *hydro fe 00
 *hydro vscls 01000
 *hydro jun hyd diam 0.132
 52251301 12.51358 13.12272 0.1 *758.611
 *hydro f velocity g velocity j velocity jun
 52251301 12.51358 13.12272 0.1 *758.611
 *hydro jun hyd diam 0.132
 52251401 0.0 1.0 1.0
 *hydro from to area floss rloss vecls
 52290101 500010000 530000000 0. 0. 0. 0.0100
 *hydro jun hyd diam
 52290110 0.120 0.0 1.0 0.0
 *hydro vel/jnw f velocity g velocity j velocity jun
 52290201 0 12.89608 13.4712 0 *1095.565
 *hydro component name component type
 "uinlet"
 5300001 6
 *hydro volarea 0.07728
 5300101 0.07728
 *hydro length 1.545
 5300301 0.1014
 5300302 0.1014
 *hydro volume 0.
 5300401 0.
 *hydro vert angle 90.
 5300601 0.044
 *hydro deliaz 1.545
 5300701 0.1014
 5300702 0.1014
 *hydro roughness hyd diam 0.044
 5300801 0.00000152
 *hydro fe 00
 5301001 00
 *hydro vscls 01000
 5301101 0.044
 *hydro ebt pressure tempe
 5301201 0 3244536. 176665. 2419602. 0. 0.1
 5301202 0 3219632. 178255.4 2419620. 0. 0.2
 5301203 0 3216117. 178311. 2419623. 0. 0.3
 5301204 0 3212604. 178364. 2419626. 0. 0.4
 5301205 0 3209088. 178416.3 2419629. 0. 0.5
 5301206 0 3205572. 178468.8 2419631. 0. 0.6
 *hydro vel/jnw
 5301300 0
 *hydro jun hyd diam
 5301401 0.120 0.0 1.0 1.0
 *hydro component name component type
 "uinlet"
 5310000
 *hydro from to area floss rloss vecls
 jun
 1

5310101	530010003	\$50010003	0.004540	2.79	2.79	01003	
• hydro	jun hyd diam						
5310110	0.010	0.010	0.010				
• hydro	vel/flw	f velocity	g velocity	j velocity			
5310201	0.7194	7.1944	0.	*35.905			
• hydro	component name	component type					
5350000	"uchelt"	pipe					
5350001	1						
• hydro	vol area	vol	vol				
5350101	0.07728	1					
• hydro	length	vol	vol				
5350301	0.050	1					
• hydro	volume	vol	vol				
5350401	0.00000	1					
• hydro	vert angle	vol	vol				
5350601	90.	1					
• hydro	delta z	vol	vol				
5350701	0.050	1					
• hydro	roughness	hyd diam	vol				
5350801	0.00000152	0.144	1				
• hydro	fc	vol	vol				
5351001	00	1					
• hydro	veals	jun	jun				
5351101	01100	1					
• hydro	ch pressure	tempc	vol				
5351201	0	3203393.	178483.6	2419633.0.	0.		
• hydro	f velocity	g velocity	j velocity	jun			
5351300	0	7.52105	7.52105	0.	2		
• hydro	component name	component type					
5370000	"Kant"	mpflun					
5370001	4	0					
• inlet loss coefficients are:							
• 0.04 (from HFIR data) + 0.0679 (10 mm unheated length)							
• hydro from to area floss veins							
5370011	\$30010000	\$55000000	0.	0.	0.	01100	
5370012	1.0	1.0	0	0	1		
5370021	\$35010000	\$40000000	0.	0.	0.		
5370022	1.0	1.0	0	0	2		
5370031	\$35010000	\$45000000	0.	0.	0.	0.079 0.079 0.0000	
5370032	1.0	1.0	0	0	3	0.079 0.079 0.0000	
5370041	\$35010000	\$46000000	0.	0.	0.	0.079 0.079 0.0000	
5370042	1.0	1.0	0	0	4		
• hydro	f velocity	g velocity	j velocity	jun			
5371011	12.04584	1 * 1059.68					
5371021	25.01847	2 * 1054.75					
5371031	25.13356	25.13356	3 * 2.464164				
5371041	25.1453	25.1453	4 * 2.465315				
5372011	0.120	0.010	0.01				
• hydro	jun hyd diam						
5401401	0.002494	0.0 1.0 1.0					
• hydro	component name	component type					
5400000	"beavchan"	pipe					
5400001	5						
• hydro	vol area	vol	vol				
5400101	0.038359	5					
• hydro	length	vol	vol				
5400301	0.1014	5					
• hydro	volume	vol	vol				
5400401	0.	5					
• hydro	vert angle	vol	vol				
5400501	90.	5					
• hydro	delta z	vol	vol				
5400701	0.1014	5					
• Calibration of roughness (SS code has determined that the pressure drop across the core is .54 MPa excluding the unheated length for perturbed LOCA case, and 1.42 MPa for the best-estimate case at 25 m/s).							
• Unheated fuel losses are included as form loss at the entrance and exit.							
• Fuel roughness (m)	Pressure drop (MPa)						
• 0.7979e-6	1.42						
• 0.8930e-6	1.433						
• 1.2000e-6	1.473						
• 2.2000e-6	1.586						
• 1.7900e-6	1.541732						
• 1.7880e-6	1.5417						
• 1.7800e-6	1.54077						
• 1.7740e-6	1.5403						
• hydro	roughness	hyd diam	vol				
5400801	1.7720e-6	0.002494	5				
• hydro	fc	vol	vol				
5401001	00	5					
• noans**5401000	00						
5401001	200	5					
• hydro	veals	jun	4				
5401101	01000						
• hydro	el pressure	tempc	vol				
5401201	0	2773144.	0.1				
5401202	0	2501446.	0.2				
5401203	0	2229980.	0.3				
5401204	0	1957245.	0.4				
5401205	0	1682786.	0.5				
5401300	0	2412805.					
• hydro	el velocity	vol					
5401301	25.12835	32.60395	1 * 1054.75				
5401302	25.27187	32.85997	0.2 * 1054.75				
5401303	25.4326	33.1015	0.3 * 1054.75				
5401304	25.60536	33.35306	0.4 * 1054.75				
• hydro	jun hyd diam						
5401401	0.002494	0.0 1.0 1.0					

```

* hydro pitch span vol      5
5401501 1.27e-3 70.29e-3 5
* component name component type
* "uchoch1" pipe
5450000 5
* hydro vol area           vol      5
5450101 8.9206d-5
* hydro length              vol      5
5450201 0.1014
* hydro volume              vol      5
5450401 0.
* hydro vert angle           vol      5
5450601 90.
* hydro delta z              vol      5
5450701 0.1014
* hydro roughness            vol      5
5450801 1.7720e-6 0.0024940
* hydro vol area           vol      5
5461001 0.1000
* hydro cht pressure         fe      00
* noans**5461001 00
* hydro jun hyd diam          vol      5
5461101 01000
* hydro jun hyd diam          vol      5
5461201 0 2772531. 237506.8 2419393. 0.
* hydro jun hyd diam          vol      5
5461202 0 2403981. 301960.6 2419710. 0.
* hydro jun hyd diam          vol      5
5461203 0 2232333. 361363.5 2417271. 0.
* hydro jun hyd diam          vol      5
5461204 0 1959149. 416606. 2415560. 0.
* hydro jun hyd diam          vol      5
5461205 0 1681704. 466543. 2412792. 0.
* hydro vel/flw             0
5461300
* hydro f velocity g velocity j velocity       jun
* noans**5451001 00
5451001 200
* hydro wsabs                jun    4
5451101 01000
* hydro cht pressure         tempe   vol
5451201 0 2772541. 235177. 2419394. 0. 0.1
5451202 0 2503655. 297123. 2418709. 0. 0.2
5451203 0 2232820. 354218. 2417259. 0. 0.3
5451204 0 1958879. 407314. 2415538. 0. 0.4
5451205 0 1681802. 4553107. 2412793. 0. 0.5
* hydro vel/flw
5451300 0
* hydro f velocity g velocity j velocity       jun
5451301 25.92116 32.81658 0. 1.*2.464164
5451302 25.5019 33.1375 0. 2.*2.464164
5451303 25.72154 33.4844 0. 3.*2.464164
5451304 25.9671 33.852 0. 4.*2.464164
* hydro jun hyd diam          jun    4
5451401 0.0024940 0.1 0 1.0
* hydro component name component type
* "uchoch2" pipe
5460000 5
* hydro vol area           vol      5
5460101 8.8206d-5
* hydro length              vol      5
5460301 0.1014
* hydro vol area           vol      5
5460401 1.7720e-6 0.0024940
* hydro vert angle           vol      5
5460501 90.
* hydro delta z              vol      5
5460701 0.1014
* hydro roughness            vol      5
5460801 1.7720e-6 0.0024940
* hydro wsabs                jun    4
* hydro cht pressure         tempe   vol
5461001 0 2772531. 237506.8 2419393. 0. 0.1
5461202 0 2403981. 301960.6 2419710. 0. 0.2
5461203 0 2232333. 361363.5 2417271. 0. 0.3
5461204 0 1959149. 416606. 2415560. 0. 0.4
5461205 0 1681704. 466543. 2412792. 0. 0.5
* hydro vel/flw             0
5461300
* hydro f velocity g velocity j velocity       jun
* noans**5461001 00
5461001 200
* hydro pitch span vol          vol      5
5461101 1.4500e-3 70.29e-3 5
* hydro component name component type
* "uchoch2" pipe
5500000 14
* hydro jun area               jun
* hydro vol area           vol      6
5500101 0.007618
* hydro wsabs                jun    11
5500102 0.004590
* hydro wsabs                jun    12
5500103 0.007618
* hydro length                 vol      6
5500301 1.545
* hydro jun area               jun
* hydro vol area           vol      6
5500302 0.1014
* hydro wsabs                jun    13
5500303 0.050
* hydro wsabs                jun    14
5500304 0.1014
* hydro length                 vol      6
5500305 0.7715
* hydro vol area           vol      14
5500401 0.
* hydro vert angle           vol      14
5500601 90.

```

* hydro roughness hyd diam vol vol
 5500801 0.00000152 0.010 6 0.07728
 5500802 0.00000152 0.006 12 *
 5500803 0.00000152 0.010 14 *
 * 5500901 0. 0. 11
 * Calibrate losses to get 4.3 m/s in CPBT
 * K = 85.00 V = 4.46
 * K = 86.00 V = 4.4437
 * K = 88.00 V = 4.4117
 * K = 91.00 V = 4.36
 * K = 93.00 V = 4.336
 * K = 95.00 V = 4.3039
 * hydro fe vol 14
 5500902 95.40 95.40 12
 5500903 0. 0. 13
 * hydro fe vol 14
 5501001 00 jun 13
 * hydro cb pressure tempc vol
 5501201 0 3165053. 20089.8 2419663. 0. 0.1
 5501202 0 3129594. 204337. 2419690. 0. 0.2
 5501203 0 3126462. 208766. 2419693. 0. 0.3
 5501204 0 3123428. 212461. 2419695. 0. 0.4
 5501205 0 3120390. 215817. 2419698. 0. 0.5
 5501206 0 3117354. 219880.3 2419700. 0. 0.6
 5501207 0 3095427. 219884.2 2419717. 0. 0.7
 5501208 0 3087670. 222617. 2419723. 0. 0.8
 5501209 0 3077389. 22757.6 2419732. 0. 0.9
 5501210 0 3067180. 232522. 2419740. 0. 0.10
 5501211 0 3057018. 238251. 2419748. 0. 0.11
 5501212 0 3046897. 243888. 2419756. 0. 0.12
 5501213 0 2083108. 252012.2 2416410. 0. 0.13
 5501214 0 2080039. 387090. 2416392. 0. 0.14
 * hydro vel/flw 0
 5501300 *
 * hydro f velocity & velocity i velocity jun
 5501301 4.29773 4.29773 0. 1 * 35.90505
 5501302 4.29982 4.29982 0. 2 * 35.90505
 5501303 4.301785 4.301785 0.3 * 35.90505
 5501304 4.30353 4.30353 0. 4 * 35.90505
 5501305 4.30519 4.30319 0. 5 * 35.90505
 5501306 4.30682 4.30682 0. 6 * 35.90505
 5501307 7.14808 7.14808 0. 7 * 35.90505
 5501308 7.15082 7.15082 0. 8 * 35.90506
 5501309 7.15468 7.15468 0. 9 * 35.90506
 5501310 7.15914 7.15914 0. 10 * 35.9051
 5501311 7.16408 7.16408 0. 11 * 35.9051
 5501312 4.31976 4.31976 0. 12 * 35.9051
 5501313 -7.11338-6 -7.11349-6 0. 13 * -5.78558-5
 * hydro jun hyd diam jun 5
 5501401 0.010 0.0 1.0 1.0 13
 5501402 0.006 0.0 1.0 1.0 *
 * hydro component name component type
 5500000 "Ecoult" pipe 1
 * hydro component name component type
 5500001 s 1
 * hydro component name component type
 5320000 "gapout" s
 * hydro from to area floss rloss veals
 5320101 550130003 55010003 0.00204 2.78 2.78 01003
 * hydro jun hyd diam
 5320110 0.0024787 0.0 1.0 1.0

*hydro	jun	hyd diam	jun	10
5611401	0.044	0.01010		
\$				
*hydro	component name	component type		
5620000	"outer"	pipe	flow around control tube	
*				
*hydro	no. volumes			
5620001	11			
\$				
*hydro	vol area	vol	vol	11
5620101	0.0164753	11		
\$				
*hydro	length	vol	vol	
5620301	0.1014	5		
5620302	0.050	6		
5620303	0.1014	11		
*				
*hydro	volume	vol	vol	
5620401	0.	11		
*				
*hydro	vert angle	vol	vol	11
5620601	90.	11		
*				
*hydro	roughness	hyd diam	vol	
5620801	1.32e-6	0.0520521	11	
*				
*hydro	tempc	vol	vol	
5621001	00	11		
*				
*hydro	vel/flows	jun	jun	10
5621101	01000			
*				
*hydro	abs pressure	tempc	tempc	
5621201	2940828.	182474.	2419692.	0.
5621202	0.0	11		
5621203	0			
*				
*hydro	vel/flows	jun	jun	
5621204	0	10		
*				
*hydro	flowrate	flowrate	flowrate	
5621205	0	2934541.	202951.7	2419681.
5621206	0	2933357.	203001.4	2419679.
5621207	0	2932160.	2062725.	2419677.
5621208	0	2930549.	210289.6	2419674.
5621209	0	2928936.	2141414.	2419671.
5621210	0	2927324.	218314.	2419668.
5621211	0	2925713.	222569.3	2419666.
*				
*hydro	vel/flows	0		
5621300				
*				
*hydro	flowrate	flowrate	flowrate	
5621301	5.96297	5.96297	0.	1 * 107.92
5621302	5.96628	5.96628	0.	2 * 107.92
5621303	5.96937	5.96937	0.	3 * 107.92
5621304	5.97236	5.97236	0.	4 * 107.92
5621305	5.9754	5.9754	0.	5 * 107.92
5621306	5.97544	5.97544	0.	6 * 107.92
5621307	5.97754	5.97754	0.	7 * 107.92
5621308	5.98014	5.98014	0.	8 * 107.92
5621309	5.98286	5.98286	0.	9 * 107.92
5621310	5.98561	5.98561	0.	10 * 107.92
*				
*hydro	fun hyd diam	jun	10	
5621401	0.0520521	0.01010		
\$				
*hydro	component name	component type		
5630000	"gap"	pipe		

* hydro volume vol
 5604041 0. 1
 * hydro vert angle vol
 5640601 90. 1
 * hydro delta z vol
 5640701 2.0568 1
 * hydro roughness hyd diam vol
 5640801 0.0000152 0.0207 1
 * hydro fe vol
 5641001 00. 1
 * hydro vabs jun
 5641101 01100 1
 * hydro ch pressure temp vol
 5641201 0 1621830. 215e20.4 2414334. 0. 0.1
 * hydro f velocity & velocity jun
 5641300 0 5641301 7.52105 7.52105 0. 2
 * hydro f velocity & velocity jun
 5641301 7.52105 7.52105 0. 2
 * hydro component name component type
 5660000 "crtail" mijlijn
 5660001 3 0
 * calibrated exit losses to get velocity to 6 m/s in CR channels
 * 55.82/55.70/52.13 ----> 5.97139 5.9983 6.01318
 * hydro from to area floss rloss vabs
 5660011 561010000 564000000 0. 55.82 55.82 01000
 5660012 1.0 1.0 0 0 1 0 0 1
 5660021 562010000 564000000 0. 55.70 55.70 01000
 5660022 1.0 1.0 0 0 0 2
 5660031 563010000 564000000 0. 52.13 52.13 01000
 5660032 1.0 1.0 0 0 0 3
 * hydro fflowrate & flowrate jun flowrate
 5661011 5.99516 1 * 30.0311
 5661021 5.98837 5.98837 2 * 107.92
 5661031 6.04437 6.04437 3 * 8.7148
 * hydro jun hyd diam
 5662011 0.044 0.0 1.0 0.1
 5662021 0.0520521 0.0 1.0 0.2
 5662031 0.006 0.0 1.0 0.3
 * hydro component name component type
 5650000 "cpbix" pipe
 5650001 1
 * hydro vol area vol
 5650101 0.24663 1
 * hydro length vol
 5650301 0.918 1
 * hydro volume vol
 5650401 0. 1
 * hydro vert angle vol
 5650601 90. 1
 * hydro delta z vol
 5650701 0.540 1
 * hydro roughness hyd diam vol
 5650801 0.0000457 0.56037 1
 * hydro ft vol
 5651001 00. 1
 * hydro vabs jun
 5651101 01100 1
 * hydro ch pressure temp vol
 5651201 0 1695541. 340731. 2412986. 0. 0.1
 * hydro f velocity & velocity jun
 5651300 0 5651301 7.52105 7.52105 0. 2
 * hydro component name component type
 5670000 "spbx" mijlijn
 5670001 4 0
 * hydro from to area floss rloss vabs
 5670011 557010000 565000000 0. 0. 0. 0.01100
 5670012 1.0 1.0 1.0 0 0 1
 5670021 525010000 565000000 0. 0. 0. 0.01100
 5670022 1.0 1.0 1.0 0 0 2
 * Kexit = 0.15*Kentrance = 22.80
 *
 5670031 564010000 563000000 0.0250334 5.25 5.25 01000
 5670032 1.0 1.0 1.0 0 0 3
 5670041 565010000 640000000 0. 0.24 0.24 01100
 5670042 1.0 1.0 1.0 0 0 4
 * hydro f velocity & velocity jun velocity
 5671011 13.28143 13.38351 1 * 1095.385
 5671021 12.5155 13.12035 2 * 758.611
 5671031 5.35405 5.77988 3 * 146.6658
 5671041 7.54176 8.22472 4 * 2000.86
 * MODERATOR TANK
 *
 * hydro component name component type
 1670000 "connect" snglijn
 * hydro from to area floss rloss fvels disch
 1670101 530010003 575020003 0.0000001 1.e6 1.e6 031000 1.0
 1670110 0.3255 0.0 1.0 1.0
 * hydro vel/w fmassrc g massrate j massrate
 1670201 0 .0704636 .0704636 0. * 7.74838-6

```

*hydro component name component type
5700000 "modcool" tmdpvol
*hydro area length volume
5700101 1.e6 .0 1.0e-06
*hydro horz angle vert angle delta z
5700102 .0 .0 .0
*hydro roughness hyd diam fc
5700103 .0 .0 10
*hydro ebt trip no. alpha vrc numeric vrc
5700200 003
*hydro time pressure tempe
5700201 0. 1.e5 300.
*hydro component name component type
5710000 "tankcool"
*hydro from to area
5710101 57000000 57500000 0.02866
*hydro vellfw trip no. alpha vrc numeric vrc
5710200 1
*hydro time fflow gflow jflow
5710201 0. 316.4 0. 0.
5710202 1.e6 316.4 0. 0.
*hydro component name component type
5750000 "moddisk" pipe
*hydro vol area
5750101 2.7539 4
*hydro length
5750301 1.2675 1
5750302 1.545 2
5750303 1.064 3
5750304 0.7715 4
*hydro volume
5750401 0. 4
*hydro vert angle
5750601 90. 4
*hydro delta z
5750701 1.2675 1
5750702 1.545 2
5750703 1.064 3
5750704 0.7715 4
*hydro roughness hyd diam
5750801 0.0000457 0.532 4
*hydro fc
5751001 00 4
*hydro vcahs
5751101 01000 jun 3
*hydro cbt pressure tempe
5751201 0 143458.7 98151.5 2339196.0 0.1
5751202 0 1282322.3 98151.4 2335630.0 0.2
5751203 0 114107.7 98151.4 231943.0 0.3
5751204 0 104170.7 98151.4 2329100.0 0.4
5751301 .104095 .1242055.0 1*316.4
5751302 .1040503 .1242064.0 2*316.4
5751303 .104061 .1242073.0 3*316.4
*hydro component name component type
5760000 "tankout"
*hydro from to area floss floss vels
5760101 575010000 580000000 0.028603 0. 0. 0.0000
*hydro vellfw fvelocity g velocity j velocity
5760201 0 10.01905 10.664420. *316.4
*hydro component name component type
5800000 "moddiskp"
*hydro area length volume
5800101 1.e6 .0 1.0e-06
*hydro horz angle vert angle delta z
5800102 .0 .0 .0
*hydro roughness hyd diam fc
5800103 .0 .0 10
*hydro cbt trip no. alpha vrc numeric vrc
5800200 003
*hydro time pressure tempe
5800201 0. 1.e5 300.
5800202 1.e6 1.e5 300.
* HOT LEG MAIN HEADER
*hydro component name component type
6400000 "coreout" pipe
*hydro vol area
6400101 0.246653 3
*hydro length
6400301 0.6367 3
*hydro volume
6400401 0. 3
*hydro volume
6400501 0. 3
*hydro vert angle
6400601 0. 3
*hydro vert length
6400701 0.00 3

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* hydro	roughness	hyd diam	vol		* hydro	vel/flow	vol	
6400801	0.0000457	0.56037	3		6411101	01000	jun	2
* hydro	floss	r loss			* hydro	vel/pressure	tempc	
6400901	0.00	0.00			6411201	0 1659459	340654.	2412425. 0.
* hydro	fc	00	vol		6411202	0 1633306.	340618.4	2412208. 0.
6410001			3		6411203	0 1607152.	340583.	2411886. 0.
* hydro	velabs				* hydro	vel/flow		
6401101	01000				6411300	0		
* hydro	vel/flow				* hydro	flowrate	flowrate	
6401300	0				6411301	7.54179	8.22550. 1.	2000.863
* hydro	fflowrate	gflowrate	i flowrate		6411302	7.54184	8.226170. 2.	* 2000.864
6401301	7.54178	7.54178	0.1 * 2000.86					
* hydro	component name	component type						
1640000	"risein"	snglun						
* hydro	from	to	ara					
1640101	640010000	641000000	0.					
* hydro	hyd diam							
1640110	0.56037	0.	1.1.					
* hydro	vel/flow	velocity	g velocity					
1640201	0	7.54175	7.54175	0. * 2000.862				
* hydro	component name	component type						
6410000	"hurser"	pipe						
* hydro	length		vol					
6410001	3		3					
* hydro	vol area		vol					
6410101	0.24663		3					
* hydro	volume		vol					
6410401	0.		3					
* hydro	vert angle		vol					
6410601	90.		3					
* hydro	vert length		vol					
6410701	2.33667		3					
* hydro	roughness	hyd diam	vol					
6410801	0.0000457	0.56037	3					
* hydro	floss	r loss						
6410901	0.	0.						
* hydro	fc		vol					
6411001	00		3					
* hydro	component name	component type						
6470001	2	0						
* hydro	from	to	ara					
6470011	641010000	645000000.	0.					
6470012	1.0	1.0	0					
6470021	645010000	650000000.	0.					

6470032 1.0 1.0 0 0 0 2
 6471011 754189 8.2268 1 * 2000.865
 6471021 20.9488 20.9488 2 * 2000.87
 *
 6472011 0.56037 0.0 1.0 0.1
 6472021 0.56037 0.0 1.0 0.2
 *
 * hydro component name component type \$
 6500000 "HotHead" pipe \$
 *
 6500001 4
 *
 * hydro volara vol 1
 6500101 0.08879 1
 6500102 0.24663 4
 *
 * hydro length vol 1
 6500301 1.68 1
 6500302 3.51 2
 6500303 1.22 3
 6500304 1.83 4
 *
 * hydro volume vol 1
 6500401 0. 4
 *
 * hydro vert angle vol 4
 6500601 0. 4
 *
 * hydro elev. change vol 4
 6500701 0. 4
 *
 * hydro roughness hyd diam vol 1
 6500801 0.0000457 0.33622 4
 6500802 0.0000457 0.56037
 *
 * hydro floss rloss jun 2
 6500901 0.00 0.00 2
 6500902 0.20 0.20 3
 *
 * hydro fc vol 4
 6501001 0.00 4
 *
 * hydro vcahs jun 3
 6501101 01000
 *
 * hydro jd pressure tempc vol
 6501201 0 1368415. 340445.5 2408383. 0. 0.1
 6501202 0 1565159. 340392.5 2411362. 0. 0.2
 6501203 0 1563230. 338636. 2411337. 0. 0.3
 6501204 0 1589808. 338555.3 2411671. 0. 0.4
 *
 * hydro vel/fhw 0
 6501300
 *
 * hydro fflowrate gflowrate jdflowrate jun
 6501301 20.9307 20.9307 0. 1 * 2000.87
 6501302 7.54182 7.54182 0. 2 * 2000.87
 6501303 2.3661 2.3661 0. 3 * 680.984
 *
 * PRESSURIZING SYSTEM
 *
 * hydro component name component type \$

8000000 "muanank" tmdprol
 * hydro area length volume
 8000101 1.e6 .0 1.0e+06
 *
 * hydro horzangle vert angle delta z
 8000102 .0 .0 .0
 *
 * hydro roughness hyd diam fc
 8000103 .0 .0 10
 *
 * hydro jd trip no. alpha vrc numeric vrc
 8000200 003
 *
 * hydro time pressure tempc
 8000201 0. 0.165e6 300.
 *
 * trip valve to isolate the pressurizing system following
 * draining of the makeup tank
 *
 8050000 isolate valve
 8050101 80000000 80000000 0.00811 0.48 0.48 01000
 8050201 0. 1.632018 1.632018 0. * 14.61378
 8050300 tpfv
 8050301 61.5
 *
 * hydro component name component type
 8100000 "suction" branch
 *
 * hydro no. juns vel/fhw
 8100001 0 0
 *
 * hydro area length volume
 8100101 0.00811 6.096 0.
 *
 * hydro horzangle vert angle delta z
 8100102 0. 0. 0.
 *
 * hydro roughness hyd diam fc
 8100103 0.0000457 0.1016 0.
 *
 * hydro jd pressure tempc
 8100200 161997. 97875.7 2343094. 0.
 *
 * hydro component name component type
 8150000 malprz pump
 *
 * hydro area length volume
 8150101 0.00811 0. .0203
 *
 * hydro equil flag
 8150103 00
 *
 * hydro from jun area floss rloss vcahs
 8150108 81001000 0.00811 0.16 0.16 01000
 *
 * hydro to jun area floss rloss vcahs
 8150109 82000000 0.00811 0.16 0.16 01000
 *
 * hydro jd pressure tempc
 8150200 883766. 100661. 2396979. 0.
 *
 * hydro vel/fhw f velocity g velocity j velocity

8150201 0 1.63202 1.63202 0. * 14.61378
 • hydro vel/w f velocity g velocity j velocity
 8150202 0 1.631706 1.631706 0. * 14.61377
 • hydro pdl 2faz diff1 torq1 pvel trip no. rvs1
 8150301 0 -1 -3 -1 0 540 0
 • hydro rated pump vel. init/rated vel. rated flow rated head
 8150302 221.55 1.080816 0.01366 106.39
 • hydro rated torque mom of inertia rated dens mir torque
 8150303 217.82 2.381 1098. .0
 • hydro coeff1f2 coeff1f0 coeff1f1 coeff1f3
 8150304 2.1782 2.1782 0. 0.
 • single phase homologous curves
 • bvn homologous data
 8151101 1 0.000 1.228 0.050 1.226 0.100 1.225
 8151101 0.150 .124 .240 .200 .223 .250 .223
 8151102 0.300 .122 .220 .250 .220 .440 .218
 8151103 0.450 .124 .360 .309 .350 .202
 8151104 0.600 .119 .350 .180 .370 .165
 8151105 0.750 .147 .380 .126 .350 .101
 8151106 0.900 .1972 .0350 1.038 1.000 1.000
 • hvn homologous data
 8151200 1.2 0.513 -270 0.526 -233 0.541 -195
 8151201 0.556 -.155 0.571 -.113 0.588 -.069
 8151202 0.406 -.023 0.625 0.025 0.645 0.076
 8151203 0.667 0.130 0.590 0.187 0.714 0.249
 8151204 0.741 0.316 0.769 0.388 0.800 0.466
 8151205 0.533 0.551 0.570 0.646 0.509 0.751
 8151206 0.552 0.868 1.000 0.000
 * had homologous data taken from bingham pump in relap
 8151300 1.3 -1.2.5 -.9 2.28 -.63 2. -.55 1.74
 8151301 -.5 1.68 -.42 1.6 -.15 1.4 0. 1.228
 * hvd homologous data taken from bingham pump in relap
 8151400 1.4 -1.2.5 -.9 2.28 -.63 2. -.55 1.74
 8151401 -.5 1.68 -.42 1.6 -.15 1.4 0. 1.228
 * bvn homologous data
 8151500 2.0 0.000 0.470 0.050 0.500 0.100 0.529
 8151501 0.550 0.559 0.200 0.589 0.250 0.618
 8151502 0.300 0.648 0.350 0.767 0.400 0.706
 8151503 0.450 0.734 0.500 0.762 0.550 0.789
 8151504 0.500 0.816 0.550 0.842 0.700 0.867
 8151505 0.550 0.892 0.800 0.915 0.550 0.938
 8151506 0.500 0.960 0.950 0.980 1.000 1.000
 * bvn homologous data
 8151600 2.2 0.513 0.283 0.526 0.302 0.541 0.321
 8151601 0.526 0.342 0.571 0.364 0.588 0.388
 8151602 0.606 0.412 0.625 0.439 0.645 0.468
 8151603 0.667 0.498 0.690 0.531 0.714 0.566
 8151604 0.741 0.604 0.769 0.645 0.800 0.691
 8151605 0.833 0.740 0.870 0.795 0.809 0.856
 8151606 0.932 0.924 1.000 1.000
 * bad homologous data taken from bingham pump in relap
 8151700 -1.2.5 -.8 2. -.6 1.45 -.46 1.15
 8151701 -.3 -.95 -.13 8 .8
 * bad homologous data taken from bingham pump in relap
 8151802 4.1.2 -.65 2.15 -.4 1.79 -.30 1.61
 8151801 -.13 1.5 1.44
 * pump trip
 8151600 620 critval 815
 *8156100 0 critval 591
 8156101 -1.6 -1.6
 8156102 1.6 1.66
 • hydro component name component type
 8200000 "mainline" singvol
 • hydro area 0.00811 length 30.48 volume 0.
 • hydro horz angle 0. vert angle 0. delta z 0.
 • hydro roughness 0.0000437 hyd diam 0.1016 fe 00
 • hydro ebt pressure tempc 8200200 1602253. 100659. 2411826. 0.
 • hydro from to area floss rloss vcahs 01000
 8250101 820010000 850000000 0.00811 1.28 1.28 01000
 * hydro vel/w f velocity g velocity j velocity 8250201 0 1.631146 1.631146 0. * 14.61316
 • hydro valve type chkv1
 8250300
 * hydro chkv1 type init_pos back_press kav_ratio 8250301 0 0 0.
 • hydro component name component type tmppvol 8260000
 • hydro area length volume 8260101 1.e6 .0 1.0e+06
 * hydro horz angle vert angle delta z 8260102 .0 .0 .0
 • hydro roughness hyd diam fe 8260103 .0 .0 10 alpha vrc numeric vrc
 * hydro time pressure tempe 8260201 0. 0.165e6 300.
 • trip valve to shut off time dependent volume from prizing system
 * following training of the makeup tank
 • hydro component name component type branch
 8270000 isolate valve
 8270101 82600000 82800000 0.00811 0.48 0.48 01000
 8270201 0 3.082857-44 -2.44452-21 0. * 2.76056-43
 8270300 upv1v
 8270301 615
 • hydro no_juns vel/w 0 0
 8280001

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*-----$-----*
hydro area length volume
*-----$-----* 0.00811 6.096 0.
hydro horz angle vert angle delta z
*-----$-----* 0. 0. 0.
hydro roughness hyd diam fc
*-----$-----* 0.0000457 0.01016 .00
hydro cht pressure uf ug voidg
*-----$-----* 1.65+5 83097. 2343686. 0.
hydro "standby" component name component type
*-----$-----* pump
hydro area length volume
*-----$-----* 0.00811 0. 0.0232
hydro horz angle vert angle delta z
*-----$-----* 0. 0. 0.
hydro equil flag
*-----$-----* 00
hydro from jun area floss rloss vcahs
*-----$-----* 828010000 0.00811 0.16 0.16 01000
hydro to jun area floss rloss vcahs
*-----$-----* 83000109 835000000 0.00811 0.16 0.16 01000
hydro cht pressure tempe
*-----$-----* 1.65+5 83054.7 2343686. 0.
hydro vel/flw fvelocity g velocity | velocity
*-----$-----* 2.38220744 1.608556-21 0. * 2.186026-43
hydro rated pump vel. hi/rated vel. rated flow rated head
*-----$-----* 33000302 221.55 0. 0.01366 106.39
hydro pidi 2faci diff1 torq1 pwel trip no. rrvsi
*-----$-----* 815 -1 -3 0 541 0
hydro rated torque mom of inertia rated dens mtr torque
*-----$-----* 2.381 1098. .0
hydro coeff. if2 coeff. if1 coeff. if3
*-----$-----* 2.1782 0. 0.
alpha vrc numeric vrc
centivar 830
hydro search urg pump vel.
*-----$-----* -1.e6 1.e6
hydro component name component type
*-----$-----* "sodice" singvol
hydro area length volume
*-----$-----* 0.00811 30.48 0.
hydro horz angle vert angle delta z
*-----$-----* 0. 0. 0.
hydro roughness hyd diam hyd diam
*-----$-----* 0.0000457 0.1016 .00
hydro cht pressure tempc
*-----$-----* 8350200 1.65+5 83054.7 2343686. 0.
hydro component name component type
*-----$-----* "stopump" valve
hydro from to area floss rloss vcahs
*-----$-----* 8400101 835010000 850000000 0.00811 1.28 1.28 01000
hydro vel/flw fvelocity g velocity | velocity
*-----$-----* 8400201 0. 0. * 0.
hydro valve type
*-----$-----* chkviv
hydro chckly typc init. posn backpress leak ratio
*-----$-----* 8400301 0 1 0.
hydro component name component type
*-----$-----* "emerpump" tmjmpin
hydro from to area
*-----$-----* 8450101 810010000 850000000 0.001
hydro vel/flw trip no. alpha vrc numeric vrc
*-----$-----* 8450200 0 542
hydro time fvelocity g velocity | velocity
*-----$-----* 8450201-1, 0. 0. 0. 00
hydro vel/flw trip no. alpha vrc numeric vrc
*-----$-----* 8450202 0. 0. 0. 00
hydro from to area
*-----$-----* 8450203 10. 25. 0. 00
hydro time fvelocity g velocity | velocity
*-----$-----* 8450204 1.e6 25. 0. 00
hydro component name component type
*-----$-----* "prout" branch
hydro no.juns vel/flw
*-----$-----* 8500001 1 0
hydro area length volume
*-----$-----* 8500101 0.00811 12.20 0.
hydro horz angle vert angle delta z
*-----$-----* 8500102 0. 0. 0. 0.
hydro roughness hyd diam fr
*-----$-----* 8500103 0.000457 0.1016 .00
hydro cht pressure tempc
*-----$-----* 8300200 1594564. 100671.9 2411730. 0.
hydro from to area floss rloss vcahs
*-----$-----* 8501101 85010002 650030001 0.00811 0. 0. 01100
hydro fvelocity g velocity | velocity
*-----$-----* 8501201 1.631208 1.631208 0. * 14.6141
LETDOWN SYSTEM

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* components 1xx - heat exchanger coolant loop 1

- * hydro component name component type
 - 1010000 "hspit" pipe
 - 1010001 3
- * hydro vol arcia
 - 1010101 0.083322
 - 1010301 1.07
 - 1010302 3.66
 - 1010303 2.21
- * hydro length
 - 1010401 0.0
- * hydro volume
 - 1010601 0.
- * hydro vert angle
 - 1010701 0.
- * hydro roughness hyd diam
 - 1010801 0.0000457 0.3255
- * hydro kf kr
 - 1010901 0.182 0.182
- * hydro fe
 - 1011001 00
- * hydro vcahs
 - 1011101 01100
- * hydro cb pressure tempc
 - 1011201 0 1560632. 338597. 2411304. 0. 0.1
 - 1011202 0 1552628. 338464. 2411203. 0. 0.2
 - 1011203 0 1543972. 338384. 2411093. 0. 0.3
- * hydro vel/w
 - 1011300 0
- * hydro f velocity & velocity j velocity
 - 1011301 7.3286 7.3286 0.
 - 1011302 7.32847 7.32847 0.
- * hydro from to area floss rloss vrabs
 - 1030011 650030002 101010001 0.24653 1.20 1.20 01000
 - 1030012 1.0 1.0 1.0 0 0 1
- * hydro 1 0
 - 103001 1 0
- * hydro component name component type
 - 1030000 "hspit" mfpjln
- * hydro from to area floss rloss vrabs
 - 1031011 2.47289 2.47289 1 * 656.248
 - 1032011 0.56037 0.1 0.1 0.1
- * hydro component name component type
 - 1020000 "isolate" valve
- * hydro from to area floss rloss vrabs
 - 1020101 101010000 104000000 0.08322 0.104 0.104 01100

* hydro vel/w f flowrate g flowrate j flowrate

- 1020201 0 7.3284 7.3284 0. 0 * 656.248

- * hydro component name component type
 - 1020300 valve type trpvl
 - 1020301 trip no. 515
- * hydro component name component type
 - 1040000 "hotleg" pipe
 - 1040001 3
- * hydro vol arcia
 - 1040101 0.08322
- * hydro length
 - 1040301 0.69
 - 1040302 12.95
 - 1040303 2.51
- * hydro volume
 - 1040401 0.
- * hydro volume
 - 1040501 0.
- * hydro vert angle
 - 1040601 0.
- * hydro delta z
 - 1040701 0.
- * hydro roughness hyd diam
 - 1040801 0.0000457 0.3255
- * hydro floss rloss hyd diam
 - 1040901 0.0 0.0 0.24
 - 1040902 0.24 0.24
- * hydro vel/w
 - 1041001 0
- * hydro f flowrate g flowrate j flowrate
 - 1041301 7.32839 7.32839 0. 1 * 656.247
 - 1041302 7.3276 7.3276 0. 2 * 656.223

\$ MAIN HEAT EXCHANGER - LOOP 1

*hydro component name component type branch \$
 1080000 "tsp1n"
 *hydro no_juns vel/flw
 1080001 2 0
 *hydro roughness hyd_diam fc
 1080103 0.0000457 0.3255 0
 *hydro arca length volume
 1080101 0.08322 1.0 0.
 *hydro horz_angle vert_angle delta_z
 1080102 0. 0. 0.
 *hydro roughness hyd_diam fc
 1080200 0.0000457 0.3255 0
 *hydro elt_pressure tempe
 1080200 15161.44. 33797.6 2410735.0.
 *hydro from to area floss rloss vels
 1080101 106000000 108000000 0. 0.15 0.15 0.000
 1082101 104010000 106000000 0. 0. 0. 0.000
 *hydro hyd_diam
 1081110 0.3255 0.0 1.0 1.0
 1082110 0.3255 0.0 1.0 1.0
 *hydro fvelocity g_velocity j_velocity
 1081201 7.27322 7.27322 0. * 651.358
 1082201 7.32758 7.91376 0. * 656.223
 *hydro component name component type pipe
 1080000 "tmeprim"
 *hydro vol_area vol
 1080101 0.8258 5
 1080102 0.841 6
 1080103 0.8258 11
 *hydro length vol
 1080301 1.11 5
 1080302 2.03 6
 1080303 1.11 11
 *hydro volume vol
 1080401 0. 11
 *hydro vert_angle vol
 1080601 0. 11
 *hydro delta_z vol
 1080701 0.0 11
 *hydro roughness hyd_diam vol
 1080801 0.0000457 0.636 5
 1080802 0.0000457 0.894 6
 1080803 0.0000457 0.636 11
 *hydro fc vol
 1081001 0. 11
 *hydro vels vol
 1081101 0.000 10
 *hydro elt_pressure tempe
 1081201 0 1510449. 301206. 2410662. 0. 0.1
 1081202 0 1510445. 270294. 2410662. 0. 0.2
 1081203 0 1510442. 24445 2410661. 0. 0.3
 1081204 0 1510437. 2214897 2410661. 0. 0.4
 1081205 0 1510432. 2021064. 2410661. 0. 0.5
 1081206 0 1510437. 202090. 2410661. 0. 0.6
 1081207 0 1510420. 195798. 2410661. 0. 0.7
 1081208 0 1510414. 195286. 2410661. 0. 0.8
 1081209 0 1510408. 185430. 2410661. 0. 0.9
 1081210 0 1510403. 181161. 2410661. 0. 0.10
 1081211 0 1510397. 177399. 2410661. 0. 0.11
 *hydro fvelocity g_velocity j_velocity jun
 1081300 0
 *hydro fvelocity g_velocity j_velocity jun
 1081301 .728927 0.1 * 651.359
 1081302 .725807 0.2 * 651.36
 1081303 .723367 0.3 * 651.361
 1081304 .721442 .721442 0.4 * 651.363
 1081305 .71991 .71991 0.5 * 651.364
 1081306 .719912 .719912 0.6 * 651.367
 1081307 .719442 .719442 0.7 * 651.368
 1081308 .71904 .71904 0.8 * 651.37
 1081309 .718656 .718656 0.9 * 651.371
 1081310 .7184 .7184 0.10 * 651.372
 *hydro jun hyd_diam
 1081401 0.100 0.0 1.0 1.0 10
 *hydro component name component type branch \$
 1120000 "tphout"
 *hydro no_juns vel/flw
 1120001 2 0
 *hydro arcu area vel/flw
 1120101 0.08322 1.0 0.
 *hydro horz_angle vert_angle delta_z
 1120102 0. 0. 0.
 *hydro roughness hyd_diam fc
 1120103 0.0000457 0.3255 0
 *hydro elt_pressure tempc
 1120200 0 1478037. 177400. 2410178. 0.
 *hydro from to area floss rloss vels
 1121101 108010000 11200000 0. 0.15 0.15 0.000
 1122101 112010000 11300000 0.08322 0. 0. 0.0000
 *hydro hyd_diam
 1122110 0.3255 0.0 1.0 1.0
 1122110 0.3255 0.0 1.0 1.0
 *hydro fvelocity g_velocity j_velocity
 1121201 7.12622 7.12622 0. * 651.374
 1122201 7.12632 7.12632 0. * 651.374
 *hydro component name component type pipe
 1130001 3
 *hydro volarea
 1130101 0.08322 3
 *hydro length
 1130301 1.981 1
 1130302 1.23 2

1350101 124010000 136000000 0.0 0. 0. 01000

- * hydro hyd diam 0.0 1.0 1.0
- * hydro vel/flw f velocity g velocity j velocity 1350110 0.01588 2.30682 2.30682 0. * 1774.07
- * hydro component name component type "seeskt"
- * hydro area length volume 1360101 1.46 .0 1.0e+06
- * hydro horz angle vert angle delta z 1360102 .0 .0 .0
- * hydro roughness hyd diam fc 1360103 .0 .0 10
- * hydro ebt trip no. alpha vrc numeric vrc 1360200 0033
- * hydro time pressure tempe 1360201 0. 4.490e5 319.
- * hydro component name component type "hpjnt1" branch 1440000
- * hydro no. juns vel/flw 1440001 2 0
- * hydro area length volume 1140101 0.08322 1.0 0.
- * hydro horz angle vert angle delta z 1140102 0. 0. 0.
- * hydro hyd diam 0.0 1.0 1.0 1140200 0 1511130. 1774.4 2410670. 0.
- * hydro from to area floss rloss vcahs 1141101 114000000 116000000 0. 0.15 0.15 01000 1142101 113010000 114000000 0. 0. 0. 01000
- * hydro hyd diam 0.0 1.0 1.0 1142110 0.3255 0.0 1.0 1.0
- * hydro f velocity g velocity j velocity 1142101 7.12632 7.12632 0. 651.375 1142201 7.12632 7.70591 0. 651.375
- * hydro component name component type "hx-prm"
- * hydro "hx-prm" pipe 1160000

* hydro vol/area 0.894 1160101

* hydro length 1.6 1160301

* hydro volume 0. 1160401

* hydro vert angle 0. 1160601

* hydro delta z 0.0 1160701

* Calibrated hydraulic diameter to match pressure drop

* hydro roughness hyd diam 0.0346 1160801 0.0000457 0.00170 4

* hydro floss rloss 0.0 0.0 1160901

* hydro fc 00 1161001

* hydro vcahs 01000 1161101

* hydro cbt pressure tempe 1161201 0 1501448. 1774.88.5 2410544. 0. 0.1 1161202 0 1493160. 176366.6 240418. 0. 0.2

* hydro jnt hyd diam 0 1476526. 175569. 2410154. 0. 0.3 1161203 0 1484836. 176386. 2410286. 0. 0.4

* hydro f velocity & velocity jun 1161300 0 1161301 .6633351. 6633351 0.1 * 651.376

* hydro cbt pressure tempe 1161302 .6633335. 6633335 0.2 * 651.377 1161303 .6633308. 6633308 0.3 * 651.378

* hydro jnt hyd diam 0 1476526. 175569. 2410154. 0. 0.4

* hydro f velocity & velocity jun 1161401 0.00170 0.0 1.0 1.0 3

* hydro component name component type "hpjnt1" branch 1200000

* hydro no. juns vel/flw 1200001 2 0

* hydro area length volume 1200101 0.08322 1.0 0.

* hydro horz angle vert angle 0. 1200102

* hydro roughness hyd diam fe 1200103 0.0000457 0.3255 0

* hydro cbt pressure tempe 1200200 1439958. 173670. 2409567. 0.

* hydro from to area floss rloss vcahs 120101 116010000 120000000 0. 0.15 0.15 01000 1202101 120310000 122000000 0.08322 0. 0. 01000


```

1461303 .0877983 .0877983 0.3 * 41.4114
*hydro jun hyd diam 1520101 150010000 154000000 0.0 0. 0. 0. 01100
*hydro jun hyd diam 1520101 150010000 154000000 0.0 1.0 1.0
*hydro component name component type
*hydro "tubeout" snrgjhn
*hydro from to area floss rloss vcahs jun 3
1480101 146010000 150000000 0.0 0. 0. 0. 01100
*hydro hyd diam
*hydro vel/flw f velocity g velocity j velocity
1480110 0.01905 0.0 1.0 1.0
*hydro vel/flw f velocity g velocity j velocity
1480201 0 .2059376 .2059376 0. * 41.41125
*hydro component name component type
*hydro "chimney" pipe $-
1500001 4
*hydro vol/area
1500101 0.203 vol 4
*hydro length
1500301 0.75 vol 4
*hydro volume
1500401 0. vol 4
*hydro vert angle
1500601 90. vol 4
*hydro elev. change
1500701 0.75 vol 4
*hydro roughness hyd diam vol 4
1500801 0.0000457 .508
*hydro floss rloss jun 3
1500901 0. 0. vol 4
*hydro fe
1501001 00 jun 3
*hydro vcahs
1501101 01000
*hydro elev pressure tempe
1501201 0 176276.3 1851602. 2524638. 0. 0.1
1501202 0 16890. 185576. 2523401. 0. 0.2
1501203 0 161704. 185553. 2521913. 0. 0.3
1501204 0 154417.8 185533.5 2520368. 0. 0.4
*hydro vel/flw
1501300 0
*hydro f flowrate g flowrate j flowrate jun
1501301 .205937 .2523523 0.1 * 41.4112
1501302 .205937 .252352 0.2 * 41.4112
1501303 .205937 .252352 0.3 * 41.4111
*hydro component name component type
*hydro "tubeout" snrgjhn
*hydro vol
1520000 00000
*hydro vcahs jun

```

156101 00000 5

- * hydro chi
 - * try for qual of 0.077054 for 0.52 m³/s vol
 - 156101.6 1482314. 106339.8 373161.. .0770037 .9983171 1
 - 1561020.0 1503427. 111229.2 2410570. 0. 0. 2
 - 1561023.0 1508426. 119898.7 2410581. 0. 0. 3
 - 1561024.0 1506024. 136776.5 2410604. 0. 0. 4
 - 1561025.0 1507319. 169782. 2410621. 0. 0. 5
 - 1561026.0 1534116. 230890.7 2410657. 0. 0. 6
- * hydro vel/flw 0
- * hydro vel/flw 0
- * hydro f velocity g velocity j velocity jun
 - 1561301 -1.171195-5.-534059 0. 1 * -0.013344
 - 1561302 -1.172064-5.-1.172205-5.0. 2 * -0.0133886
 - 1561303 -1.17303-5.-1.173175-5. 3 * -0.0133163
 - 1561304 -1.174285-5.-1.1744-5. 0. 4 * -0.0129592
 - 1561305 -2.332057-4.-2.33157-4. 0. 5 * -0.0119257
- \$
- * hydro component name component type
 - 1570000 "accumulor" sngjln
- * hydro from to area floss r loss walls
 - 1570101 156060002 104020001 0.083322 0. 0. 0.000
- * hydro vel/flw f velocity g velocity j velocity
 - 1570201 0 -2.384177-4.-2.384177-4. 0. * -0.013515
- \$
- * hydro component name component type
 - 1220000 "coldleg" pipe
- * hydro vol area 3
 - 1220101 0.08322
- * hydro length vol
 - 1220301 2.31 1
 - 1220302 2.13 2
 - 1220303 0.762 3
- * hydro volume vol
 - 1220401 0. 3
- * hydro volume vol
 - 1220501 0. 3
- * hydro vert angle vol
 - 1220601 -7.6 1
 - 1220602 0. 2
 - 1220603 90. 3
- * hydro delta z vol
 - 1220701 -0.305 1
 - 1220702 0. 2
 - 1220703 0.762 3
- * hydro roughness hyd diam vol
 - 1220801 0.0000457 0.3255 3
- * hydro floss r loss jun
 - 1220901 0.182 0.182 2
- * hydro fc vol
 - 1221001 0. 3
- * hydro vels 0.0000 jun 2
- * hydro 1221101 0.0000 jun 2
- * hydro chi pressure temp
 - 1221201 0 1439733. 157561.6 2409563. 0. 0.1
 - 1221202 0 1433788. 175634. 2409466. 0. 0.2
 - 1221203 0 1422959. 175651.2 2409290. 0. 0.3
- * hydro vel/flw 0
- * hydro f flowrate g flowrate j flowrate
 - 1221301 7.1234 7.1234 0. 1 * 651.38
 - 1221302 7.1235 7.1235 0. 2 * 651.38
- * PRIMARY COOLANT PUMP - LOOP 1
- \$
- * hydro component name component type
 - 1240000 "repump" pump
- * hydro area length volume
 - 1240101 0. 0.300 0.739
- * hydro horz angle vert angle delta z
 - 1240102 0. 0. 0. 0.000
- * hydro equiflag 00
 - 1240103 0. 0. 0. 0.000
- * Assume k=2.0 for strainer loss coefficient
- * hydro to jun area floss r loss vcahs
 - 1240108 122010000 0. 0. 0. 0. 0.01000
- * hydro chi pressure temp
 - 1240200 2316015. 175700. 2418750. 0.
- * hydro vel/flw f flowrate g flowrate j flowrate
 - 1240210 7.12538 7.70508 0. * 651.38
- * hydro vel/flw f flowrate g flowrate j flowrate
 - 1240301 0 0 0 555 0
- * hydro rated pump vel. init/rated vel. rated flow rated head
 - 1240302 188.5 .36383 0.643 207.3
- * hydro pdi 2/rev diffl torq1 pval trip no. rvs1
 - 1240303 0 0 0 1 0
- * hydro curve type regime
 - 1241100 1
- * hydro v/a head \$normal (q1,n)
 - 1241101 0. 1.126 1.147
 - 1241102 .196 1.147


```

1261201 0 3501653. 175698. 2419412. 0. 0. 1
*hydro vel/flw
*1261300 0
*hydro fflowrate gflowrate jflowrate jun
*1261301 7.21537 7.92538 0.2 659.73
*hydro component name component type
1280000 "check" valve
*hydro from to area floss rloss vcahs
1280101 126010000 129000000 0.08322 0.98 0.98 01100
*hydro vel/flw fflowrate gflowrate jflowrate
1280201 0 7.11892 7.11892 0.* 651.38
*hydro valve type chkviv
*hydro chkviv type init_posn back_press leak_ratio
1280301 0 0 0. 0.
*hydro component name component type
1290000 "eljion" pipe
*hydro volarea vol 1
*hydro length vol 1
*hydro volume vol 1
*hydro volume vol 1
*hydro vertangle vol 1
*hydro volume vol 1
*hydro delta z 0.0
*hydro roughness hyd_diam
1290101 0.0000457 0.3255
*hydro volarea vol 1
*hydro length vol 1
*hydro volume vol 1
*hydro volume vol 1
*hydro roughness hyd_diam
1290201 0.0000457 0.3255
*hydro floss rloss jun 1
*hydro fe 0.0000
1291001 00
*hydro vcahs vol 1
*hydro roughness hyd_diam
1291101 0.0000457 0.3255
*hydro floss rloss jun 1
*hydro fe 0.0000
1291201 0.0000457 0.3255
*hydro chb_pressure tempe
1291201 0 3470288. 175675.2 2419434. 0. 0. 1
*hydro vel/flw
*1291300 0
*hydro fflowrate gflowrate jflowrate jun
*1291301 7.21537 7.92538 0.2 659.73
*hydro component name component type
1310000 "elbow1" sngljun
*hydro from to area floss rloss vcahs
1310101 129010000 158000000 0.083220 0.182 0.182 01000
*hydro vel/flw fvelocity gvelocity jvelocity
1310201 0 7.11901 7.11901 0.* 651.38
*hydro component name component type
1380000 "coldleg" pipe
*hydro volarea vol 2
*hydro volarea vol 2
*hydro length 4.50
1380301 0.
*hydro volume vol 2
1380401 0.
*hydro horz_angle 0.
1380501 0.
*hydro vert_angle 0.
1380601 0.
*hydro delta_z 0.
1380701 0.
*hydro roughness hyd_diam
1380801 0.0000457 0.3255
*hydro vcahs jun 1
*hydro kf kr 0.0 0.0
1380901 0.0 0.0
*hydro te 00
1381001 00
*hydro kf kr 0.0 0.0
1381101 01000 jun 1
*hydro chb_pressure tempe
1381201 0 3459148. 175637.7 2419442. 0. 0. 1
1381202 0 3454074. 175642.7 2419446. 0. 0. 2
*hydro vel/flw
1381300 0
*hydro vel/flw fvelocity gvelocity jvelocity
1381401 7.11902 7.11902 0.1 651.38
*hydro component name component type
1600000 "elbow1" sngljun
*hydro from to area floss rloss vcahs
1600101 158010000 162000000 0.083220 0.182 0.182 01000
*hydro vel/flw fvelocity gvelocity jvelocity
1600201 0 7.11904 7.11904 0.* 651.38!
*hydro component name component type
1620000 "14inchg" pipe
1620001 4
*hydro volarea vol 1

```

1620101	0.08322	4
1620101	*	*
*hydro	length	vol
1620301	1.83	1
1620302	1.57	2
1620303	1.45	3
1620304	12.10439	4
*hydro	volume	vol
1620401	0	4
*	*	*
*hydro	horz angle	vol
1620501	0.	4
*	*	*
*hydro	vert angle	vol
1620601	-90.	1
1620602	0.	3
1620603	-90.	4
*	*	*
*hydro	delta z	vol
1620701	-1.83	1
1620702	0.	3
1620703	-12.10439	4
*	*	*
*hydro	roughness	hyd diam
1620801	0.0000457	0.3255
*	*	*
*hydro	kf	kr
1620901	0.182	0.182
1620902	0.13	0.13
1620903	0.182	0.182
*	*	*
*hydro	fe	vol
1621001	00	4
*	*	*
*hydro	weirs	jun
1621101	01000	3
*	*	*
*hydro	ekt pressure	tempe
1621201	3455294.	vol
1621202	7.6668	0.1
1621203	3458164.	0.2
1621204	3452834.	0.3
1621205	7.6668	0.4
*	*	*
*hydro	vel/flw	0
1621300	*	*
*	*	*
*hydro	component name	component type
1720000	"Inlet"	snglun
*	*	*
*hydro	from	to
1720101	162010000	17100000
*	*	*
*hydro	jun hyd diam	area
1720110	0.1985	floss
*	*	*
*hydro	vel/flw	g velocity
1720201	0.191453	j velocity
*	*	*
*hydro	component name	component type
1710000	"Ridhrot"	pipe

```

*hydro vol area 1740101 0.08322 vol 1
*hydro length 1740301 0.50 vol 1
*hydro volume 1740401 0. vol 1
*hydro volume 1740501 0. vol 1
*hydro vert angle 1740601 45.0 vol 1
*hydro delta z 1740701 0.50 vol 1
*hydro roughness 1740801 0.0000457 hyd diam 0.3255 vol 1
*hydro floss 1740901 0.0 r loss 0.0 jun 1
*hydro fe 1741001 0.0 vol 1
*hydro vcahs 1741101 0.01000 jun 2
*hydro cbt pressure 1741201 0.3356308. 175623.22419518. 0. vol 0.1
*hydro velJlw 1741300 0 1741301 7.21537 7.79558 0.2 * 65973 jun
* components 2xx - heat exchanger coolant loop 2
*hydro component name component type 20100000 "Hsp12" pipe
*hydro vol area 2010001 3 vol 3
*hydro length 2010101 0.08322 vol 3
*hydro length 2010301 1.07 vol 1
*hydro length 2010302 3.66 2 vol 2
*hydro length 2010303 2.21 3 vol 3
*hydro volume 2010401 0.0 vol 3
*hydro vert angle 2010601 0. vol 3
*hydro delta z 2010701 0. vol 3
*hydro roughness 2010801 0.0000457 hyd diam 0.3255 vol 3
*hydro vol area 2010901 0.182 0.182 jun 2
*hydro fe 2011001 0.0 vol 3
*hydro vcahs 2011101 0.01100 jun 2
*hydro cbt pressure 2011201 0 158346. 338398.3 2411276. 0. vol 0.1
*hydro cbt pressure 2011202 0 156979. 338370. 2411167. 0. 0.2
*hydro cbt pressure 2011203 0 150553. 338392.4 2410349. 0. 0.3
*hydro velJlw 2011300 0
*hydro component name component type 2030000 "Hsp11" mpujpn
*hydro component name component type 2030001 1 0
*hydro from to area 2030002 201010001 0.24663 1.20 1.20 0.1000
*hydro from to area 2030012 1.0 1.0 0 0 0 1
*hydro velJlw 2030101 2.553817 2.553817 1 * 678.254
*hydro component name component type 2030200 "Isolate"
*hydro from to area 2030300 204000000 0.08322 0.104 0.104 0.1100
*hydro velJlw 2030301 0 7.57417 7.57417 0.104 0.104 0.1100
*hydro valve type tripVlv 2030300
*hydro component name component type 2040000 "Holeg" pipe
*hydro vol area 2040101 0.08322 vol 3
*hydro length 2040301 0.69 vol 1
*hydro component name component type 2040302 12.95 2
*hydro component name component type 2040303 2.51 3
*hydro volume 2040401 0. vol 3
*hydro volume 2040501 0. vol 3

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2120000 "heplout1" branch
*hydro no. juns vel/flw
2120001 2 0
*hydro area length volume
2120101 0.08322 1.0 0.
*hydro horz angle vert angle delta z
2120102 0. 0. 0.
*hydro roughness hyd diam fe
2120103 0.0000457 0.3255 0
*hydro cbt pressure tempe
2120200 1473655. 178599. 2410108. 0.
*hydro from to area floss rloss wcats
2121101 208010000 212000000 0. 0.15 01000
2122101 212010000 215000000 0.08322 0. 0.0000
*hydro hyd diam
2122110 0.3255 0.0 1.0
2122110 0.3255 0.0 1.0
*hydro f velocity g velocity j velocity
2121201 7.36806 7.36806 0. * 673.363
2122201 7.36817 7.36817 0. * 673.364
*hydro component name component type
2130000 "joints" pipe
*hydro vol area
2130101 0.08322
*hydro length
2130301 1.981
2130302 1.23
2130303 0.6096
*hydro volume
2130401 0.
*hydro vert angle
2130601 -22.6
2130602 -29.7
2130603 -.90.
*hydro elev change
2130701 -0.762
2130702 -0.6093
2130703 -0.6096
*hydro roughness hyd diam
2130801 0.0000457 0.3255
*hydro floss rloss
2130901 0.182 0.182
*hydro fe
2131001 00
*hydro wcats
2131101 01000
*hydro cbt pressure tempe
2131201 0 1475968. 178901. 2410146. 0. 0.1
2131202 0 147593. 178902. 3 2410146. 0. 0.2
2131203 0 1476019. 178903. 2410146. 0. 0.3
*hydro vel/flw
2131300 0
*hydro fflowrate g flowrate j flowrate
2131301 7.36817 7.36817 0. 1 * 673.384
2131302 7.36817 7.36817 0. 2 * 673.384
*main heat exchanger secondary flow system (tube side)
*$*
*hydro component name component type
2300000 "secdir2" tmdflow
*hydro area length volume
2300101 1.e6 0 1.0e+06
*hydro horz angle vert angle delta z
2300102 .0 .0 .0
*hydro roughness hyd diam fe
2300103 .0 .0 10
*hydro cbt trip no. alpha vrc numeric vrc
2300200 003 302.55
*hydro time pressure tempe
2300201 0. 5.000e5 302.55
*hydro component name component type
2320000 "secdir1" tmdflow
*hydro from to area
2320101 230000000 234000000 0.7122
*hydro vel/flw trip no. alpha vrc numeric vrc
2320200 1 0 cntrivar 586
*hydro time fflow g flow jflow
2320201 -1.e6 0. 0. 0.
2320202 1.e6 1.e6 0. 0.
*hydro component name component type
2340000 "mink-sec" pipe
*hydro volarea
2340001 10
*hydro volarea
2340101 0.776
*hydro length
2340301 1.314
*hydro volume
2340401 0.
*hydro vert angle
2340601 0.
*hydro delta z
2340701 0.

```

EMERGENCY HEAT EXCHANGER - LOOP 2

- * hydro roughness hyd diam vol 10
2340801 0.0000457 0.015388
- * hydro fe vol 10
2341001 00
- * hydro vessels jun 9
2341101 Q1000
- * hydro ebt pressure temps vol
2341201 0 502324. 1304704.2560195. 0. 0.1
2341202 0 498111. 131991.255807. 0. 0.2
2341203 0 492011. 148901.6.2559417. 0. 0.3
2341204 0 485937. 160500.5.2559024. 0. 0.4
2341205 0 479889. 174164.6.2558630. 0. 0.5
2341206 0 473814. 175596.6.2558229. 0. 0.6
2341207 0 467107. 177214.6.2557822. 0. 0.7
2341208 0 461164. 179045.7.2557412. 0. 0.8
2341209 0 455505. 181121.2556997. 0. 0.9
2341210 0 449410. 183477.2556578. 0. 0.10
- * hydro f velocity g velocity jun
2341300 0 2.29634. 2.29634. 0. 1 * 1774.07
2341301 2.297187 2.297187 0. 2 * 1774.07
2341302 2.299752 2.299752 0. 3 * 1774.07
2341303 2.30209 2.30209 0. 4 * 1774.07
2341304 2.30209 2.30209 0. 4 * 1774.07
2341305 2.305026 2.305026 0. 5 * 1774.07
2341306 2.305335 2.305335 0. 6 * 1774.07
2341307 2.30572 2.30572 0. 7 * 1774.07
2341308 2.306137 2.306137 0. 8 * 1774.07
2341309 2.306616 2.306616 0. 9 * 1774.07
- * hydro jun hyd diam jun 9
2341401 0.01588 0.01010
- * hydro component name component type
2350000 "tubeout"
- * hydro from to area floss rloss vcols
2350101 234010000 236000000 0. 0. 0. 0.01000
- * hydro hyd diam
2350110 0.01588 0. 1.0 1.0
- * hydro vel/wr f velocity g velocity jun
2350201 0 2.307163 2.307163 0. * 1774.07
- * hydro component name component type
23560000 "secnki"
2360102 trndvol
- * hydro roughness hyd diam fe
2360103 .0 .0 10
2360104 1.6 .0 1.0e+06
- * hydro ebt trip no. alpha vrc numeric vrc
23602000 003
- * hydro time pressure tempe
2360201 0. 4.49e5 319.
- * hydro roughness hyd diam vol 4
2160801 0.0000457 0.0346
2160801 0.0000457 0.00170
- * hydro delta z vol 4
2160701 0.0
- * hydro floss rloss jun 3
2160901 0.0 0.0
- * hydro fe vol 4
2161001 0.0000457 0.0346
2161001 0.0000457 0.00170
- Calibrated hydraulic diameter to match pressure drop

* hydro vrehs jun 3
2161101 01000

* hydro ebt pressure temp vol
2161201 0 1497384. 178674.6 2410484.0. 0.1
2161202 0 1488870. 17835. 2410350. 0. 0.2
2161203 0 1480338. 177837. 2410215. 0. 0.3
2161204 0 1471782. 177128.5 2410079. 0. 0.4

* hydro f velocity g velocity j velocity jun
2161300 0
2161301 .685863 .685863 0.1 * 673.385
2161302 .685845 .685845 0.2 * 673.387
2161303 .685818 .685818 0.3 * 673.388

* hydro jun hyd diam 3
2161401 0.000170 0.101.0

* hydro component name component type
2200000 hxpout branch \$

* hydro no. juns veflw
2200001 2 0

* hydro area length volume
2200101 0.08322 1.0 0.

* hydro horz angle vert angle delta z
2200102 0. 0. 0. 0.

* hydro roughness hyd diam fe
2200103 0.0000457 0.3255 0

* hydro ebt pressure temp
2200200 1432869. 177129.6 2409452. 0.

* hydro from to area floss rloss vrehs
2201101 216010000 22000000 0. 0.15 01000
2202110 220010000 22200000 0.08322 0. 0. 01000

* hydro hyd diam
2201110 0.3255 0.101.0
2202110 0.3255 0.101.0

* hydro f velocity g velocity j velocity
2201201 7.367 7.367 0. * 673.389
2202201 7.36713 7.36713 0. * 673.389

* emergency heat exchanger secondary flow system (tube side) \$

* hydro component name component type
2380000 "secure" imdpvol

* hydro area length volume
2380101 1.e6 .0 1.0e+06

* hydro horz angle vert angle delta z
2380102 .0 .0 ,0

* hydro roughness hyd diam fe
2380103 .0 .0 10

* hydro ebt trip no. alpha vrc numeric vrc
2380200 003

* hydro time pressure tempe
2380201 0. 1.800e5 311.15

* hydro component name component type
2400000 "tubin" snglun

* hydro from to area floss rloss vrehs
2400101 238000000 242000000 0. 0. 0. 01100

* hydro hyd diam
2400110 0.4573 0. 0. 1.0 1.0

* hydro vel/flw f velocity g velocity j velocity
2400201 0 .0980432 .0980432 0. * 41.5164

* hydro component name component type
2420000 "ebc-sec" pipe \$

* hydro vol area
2420001 2

* hydro vol area
2420101 0.4264 2

* hydro length
2420301 0.1622 2

* hydro volume
2420401 0. 2

* hydro vert angle
2420601 0. 2

* hydro delta z
2420701 0.0 2

* hydro roughness hyd diam
2420801 0.0000457 0.4573 2

* hydro fe
2421001 00 2

* hydro vrehs
2421101 01000 jun 1

* hydro ebt pressure tempe
2421201 0 17993. 159067.4 2525552. 0. 0.1
2421202 0 17993. 159067.4 2525552. 0. 0.2

* hydro f velocity g velocity j velocity jun
2421300 0

* hydro jun hyd diam
2421401 0.4573 0. 0.10.0 jun 1

* hydro component name component type
2440000 "tubin" snglun

* hydro from to area floss rloss vrehs
2440101 242010000 246000000 0. 0. 0. 01100

* hydro hyd diam
2440110 0.01905 0. 0. 1.0 1.0

* hydro vel/flw f velocity g velocity j velocity
2440201 0 .0980432 .0980432 0. * 41.5164

ACCUMULATOR AND SURGE LINE - LOOP 2
assembled from normal relaps components.
a tank wall heat structure (#2561) has been defined

* hydro vel/flw f velocity g velocity j velocity
2570201 0 -2.374754 -2.374754 0. * .0212664

	hydro	component name	component type	vol/flw	f velocity	g velocity	j velocity	tempc	flowrate	flowrate	area	length	volume
\$	"hydro"	"accum2"	pipe	2220000	2220000	"coldig"	"coldig"	2220001	3	3	0.01000	0.01000	\$
\$	"hydro"	"no. volumes"	pipe	2560001	6			2220101	0.08322	0.08322			\$
*	"hydro"	vol area	vol	2560101	1.65	5	6	2220301	2.31	2.31			\$
*	"hydro"	length	vol	2560102	0.08322	5	6	2220302	2.13	2.13			\$
*	"hydro"	length	vol	2560301	4.09	1	5	2220303	0.762	0.762			\$
*	"hydro"	length	vol	2560302	0.12	5	6	2220401	0.	0.			\$
*	"hydro"	volume	vol	2560303	4.88	6	6	2220501	0.	0.			\$
*	"hydro"	vert angle	vol	2560401	0.	6	6	2220601	-7.6	-7.6			\$
*	"hydro"	roughness	hyd diam	2560801	0.0000457	1.49	5	2220802	0.	0.			\$
*	"hydro"	roughness	hyd diam	2560802	0.0000457	0.3255	6	2220803	90.	90.			\$
*	"hydro"	f loss	r loss	2560801	0	0.	4	2220701	-0.305	-0.305			\$
*	"hydro"	f loss	r loss	2560802	0.5	1.0	5	2220702	0.	0.			\$
*	"hydro"	fc	vol	2561001	00000	6	6	2220703	0.762	0.762			\$
*	"hydro"	vel/flw	vol	2561101	00000	5	5	2220801	0.0000457	0.0000457			\$
*	"hydro"	chb	vol	2561201	6	373154.	.0770027	2221001	0.3255	0.3255			\$
*	"hydro"	velocity	g velocity	2561202	1.09214	2410340.	0.0.2	2221201	1.432517.	1.432517.			\$
*	"hydro"	velocity	g velocity	2561203	1.091088.	1109121.	2409446.0.	2221202	1.77113.	1.77113.			\$
*	"hydro"	velocity	g velocity	2561204	15023287.	119419.	2410556.0.	2221203	2.2409340.	2.2409340.			\$
*	"hydro"	velocity	g velocity	2561205	15036384.	136328.7	2410574.0.	2221204	0.4	0.4			\$
*	"hydro"	velocity	g velocity	2561206	1504980.	168508.6	2410590.0.	2221205	0.5	0.5			\$
*	"hydro"	velocity	g velocity	2561207	1531798.	223321.	2410937.0.	2221206	0.6	0.6			\$
*	"hydro"	vel/flw	vol	2561300	0			2221300	0	0			\$
*	"hydro"	component name	component type	2570000	"accumout"	sngflun		2221301	7.36713	7.36713	0.1	0.1	\$
*	"hydro"	component name	component type	2570002	204020001	area floss rloss vcahs		2221302	7.36715	7.36715	0.2	0.2	\$
*	"hydro"	from to	area floss rloss vcahs	2570101	256060002	0.08322 0.	0.	2221303	177110.5	177110.5	2409156.	0.	\$
*	"hydro"	area	length	2570102	0.01000			2221304	0.01000	0.01000			\$
*	"hydro"	component name	component type	2240000	"recpump2"	pump		2221305	-2.3177144	-2.3177144	0.		\$

* hydro 0. 0.500 0.7739
 * hydro horz angle vert angle delta z
 2240102 0. 0. 0.
 * hydro equil flag
 2240103 00
 * hydro from jun area floss rloss vcahs
 2240108 222010000 0. 0.00 0.00 01000
 * Assume k=2.0 for strainer loss coefficient
 * hydro to jun area floss rloss vcahs
 2240109 226000000 0. 2.0 2.0 01000
 * hydro cht pressure tempc
 2240200 2495248. 177155. 2418673. 0.
 * hydro vel/flw fflowrate gflowrate jflowrate
 2240201 0 7.36718 7.9574 0. * 673.389
 * hydro vel/vlw fflowrate gflowrate jflowrate
 2240202 0 7.36372 7.36372 0. * 673.39
 * hydro pdi 2fazi diffi tork i pval1 trip no. rvs i
 2240301 124 124 -1 0 555 0
 * hydro rated pump vel. hydrated vel. rated flow rated head
 2240302 188.5 .988583 0.643 207.3
 * hydro rated torque mom of inertia rated dens mir torque
 2240303 7616.8 91.50 1098. 0
 * hydro coeffi tff coeffi ff0 coeffi ffi coeffi ffs
 2240304 10.0 150.0 0. 0.
 * pump speed table
 * 2246100 0 cnitivar 136
 2246100 619 cnitivar 195
 2246101 -1.e6 -1.e6
 2246102 1.e6 1.e6
 * hydro component name component type
 2260000 "pumpdisc" pipe
 * hydro component name component type
 2260001 1
 * hydro vol area vol
 2260101 0.08322 1
 * hydro length vol
 2260301 0.9146 1
 * hydro volume vol
 2260501 0. 1
 * hydro vert angle vol
 2260601 0.0 1
 * hydro delta z vol
 2260701 0.0 1
 * hydro roughness hyd diam vol
 2260801 0.000457 0.3255 1
 * hydro floss rloss jun
 2260901 0.0 1
 * hydro 0.00 0.00 01000
 * hydro cht pressure tempc
 2291201 0 3460638. 177153. 2419441. 0. 0.1
 * hydro vel/flw

2710301	0.30	1	hydro	volume	vol
2710302	0.29	2		0.	1
2710303	0.94	3		2740401	*
*	*	*	hydro	volume	vol
*hydro	volume	vol		0.	1
2710401	0.	3		2740501	*
*	*	*	hydro	vert angle	vol
*hydro	volume	vol		2740501	45.0
2710501	0.	3		*	1
*	*	*	hydro	delta z	vol
*hydro	vert angle	vol		2740701	0.50
2710601	-90.0	1		*	1
2710602	0.0	2	hydro	roughness	vol
2710603	0.0	3		0.0000457	0.3255
*	*	*	hydro	hyd diam	vol
*hydro	delta z	vol		2740801	1
2710701	-0.3	1		*	*
2710702	0.0	2	hydro	floss	jun
2710703	0.0	3		0.0	1
*	*	*	hydro	fc	vol
*hydro	roughness	hyd diam		2741001	00
2710801	0.0000457	0.1985		*	1
*	*	*	hydro	vcals	jun
*hydro	floss	r loss		2741101	01000
2710901	0.196	0.196		*	2
*	*	*	hydro	el pressure	vol
*hydro	el pressure	temp		2741201	0 354407.
2711001	00	vol		177057.8 2419519.0	0.1
*	*	*	hydro	vel/flw	*
*hydro	vels	g		*	*
2711101	01000	jun		hydro	flowrate
*	*	*		g flowrate	jun
*hydro	el pressure	temp		2741300	0 721537 7.79558 0.2 * 659.73
2711201	0	3298269.		*	*
2711202	0	3253064.		*	*
2711203	0	3201296.		*	*
*	*	*	components 3xx - heat exchanger coolant loop 3	*	*
*hydro	vel/flw	component name		hydro	component type
*	*	*		3010000	"hplus3"
*hydro	f flowrate	g flowrate		*	*
2711300	0	27400000		*	*
2711301	19.7928	20.62123.0.1 * 673.39		*	*
2711302	19.7932	19.7932 0.2 * 673.39		*	*
*	*	*	component name	component type	
*hydro	component type	sngfln		3010001	1
2730000	"sngfln"	*		*	*
*	*	*	hydro	vol area	vol
*hydro	from	to		3010101	0.08322
2730101	271010000	274000000		*	*
*	*	*	hydro	length	vol
*hydro	jun hyd diam	vol		3010301	3.28
2730110	0.1985	0.0 1.0 1.0		*	*
*	*	*	hydro	volume	vol
*hydro	vel/flw	f velocity		3010401	0.0
2730201	19.79367	19.79367 0. * 673.39		*	*
*	*	*	hydro	vert angle	vol
*hydro	component type	pipe		3010601	0.
2740000	"psraw-2"	*		*	*
*	*	*	hydro	delta z	vol
2740001	1	*		3010701	0.
*	*	*	hydro	roughness	vol
*hydro	vol area	vol		3010801	0.0000457 0.3255
2740101	0.08322	1		*	*
*	*	*	hydro	vcals	jun
*hydro	length	vol		3011101	01100
2740301	0.50	1		*	*
*	*	*	hydro	f velocity	jun
*3011300	0	*		*3011300	0

```

*3011301 7.44853 7.44853 0.          2
*hydro ch pressure tempe          vol
 3011201 0 1559498. 338441. 2411290. 0.   0.1
*hydro component name component type
  * "mfp1j"
*3030000 1 0
*hydro from to area floss rloss vcahs      $ 
 3030011 630010000 301000000 0.246633 0.17 0.17 01000
 3030012 1.0 1.0 1.0 0 0 1
*3031011 2.56604 2.56604 1 * 680.984
*3032011 0.3235 0.0 1.0 1.0 1
*hydro component name component type
  * "Isolate"
*3020000 "Isolate" valve      $ 
*hydro from to area floss rloss vcahs      $ 
 3020101 301010000 304000000 0.08322 0.104 0.104 01100
*hydro vch/w f flowrate & flowrate j flowrate
 3020201 0 7.60466 7.60466 0. * 680.984
*hydro component name component type
  * "tipiv"
*3020300 trip no.
  * 515
*hydro component name component type
  * "holeg"
*3040000 "holeg" pipe      $ 
*hydro volume
 3040101 0.          vol
 3040101 0.08322    3
*hydro length
 3040301 0.69       vol
 3040302 12.96      1
 3040303 2.51       2
 3040304 3.          3
*hydro volume
 3040401 0.          vol
 3040501 0.          3
*hydro vert angle
 3040601 0.          vol
 3040602 90.         2
 3040603 3.          3
*hydro delta z
 3040701 0.          vol
 3040702 2.44       2
 3040703 3.          3
*hydro roughness hyd diam      vol
 3040801 0.0000457   0.3255   3
*hydro floss rloss jun
 3040901 0.0         0.0     1
 3040902 0.182      0.182    2
*hydro fe
 3041001 00          0
*hydro vcahs
 3041101 010000      1
*hydro ch pressure tempe
 3041201 0 1553704. 338416.6 2411218.0.   0.1
 3041202 0 1545327. 337962.7 2411110.0.   0.2
 3041203 0 1517198. 337876. 2410749.0.   0.3
*hydro vch/w
*hydro f flowrate g flowrate j flowrate jun
 3041301 7.60465 7.60465 0.1 * 680.984
 3041302 7.60385 7.60385 0.2 * 680.2558
*MAIN HEAT EXCHANGER - LOOP 3
*hydro component name component type
  * "ExpIn3"
*3060000 no. ijns
  * 2
*hydro component name component type
  * "ExpIn3"
*3060001 no. ijns
  * 2
*hydro area
 3060101 0.08322    area
*hydro length
 3060102 1.0        length
*hydro volume
 3060103 0.0000457  volume
*hydro ch pressure tempe
 3060200 0 1532651. 337877. 2410948.0.
*hydro from to area floss rloss walls
 3061101 306000000 308000000 0. 0.15 0.15 0.000
 3062101 304010000 306000000 0. 0. 0. 0.01000
*hydro hyd diam
 3063110 0.3255 0.1 0.1 0.0
*hydro f velocity g velocity j velocity
 3061201 7.54915 7.54915 0. * 676.966
 3062201 7.60384 8.20134 0. * 680.958
*hydro component name component type
  * "mbs-pnt"
*3080000 no. ijns
  * 11
*hydro volera
 3080101 0.8258    vol
 3080102 0.841     5
 3080103 0.8258    6
*hydro length
 3080301 1.11      11
 3080302 2.03      6

```

* hydro from to area floss rloss wels
 3121101 30801000 31200000 0. 0.15 0.15 0.0000
 * hydro hyd diam
 3121100 0.3255 0.1 0.1 0
 3122110 0.3255 0.1 0.1 0
 * hydro f velocity g velocity j velocity
 3121201 7.39762 7.39762 0. * 676.081
 * hydro
 3122201 7.39773 7.39773 0. * 676.081
 * hydro component name component type
 3130000 "Johns" pipe
 * hydro
 3130001 3
 * hydro vol area
 3130101 0.08322
 * hydro lenetb
 3130301 1.381
 3130302 1.23
 3130303 0.696
 * hydro volume
 3130401 0.
 * hydro vert angle
 3130601 -22.6
 3130602 -29.7
 3130603 -.90.
 * hydro elev. change
 3130701 -0.762
 3130702 -0.693
 3130703 -0.696
 * hydro roughness hyd diam
 3130801 0.000457 0.3255
 * hydro
 3131001 0
 * hydro flowrate flowrate
 3131201 0 1493892. 179042.3 2410429. 0. 0.1
 3131202 0 1493358. 179043.6 2410429. 0. 0.2
 3131203 0 1493832. 179044.2 2410428. 0. 0.3
 * hydro vel/w
 3131300 0
 * hydro wels
 3131101 01000
 * hydro ch pressure temp
 3131201 0 1493892. 179042.3 2410429. 0. 0.1
 3131301 7.39773 7.39773 0.1 676.082
 3131302 7.39773 7.39773 0.2 * 676.082
 * main heat exchanger secondary flow system (tube side)
 * hydro jun hyd diam
 3081401 0.100 0.0 1.0 1.0
 * hydro component name component type
 3120000 "hplnt3" branch
 * hydro no. juns vel/w
 3120001 2 0
 * hydro area length volume
 3120101 0.08322 1.0 0.
 * hydro horz angle vert angle delta z
 3120102 0. 0. 0.
 * hydro roughness hyd diam fc
 3120103 0.000457 0.3255 0
 * hydro ch pressure temp
 3120200 1491592. 179040.3 2410593. 0.
 * hydro

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*hydro component name component type
3300000 "secr3" tmdpoly jun
*hydro area length volume
3300101 1.e6 .0 1.0e+06
*hydro horz angle vert angle delta z
3300102 ,0 ,0 ,0
*hydro roughness hyd diam fc
3300103 ,0 ,0 10
*hydro cbt trip no. alpha vrc numeric vrc
3300200 003
*hydro time pressure tempc
3300201 0. 5.000e5 302.55
*hydro component name component type
3320000 "secr1" tmdpoly jun
*hydro from to area
3320101 33000000 334000000 0.7122
*hydro trip no. alpha vrc numeric vrc
3320200 1 0 currvr 586
*hydro time fflow gflow jflow
3320201 -1.e6 -1.e6 0. 0
3320202 1.e6 1.e6 0. 0
*hydro component name component type
3340000 "Tmhc-sec" pipe $ jun
*hydro vol area vol
3340101 0.776 10
*hydro length vol
3340301 1.314 10
*hydro volume vol
3340401 0. 10
*hydro vert angle vol
3340601 0. 10
*hydro delta z vol
3340701 0.0 10
*hydro roughness hyd diam vol
3340801 0.0000457 0.01588 10
*hydro fc vol
3341001 0 10
*hydro cbt pressure tempc
3341201 0 504232. 130496.6 2560195.0. 0.1
3341202 0 498169. 1390453.4 2559807.0. 0.2
3341203 0 492010. 148979.4 2559417.0. 0.3
3341204 0 488936. 160601.6 2559024.0. 0.4
3341205 0 479838. 174285.2 2558630.0. 0.5
3341206 0 473813. 175722.4 2558229.0. 0.6
*hydro f velocity g velocity j velocity
3341300 0 2.296346 2.296346 0.1 * 1774.07
3341301 2.296346 2.296346 0.1 * 1774.07
3341302 2.29788 2.29788 0.2 * 1774.07
3341303 2.29977 2.29977 0.3 * 1774.07
3341304 2.30211 2.30211 0.4 * 1774.07
3341305 2.305053 2.305053 0.5 * 1774.07
3341306 2.30538 2.30538 0.6 * 1774.07
3341307 2.30575 2.30575 0.7 * 1774.07
3341308 2.30617 2.30617 0.8 * 1774.07
3341309 2.30665 2.30665 0.9 * 1774.07
*hydro jun hyd diam jun
3341401 0.01588 0.0 1.0 1.0
*hydro component name component type
3350000 "tubeout" smejun jun
*hydro from to area floss vrcas
3350101 33401000 336000000 0.0 0. 0. 0.0100
*hydro hyd diam
3350110 0.01588 0.0 1.0 1.0
*hydro vel/fw f velocity g velocity j velocity
3350201 0 2.307196 2.307196 0. * 1774.07
*hydro component name component type
3360000 "secn1" tmdpol jun
*hydro area length volume
3360101 1.e6 ,0 1.0e+06
*hydro horz angle vert angle delta z
3360102 ,0 ,0 ,0
*hydro roughness hyd diam fc
3360103 ,0 ,0 10
*hydro cbt trip no. alpha vrc numeric vrc
3360200 003
*hydro component name component type
3140000 hxpml branch $ jun
*hydro no. junks vel/flw
3140001 2 0
*hydro component name component type
3140101 area length volume
3140101 0.08322 1.0 0
*hydro horz angle vert angle
3140101 0.08322 1.0 0

```

* hydro roughness hyd diam fc
 * 3140102 0. 0. 0. 0.
 * 3140103 0.0000457 0.3255 0
 * hydro cbt pressure tempc
 * 3140200 1525599. 1790452.2410857.0.
 * hydro from to area floss rloss vrabs
 * 3141101 31400000 31600000 0. 0.15 0.15 01000
 * 3142101 313010000 314000000 0. 0. 0. 01000
 * hydro hyd diam
 * 3141110 0.3255 0.0 1.0 1.0
 * 3142110 0.3255 0.0 1.0 1.0
 * hydro f velocity g velocity j velocity
 * 3141201 7.39763 7.39763 0. * 676.082
 * 3142201 7.39773 7.39773 0. * 676.082
 * hydro component name component type
 * 3160000 "elix prim" pipe
 * 3160001 4
 * hydro vol area vol
 * 3160101 0.894 4
 * hydro length vol
 * 3160301 1.6 4
 * hydro volume vol
 * 3160401 0. 4
 * hydro vert angle vol
 * 3160601 0. 4
 * hydro delta z vol
 * 3160701 0.0 4
 * Calibrated hydraulic diameter to match pressure drop
 * hydro roughness hyd diam vol
 * 3160801 0.0000457 0.0346 4
 * 3160801 0.0000457 0.00170 4
 * hydro floss rloss jun
 * 3160901 0.0 0.0 jun
 * hydro fc vol
 * 3161001 00 4
 * hydro vrabs jun
 * 3161101 01000 3
 * hydro cbt pressure tempc
 * 3161201 0 1515362. 178822.3 2410725. 0. 0.1
 * 3161202 0 1506819. 178491. 2410614. 0. 0.2
 * 3161203 0 1498359. 177965.8 2410498. 0. 0.3
 * 3161204 0 1489673. 177259.6 2410363. 0. 0.4
 * hydro f velocity g velocity j velocity jun
 * 3161300 0 1515362. 178822.3 2410725. 0. 0.1
 * 3161301 .688615 .688615 0.1 * 676.083
 * 3161302 .688597 .688597 0.2 * 676.084
 * 3161303 .688569 .688569 0.3 * 676.086
 * hydro jun hyd diam jun

3161401 0.00170 0.010.1.0 3
 * hydro component name component type
 * 3200000 branch
 * hydro no. juns vel/fw
 * 3200001 2 0
 * hydro area length volume
 * 3200101 0.08322 1.0 0.
 * hydro horzangle vert angle delta z
 * 3200102 0. 0. 0.
 * hydro roughness hyd diam fc
 * 3200103 0.0000457 0.3255 0
 * hydro cbt pressure tempe
 * 3200200 1450468. 177260.7 2409737.0.
 * hydro from to area floss vrabs
 * 3201101 316010000 320000000 0. 0.15 0.15 01000
 * 3202101 320010000 322000000 0.08322 0. 0. 01000
 * hydro hyd diam
 * 320110 0.3255 0.0 1.0 1.0
 * 3202110 0.3235 0.0 1.0 1.0
 * hydro f velocity g velocity j velocity
 * 3201201 7.39652 7.396550. * 676.087
 * 3202201 7.39668 7.3966830. * 676.087
 * emergency heat exchanger secondary flow system (tube side)
 * hydro component name component type
 * 3380000 "secrec" tndpvol
 * hydro area length volume
 * 3380101 1.6 0 1.0e-06
 * hydro horzangle vert angle delta z
 * 3380102 0. 0. 0.
 * hydro roughness hyd diam fc
 * 3380103 .0 0 10
 * hydro cbt trip no. alpha vrc numeric vrc
 * 3380200 003 1.80e-5 311.15
 * hydro component name component type
 * 3400000 "tubecn" smgjum
 * hydro from to area floss vrabs
 * 3400101 338000000 342000000 0. 0. 0. 0100
 * hydro hyd diam
 * 3400110 0.4573 0.0 1.0 1.0
 * hydro vel/fw f velocity g velocity j velocity
 * 3400201 0 .099223 .099223 0. * 42.016

* hydro volume vol 3
 * hydro volume vol 3
 * hydro volume vol 3
 * hydro vert angle vol 3
 * hydro -7.6 1
 3220602 0. 2
 3220603 90. 3
 * hydro delta z vol 1
 3220701 -0.305 1
 3220702 0. 2
 3220703 0.762 3
 * hydro roughness hyd diam vol 3
 3220801 0.0000457 0.3255
 * hydro floss rloss jun 2
 3220901 0.182 2
 * hydro fe 00 vol 3
 * hydro vchls jun 2
 3221101 01000 2
 * hydro cbt pressure tempe vol
 3221201 0 1450100. 177252.3 2409731. 0.
 3221202 0 143570. 177244.5 2409625. 0.
 3221203 0 1432234. 177242. 2409441. 0.
 0.3
 * hydro fflowrate gflowrate jflowrate jun
 3221300 0 7.39668 7.39668 0.1 * 676.087
 3221301 7.39668 7.39668 0.1 * 676.087
 3221302 7.3967 7.3967 0.2 * 676.087
 * PRIMARY COOLANT PUMP - LOOP 3
 * hydro component name component type
 * "Topump3" pump
 * hydro area length volume
 3240101 0. 0.500 0.7739
 * hydro horz angle vert angle delta z
 3240102 0. 0. 0. 0.
 * hydro equil flag
 3240103 00
 * hydro from jun area floss rloss vchls
 3240108 322010000 0. 0.00 0.00 01000
 * Assume k=2.0 for strainer loss coefficient
 * hydro to jun area floss rloss vchls
 3240109 326000000 0. 2.0 2.0 01000
 * hydro cbt pressure tempe
 3240200 2511077. 177286.5 2418733. 0.
 * hydro vchls/vf
 3240201 0 7.39673 7.39685 0. * 676.087
 * hydro vchls/vf flowrate gflowrate jflowrate
 3240202 0 7.39326 0. * 676.088
 * hydro pdi 2fac diffi torq i previ tip no. rvs i
 3240301 124 124 -1 0 555 0
 * hydro rated pump vel initiated vel rated flow rated head
 3240302 188.5 .968583 0.643 207.3
 * hydro rated torque mom of inertia rated dens mtr torque
 3240303 7616.8 91.50 1098. 0
 * hydro coeff. n2 coeff. n0 coeff. n1 coeff. n3
 3240304 10.0 150.0 0. 0.
 * pump speed table
 3246100 0 centivar 186
 3246100 619 centivar 195
 3246101 1.65 -1.65
 3246102 1.65 1.65
 * hydro component name component type
 * "pimpulse" pipe
 3260000 1
 3260001 1
 * hydro volarca vol 1
 3260101 0.08322 1
 * hydro length vol 1
 3260301 0.9146 1
 * hydro volume vol 1
 3260401 0. 1
 * hydro volume vol 1
 3260501 0. 1
 * hydro vert angle vol 1
 3260601 0.0 1
 * hydro delta z vol 1
 3260701 0.0 1
 * hydro roughness hyd diam vol 1
 3260801 0.0000457 0.3255
 * hydro floss rloss jun 1
 3260901 0.0 0.0 1
 * hydro cbt pressure tempc
 3261201 0 3473876. 177284.5 2419432. 0. 0.1
 * hydro fflowrate gflowrate jflowrate jun
 3261300 0
 * hydro vchls/vf
 3261301 7.21537 7.79558 0.2 * 639.73
 *

3620401 0. 2
 *hydro horz angle vol 2
 3620501 0. vol 2
 *hydro vert angle vol 1
 3620601 0. 2
 3620602 -90. 2
 *hydro delta z vol 1
 3620701 0. 2
 3620702 -13.93439 2
 *hydro roughness hyd diam vol 2
 3620801 0.0000457 0.3255 2
 *hydro kf kr jun 1
 3620901 0.182 0.182 jun 1
 *hydro fe vol 2
 3621001 00 jun 1
 *hydro vels 01000
 3621101 01000
 *hydro ebt pressure tempc vol
 3621201 0 3407042. 1772047.2419480. 0. 0.1
 3621202 0 3467488. 1771563.2419496. 0. 0.2
 *hydro vel/flw jun 1
 3621300 0
 *hydro f velocity g velocity j velocity jun
 3621301 7.39032 7.39032 0.1 * 676.089
 *hydro component name component type
 3720000 "Int!" singlin
 *hydro jun hyd diam
 3720110 0.1985 0.0101.0
 *hydro from to area floss vels
 3720101 362010000 371000000 0.03095 0.2062 0.4513 01000
 *hydro jun hyd diam
 3720210 19.87086 20.69764 0. * 676.059
 *hydro component name component type
 3710000 "Effthrot" pipe \$
 *hydro vol area 3
 3710101 0.03095
 *hydro length vol 1
 3710301 0.30 2
 3710302 0.51 3
 3710303 0.98
 *hydro volume vol 3
 3710401 0.
 *hydro volume vol 3
 3710501 0.
 *hydro vert angle vol 1
 3710601 -90. 2
 3710602 0.0

3710603 0.0 3
 *hydro delta z vol 1
 3710701 -0.3 1
 3710702 0.0 2
 3710703 0.0 3
 *hydro roughness hyd diam vol 3
 3710801 0.0000457 0.1985
 *hydro floss rloss jun 2
 3710901 0.196
 *hydro fe vol 3
 3711001 00 jun 2
 *hydro vels 01000
 3711101
 *hydro ebt pressure tempc vol 0.1
 3711201 0 3301635. 177159.22419558. 0. 0.1
 3711202 0 3254335. 177164.22419594. 0. 0.2
 3711203 0 3200119. 177174. 2419636. 0. 0.3
 *hydro vel/flw
 *hydro f flowrate g flowrate j flowrate jun
 3711300 0
 3711301 19.8723 20.7024 0.1 * 676.089
 3711302 19.87272 19.87272 0.2 * 676.089
 *hydro component name component type
 3730000 "Effexit" singlin
 *hydro from to area floss rloss walls
 3730101 371010000 374000000 0.03095 0.1028 0.04696 01000
 *hydro jun hyd diam
 3730110 0.1985 0.0101.0
 *hydro vel/flw f velocity g velocity j velocity
 3730201 0 19.8732 19.8732 0. * 676.059
 *hydro component name component type
 3740000 "psaww-3" pipe \$
 3740001 1
 *hydro vol area 1
 3740101 0.03095
 *hydro length vol 1
 3740301 0.50 1
 *hydro volume vol 1
 3740401 0. 1
 *hydro volume vol 1
 3740501 0. 1
 *hydro vert angle vol 1
 3740601 45.0
 *hydro delta z vol 1
 3740701 0.50 1
 *hydro roughness hyd diam vol

* 3740801 0.0000457 0.3255 1
 * hydro floss r loss jun 1
 * 3740801 0.0 0.0 1
 * hydro fc vol 1
 * 3741001 00 1
 * hydro vcais jun 2
 * 3741101 01000 1
 * hydro cbt pressure tempe vol 0.1
 3741201 0 3354170. 177172.4 2419519. 0.
 * hydro vel/fw
 * hydro f flowrate g flowrate j flowrate jun
 * 37413000 0 7.79558 0.2 * 659.73
 * 3741301 7.21537
 * components 4xx - inactive heat exchanger/pump loop
 * 4510000 1
 * hydro component name component type
 * "hspil4" pipe
 * 4510001 1
 * hydro vol area vol 1
 * 4510101 0.08322 1
 * hydro length vol 1
 * 4510301 3.28 1
 * hydro volume vol 1
 * 4510401 0.0 1
 * hydro vert angle vol 1
 * 4510601 0. 1
 * hydro delta z vol 1
 * 4510701 0. 1
 * hydro roughness hyd diam vol 1
 * 4510801 0.0000457 0.3255 1
 * hydro fe vol 1
 * 4511001 00 1
 * hydro vcais jun 1
 * hydro f velocity g velocity j velocity jun
 * 45113000 0 1
 * 4511301 0. 0. 0. 2
 * hydro cbt pressure tempe vol 0.1
 4511201 0 1593319. 154261.6 2411714. 0.
 * hydro component name component type
 * "hspilj" mfpjnj
 * 4530001 1 0
 * hydro from to area floss r loss vcais
 4530011 650010000 451000000 0.24663 0.00 0.00 01000
 * hydro vol area vol
 * 4530012 1.0 1.0 1.0 0 0 0 1
 * 4531011 -5.69197 -5.691927 1 * 1.545093.4
 * 4532011 0.3255 0.0 1.0 0.1
 * hydro component name component type
 * "eljoin" pipe
 * 4290000 1
 * hydro vol area 1
 * 4290101 0.08322 1
 * hydro length vol 1
 * 4290301 6.25 1
 * hydro volume vol 1
 * 4290401 0. 1
 * hydro volume vol 1
 * 4290501 0. 1
 * hydro vert angle vol 1
 * 4290601 0.0 1
 * hydro delta z vol 1
 * 4290701 0.0 1
 * hydro roughness hyd diam vol 1
 * 4290801 0.0000457 0.3255 1
 * hydro floss r loss jun 1
 * 4290901 0.0 0.0 1
 * hydro fe vol 1
 * 4291001 00 1
 * hydro vcais jun 2
 * hydro cbt pressure tempe vol 0.1
 4291201 0 32232759. 1.545 2419610. 0.
 * hydro vel/fw
 * 4291300 1
 * hydro f flowrate g flowrate j flowrate jun
 * 4291301 7.21537 7.79558 0.2 * 659.73
 * hydro component name component type
 * "elbow1" sngljan
 * 4310000 1
 * hydro from to area floss r loss vcais
 4310101 429010000 458000000 0.083220 0.182 0.182 01000
 * hydro vel/fw f velocity g velocity l velocity
 4310201 0 4.54971-6 4.54971-6 0. * 4.171873.4
 * hydro component name component type
 * "coldcg" pipe
 * 4580000 2
 * hydro vol area vol
 * 4580001 1
 * hydro vol area vol

4580101	0.08322	2	*hydro	delta z	vol
*hydro	length	vol	4620701	0.0	1
4580301	7.24	2	4620702	-13.93439	2
*hydro	volume	vol	*hydro	roughness	hyd diam
4580401	0.	2	4620801	0.0000457	0.3255
*hydro	horz angle	vol	*hydro	kf	kr
4580501	0.	2	4620901	0.182	0.182
*hydro	vert angle	vol	*hydro	fc	
4580601	0.	2	4621001	00	
*hydro	delta z	vol	*hydro	vcahs	
4580701	0.	2	4621101	01000	
*hydro	roughness	hyd diam	*hydro	cbt pressure	temp
4580801	0.0000457	0.3255	4621201	0 3232766.	150422.2 2419610.0.
*hydro	kf	kr	4621202	0 3308056.	150056.4 2419554.0.
4580901	0.0	0.0	*hydro	f velocity	g velocity
*hydro	fc		4621300	0	j velocity
4581001	00		4621301	1.44641-5	1.44641-5 0.1 * .001326246
*hydro	vcahs	jun	*hydro	component name	component type
4581101	01000	1	4720000	"Inlet"	sngljm
*hydro	cbt pressure	vol	*hydro	from to	area
4581201	0 3232760.	146227.6 2419610.0.	4720101	462010000	471000000 0.03095 0.2062 0.4513 01000
4581202	0 3232763.	173850.4 2419610.0.	*hydro	jun hyd diam	
*hydro	vcahs	jun	4720110	0.1985	0.1 0.1 0
4581300	0	1	*hydro	refl/w	f velocity
4581301	9.83857-6	9.83857-6 0.1 * 9.02424-4	4720201	0 3.88559-5	3.88742-5 0. * .001325103
*hydro	component name	component type	*hydro	component name	component type
4600000	"elbow3"	sngljm	4710000	"Elbow"	pipe
*hydro	from to	area	*hydro	volarea	vol
4600101	458010000	462000000	4710001	0.03095	3
*hydro	vel/w	f velocity	*hydro	length	vol
4600201	1.413168-5	1.413168-5 0. * .001293117	4710301	0.30	1
*hydro	component name	component type	4710302	0.51	2
4620000	"14nedig"	pipe	4710303	0.98	3
*hydro	volarea	vol	*hydro	volume	vol
4620101	0.08322	2	4710401	0.	3
*hydro	length	vol	*hydro	volume	vol
4620301	1.2166	1	4710501	0.	3
4620302	13.93439	2	*hydro	verangle	vol
*hydro	volume	vol	4710601	-90.0	1
4620401	0.	2	4710602	0.0	2
*hydro	horz angle	vol	4710603	0.0	3
4620501	0.	2	*hydro	delta z	vol
*hydro	vert angle	vol	4710701	-0.3	1
4620601	0.	1	4710702	0.0	2
4620602	-90.	2	4710703	0.0	3
*hydro	roughness	hyd diam	*hydro	0.0000457	0.1985
4710801					3

MATERIAL PROPERTIES						
hydro	flss	r lss	vol	vol	vol	vol
1710901	0.196	0.196	jun	0.1	0.1	0.1
hydro	fc	vol	vol	vol	vol	vol
1711001	00	3	3	3	3	3
hydro	vehrs	jun	jun	jun	jun	jun
1711101	01000	2	2	2	2	2
hydro	ebt pressure	tempc	tempc	tempc	tempc	tempc
1711201	0.3384970.	146974.2419496.	0.	0.	0.	0.
1711202	0.3386593.	146594.5419495.	0.	0.	0.	0.
1711203	0.3386595.	146686.2419495.	0.	0.	0.	0.
hydro	flowrate	g flowrate	j flowrate	j flowrate	j flowrate	j flowrate
1711300	0	5	5	5	5	5
1711301	3.88531-5	3.88531-5	0.1	0.1	0.1	0.1
1711302	3.88666-5	3.88666-5	0.2	0.2	0.2	0.2

MATERIAL PROPERTIES

\$

component type	component name	sgn jum
"Index"	"Index"	
area	from to	area
floss		floss veins
veins		
0.0466	0.0466	0.0466
0.0172	0.0172	0.0172
0.4740	0.4740	0.4740
0.4710	0.4710	0.4710
0.7300	0.7300	0.7300
hydro		hydro

MATERIAL PROPERTIES					
Hydro obt pressure	tempc				
1547/41201 0	33133896.	151712.6	2419497.0.	vol	0.1
Hydro flowrate	g/min				
*#74713000	*#7471500	j flowrate	j flowrate	jun	
composition 1	stainless 3041				
composition 2	6061 aluminum				
composition 3	hafnium				
composition 4	boehmite (oxide)				
composition 5	Si3N4-al fuel meat				

\$

1						
1740001	hydro	vol area	vol	1		
1740101		0.08322				
1740001	hydro	length	vol	1		
1740301		0.50				
1740001	hydro	volume	vol	1		
1740401		0.				
1740001	hydro	volume	vol	1		
1740501		0.				
1740001	hydro	vert angle	vol	1		
1740601		45.0				
1740001	hydro	delta z	vol	1		
1740701		0.30				
1740001	hydro	roughness	hyd diam	1		
1740801		0.0000437	0.3235			
1740001	hydro	floss	r loss	jun		
1740901		0.0	0.0	1		
1741001	hydro	fc			vol	
1741101		00			1	
1741201	hydro	watts			jun	
1741301		01000			2	

MATERIAL PROPERTIES					
Hydro obt pressure	tempc				vol
1547/41201 0	33133896.	151712.6	2419497.0.	0.1	
Hydro flowrate	g/min				jun
*#47413000	*#4741500	0.0.2			
composition 1 stainless 3041					
composition 2 6061 aluminum					
composition 3 hafnium					
composition 4 bohemic (oxide)					
composition 5 ussi2-al fuel meat					

\$

1						
1740001	hydro	vol area	vol	1		
1740101		0.08322				
1740001	hydro	length	vol	1		
1740301		0.50				
1740001	hydro	volume	vol	1		
1740401		0.				
1740001	hydro	volume	vol	1		
1740501		0.				
1740001	hydro	vert angle	vol	1		
1740601		45.0				
1740001	hydro	delta z	vol	1		
1740701		0.30				
1740001	hydro	roughness	hyd diam	1		
1740801		0.0000437	0.3235			
1740001	hydro	floss	r loss	jun		
1740901		0.0	0.0	1		
1741001	hydro	fc				
1741101		00				
1741201	hydro	watts				
1741301		01000				


```

*hsir left vol incr bcond sa code area/factor ht str no.
11081501 108010000 10000 1 1 0.555 5
*hsir right vol incr bcond sa code area/factor ht str no.
11081502 108070000 10000 1 1 0.555 10
*hsir right.vol.incr.bcond.sa.code.area/factor ht str.no.
11081601 .501 0 4599 1 0.555 10
*hsir s.type s.mult left heat right heat ht str no.
11081701 0 0 0 0 0 10
*hsir chflag hyd diam equiv diam ch.len ht str no.
11081801 0 10. 10. 0. 0. 1. 10
*hsir chflag hyd diam equiv diam ch.len ht str no.
11081901 0 10. 10. 0. 0. 1. 10
*hsir left.vol.incr.bcond.sa.code.area/factor ht str.no.
11081901 0 10. 10. 0. 0. 1. 10
*hsir s.type s.mult left heat right heat ht str no.
11082000 1 4 1 1 0.00 0 0 0 0
*hsir mesh locn mesh fmat
11082100 0 1
*hsir intervals rt.coord
11082101 3 0.0445
*hsir compnn.no. interval
11082201 1 3
*hsir temp flg
11082400 0
*hsir temp
11082401 302.
*hsir left.vol.incr.bcond.sa.code.area/factor ht str.no.
11082501 108060000 00000 1 1 3.49 1
*hsir right.vol.incr.bcond.sa.code.area/factor ht str.no.
11082601 .501 0 4581 1 3.49 1
*hsir s.type s.mult left heat right heat ht str no.
11082701 0 0 0 0 1
*hsir chflag hyd diam equiv diam ch.len ht str no.
11082801 0 10. 10. 0. 0. 1. 1
*hsir left.vol.incr.bcond.sa.code.area/factor ht str.no.
11082901 0 10. 10. 0. 0. 1. 1
*hsir s.type s.mult left heat right heat ht str no.
11083000 10 4 2 1 7.049e-3 0 0 0
*hsir mesh locn mesh fmat
11083100 0 1
*hsir intervals rt.coord
11083101 3 7.928e-3
*hsir compnn.no. interval
11083201 1

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12501501 250010000 10000 1 1 0.75 4
*hsir chflag hyd diam equiv diam ch.len ht str no.
12161901 0.10.0.0.0.1.4
*hsir ht str mps geom init lcond refl b.vol axl.incr
12163100 4 4 2 1 8.63e-3 0 0 0
$ ht str no. 2163 ht tube $ *
*hsir mesh locn mesh fint
12163100 0 0 1
*hsir intervals rt.coord
12163101 3 9.55e-3
*hsir compn no. interval
12163201 1 3
*hsir source interval
12163301 0. 3
*hsir temp flg
12163400 0
*hsir temp mesh pt.
12163401 302. 4
*hsir left vol incr b.cond sa code area/factor ht str no.
12163501 216010000 10000 1 1 2672. 4
*hsir right vol incr b.cond sa code area/factor ht str no.
12163601 246040000 -10000 1 1 2672. 4
*hsir s.type s.mult left heat right heat ht str no.
12163701 0 0 0 0 4
*hsir chflag hyd diam equiv diam ch.len ht str no.
12163801 0.10.0.0.0.1.4
$ ht str no. 2501 rhumey $ *
*hsir ht str mps geom init lcond refl b.vol axl.incr
12501100 4 4 2 1 0.2287 0 0 0
*hsir mesh locn mesh fint
12501100 0 0 1
*hsir intervals rt.coord
12501101 3 0.2541
*hsir compn no. interval
12501201 1 3
*hsir temp flg
12501301 0. 3
*hsir source interval
12501400 0
*hsir temp mesh pt.
12501401 302. 4
*hsir left vol incr b.cond sa code area/factor ht str no.
12501601 -501 0 4381 1 0.75 4
*hsir s.type s.mult left heat right heat ht str no.
12501701 0 0 0 0 4
*hsir chflag hyd diam equiv diam ch.len ht str no.
12501801 0.10.0.0.0.1.4
*hsir accumulator heat structure - loop2
$ *
*hsir ht str no. 2561 tankwall $ *
*hsir ht str mps geom init lcond refl b.vol axl.incr
12561000 5 4 2 1 0.7245 0 0 0
*hsir mesh locn mesh fint
12561100 0 0 1
*hsir intervals rt.coord
12561101 3 0.7396
*hsir compn no. interval
12561201 1 3
*hsir source interval
12561301 0. 3
*hsir temp flg
12561400 0
*hsir temp mesh pt.
12561401 302. 4
*hsir left vol incr b.cond sa code area/factor ht str no.
12561501 256010000 10000 1 1 4.09 1
12561502 256020000 10000 1 1 0.12 5
*hsir right vol incr b.cond sa code area/factor ht str no.
12561601 0 0 0 1 4.09 1
12561602 0 0 0 1 0.12 5
*hsir s.type s.mult left heat right heat ht str no.
12561701 0 0 0 0 5
*hsir chflag hyd diam equiv diam ch.len ht str no.
12561801 0.10.0.0.0.1.5
$ *
*loop3*loop3*loop3*loop3*loop3*loop3*loop3*loop3*loop3*loop3*
$ *
*hsir ht str no. 3081 hx shell $ *
*hsir ht str mps geom init lcond refl b.vol axl.incr
13081000 10 4 2 1 1.009 0 0 0
*hsir mesh locn mesh fint
13081100 0 0 1
*hsir intervals rt.coord
13081101 3 1.054
*hsir compn no. interval
13081201 1 3

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* histr source interval
* 13081301 0. 3
* histr temp lg 0
* 13081400
* histr temp mesh pt.
13081401 302. 4
* histr left vol incr bcond sa code area/factor ht str no.
13081501 308010000 10000 1 1 0.355 5
13081502 308070000 10000 1 1 0.355 10
* histr right vol incr bcond sa code area/factor ht str no.
13081601 -501 0 4599 1 0.555 10
* histr s_type s_mult left heat right heat ht str no.
13081701 0 0 0 0 10
* histr chflag hyd diam equiv diam ch. len ht str no.
13081801 0.10.10.0.0.0.1.10
* histr chflag hyd diam equiv diam ch. len ht str no.
13081901 0.10.10.0.0.0.1.10
$ ht str no. 3082 hx shell
* histr ht str m ps geom init lcoord refl b.vol axl.incr
13082000 1 4 1 1 0.00 0 0 0 0
* histr mesh locn mesh fint
13082100 0 1
* histr intervals rt.coord
13082101 3 0.0445
* histr compn.no. interval
13082201 1 3
* histr temp flg 0
* histr source interval
13082301 0.
* histr temp mesh pt.
13082401 302. 4
* histr left vol incr bcond sa code area/factor ht str no.
13082501 308060000 00000 1 1 2.49 1
* histr right vol incr bcond sa code area/factor ht str no.
13082601 -501 0 4581 1 2.49 1
* histr s_type s_mult left heat right heat ht str no.
13082701 0 0 0 0 1
* histr chflag hyd diam equiv diam ch. len ht str no.
13082801 0.10.10.0.0.0.1.1
$ ht str no. 3083 hx tube 5
* histr ht str m ps geom init lcoord refl b.vol axl.incr
13082901 0.10.10.0.0.0.1.1
$ ht str no. 3161 hx shell
* histr ht str m ps geom init lcoord refl b.vol axl.incr
1308300 0.10.10.0.0.1.10
* histr chflag hyd diam equiv diam ch. len ht str no.
13083100 10000 1 1 8700.4 5
13083101 0.10.10.0.0.1.10
* histr right vol incr bcond sa code area/factor ht str no.
13083200 1 334100000 -10000 1 1 8700.4 10
* histr s_type s_mult left heat right heat ht str no.
13083701 0 0 0 0 10
* histr chflag hyd diam equiv diam ch. len ht str no.
13083801 0.10.10.0.0.1.10
* histr chflag hyd diam equiv diam ch. len ht str no.
13083901 0.10.10.0.0.1.10
* tube and shell heat structures for emergency heat exchanger
$ ht str no. 3161 hx shell
* histr ht str m ps geom init lcoord refl b.vol axl.incr
13161000 4 4 2 1 0.5334 0 0 0
* histr mesh locn mesh fint
13161100 0 1
* histr intervals rt.coord
13161101 3 0.5356
* histr compn.no. interval
13161201 1 3
* histr source interval
13161301 0.
* histr temp mesh pt.
13161401 302. 4
* histr left vol incr bcond sa code area/factor ht str no.
13161501 316010000 10000 1 1 1.6 4
* histr right vol incr bcond sa code area/factor ht str no.
13161601 -501 0 4591 1 1.6 4

```


*hstr ht str mps geom init lcond refl b.vol axl.incr
11291000 1 4 2 1 0.1627 0 0 0

*hstr mesh locn mesh fmt
11291100 0 1

*hstr intervals rt.coord
11291101 3 0.1778

*hstr compn.no. interval
11291201 1 3

*hstr source interval
11291301 0. 3

*hstr 400. 4

*hstr left vol incr b.cond sa code area/factor ht str no.
11291501 129010000 0 1 1 6.25 1

*hstr right vol incr b.cond sa code area/factor ht str no.
11291601 -501 0 4511 1 6.25 1

*hstr s. type s. mult klf heat right heat ht str no.
11291701 0 0 0 0 1

*hstr mod2.5*11291801 0 0 0 0 0 0 1
11291801 0. 10. 10. 0. 0. 0. 1. 1
*mod2.5*11291901 0 0 0 0 0 0 1
11291901 0. 10. 10. 0. 0. 0. 1. 1

*ht str no. 1581 14-in colleg \$

*hstr ht str mps geom init lcond refl b.vol axl.incr
11581000 2 4 2 1 0.1627 0 0 0

*hstr mesh locn mesh fmt
11581100 0 1

*hstr intervals rt.coord
11581101 3 0.1778

*hstr compn.no. interval
11581201 1 3

*hstr source interval
11581301 0. 3

*hstr 400. 4

*hstr left vol incr b.cond sa code area/factor ht str no.
11581501 138010000 0 1 1 4.50 2

*hstr right vol incr b.cond sa code area/factor ht str no.
11581601 -501 0 4511 1 4.50 2

*hstr s. type s. mult klf heat right heat ht str no.
11581701 0 0 0 0 2

*hstr mod2.5*11581801 0 0 0 0 0 0 2
11581801 0. 10. 10. 0. 0. 0. 1. 2

*hstr

*mod2.5*11581901 0 0 0 0 0 0 2
11581901 0. 10. 10. 0. 0. 0. 1. 2

*ht str no. 1621 14-in colleg \$

*hstr ht str mps geom init lcond refl b.vol axl.incr
11621000 4 4 2 1 0.1627 0 0 0

*hstr mesh locn mesh fmt
11621100 0 1

*hstr intervals rt.coord
11621101 3 0.1778

*hstr compn.no. interval
11621201 1 3

*hstr source interval
11621301 0. 3

*hstr 400. 4

*hstr left vol incr b.cond sa code area/factor ht str no.
11621501 162010000 0 1 1 1.83 1

11621502 162020000 0 1 1 1.57 2

11621503 162030000 0 1 1 1.45 3

11621504 162040000 0 1 1 12.10439 4

*hstr right vol incr b.cond sa code area/factor ht str no.
11621601 -501 0 4581 1 1.83 1

11621602 -501 0 4511 1 1.57 2

11621603 -501 0 4511 1 1.45 3

11621604 -501 0 4581 1 12.10439 4

*hstr s. type s. mult klf heat right heat ht str no.
11621701 0 0 0 0 4

*ht str no. 1711 8-in colleg \$

*hstr mod2.5*11581901 0 0 0 0 0 0 4
11621801 0. 10. 10. 0. 0. 0. 1. 4

*hstr mod2.5*11581901 0 0 0 0 0 0 4
11621901 0. 10. 10. 0. 0. 0. 1. 4

*ht str no. 1711 8-in colleg \$

*hstr ht str mps geom init lcond refl b.vol axl.incr
11711000 3 4 2 1 0.095925 0 0 0

*hstr mesh locn mesh fmt
11711100 0 1

*hstr intervals rt.coord
11711101 3 0.1016

*hstr compn.no. interval
11711201 1 3

*hstr source interval
11711301 0. 3

*hstr 400. 4

*hstr left vol incr b.cond sa code area/factor ht str no.
11711501 171010000 0 1 1 0.300 1

11711502 171020000 0 1 1 2.000 2

11711503 171030000 0 1 1 2.280 3

*hstr right vol incr b.cond sa code area/factor ht str no.
11711601 -501 0 4581 1 0.300 1

11711602 -501 0 4531 1 2.000 2

```

11711603 -501 0 4531 1 2280 3
*hsnr s. type s. mult left heat right heat ht str no.
11711701 0 0 0 0 0 3
*hsnr
*mod2.5*1711801 0 0 0 0 0 0.03
11711801 0.10. 0.0. 0.1. 3
*hsnr
*mod2.5*1711901 0 0 0 0 0 0.03
11711901 0.10. 0.0. 0.1. 3
*hsnr ht str no. 1741 14-in colleg $ *
*hsnr ht str n ps geom init lcoord refl b.vol axl.incr
11741000 1 4 2 1 0.1627 0 0 0
*hsnr mesh locn mesh fnt
11741100 0 1
*hsnr intervals rt.coord
11741101 3 0.1778
*hsnr compnx.no. interval
11741201 1 3
*hsnr source interval
11741301 0 3
11741401 400. 4
*hsnr left vol incr bcond sa code area/factor ht str no.
11741501 17401000 0 1 1 0.50 1
*hsnr right vol incr bcond sa code area/factor ht str no.
11741601 -501 0 4511 1 0.50 1
*hsnr s. type s. mult left heat right heat ht str no.
11741701 0 0 0 0 1
*hsnr
*mod2.5*11581901 0 0 0 0 0 0.01
11741801 0.10. 0.0. 0.0. 1. 1
*hsnr
*mod2.5*11581901 0 0 0 0 0 0.01
11741901 0.10. 0.0. 0.0. 1. 1
*hsnr ht str no. 2011 holeg $ *
*hsnr ht str n ps geom init lcoord refl b.vol axl.incr
12011000 3 4 2 1 0.1627 0 0 0
*hsnr mesh locn mesh fnt
12011100 0 1
*hsnr compnx.no. interval
12011201 1 3
*hsnr source interval
12011301 0 3
12011401 400. 4
*hsnr left vol incr bcond sa code area/factor ht str no.
12011501 20101000 0 1 1 1.07 1
12011502 20102000 0 1 1 3.66 2
12011503 20103000 0 1 1 2.21 3
*hsnr right vol incr bcond sa code area/factor ht str no.
12011601 -501 0 4511 1 1.07 1
12011602 -501 0 4511 1 3.66 2
12011603 -501 0 4511 1 2.21 3
*hsnr s. type s. mult left heat right heat ht str no.
12011701 0 0 0 0 0 3
*hsnr
*mod2.5*12011801 0 0 0 0 0 0.03
12011801 0.10. 0.0. 0.0. 1. 3
*mod2.5*12011901 0 0 0 0 0 0.3
12011901 0.10. 0.0. 0.0. 1. 3
*hsnr ht str mps geom init lcoord refl b.vol axl.incr
12041000 3 4 2 1 0.1627 0 0 0
*hsnr mesh locn mesh fnt
12041100 0 1
*hsnr intervals rt.coord
12041101 3 0.1778
*hsnr compnx.no. interval
12041201 1 3
*hsnr source interval
12041301 0 3
12041401 400. 4
*hsnr temp fng
*hsnr temp mesh pt.
*hsnr left vol incr bcond sa code area/factor ht str no.
12041501 204010000 0 1 1 6098 1
12041502 204020000 0 1 1 3048 2
12041503 204030000 0 1 1 2.51 3
*hsnr right vol incr bcond sa code area/factor ht str no.
12041601 -501 0 4511 1 6098 1
12041602 -501 0 4511 1 3048 2
12041603 -501 0 4581 1 2.51 3
*hsnr s. type s. mult left heat right heat ht str no.
12041701 0 0 0 0 0 3
*hsnr
*mod2.5*12041801 0 0 0 0 0 0.3
12041801 0.10. 0.0. 0.0. 1. 3
*mod2.5*12041901 0 0 0 0 0 0.3
12041901 0.10. 0.0. 0.0. 1. 3
*hsnr ht str mps geom init lcoord refl b.vol axl.incr
12221000 3 4 2 1 0.1627 0 0 0
*hsnr mesh locn mesh fnt
12221100 0 1
*hsnr intervals rt.coord
12221201 1 3
*hsnr left vol incr bcond sa code area/factor ht str no.

```

```

12221101 3 0.1778
*hsir compn no. interval
12221201 1 3
*hsir source interval
12221301 0 3
12221401 400.4
*hsir left vol incr bcond sa code area/factor ht str no.
12221501 222010000 0 1 1 2.31 1
12221502 222020000 0 1 1 2.13 2
12221503 222030000 0 1 1 0.762 3
*hsir right vol incr bcond sa code area/factor ht str no.
12221601 -501 0 4511 1 2.31 1
12221602 -501 0 4511 1 2.13 2
12221603 -501 0 4581 1 0.762 3
*hsir s.type s.mult left heat right heat ht str no.
12221701 0 0 0 0 3
*hsir
*mod2.5*12221801 0 0 0 0 0.03
12221801 0 10.10.0.0.0.1.3
*mod2.5*12221901 0 0 0 0 0.03
12221901 0 10.10.0.0.0.1.3
*hsir ht str no. 2261 coldeg $ .....*
*hsir ht str mps geom init lcond refl bvol axl incr
12261000 1 4 2 1 0.1627 0 0 0
*hsir mesh locn mesh fmt
12261100 0 1
*hsir intervals rt.coord
12261101 3 0.1778
*hsir compn no. interval
12261201 1 3
*hsir source interval
12261301 0 3
12261401 400.4
*hsir left vol incr bcond sa code area/factor ht str no.
12261501 226010000 0 1 1 0.9146 1
*hsir right vol incr bcond sa code area/factor ht str no.
12261601 -501 0 4511 1 0.9146 1
*hsir s.type s.mult left heat right heat ht str no.
12261701 0 0 0 0 1
*hsir
*mod2.5*12261801 0 0 0 0 0.01
12261801 0 10.10.0.0.0.1.1
*mod2.5*12261901 0 0 0 0 0.01
12261901 0 10.10.0.0.0.1.1
*hsir ht str no. 2291 14-indeg $ .....*
*hsir ht str mps geom init lcond refl bvol axl incr
12291000 1 4 2 1 0.1627 0 0 0
*hsir mesh locn mesh fmt
*hsir compn no. interval
12291101 3 0.1778
*hsir
*mod2.5*12291201 0 0 0 0 0.02
12291201 0 10.10.0.0.0.1.2
*hsir
*mod2.5*12291301 0 0 0 0 0.0002
12291301 0 10.10.0.0.0.1.2
*hsir ht str no. 2321 14-indeg $ .....*
*hsir ht str mps geom init lcond refl bvol axl incr
12291501 229010000 0 1 1 6.25 1
*hsir right vol incr bcond sa code area/factor ht str no.
12291601 -501 0 4511 1 6.25 1
*hsir s.type s.mult left heat right heat ht str no.
12291701 0 0 0 0 1
*hsir
*mod2.5*12291801 0 0 0 0 0.01
12291801 0 10.10.0.0.0.1.1
*mod2.5*12291901 0 0 0 0 0.01
12291901 0 10.10.0.0.0.1.1
*hsir ht str no. 2581 14-indeg $ .....*
*hsir ht str mps geom init lcond refl bvol axl incr
12581000 2 4 2 1 0.1627 0 0 0
*hsir mesh locn mesh fmt
12581100 0 1
*hsir intervals rt.coord
12581101 3 0.1778
*hsir compn no. interval
12581201 1 3
*hsir source interval
12581301 0 3
12581401 400.4
*hsir left vol incr bcond sa code area/factor ht str no.
12581501 236010000 0 1 1 4.50 2
*hsir right vol incr bcond sa code area/factor ht str no.
12581601 -501 0 4511 1 4.50 2
*hsir s.type s.mult left heat right heat ht str no.
12581701 0 0 0 0 2
*hsir
*mod2.5*12581801 0 0 0 0 0.02
12581801 0 10.10.0.0.0.1.2
*hsir
*mod2.5*12581901 0 0 0 0 0.0002
12581901 0 10.10.0.0.0.1.2
*hsir ht str no. 2621 14-indeg $ .....*
*hsir ht str mps geom init lcond refl bvol axl incr
12621000 2 4 2 1 0.1627 0 0 0
*hsir mesh locn mesh fmt

```

```

*mod2.5*12711901 0.0.0.0.0.0.3
12711901 0. 10. 0. 0. 0. 1.3
*          mesh locn      mesh fint
12621100 0           1
*          intervals    rt.coord
12621101 3           0.1778
*          compn.no.   interval
12621201 1           3
*          histr      source    interval
12621301 0           3
12621401 400. 4
*          histr      left vol  incr bcond sa code area/factor ht str no.
12621501 262010000 0 1 1 0.64538 1
12621502 262020000 0 1 1 13.93439 2
*          histr      right vol incr bcond sa code area/factor ht str no.
12621601 -501 0 4511 1 0.64538 1
12621602 -501 0 4581 1 13.93439 2
*          histr      s.type  s. mult  left heat right heat ht str no.
12621701 0 0 0 0 2
*          histr
*mod2.5*1581901 0.0.0.0.0.0.2
12621801 0. 10. 0. 0. 0. 1.2
*          histr
*mod2.5*1581901 0.0.0.0.0.0.2
12621901 0. 10. 0. 0. 0. 1.2
*          histr      mesh locn      mesh fint
12711100 0           1
*          intervals    rt.coord
12711101 3           0.1016
*          histr      compn.no.   interval
12711201 1           3
*          histr      source    interval
12711301 0           3
12711401 400. 4
*          histr      left vol  incr bcond sa code area/factor ht str no.
12711501 271010000 0 1 1 0.300 1
12711502 271020000 0 1 1 0.290 2
12711503 271030000 0 1 1 0.940 3
*          histr      s.type  s. mult  left heat right heat ht str no.
12711701 0 0 0 0 3
*          histr
*mod2.5*12711801 0.0.0.0.0.0.3
12711801 0. 10. 0. 0. 0. 1.3
*          histr      mesh locn      mesh fint
ht str no. 27411 14-in edeg      $
```

```

*          histr      ht str m ps geom init lcond refl b.vol ext.incr
12741000 1 4 2 1 0.1627 0 0 0
*          histr      mesh locn      mesh fint
12741100 0           1
*          histr      intervals  rt.coord
12741101 3           0.1778
*          histr      compn.no.   interval
12741201 1           3
*          histr      source    interval
12741301 0           3
12741401 400. 4
*          histr      ht vol  incr bcond sa code area/factor ht str no.
12741501 274010000 0 1 1 0.50 1
*          histr      right vol incr bcond sa code area/factor ht str no.
12741601 -501 0 4511 1 0.50 1
*          histr      s.type  s. mult  left heat right heat ht str no.
12741701 0 0 0 0 1
*          histr
*mod2.5*11581901 0.0.0.0.0.0.1
12741801 0. 10. 10. 0. 0. 0. 1.1
*          histr
*mod2.5*11581901 0.0.0.0.0.0.1
12741901 0. 10. 10. 0. 0. 0. 1.1
*          histr      ht str no. 30111  hotleg      $
*          histr      ht str m ps geom init lcond refl b.vol ext.incr
13011000 1 4 2 1 0.1627 0 0 0
*          histr      mesh locn      mesh fint
13011100 0           1
*          histr      intervals  rt.coord
13011101 3           0.1778
*          histr      compn.no.   interval
13011201 1           3
*          histr      source    interval
13011301 0           3
13011401 400. 4
*          histr      left vol  incr bcond sa code area/factor ht str no.
12711601 -501 0 4581 1 0.300 1
12711602 -501 0 4531 1 0.290 2
12711603 -501 0 4531 1 0.940 3
*          histr      s.type  s. mult  left heat right heat ht str no.
12711701 0 0 0 0 3
*          histr
*mod2.5*12711801 0.0.0.0.0.0.3
12711801 0. 10. 0. 0. 0. 1.3
*          histr
```

```

*hsr source interval
13741301 0. 3
13741401 400. 4
*hsr left vol incr bcond sa code area/factor ht str no.
13741501 374010000 0 1 0.50 1
*hsr right vol incr bcond sa code area/factor ht str no.
13741601 -501 0 4511 1 0.50 1
*hsr s_type s_mult left heat right heat ht str no.
13741701 0 0 0 0 1
*hsr
*mod2.5*1581901 0 0 0 0 0.001
13741801 0 10. 10. 0. 0. 0. 1.1
*hsr
*mod2.5*1581901 0 0 0 0 0.001
13741901 0 10. 10. 0. 0. 0. 1.1
*hsr
ht str no. 4011 hotleg $*
*hsr ht str m pts geom init lcoord refl b.vol axl incr
14011000 1 4 2 1 0.1627 0 0 0
*hsr mesh locn mesh fnt
14011100 0 1
*hsr intervals rt.coord
14011101 3 0.1778
*hsr compnx no. interval
14011201 1 3
*hsr source interval
14011301 0. 3
14011401 400. 4
*hsr left vol incr bcond sa code area/factor ht str no.
14011501 451010000 0 1 3.28 1
*hsr right vol incr bcond sa code area/factor ht str no.
14011601 -501 0 4511 1 3.28 1
*hsr s_type s_mult left heat right heat ht str no.
14011701 0 0 0 0 1
*hsr
*mod2.5*14011801 0 0 0 0 0.01
14011801 0 10. 10. 0. 0. 0. 1.1
*mod2.5*14011901 0 0 0 0 0.01
14011901 0 10. 10. 0. 0. 0. 1.1
*hsr
ht str no. 4291 14-incdeg $*
*hsr ht str m pts geom init lcoord refl b.vol axl incr
14291000 1 4 2 1 0.1627 0 0 0
*hsr mesh locn mesh fnt
14291100 0 1
*hsr intervals rt.coord
14291101 3 0.1778
*hsr
ht str no. 4581 14-incdeg $*
*hsr
*mod2.5*14291801 0 0 0 0 0.001
14291801 0 10. 10. 0. 0. 0. 1.1
*mod2.5*14291901 0 0 0 0 0.01
14291901 0 10. 10. 0. 0. 0. 1.1
*hsr
ht str no. 4581 14-incdeg $*
*hsr ht str m pts geom init lcoord refl b.vol axl incr
14381000 2 4 2 1 0.1627 0 0 0
*hsr mesh locn mesh fnt
14381100 0 1
*hsr intervals rt.coord
14381101 3 0.1778
*hsr compnx no. interval
14381201 1 3
*hsr left vol incr bcond sa code area/factor ht str no.
14381501 458010000 0 1 1 7.24 2
*hsr
*mod2.5*14581801 0 0 0 0 0.002
14581801 0. 10. 10. 0. 0. 0. 1.2
*hsr right vol no. ht str no.
14581601 -501 0 4511 1 7.24 2
*hsr s_type s_mult left heat right heat ht str no.
14581701 0 0 0 0 2
*hsr
*mod2.5*14581901 0 0 0 0 0.002
14581901 0. 10. 10. 0. 0. 0. 1.2
*hsr
ht str no. 4621 14-incdeg $*
*hsr ht str m pts geom init lcoord refl b.vol axl incr
14621000 2 4 2 1 0.1627 0 0 0
*hsr mesh locn mesh fnt
14621100 0 1
*hsr intervals rt.coord
14621101 3 0.1778
*hsr
ht str no. 4621 14-incdeg $*

```

```

*histr compno. interval
14621201 1 3
*histr source interval
14621301 0. 3
14621401 400. 4
*histr left vol incr bcond sa code area/factor ht str no.
14621501 462010000 0 1 1 1.2166 1
14621502 462020000 0 1 1 13.93439 2
*histr right vol incr bcond sa code area/factor ht str no.
14621601 .501 0 4511 1 1.2166 1
14621602 .501 0 4581 1 13.93439 2
*histr s.type s.mult left heat right heat ht str no.
14621701 0 0 0 0 2
*histr
*mod2.5*11581901 0 0 0 0 0.002
*mod2.5*11581901 0 0 0 0 0.002
14621801 0.10.10.0.0.0.1.2
*histr
*mod2.5*11581901 0 0 0 0 0.002
*mod2.5*11581901 0 0 0 0 0.002
14621901 0.10.10.0.0.0.1.2
*histr ht str no. 4711 8-in cdleg S
*histr ht str no. 471100 3 4 2 1 0.09925 0 0 0
*histr source interval
14711101 0. 3
*histr intervals rt.coord
14711101 3 0.1016
*histr compno. interval
14711201 1 3
*histr mesh locn mesh fint
14711301 0 0
*histr source interval
14711401 400. 4
*histr left vol incr bcond sa code area/factor ht str no.
14711501 471010000 0 1 1 0.300 1
14711502 471020000 0 1 1 0.510 2
14711503 471030000 0 1 1 0.980 3
*histr right vol incr bcond sa code area/factor ht str no.
14711601 .501 0 4581 1 0.300 1
14711602 .501 0 4531 1 0.510 2
14711603 .501 0 4531 1 0.980 3
*histr s.type s.mult left heat right heat ht str no.
14711701 0 0 0 0 3
*histr
*mod2.5*14711801 0 0 0 0 0.003
*mod2.5*14711901 0 0 0 0 0.003
14711801 0.10.10.0.0.0.1.3
*histr ht str no. 4741 14-in cdleg S

```

* heat structures in core region *

* ht str 5001 - core inlet pipe wall (lower cphi wall) *

* htstr ht str mps geom init lcoord refl bvol axl incr 15001000 1 4 2 1 0.2265 0 0 0

* htstr mesh locn mesh fnt 15001100 0 0 1

* htstr intervals rt.coord 15001101 3 0.2465

* htstr compnn no. interval 15001201 1 3

* htstr source interval 15001301 0. 3

* htstr 15001401 400. 4

* htstr left vol incr bcond sa code area/factor ht str no. 15001501 500010000 0 1 1 0.331 1

* htstr right vol incr bcond sa code area/factor ht str no. 15001601 -301 0 4581 1 0.331 1

* htstr s. type s. mult left heat right heat ht str no. 15001701 0 0 0 0 0 1

* htstr *mod2.5*150018010 0.0.0.0.0.1

* htstr 15001801 0.0 10. 10. 0. 0. 0. 1. 1

* htstr *mod2.5*15001901 0.0.0.0.0.1

* htstr 15001901 0.0 10. 10. 0. 0. 0. 1. 1

* ht str 5051 - control rod shroud in core inlet region *

* htstr ht str mps geom init lcoord refl bvol axl incr 15051000 1 4 2 1 0.6955 0 0 0

* htstr mesh locn mesh fnt 15051100 0 0 1

* htstr intervals rt.coord 15051101 3 0.102

* htstr compnn no. interval 15051201 2 3

* htstr left vol incr bcond sa code area/factor ht str no. 15051301 500010000 0 1 1 1.545 1

* htstr right vol incr bcond sa code area/factor ht str no. 15051401 400. 4

* htstr left vol incr bcond sa code area/factor ht str no. 15051501 500010000 0 1 1 1.545 1

* htstr right vol incr bcond sa code area/factor ht str no. 15051601 500010000 0 1 1 1.545 1

* htstr left vol incr bcond sa code area/factor ht str no. 15051701 0 0 0 0 0 1

* htstr right vol incr bcond sa code area/factor ht str no. 15051801 0.0 10. 10. 0. 0. 0. 1. 1

* htstr ht str mps geom init lcoord refl bvol axl incr 15051901 0.0 10. 10. 0. 0. 0. 1. 1

* htstr ht str mps geom init lcoord refl bvol axl incr 15052000 1 4 2 1 0.168 0 0 0

* htstr mesh locn mesh fnt 15052100 0 0 1

* htstr intervals rt.coord 15052101 3 0.175

* htstr compnn no. interval 15052201 2 3

* htstr source interval 15052301 0. 3

* htstr 15052401 400. 4

* htstr left vol incr bcond sa code area/factor ht str no. 15052501 505010000 0 1 1 1.545 1

* htstr right vol incr bcond sa code area/factor ht str no. 15052601 530010000 0 1 1 1.545 1

* htstr s. type s. mult left heat right heat ht str no. 15052701 0 0 0 0 0 1

* htstr *mod2.5*15052801 0.0.0.0.0.1

* htstr 15052801 0.0 10. 10. 0. 0. 0. 1. 1

* fuel region heat structures *

* ht str 5101 - lower core average fuel plates *

* htstr ht str mps geom init lcoord refl bvol axl incr 15101000 5 11 1 1 0. 0 0 0

* htstr mesh locn mesh fnt 15101100 0 0 1

* htstr intervals rt.coord 15101101 2 1.020e-5

* htstr 15101102 2 2.570e-4

* htstr 15101103 6 6.380e-4

* htstr compnn no. interval 15101201 4 2

* htstr 15101202 2 4

* htstr 15101203 5 10

* htstr source interval 15101301 0. 2

* htstr 15101302 0.00150 4

* htstr 15101303 0.25440 10

* htstr 15101401 400. 11

*histr left vol incr bcond sa code area/factor ht str no.
 *mod2.5*15101501 510010000 10000 1 0 4.31 5
 15101501 510010000 10000 102 0 4.31 5
 *histr right vol incr bcond sa code area/factor ht str no.
 15101601 0 0 0 4.31 5
 *histr s_type s_mult left heat right heat ht str no.
 15101701 1000 6.0236258d-02 3.01293898d-04 0.0000000d+00 1
 15101702 1000 5.4739700d-02 2.3380545d-04 0.0000000d+00 2
 15101703 1000 4.7963121d-02 2.3990931d-04 0.0000000d+00 3
 15101704 1000 4.4273650d-02 2.2145475d-04 0.0000000d+00 4
 15101705 1000 4.4198355d-02 2.2107813d-04 0.0000000d+00 5
 *histr mod2.5*15101801 0 0 0 0 0 0.5
 15101801 10 10 0 0 0 1.5
 *histr mesh locn mesh fnt
 *mod2.5*15101901 0 0 0 0 0.5
 15101901 10 10 0 0 0 1.5
 *histr ht str 5102 - lower core average channel inner side plate
 *histr ht str m pls geom init Lcond refl bvol axl incr
 15102000 5 4 2 1 0.095 0 0 0
 *histr mesh locn mesh fnt
 15102100 0 1
 *histr intervals rt.coord
 15102101 3 0.102
 *histr compnx.no. interval
 15102201 2 3
 *histr source interval
 15102301 1.
 15102401 400.4
 *histr left vol incr bcond sa code area/factor ht str no.
 15102501 562010000 10000 1 1 0.10098 5
 *histr right vol incr bcond sa code area/factor ht str no.
 15102601 510010000 10000 1 1 0.10098 5
 *histr s_type s_mult left heat right heat ht str no.
 15102701 1000 5.15517397d-04 1.3817393d-03 0.0000000d+00 1
 15102702 1000 4.684640d-04 1.2556537d-03 0.0000000d+00 2
 15102703 1000 4.1046984d-04 1.0920916d-03 0.0000000d+00 3
 15102704 1000 3.7885932d-04 1.0155776d-03 0.0000000d+00 4
 15102705 1000 3.7825086d-04 1.0138505d-03 0.0000000d+00 5
 *histr mod2.5*15102801 0 0 0 0 0.5
 15102801 10 10 0 0 0 1.5
 *histr mesh locn mesh fnt
 *mod2.5*15102901 0 0 0 0 0.5
 15102901 10 10 0 0 0 1.5
 *histr ht str m pls geom init Lcond refl bvol axl incr
 15103000 5 4 2 1 0.168 0 0 0
 *histr mesh locn mesh fnt

*histr intervals rt.coord
 15103101 3 0.175
 *histr compnx.no. interval
 15103201 2 3
 *histr source interval
 15103301 1.
 15103401 400.4
 *histr left vol incr bcond sa code area/factor ht str no.
 15103501 510010000 10000 1 1 0.10098 5
 *histr right vol incr bcond sa code area/factor ht str no.
 15103601 530020000 0 1 1 0.10098 5
 *histr s_type s_mult left heat right heat ht str no.
 15103701 1000 4.6136406d-04 0.0000000d+00 8.5681597d-04 1
 15103702 1000 4.1926459d-04 0.0000000d+00 7.786342d-04 2
 15103703 1000 3.6736113d-04 0.0000000d+00 6.822421d-04 3
 15103704 1000 3.3910259d-04 0.0000000d+00 6.2976195d-04 4
 15103705 1000 3.3852538d-04 0.0000000d+00 6.2869925d-04 5
 *histr mod2.5*15103801 0 0 0 0 0.5
 15103801 10 10 0 0 0 1.5
 *histr mesh locn mesh fnt
 *mod2.5*15103901 0 0 0 0 0.5
 15103901 10 10 0 0 0 1.5
 *histr ht str 5151 - lower core hot channel fuel plates
 *histr ht str m pls geom init Lcond refl b.vol ext.incr
 15151000 5 11 1 1 0 0 0 0
 *histr mesh locn mesh fnt
 15151100 0 1
 *histr intervals rt.coord
 15151101 2 1.02e-5
 15151102 2 2.5700e-4
 15151103 6 6.3800e-4
 *histr compnx.no. interval
 15151201 4 2
 15151202 2 4
 15151203 5 10
 *histr source interval
 15151301 0 2
 15151302 0.00150 4
 15151303 0.25440 10
 *histr mod2.5*15151401 400.11
 *histr left vol incr bcond sa code area/factor ht str no.
 *mod2.5*15151501 515010000 10000 1 0 0.017102 5
 15151501 515010000 10000 102 0 0.017102 5
 *histr right vol incr bcond sa code area/factor ht str no.
 15151601 0 0 0 0.017102 5
 *histr s_type s_mult left heat right heat ht str
 15151701 1000 5.3240879d-04 2.6630832d-06 0.0000000d+00 1
 15151702 1000 4.8831358d-04 2.4425220d-06 0.0000000d+00 2

*hstr left vol incr bcond sa code area/factor ht str no.
 15153501 515010000 10000 1 1 0.0004024 5
 *hstr right vol incr bcond sa code area/factor ht str no.
 15153601 530020000 0 1 1 0.0004024 5
 *hstr s. type s. mult left heat right heat ht str no.
 15153701 1000 4.0778476d-06 0.0000000d+00 7.5731456d-06 1
 15153702 1000 3.7401118d-06 0.0000000d+00 6.3459218d-06 2
 15153703 1000 3.3948707d-06 0.0000000d+00 6.3047598d-06 3
 15153704 1000 3.0646401d-06 0.0000000d+00 5.6914744d-06 4
 15153705 1000 2.6686204d-06 0.0000000d+00 4.8412378d-06 5
 *hstr
 *mod2.5*15151801 0 0 0 0 0 0.5
 15151801 0.10.10.0.0.1.5
 *hstr
 *mod2.5*15151901 0 0 0 0 0 0.5
 15151901 0.10.10.0.0.1.5
 *hstr ht str m pts geom init lcond refl bvol asl incr
 15152000 5 4 2 1 0.095 0 0 0 0
 *hstr mesh locn mesh fnt
 15152100 0 1
 *hstr intervals rt.coord
 15152101 3 0.02
 *hstr compnx.no. interval
 15152201 2 3
 *hstr source interval
 15152301 1 3
 15152401 400.4
 *hstr left vol incr bcond sa code area/factor ht str no.
 15152501 .562010000 10000 1 1 0.0004024 5
 *hstr right vol incr bcond sa code area/factor ht str no.
 15152601 .515010000 10000 1 1 0.0004024 5
 *hstr s. type s. mult left heat right heat ht str no.
 15152701 1000 4.5563705d-06 1.22121737d-05 0.0000000d+00 1
 15152702 1000 4.1790024d-06 1.1201253d-05 0.0000000d+00 2
 15152703 1000 3.7932484d-06 1.0167291d-05 0.0000000d+00 3
 15152704 1000 3.4242652d-06 9.1782843d-06 0.0000000d+00 4
 15152705 1000 2.9127228d-06 7.8071610d-06 0.0000000d+00 5
 *hstr
 *mod2.5*15152801 0 0 0 0 0 0.5
 15152801 0.10.10.0.0.1.5
 *hstr
 *mod2.5*15152901 0 0 0 0 0 0.5
 15152901 0.10.10.0.0.1.5
 *hstr ht str m pts geom init lcond refl bvol asl incr
 15153000 5 4 2 1 0.168 0 0 0
 *hstr mesh locn mesh fnt
 15153100 0 1
 *hstr intervals rt.coord
 15153101 3 0.175
 *hstr compnx.no. interval
 15153201 2 3
 *hstr source interval
 15153301 1 3
 *hstr
 *mod2.5*15154801 0 0 0 0 0 0.5
 15154801 0.10.10.0.0.1.5
 *hstr
 *mod2.5*15154901 0 0 0 0 0 0.5
 15154901 0.10.10.0.0.1.5

* ht str 5155 - lower core hot strips - 99% probability -TE*

*htstr ht str mps geom init lcoord refl b.vol adl.incr

15155000 511 1 1 0 0 0 0

*htstr mesh locn mesh fmt

15155100 0 1

*htstr intervals rt.coord

15155101 2 1.02-5

15155102 2 2.5700e-4

15155103 6 6.3800e-4

*htstr compnx.no. interval

15155201 4 2

15155202 2 4

15155203 5 10

*htstr source interval

15155301 0 2

15155302 0.00150 4

15155303 0.5075 10

15155401 400. 11

*htstr left vol incr bcond sa code area/factor ht str no.

*mod2.5*15161501 516010000 10000 1 0 0.00017102 5

15161501 516010000 10000 102 0 0.017102 5

*htstr right vol incr bcond sa code area/factor ht str no.

*htstr s.type s.mult left heat right heat ht str

15155701 1000 6.1159857e-06 0.0000000d+00 0.0000000d+00 1

15155702 1000 5.508759d-06 0.0000000d+00 0.0000000d+00 2

15155703 1000 5.1714013d-06 0.0000000d+00 0.0000000d+00 3

15155704 1000 4.5641685d-06 0.0000000d+00 0.0000000d+00 4

15155705 1000 3.0361642d-06 0.0000000d+00 0.0000000d+00 5

*htstr

*mod2.5*15155801 0 0 0 0.0 0.5

15155801 0 10. 10. 0. 0. 0. 1. 5

*htstr

*mod2.5*15155901 0 0 0 0.0 0.5

15155901 0 10. 10. 0. 0. 0. 1. 5

*htstr ht str mps geom init lcoord refl b.vol adl.incr

15161000 511 1 1 0 0 0 0

*htstr mesh locn mesh fmt

15161100 0 1

*htstr intervals rt.coord

15161101 2 1.02e-5

15161102 2 2.5700e-4

15161103 6 6.3800e-4

*htstr compnx.no. interval

15161201 4 2

15161202 2 4

15161203 5 10

*htstr source interval

htstr left vol incr bcond sa code area/factor ht str no.

*mod2.5*15161501 516010000 10000 1 0 0.00017102 5

15161501 516010000 10000 102 0 0.017102 5

*htstr right vol incr bcond sa code area/factor ht str no.

*htstr s.type s.mult left heat right heat ht str

15161701 1000 5.5174206d-04 2.7597883d-06 0.0000000d+00 1

15161702 1000 5.0604563d-04 2.5312163d-06 0.0000000d+00 2

15161703 1000 4.5933373d-04 2.2975651d-06 0.0000000d+00 3

15161704 1000 4.1465278d-04 1.0740740d-06 0.0000000d+00 4

15161705 1000 3.5270873d-04 1.7642328d-06 0.0000000d+00 5

*htstr

*mod2.5*15161801 0 0 0 0.0 0.5

15161801 0. 10. 10. 0. 0. 0. 1. 5

*htstr

*mod2.5*15161901 0 0 0 0.0 0.5

15161901 0. 10. 10. 0. 0. 0. 1. 5

*htstr

*mod2.5*15162000 5 4 2 1 0.095 0 0 0

*htstr ht str mps geom init lcond refl b.vol atl.incr

15162000 5 4 2 1 0.095 0 0 0

*htstr mesh locn mesh fmt

15162100 0 1

*htstr intervals rt.coord

15162101 3 0.102

*htstr compnx.no. interval

15162201 2 3

*htstr source interval

15162301 1. 3

15162401 400. 4

*htstr left vol incr bcond sa code area/factor ht str no.

15162501 562010000 10000 1 1 0.0004024 5

*htstr right vol incr bcond sa code area/factor ht str no.

15162601 516010000 10000 1 1 0.0004024 5

*htstr s.type s.mult left heat right heat ht str

15162701 1000 4.7218253d-06 1.2656217d-05 0.0000000d+00 1

15162702 1000 4.3307533d-06 1.1603002d-05 0.0000000d+00 2

15162703 1000 3.9309919d-06 1.0536494d-05 0.0000000d+00 3

15162704 1000 3.5486110d-06 9.5115738d-06 0.0000000d+00 4

15162705 1000 3.0184920d-06 8.0906611d-06 0.0000000d+00 5

*htstr

*mod2.5*15162801 0 0 0 0.0 0.5

15162801 0. 10. 10. 0. 0. 0. 1. 5

*htstr

*mod2.5*15162901 0 0 0 0.0 0.5

15162901 0. 10. 10. 0. 0. 0. 1. 5

```

* ht str 5163 - lower core hot channel outer side plate (99.9%)
* ht str m ps geom init lcoord refl b.vol axl.incr
  15163000 5 4 2 1   0.168   0   0   0
* htstr mesh locn
  15163100   0     1
* htstr intervals rt.coord
  15163101   3   0.175
* htstr compn.no. interval
  15163201   2   3
  15163301   1   4
  15163401 400. 4

* htstr left.vol incr bcond sa code area/factor ht str no.
  15163501 516010000 10000 1   0.0004024 5
* htstr right.vol incr bcond sa code area/factor ht str no.
  15163601 530020000 0   1   0.0004024 5

* htstr s.type s.mult left heat right heat ht str no.
  15163701 1000 4.235238d-06 0.00000000d+00 7.3841794-06 1
  15163702 1000 3.795238d-06 0.00000000d+00 7.19814794-06 2
  15163703 1000 3.51814804-06 0.00000000d+00 6.53370354-06 3
  15163704 1000 3.1759238d-06 0.00000000d+00 5.8981804-06 4
  15163705 1000 2.70148144-06 0.00000000d+00 5.01703694-06 5

* htstr
  *mod2.5*15163801 0.0 0.0 0.0 5
  15163801 0. 10. 10. 0. 0. 1.5
* htstr
  *mod2.5*15163901 0.0 0.0 0.0 5
  15163901 10. 10. 0. 0. 0. 1.5

* ht str m ps geom init lcoord refl b.vol axl.incr
  15164000 5 11 1 1   0   0   0
* htstr mesh locn
  15164100   0     1
* htstr intervals rt.coord
  15164101   2   1.02-5
  15164102   2   2.5700e-4
  15164103   6   6.3800e-4
* htstr compn.no. interval
  15164201   4   2
  15164202   2   4
  15164203   5   10
  15164301   0   11

* htstr source interval
  15164301   0   2
  15164302   0.0150   4
  15164303   0.25440  10
* htstr
  *mod2.5*15164501 516010000 10000 1   0   0.000171702 5
* htstr left.vol incr bcond sa code area/factor ht str no.
  15164501 516010000 10000 102 0   0.000171702 5

* htstr right.vol incr bcond sa code area/factor ht str no.
  15164501 0   0   0   0.000171702 5

* htstr s.type s.mult left heat right heat ht str no.
  15165701 1000 7.4610339d-06 0.00000000d+00 1
  15165702 1000 6.7202563d-06 0.00000000d+00 2
  15165703 1000 6.3087132d-06 0.00000000d+00 3
  15165704 1000 5.5679357d-06 0.00000000d+00 4
  15165705 1000 3.7038876d-06 0.00000000d+00 5

* htstr
  *mod2.5*15165801 0.0 0.0 0.0 5
  15165801 0. 10. 10. 0. 0. 1.5
* htstr
  *mod2.5*15165901 0.0 0.0 0.0 5
  15165901 0. 10. 10. 0. 0. 1.5

* ht str 5201 - control rod shroud in mid core region

```

```

*hsur h.srs mps geom init lcond refl b.vol axl.incr
15201000 1 4 2 1 0.095 0 0 0
*hsur mesh.loen mesh.fmt
15201100 0 1
*hsur intervals rt.coord
15201101 3 0.102
*hsur compn.no. interval
15201201 2 3
*hsur source interval
15201301 0. 3
15201401 400. 4
*hsur left.vol incr.bcond.sa.code area/factor ht.str.no.
15201501 562060000 0 1 1 0.050 1
*hsur right.vol.hcr bcond.sa.code area/factor ht.str.no.
15201601 520010000 0 1 1 0.050 1
*hsur s.type s.mult left heat right heat ht.str.no.
15201701 0 0 0 1
*hsur
*mod2.5*15201801 0 0 0 0.000 1
15201801 0.19 10. 10. 0. 0. 0. 1. 1
*hsur
*mod2.5*15201901 0 0 0 0.000 1
15201901 10. 10. 0. 0. 0. 1. 1
*hsur h.srs mps geom init lcond refl b.vol axl.incr
15202000 1 4 2 1 0.168 0 0 0
*hsur mesh.loen mesh.fmt
15202100 0 1
*hsur intervals rt.coord
15202101 3 0.175
*hsur compn.no. interval
15202201 2 3
*hsur source interval
15202301 0. 3
15202401 400. 4
*hsur left.vol incr.bcond.sa.code area/factor ht.str.no.
15202501 535010000 0 1 1 0.050 1
*hsur s.type s.mult left heat right heat ht.str.no.
15202701 0 0 0 1
*hsur right.vol incr.bcond.sa.code area/factor ht.str.no.
15202801 535010000 0 1 1 0.050 1
*hsur
*mod2.5*15202801 0 0 0 0.000 1
15202801 0.19 10. 10. 0. 0. 0. 1. 1
*hsur
*mod2.5*15202901 0 0 0 0.000 1
15202901 0.10 10. 0. 0. 0. 1. 1
*hsur h.srs mps geom init lcond refl b.vol axl.incr
15251000 5 4 2 1 0.095 0 0 0
*hsur mesh.loen mesh.fmt
15251100 0 1
*hsur intervals rt.coord
15251101 3 0.102
*hsur compn.no. interval
15251201 2 3
*hsur source interval
15251301 1.
15251401 400. 4
*hsur left.vol incr.bcond.sa.code area/factor ht.str.no.
15251501 562070000 10000 1 1 0.014 5
*hsur right.vol.incr.bcond.sa.code.area/factor ht.str.no.
15251601 525010000 0 1 1 0.014 2
15251602 525020000 0 1 1 0.014 5
*hsur s.type s.mult left heat right heat ht.str.no.
15251701 0 0. 0. 0. 5
*hsur
*mod2.5*15251801 0 0 0 0.005
15251801 0.19 10. 10. 0. 0. 0. 1. 5
*hsur
*mod2.5*15251901 0 0 0 0.005
15251901 0.10 10. 0. 0. 0. 1. 5
*hsur h.srs mps geom init lcond refl b.vol axl.incr
15351000 1 4 2 1 0.247 0 0 0
*hsur mesh.loen mesh.fmt
15351100 0 1
*hsur intervals rt.coord
15351101 3 0.2595
*hsur compn.no. interval
15351201 2 3
*hsur source interval
15351301 0.
15351401 400. 4
*hsur left.vol.incr.bcond.sa.code.area/factor ht.str.no.
15351501 535010000 0 1 1 0.050 1
*hsur right.vol.incr.bcond.sa.code.area/factor ht.str.no.
15351701 1000 0. 0. 0. 0.0245 1
*hsur
*mod2.5*15351801 0 0 0 0.000 1
15351801 0.10 10. 0. 0. 0. 0. 1. 1
*include all of the d2o heating in cphi annulus here
*hsur s.type s.mult left heat right heat ht.str.no.
15351701 1000 0. 0. 0. 0.0245 1
*hsur
*mod2.5*15351901 0 0 0 0.000 1
15351901 0.10 10. 0. 0. 0. 0. 1. 1

```

```

*histr
*mod2.5*15351901 0 0 0 0 0 0 1
*mod2.5*15351901 10. 10. 0. 0. 0. 1. 1
*histr left vol incr bcond sa code area/factor ht str no.
15351901.0. 10. 10. 0. 0. 0. 1. 1
*histr ht str m ps geom init lcond refl bvol axl incr
*histr ht str m ps - upper core average channel fuel plates
*histr ht str m ps geom init lcond refl bvol axl incr
*histr ht str m ps - upper core average channel fuel plates
*histr mesh locn mesh fmt
15401000 0 1
*histr intervals rt.coord
15401001 2 1.02-5
15401002 2 2.5700e-4
15401003 6 6.3500e-4
*histr compnx no. interval
15401201 4 2
15401202 2 4
15401203 5 10
*histr source interval
15401301 . 0.
15401302 0.00441 2
15401303 0.6485 10
*histr
15401401 400. 11
*histr left vol incr bcond sa code area/factor ht str no.
*mod2.5*15401501 540010000 10000 1 0 5.91 5
15401501 540010000 10000 102 0 5.91 5
*histr right vol incr bcond sa code area/factor ht str no.
15401601 0 0 0 5.91 5
*histr s. type s. mult left heat right heat ht str no.
15401701 1000 1.2215527d-01 3.2923931d-04 0.0000000d+00 1
15401702 1000 1.3883680d-01 3.7420025d-04 0.0000000d+00 2
15401703 1000 1.3588658d-01 3.6623249d-04 0.0000000d+00 3
15401704 1000 1.3070720d-01 3.5228891d-04 0.0000000d+00 4
15401705 1000 1.2152180d-01 3.2753193d-04 0.0000000d+00 5
*histr
*mod2.5*15401801 0 0 0 0 0 0 5
15401801 0. 10. 10. 0. 0. 0. 1. 5
*histr
*mod2.5*15401901 0 0 0 0 0 0 5
15401901 0. 10. 10. 0. 0. 0. 1. 5
*histr ht str m ps geom init lcond refl bvol axl incr
*histr ht str m ps - upper core average channel finer side plate
*histr ht str m ps geom init lcond refl bvol axl incr
*histr ht str m ps - upper core average channel finer side plate
*histr mesh locn mesh fmt
15402000 0 1
*histr intervals rt.coord
15402001 3 0.175
*histr compnx no. interval
15402201 2 3
*histr source interval
*histr
*mod2.5*15451801 0 0 0 0 0 0 5
15451801 0. 10. 10. 0. 0. 0. 1. 5
*histr left vol incr bcond sa code area/factor ht str no.
15451901 525010000 0 1 1 0.012 2
154520000 0 1 1 0.012 5
*histr right vol incr bcond sa code area/factor ht str no.
15452601 540010000 10000 1 1 0.012 5
*histr s. type s. mult left heat right heat ht str no.
15452701 1000 2.5628287d-04 5.686861608d-04 0.0000000d+00 1
15452702 1000 2.9128088d-04 6.4634559d-04 0.0000000d+00 2
15452703 1000 2.8507876d-04 6.3258349d-04 0.0000000d+00 3
15452704 1000 2.7422489d-04 6.0849902d-04 0.0000000d+00 4
15452705 1000 2.5495384d-04 5.6573698d-04 0.0000000d+00 5
*histr
*mod2.5*15402801 0 0 0 0 0 0 5
15402801 10. 10. 0. 0. 0. 1. 5
*histr
*mod2.5*15402901 0 0 0 0 0 0 5
15402901 10. 10. 0. 0. 0. 1. 5
*histr ht str m ps geom init lcond refl b.vol axl incr
15451000 511 1 1 0. 0 0 0
*histr mesh locn mesh fmt
15451100 0 1
*histr intervals rt.coord
15451101 2 1.02-5
15451102 2 2.5700e-4
15451103 6 6.3500e-4
*histr compnx no. interval
15451201 4 2
15451202 2 4
15451203 5 10
*histr
15451301 0 0
15451302 0.00441 4
15451303 0.6485 10
*histr source interval
15451301 0 2
15451302 0.00441 4
15451303 0.6485 10
*histr
*mod2.5*15451501 545010000 10000 1 0 0.013711 5
*histr s. type s. mult left heat right heat ht str no.
15451701 1000 3.9080633d-04 1.0533218d-06 0.0000000d+00 1
15451702 1000 4.2883073d-04 1.1558071d-06 0.0000000d+00 2
15451703 1000 3.9329552d-04 1.0654207d-06 0.0000000d+00 3
15451704 1000 3.6756919d-04 9.9069182d-07 0.0000000d+00 4
15451705 1000 3.319212d-04 8.946179d-07 0.0000000d+00 5
*histr
*mod2.5*15451801 0 0 0 0 0 0 5
15451801 0. 10. 10. 0. 0. 0. 1. 5

```

```

*histr      15454401 400.11
*mod2.5*15451901 0.0.0.0.0.5
15451901 0.10.10.0.0.0.1.5
* histr      left vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15454501 545010000 10000 1 0 0.00013711 5
15454501 545010000 10000 102 0 0.00013711 5
* histr      right vol incr bcond sa code area/factor ht str no.
15454601 0 0 0 0.00013711 5
* histr      left vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15454601 1000 6.6203063d-06 0.0000000d+00 1
15454701 1000 6.6203063d-06 0.0000000d+00 0.0000000d+00
15454702 1000 5.9933244d-06 0.0000000d+00 0.0000000d+00
15454703 1000 5.9933244d-06 0.0000000d+00 0.0000000d+00
15454704 1000 5.6233651d-06 0.0000000d+00 0.0000000d+00
15454705 1000 5.1246950d-06 0.0000000d+00 0.0000000d+00
* histr      source interval
15452201 2 3
* histr      compen no. interval
15452201 1
* histr      source interval
15452301 1, 3
*mod2.5*15454801 0.0.0.0.0.5
15454801 0.10.10.0.0.0.1.5
* histr      type s. mult
*mod2.5*15454901 0.0.0.0.0.5
15454901 0.10.10.0.0.0.1.5
* histr      left vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15455000 511 1 1 0 0 0
15455000 511 1 1 0 0 0
* histr      right vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15455100 0 1
15455100 0 1
* histr      mesh locn mesh fnt
*histr      mesh locn mesh fnt
* histr      left vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15455201 4 2
15455201 4 2
* histr      intervals rt.coord
*histr      intervals rt.coord
* histr      mesh locn mesh fnt
*histr      mesh locn mesh fnt
* histr      source interval
15455301 0
*histr      source interval
15455302 0.00441 4
*histr      source interval
15455303 0.6485 10
* histr      compnx no. interval
15455201 4
*histr      source interval
15455202 2
*histr      source interval
15455203 5 10
* histr      right vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15455301 0
15455301 0
* histr      left vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15455501 545010000 10000 1 0 0.00013711 5
15455501 545010000 10000 102 0 0.00013711 5
* histr      right vol incr bcond sa code area/factor ht str no.
15455601 0 0 0 0.00013711 5
* histr      type s. mult
*mod2.5*15455601 0.0.0.0.0.5
15455601 0.10.10.0.0.0.1.5
* histr      source interval
15455301 0
*histr      source interval
15455302 0.00441 4
*histr      source interval
15455303 0.6485 10
* histr      left vol incr bcond sa code area/factor ht str no.
*histr      *mod2.5*15455701 1000 5.366632d-06 0.0000000d+00 1
15455701 1000 4.952113d-06 0.0000000d+00 0.0000000d+00
15455702 1000 4.952113d-06 0.0000000d+00 0.0000000d+00
15455703 1000 4.581078d-06 0.0000000d+00 0.0000000d+00
15455704 1000 4.2185705d-06 0.0000000d+00 0.0000000d+00
15455705 1000 3.9972159d-06 0.0000000d+00 0.0000000d+00
* histr      source interval
15455301 0
*histr      source interval
15455302 0.00441 4
*histr      source interval
15455303 0.6485 10

```

*mod2.5*15455901 0.000.000.0.5
15455901 0.10. 0.0. 0.1.5

*htstr 5461 - upper core hot channel fuel plates (99.9%)

*htstr hi str m pfs geom int lcond refl b.vol axl.incr

15461000 5 11 1 0. 0. 0 0

*htstr mesh locn mesh fnt

15461100 0 1

*htstr intervals rt.coord

15461101 2 1.02-5

15461102 2 2.5700c-4

15461103 6 6.3800c-4

*htstr compnx.no. interval

15461201 4 2

15461202 2 4

15461203 5 10

*htstr source interval

15461301 0 2

15461302 0.00441 4

15461303 0.6485 10

15461401 400. 11

*htstr left vol incr b.cond sa code area/factor ht str.no.

*mod2.5*15461501 546010000 10000 1 0 0.013711 5

15461501 546010000 10000 102 0 0.013711 5

*htstr right vol incr b.cond sa code area/factor ht str.no.

15461601 0 0 0 0.013711 5

*htstr s. type s. mult left heat right heat ht str.no.

*mod2.5*15461701 4.0499763d-04 1.0915709d-06 0.0000000d+0-0 1

15461702 1000 4.4440280d-04 1.1977778d-06 0.0000000d+0-0 2

15461703 1000 4.0964963d-04 1.041092d-06 0.0000000d+0-0 3

15461704 1000 3.8091669d-04 1.0266667d-06 0.0000000d+0-0 4

15461705 1000 3.4397434d-04 9.2709772d-07 0.0000000d+0-0 5

*htstr

*mod2.5*15461801 0.000.000.0.5

15461801 0.10. 0.0. 0.1.5

*htstr

*mod2.5*15461901 0.000.000.0.5

15461901 0.10. 0.0. 0.1.5

*htstr hi str m pfs geom int lcond refl b.vol axl.incr

15462000 5 4 2 1 0.168 0 0 0

*htstr mesh locn mesh fnt

15462100 0 1

*htstr intervals rt.coord

15462101 3 0.175

*htstr compnx.no. interval

15462201 2 3

*htstr source interval

15462301 1. 3

15462401 400. 4

*htstr left vol incr b.cond sa code area/factor ht str.no.

15462501 525010000 0 1 1 0.000235 2

15462502 525020000 0 1 1 0.000235 5

*htstr right vol incr b.cond sa code area/factor ht str.no.

15462601 546010000 10000 1 1 0.000235 5

*htstr s. type s. mult left heat right heat ht str.no.

15462701 1000 8.4968871d-07 1.8834406d-06 0.0000000d+0-0 1

15462702 1000 9.3236113d-07 2.068889d-06 0.0000000d+0-0 2

15462703 1000 8.5944865d-07 1.9070577d-06 0.0000000d+0-0 3

15462704 1000 7.5916656d-07 1.7733334d-06 0.0000000d+0-0 4

15462705 1000 7.2166129d-07 1.6013506d-06 0.0000000d+0-0 5

*htstr

*mod2.5*15462801 0.000.000.0.5

15462801 10. 10. 0.0. 0.1.5

*htstr

*mod2.5*15462901 0.000.000.0.5

15462901 0.10. 0.0. 0.1.5

*htstr 5464 - upper core hot stripe - 99.9% probability - CHF

*htstr

*htstr hi str m pfs geom int lcond refl b.vol axl.incr

15464000 5 11 1 0. 0 0 0

*htstr mesh locn mesh fnt

15464100 0 1

*htstr intervals rt.coord

15464101 2 1.02-5

15464102 2 2.5700c-4

15464103 6 6.3800c-4

*htstr compnx.no. interval

15464201 4 2

15464202 2 4

15464203 5 10

*htstr source interval

15464301 0. 2

15464302 0.00441 4

15464303 0.6485 10

15464401 400. 11

*htstr

*mod2.5*15464501 546010000 10000 1 0 0.0013711 5

15464501 546010000 10000 102 0 0.0013711 5

*htstr right vol incr b.cond sa code area/factor ht str.no.

*mod2.5*15464601 1000 8.0931850d-06 0.0000000d+0-0 1

15464601 1000 8.0931850d-06 0.0000000d+0-0 2

15464703 1000 7.3267128d-06 0.0000000d+0-0 3

15464704 1000 6.3744465d-06 0.0000000d+0-0 4

15464705 1000 6.2650773d-06 0.0000000d+0-0 5

*htstr

*mod2.5*15464801 0.000.000.0.5

15464801 10. 10. 0.0. 0.1.5

*htstr

*mod2.5*15464901 0.000.000.0.5

15464901 0.10.10.0.0.0.1.5
 •
 • ht str 5465 - upper core hot stripe - 99.9% probability - FE
 •
 *htstr hi str m ps geom int lcond refl b.vol axl.incr
 15465000 511 1 1 0. 0 0 0
 •
 *htstr mesh locn mesh fmt
 15465100 0 1
 •
 *htstr intervals rt.coord
 15465101 2 1.025
 15465102 2 2.3700e-4
 15465103 6 6.3800e-4
 •
 *htstr compan.no. interval
 15465201 4 2
 15465202 2 4
 15465203 5 10
 •
 *htstr source interval
 15465301 0. 2
 15465302 0.00441 4
 15465303 0.6485 10
 •
 15465401 400. 11
 •
 *htstr left vol incr b.cond sa code area/factor ht str no.
 *mod2.5*15465501 546010000 10000 1. 0 0.00013711 5
 15465501 546010000 10000 102 0 0.00013711 5
 •
 *htstr right vol incr bcond sa code area/factor ht str no.
 15465601 0 0 0 0.00013711 5
 •
 *htstr s. type s. mult left heat right heat ht str no.
 15465701 1000 6.53925606d-06 0.00000000d+00 1
 15465702 1000 6.042384d-06 0.00000000d+00 2
 15465703 1000 5.5883653d-06 0.00000000d+00 3
 15465704 1000 5.1465329d-06 0.00000000d+00 4
 15465705 1000 4.8762972d-06 0.00000000d+00 5
 •
 *htstr
 *mod2.5*15465801 0.0 0.0 0.5
 15465801 0.10.10.0.0.0.1.5
 •
 *htstr
 *mod2.5*15465901 0.0 0.0 0.0 0.5
 15465901 0.10.10.0.0.0.1.5
 •
 *htstr mesh locn mesh fmt
 15501100 0 1
 •
 *htstr intervals rt.coord
 15501101 3 0.253
 •
 *htstr compan.no. interval
 15501201 2 3
 •
 *htstr source interval
 15501301 1. 3
 15501401 400. 4
 •
 *htstr left vol incr bcond sa code area/factor ht str no.
 15501501 550200000 10000 1 1 0.1014 5
 •
 *htstr right vol incr b.cond sa code area/factor ht str no.
 15501601 575010000 0 1 1 0.1014 10
 •
 *htstr s. type s. mult left heat right heat ht str no.
 15501701 10775 0.626 0.0 0.0 1
 15501702 10774 0.626 0.0 0.0 2
 15501703 10773 0.626 0.0 0.0 3
 15501704 10772 0.626 0.0 0.0 4
 15501705 10771 0.626 0.0 0.0 5
 15501706 10735 0.789 0.0 0.0 6
 15501707 10734 0.789 0.0 0.0 7
 15501708 10733 0.789 0.0 0.0 8
 15501709 10732 0.789 0.0 0.0 9
 15501710 10731 0.789 0.0 0.0 10
 •
 *htstr
 *mod2.5*15501801 0.0 0.0 0.0 0.0 10
 15501801 0.10.10.0.0.0.1.10
 •
 *htstr
 *mod2.5*15501901 0.0 0.0 0.0 0.0 10
 15501901 0.10.10.0.0.0.1.10
 •
 • ht str 5502 - inner cplt in lower core region
 •
 *htstr hi str m ps geom int lcond refl b.vol axl.incr
 15502000 5 4 2 1 0.235 0 0 0
 •
 *htstr mesh locn mesh fmt
 15502100 0 1
 •
 *htstr intervals rt.coord
 15502101 3 0.240
 •
 *htstr compan.no. interval
 15502201 2 3
 •
 *htstr source interval
 15502301 1.
 15502401 400. 4
 •
 *htstr left vol incr bcond sa code area/factor ht str no.
 15502501 550200000 10000 1 1 0.1014 5
 •
 *htstr right vol incr bcond sa code area/factor ht str no.
 15502601 550200000 10000 1 1 0.1014 5
 •
 *htstr s. type s. mult left heat right heat ht str no.
 15502701 10775 0.374 0. 0. 1
 15502702 10774 0.374 0. 0. 2
 15502703 10773 0.374 0. 0. 3
 15502704 10772 0.374 0. 0. 4
 15502705 10771 0.374 0. 0. 5
 •
 *htstr
 *mod2.5*15502801 0.0 0.0 0.0 0.5
 15502801 0.10.10.0.0.0.1.5
 •
 *htstr
 *mod2.5*15502901 0.0 0.0 0.0 0.5
 15502901 0.10.10.0.0.0.1.5
 •
 • ht str 5503 - inner cplt in upper core region

*htstr ht str m ps geom init Lcond refl b.vol ext.incr
 15503000 5 4 2 1 0.235 0 0 0

*htstr mesh locn mesh fmtn
 15503100 0 1

*htstr intervals rt.coord
 15503101 3 0.242

*htstr compnn.no. interval
 15503201 2 3

*htstr source interval
 15503301 1. 3

*htstr 15503401 400.4

*htstr left vol incr b.cond sa code area/factor ht str no.
 15503501 540010000 10000 1 1 0.1014 5

*htstr right vol incr b.cond sa code area/factor ht str no.
 15503601 250080000 10000 1 1 0.1014 5

*htstr s.type s.mult left heat right heat ht str no.
 15503701 10735 0.211 0. 0. 1
 15503702 10734 0.211 0. 0. 2
 15503703 10733 0.211 0. 0. 3
 15503704 10732 0.211 0. 0. 4
 15503705 10731 0.211 0. 0. 5

*htstr *mod2.5*15503801 0 0 0 0 0.5
 15503801 0. 10. 0. 0. 0. 1.5

*htstr *mod2.5*15503901 0 0 0 0 0.5
 15503901 0. 10. 0. 0. 0. 1.5

*htstr ht str m ps geom init Lcond refl b.vol ext.incr
 15551000 2 4 2 1 0.168 0 0 0

*htstr mesh locn mesh fmtn
 15551100 0 1

*htstr intervals rt.coord
 15551101 3 0.173

*htstr compnn.no. interval
 15551201 2 3

*htstr left vol incr b.cond sa code area/factor ht str no.
 15551301 525010000 0 1 1 0.7715 2

*htstr right vol incr b.cond sa code area/factor ht str no.
 15551601 555010000 2000000 1 1 0.7715 2

*htstr s.type s.mult left heat right heat ht str no.
 15551701 0 0 0 0 2

*htstr *mod2.5*15551801 0 0 0 0 0.2
 15551801 0. 10. 0. 0. 0. 1.2

*htstr ht str m ps geom init Lcond refl b.vol ext.incr
 15552000 2 4 2 1 0.235 0 0 0

*htstr ht str m ps geom init Lcond refl b.vol ext.incr
 15552100 2 4 2 1 0.235 0 0 0

*htstr mesh locn mesh fmtn
 15552100 0 1

*htstr intervals rt.coord
 15552101 3 0.240

*htstr compnn.no. interval
 15552201 2 3

*htstr source interval
 15552301 0. 3

*htstr left vol incr b.cond sa code area/factor ht str no.
 15552501 555010000 2000000 1 1 0.7715 2

*htstr right vol incr b.cond sa code area/factor ht str no.
 15552601 550130000 10000 1 1 0.7715 2

*htstr s.type s.mult left heat right heat ht str no.
 15552701 0 0 0 0 2

*htstr *mod2.5*15552801 0 0 0 0 0.2
 15552801 0. 10. 0. 0. 0. 1.2

*htstr *mod2.5*15552901 0 0 0 0 0.2
 15552901 0. 10. 0. 0. 0. 1.2

\$ ht str no. 5611 control rod aluminum (8-35 deg sectors)

*htstr ht str m ps geom init Lcond refl b.vol ext.incr
 15611000 11 4 2 1 0.022 0 0 0

*htstr mesh locn mesh fmtn
 15611100 0 .1

*htstr intervals rt.coord
 15611101 3 0.0285

*htstr compnn.no. interval
 15611201 2 3

*htstr source interval
 15611301 1. 3

*htstr left vol incr b.cond sa code area/factor ht str no.
 15611501 561010000 10000 1 1 0.23660 5

*htstr right vol incr b.vol ext.incr ht str no.
 15611502 561050000 0 1 1 0.11667 6

*htstr right vol incr b.vol ext.incr ht str no.
 15611503 561070000 10000 1 1 0.23660 11

*htstr left vol incr b.vol ext.incr ht str no.
 15611601 553010000 10000 1 1 0.23660 5

*htstr left vol incr b.vol ext.incr ht str no.
 15611602 553060000 0 1 1 0.11667 6

• 15611603 563070000 10000 1 1 0.23660 11

• *hsur s.type s.mult left heat right heat ht str no.

• 15611701 10641 0.166 0. 0. 0. 1

• 15611702 10641 0.205 0. 0. 0. 2

• 15611703 10641 0.211 0. 0. 0. 3

• 15611704 10641 0.210 0. 0. 0. 4

• 15611705 10641 0.208 0. 0. 0. 5

• 15611706 10641 0. 0. 0. 0. 0. 6

• 15611707 10641 0. 0. 0. 0. 0. 7

• 15611708 10641 0. 0. 0. 0. 0. 8

• 15611709 10641 0. 0. 0. 0. 0. 9

• 15611710 10641 0. 0. 0. 0. 0. 10

• 15611711 10641 0. 0. 0. 0. 0. 11

• \$ ht str no. 5631 control rod hafnium structure (8-35 degree sectors)

• *hsur chf flag hyd diam equiv diam ch. len ht str no.

• *mod2.5*15611801 0 0 0 0 0 0 11

• 15611801 0.10.0.0.0.0.1.11

• *

• \$ ht str no. 5631 control rod hafnium/aluminum (8-10 degree sectors)

• *hsur chf flag hyd diam equiv diam ch. len ht str no.

• *mod2.5*15611901 0 0 0 0 0 0 11

• 15611901 0.10.0.0.0.0.1.11

• *

• \$ ht str no. 5621 control rod hafnium/aluminum (8-10 degree sectors)

• *hsur ht str no m ps geom init Lcond refl bvol adl incr

• 15621000 11 10 2 1 0.022 0 0 0

• *

• *hsur mesh locn mesh fmt

• 15621100 0 0 1

• *

• *hsur intervals rt. coord

• 15621101 3 0.285

• 15621102 2 0.03125

• 15621103 1 0.0315

• 15621104 3 0.0335

• *

• *hsur compn no. interval

• 15621201 2 5

• 15621202 6 6

• 15621203 3 9

• *

• *hsur source interval

• 15621301 0.2 5

• 15621302 0. 6

• 15621303 0.8 9

• *

• *hsur right vol incr b.cond sa code area/factor ht str no.

• 15621401 400. 10

• *

• *hsur left vol incr b.cond sa code area/factor ht str no.

• 15621501 562010000 10000 1 1 0.0676 5

• 15621502 562065000 0 1 0.0333 6

• 15621503 562070000 10000 1 1 0.0676 11

• *

• *hsur s.type s.mult left heat right heat ht str no.

• 15621701 10642 0.166 0. 0. 1

• 15621702 10642 0.205 0. 0. 2

• 15621703 10642 0.211 0. 0. 3

• 15621704 10642 0.210 0. 0. 4

• 15621705 10642 0.208 0. 0. 5

• 15621706 0 0 0 0 0 6

• 15621707 0 0 0 0. 0. 7

• 15621708 0 0 0 0. 0. 8

• \$ ht str no. 5631 control rod hafnium structure (8-35 degree sectors)

• *hsur ht str no m ps geom init Lcond refl bvol adl incr

• 15631000 11 4 2 1 0.03125 0 0 0

• *

• *hsur mesh locn mesh fmt

• 15631100 0 1

• *

• *hsur intervals rt. coord

• 15631101 3 0.0355

• *

• *hsur compn no. interval

• 15631201 3 3

• *

• *hsur left vol incr b.cond sa code area/factor ht str no.

• 15631301 1. 1.

• 15631401 400. 4

• *

• *hsur right vol incr b.cond sa code area/factor ht str no.

• 15631601 562010000 10000 1 1 0.23660 5

• 15631602 562050000 0 1 1 0.11667 6

• 15631603 562070000 10000 1 1 0.23660 11

• *

• *hsur s.type s.mult left heat right heat ht str no.

• 15631701 10643 0.166 0. 0. 1

• 15631702 10643 0.205 0. 0. 2

• 15631703 10643 0.211 0. 0. 3

• 15631704 10643 0.210 0. 0. 4

• 15631705 10643 0.208 0. 0. 5

• 15631706 0 0 0 0 0 6

• 15631707 0 0 0 0. 0. 7

• 15631708 0 0 0 0. 0. 8

• 15631709 0 0 0 0. 0. 9

• 15631710 0 0 0 0. 0. 10

• 15631711 0 0 0 0. 0. 11

• *

• *hsur chf flag hyd diam equiv diam ch. len ht str no.

• *mod2.5*15631801 0 0 0 0 0 1.11

• 15631801 0.10.0.0.0.1.11

• \$ ht str no. 5612 structure for gamma heating of inner flow

• *hsur ht str no m ps geom init Lcond refl bvol adl incr

• 156212000 11 2 1 1 0. 0. 0 0 0

• *

• *hsur mesh locn mesh fmt

15612100 0 1
 • *hsnr intervals rt.coord
 15612101 1 0.001
 • *hsnr compn no. interval
 15612201 2 1
 • *hsnr source interval
 15612301 1 1
 15612401 400.2
 • *hsnr left vol incr bcond sa code area/factor ht str no.
 15612501 561010000 10000 1 0 0.01 11
 • *hsnr right vol incr bcond sa code area/factor ht str no.
 15612601 0 0 0 0.01 11
 •
 • *hsnr s.type s.mult left heat right heat ht str no.
 15612701 10613 0 .166 0 1
 15612702 10613 0 .205 0 2
 15612703 10613 0 .211 0 3
 15612704 10613 0 .210 0 4
 15612705 10613 0 .208 0 5
 15612706 0 0 .166 0 6
 15612707 10640 0 .205 0 7
 15612708 10640 0 .211 0 8
 15612709 10640 0 .210 0 9
 15612710 10640 0 .208 0 10
 15612711 10640 0 .208 0 11
 • *hsnr chflag hyd diam equiv diam ch.len ht str no.
 *mod2.5*15622801 0 0 0 0 0 0 11
 15622709 10673 0 1 0 9
 15622710 10672 0 1 0 10
 15622711 10671 0 1 0 11
 • *hsnr chflag hyd diam equiv diam ch.len ht str no.
 *mod2.5*15622901 0 0 0 0 0 0 11
 15622801 0 10.10.0.0.0.1.11
 • *hsnr chflag hyd diam equiv diam ch.len ht str no.
 *mod2.5*15622901 0 0 0 0 0 0 11
 15622901 0 10.10.0.0.0.1.11
 • *hsnr ht str m/pis geom init Lcond refl b.vol adr.incr
 15631000 1 4.2 1 0.28019 0 0 0
 • *hsnr mesh locn mesh fnt
 15631100 0 1
 • *hsnr intervals rt.coord
 15631101 3 0.3048
 • *hsnr compn no. interval
 15631201 1 3
 • *hsnr source interval
 15631301 0 3
 • *hsnr left vol incr bcond sa code area/factor ht str no.
 15631501 565010000 0 1 1 0.918 1
 • *hsnr right vol incr bcond sa code area/factor ht str no.
 15631601 0 0 1 0.918 1
 • *hsnr s.type s.mult left heat right heat ht str no.
 15631701 0 0 0 0 1
 • *hsnr ht str m/pis geom init Lcond refl b.vol adr.incr
 *mod2.5*15651801 0 0 0 0 0 0 1
 15651801 0 10.10.0.0.0.1.1
 • *hsnr intervals rt.coord
 *mod2.5*15651901 0 0 0 0 0 0 1
 15651901 0 10.10.0.0.0.1.1
 • *hsnr ht str no. 5401 holpipe \$
 16401000 6.4.2.1 0.28019 0 0 0
 • *hsnr mesh locn mesh fnt
 16401100 0 1
 • *hsnr intervals rt.coord
 16401101 3 0.3048
 • *hsnr compn no. interval
 16401201 1 3
 • *hsnr source interval
 16401301 0 3
 16401401 400.4
 • *hsnr left vol incr bcond sa code area/factor ht str no.
 16401501 64010000 10000 1 1 0.91463 3
 16401502 641010000 10000 1 1 2.31667 6

16501401 400.4

*hsir right vol incr bcond sa code area/factor ht str no.
16401601 0 -501 0 4521 1 0.91463 3
16401602 -501 0 4581 1 2.33657 6

*hsir s. type s. mult left heat right heat ht str no.
16401701 0 0 0 0 0 0 6

*hsir *mod2.5*6401801 0 0 0 0 0 0 6
16401801 10. 10. 0. 0. 0. 1. 6

*hsir *mod2.5*6401901 0 0 0 0 0 0 6
16401901 10. 10. 0. 0. 0. 1. 6

hit str no. 6451 hotpipe \$

*hsir hsirs n pfs geom init Lcond refl b.vol axd.incr
16431000 2 4 2 1 0.28019 0 0 0

*hsir mesh locn mesh fnt
16431100 0 1

*hsir intervals rt.coord
16431101 3 0.3048

*hsir compnx.no. interval
16431201 1 3

*hsir source interval
16431301 0. 3

16451401 400.4

*hsir left vol incr bcond sa code area/factor ht str no.
16451501 645010000 0 1 1 4.88 1
16451502 645020000 0 1 1 3.35 2

*hsir right vol incr bcond sa code area/factor ht str no.
16431601 -501 0 4521 1 4.88 1
16431602 -501 0 4521 1 3.35 2

*hsir s. type s. mult left heat right heat ht str no.
16431701 0 0 0 0 0 2

*mod2.5*6451801 0 0 0 0 0 2
16451801 10. 10. 0. 0. 0. 1. 2

*mod2.5*6451901 0 0 0 0 0 0 2
16451901 10. 10. 0. 0. 0. 1. 2

hit str no. 6501 hothead \$

*hsir hsirs n pfs geom init Lcond refl b.vol axd.incr
16501000 4 4 2 1 0.28019 0 0 0

*hsir mesh locn mesh fnt
16501100 0 1

*hsir intervals rt.coord
16501101 3 0.3048

*hsir compnx.no. interval
16501201 1 3

*hsir source interval
16501301 0. 3

16501501 650010000 0 1 1 1.68 1
16501502 650020000 0 1 1 3.51 2
16501503 650030000 0 1 1 1.22 3
16501504 650040000 0 1 1 1.83 4

*hsir right vol incr bcond sa code area/factor ht str no.
16501601 -501 0 4521 1 1.68 1
16501602 -501 0 4521 1 3.51 2
16501603 -501 0 4521 1 1.22 3
16501604 -501 0 4521 1 1.83 4

*hsir s. type s. mult left heat right heat ht str no.
16501701 0 0 0 0 0 4

*hsir *mod2.5*6501801 0 0 0 0 0 4
16501801 10. 10. 0. 0. 0. 1. 4
*mod2.5*6501901 0 0 0 0 0 4
16501901 10. 10. 0. 0. 0. 1. 4

GENERAL DATA TABLES

saturation table (pressure as a fn. of temperature)

20203300 react-t

20203303 40. 6.549e-3
20203305 50. 11.121e3
20203306 60. 18.200e3
20203307 70. 28.80e3
20203308 80. 44.23e3
20203309 90. 66.07e3
20203310 100. 96.725e3
20203311 110. 137.06e3
20203312 120. 191.1e3
20203313 130. 261.5e3
20203314 140. 351.7e3
20203315 150. 465.3e3
20203316 160. 606.7e3
20203317 170. 780.3e3
20203318 180. 991.2e3
20203319 190. 1244.5e3
20203320 200. 1546.0e3

primary coolant pump post-cavitation head degradation factor

20203900 react-t

20203901 0.0 0.0
20203902 0.7 0.0
20203903 0.8 0.95
20203904 1.0 1.0

main circulation pump homologous curve: hvn

20204100 react-t

20204101 0. -0.35
20204102 0.425 0
20204103 0.567 0.142
20204104 0.637 0.239
20204105 0.728 0.391
20204106 0.850 0.644
20204107 1. 1.

* main circulation pump homologous curve: invn inverse

20204200 reac-t		
20204201	-0.35	0.
20204202	0.	0.425
20204203	0.142	0.567
20204204	0.239	0.637
20204205	0.391	0.728
20204206	0.644	0.850
20204207	1.	1.

- * main circulation pump speed vs. frictional torque
- * $T_f = 150 + 10^n \cdot \tau^2$

\$

20204300 reac-t

20204301.000	0.100	150.1	.200	150.4	300	150.9	
20204302.400	151.6	500	132.5	.600	153.6	700	154.9
20204303.800	156.4	900	138.1	1.0	160.		

* main circulation pump

- * relative speed vs. pony motor torque (N·m)
- * pony motor locked-rotor torque and the main motor rated torque constant.

* the HFIR data have been normalized keeping the ratio between the

* pony motor locked-rotor torque and the main motor rated torque constant.

20204400 reac-t

20204401.00000	2408.	
20204402	0.0731	1035.4
20204403	0.1134	613.1
20204404	0.1537	382.1
20204405	0.2142	203.9
20204406	0.2681	126.8
20204407	0.4032	0.0
20204408	1.00000	0.0

* table no. 135 - mep coastdown

\$

20213500 reac-t 635

* table no. 135 - mep coastdown

* 20213501 -1, 1.

20213502	0.	1.
20213503	0.001	0.9995
20213504	0.005	0.9975
20213505	0.1	0.9529
20213506	0.2	0.9100
20213507	0.5	0.8021
20213508	1.	0.6704
20213509	2.	0.3064
20213510	3.	0.4991
20213511	6.	0.2644
20213512	9.	0.2010
20213513	10.	0.1874
20213514	15.	0.1457
20213515	20.	0.1256
20213516	50.	0.1012
20213517	100.	0.1000
20213518	1.e6	0.1000

* 20223500 reac-t 1635

* 20223501 -1, 1.

* 20223502 0.

* 1.

* 20223503 0.001

* 0.9995

* 20223504 0.005

* 0.9975

* 20223505 0.1

* 0.9529

* 20223506 0.2

* 0.9100

* 20223507 0.5

* 0.8021

* 20223508 1.

* 0.6704

* 20223509 2.

* 0.3064

* 20223510 3.

* 0.4991

* 20223511 6.

* 0.2644

* 20223512 9.

* 0.2010

* 20223513 10.

* 0.1874

* 20223514 15.

* 0.1457

* 20223515 20.

* 0.1256

* 20223516 50.

* 0.1012

* 20223517 100.

* 0.1000

* 20223518 1.e6

* 0.1000

* 20233500 reac-t 635

* 20233501 -1, 1.

* 20233502 0.

* 1.

* 20233503 0.001

* 0.9995

* 20233504 0.005

* 0.9975

* 20233505 0.1

* 0.9529

* 20233506 0.2

* 0.9100

* 20233507 0.5

* 0.8021

* 20233508 1.

* 0.6704

* 20233509 2.

* 0.3064

* 20233510 3.

* 0.4991

* 20233511 6.

* 0.2644

* 20233512 9.

* 0.2010

* 20233513 10.

* 0.1874

* 20233514 15.

* 0.1457

* 20233515 20.

* 0.1256

* 20233516 50.

* 0.1012

* 20233517 100.

* 0.1000

* 20233518 1.e6

* 0.1000

* 20233500 reac-t 1635

* 20233501 -1, 1.

* 20233502 0.

* 1.

* 20233503 0.001

* 0.9995

* 20233504 0.005

* 0.9975

* 20233505 0.1

* 0.9529

* 20233506 0.2

* 0.9100

* 20233507 0.5

* 0.8021

* 20233508 1.

* 0.6704

* 20233509 2.

* 0.3064

* 20233510 3.

* 0.4991

* 20233511 6.

* 0.2644

* 20233512 9.

* 0.2010

* 20233513 10.

* 0.1874

* 20233514 15.

* 0.1457

* 20233515 20.

* 0.1256

* 20233516 50.

* 0.1012

* 20233517 100.

* 0.1000

* 20233518 1.e6

* 0.1000

* 20233500 reac-t 1635

* 20233501 -1, 1.

* 20233502 0.

* 1.

* 20233503 0.001

* 0.9995

* 20233504 0.005

* 0.9975

* 20233505 0.1

* 0.9529

* 20233506 0.2

* 0.9100

* 20233507 0.5

* 0.8021

* 20233508 1.

* 0.6704

* 20233509 2.

* 0.3064

* 20233510 3.

* 0.4991

* 20233511 6.

* 0.2644

* 20233512 9.

* 0.2010

* 20233513 10.

* 0.1874

* 20233514 15.

* 0.1457

* 20233515 20.

* 0.1256

* 20233516 50.

* 0.1012

* 20233517 100.

* 0.1000

* 20233518 1.e6

* 0.1000

* 20233500 reac-t 1635

* 20233501 -1, 1.

* 20233502 0.

* 1.

* 20233503 0.001

* 0.9995

* 20233504 0.005

* 0.9975

* 20233505 0.1

* 0.9529

* 20233506 0.2

* 0.9100

* 20233507 0.5

* 0.8021

* 20233508 1.

* 0.6704

* 20233509 2.

* 0.3064

* 20233510 3.

* 0.4991

* 20233511 6.

* 0.2644

* 20233512 9.

* 0.2010

* 20233513 10.

* 0.1874

* 20233514 15.

* 0.1457

* 20233515 20.

* 0.1256

* 20233516 50.

* 0.1012

* 20233517 100.

* 0.1000

* 20233518 1.e6

* 0.1000

* 20233500 reac-t 1635

* 20233501 -1, 1.

* 20233502 0.

* 1.

* 20233503 0.001

* 0.9995

* 20233504 0.005

* 0.9975

* 20233505 0.1

* 0.9529

* 20233506 0.2

* 0.9100

* 20233507 0.5

* 0.8021

* 20233508 1.

* 0.6704

* 20233509 2.

* 0.3064

* 20233510 3.

* 0.4991

•	table no. 531 - htc from outside of 8-in. horizontal pipe assumes pool temperature of 311.15 K	\$
•	20252102 350. 1186. 360. 1301. 370. 1423. 20252103 380. 1579. 390. 1713. 400. 1829. 20252104 410. 1926. 420. 2006. 430. 2125. 20252105 440. 2242. 450. 2345. 460. 2435.	*
•	20253100 htc-temp 20253101 320. 652. 330. 893. 340. 1073. 20253102 350. 1218. 360. 1334. 370. 1458. 20253103 380. 1616. 390. 1752. 400. 1868. 20253104 410. 1957. 420. 2048. 430. 2168. 20253105 440. 2286. 450. 2390. 460. 2482.	*
•	table no. 581 - htc from vertical piping - independent of length assumes pool temperature of 311.15 K. McAdams 0.13 Ra**1/3	\$
•	20258100 htc-temp 20258101 320. 613. 330. 855. 340. 1042. 20258102 350. 1197. 360. 1327. 370. 1467. 20258103 380. 1639. 390. 1793. 400. 1929. 20258104 410. 2049. 420. 2153. 430. 2295. 20258105 440. 2435. 450. 2562. 460. 2677.	*
•	table no. 591 - htc from outside of 43.75-in. horizontal EHIX shell assumes pool temperature of 311.15 K	\$
•	20259100 Htc-temp 20259101 320. 622. 330. 856. 340. 1033. 20259102 350. 1175. 360. 1289. 370. 1411. 20259103 380. 1566. 390. 1700. 400. 1815. 20259104 410. 1912. 420. 1992. 430. 2110. 20259105 440. 2226. 450. 2329. 460. 2419.	*
•	table no. 599 - htc from outside of 83-in. horizontal HK shell assumes pool temperature of 311.15 K	\$
•	20259900 htc-temp 20259901 320. 615. 330. 849. 340. 1025. 20259902 350. 1167. 360. 1280. 370. 1402. 20259903 380. 1536. 390. 1689. 400. 1804. 20259904 410. 1901. 420. 1980. 430. 2098. 20259905 440. 2214. 450. 2316. 460. 2407.	*
•	table no. 606 - normalized fission power as a function of time after scram	\$
•	table no. 606 - norm fns power	*
•	*table table type trip no. factor1 factor2 20260600 race-1 510 1.0 1.0	*
•	*table * time power 20260601 -1. 1.000000 + 0. 1.000000 ++ 0.001000 1.000000 ++ 0.002000 1.000000 ++ 0.003000 1.000000 ++ 0.004000 1.000000 ++ 0.005000 1.000000 ++ 0.006000 1.000000	*

+	40.000000	0.00255227
+	50.000000	0.0029821
+	60.000000	0.0017350
+	70.000000	0.0014720
+	80.000000	0.0012695
+	90.000000	0.0011122
+	100.000000	9.89e-04
+	110.000000	8.918e-04
+	120.000000	8.146e-04
+	130.000000	7.529e-04
+	140.000000	7.031e-04
+	150.000000	6.628e-04
+	160.000000	6.299e-04
+	170.000000	6.028e-04
+	180.000000	5.804e-04
+	190.000000	5.618e-04
+	200.000000	5.463e-04

\$ table 607 - fusion product decay power as a function of time after scram

*	table	type	trip factor1	factor2
*	20260700	react	510	1.0

* table no. 607 - norm fpd power

* table 970 - control rod reactivity as function of normalized rod position (biased to zero at initial position)

react-t	table type	trip no.	factor 1	factor 2
0.000000	*table			
0.000000	*table	20295602	0.	0.
0.000000	*table	20295603	0.005	0.2931
0.000000	*table	20295604	0.01	0.5802
0.000000	*table	20295605	0.015	0.8555
0.000000	*table	20295606	0.02	1.1133
0.000000	*table	20295607	0.025	1.3485
0.000000	*table	20295608	0.03	1.5561
0.000000	*table	20295609	0.035	1.7321
0.000000	*table	20295610	0.04	1.8727
0.000000	*table	20295611	0.045	1.9752
0.000000	*table	20295612	0.0491	2.0292
0.000000	*table	20295613	0.06	2.1360
0.000000	*table	20295614	1.0	11.3480

* table 970 - control rod reactivity as function of normalized rod position (biased to zero at initial position)

react-t	table type	trip no.	factor 1	factor 2
0.000000	*table			
0.000000	*table	20297000		
0.000000	*table	20297001	time	reactivity
0.000000	*table	20297002	0.	3.93
0.000000	*table	20297003	0.1218	3.50
0.000000	*table	20297004	0.2195	2.33
0.000000	*table	20297005	0.2790	0.
0.000000	*table	20297006	0.4391	-6.27
0.000000	*table	20297007	0.6098	-18.18
0.000000	*table	20297008	0.7805	-28.89
0.000000	*table			-32.78

* CONTROL VARIABLE INPUT

loop 1	loop 2	loop 3	loop 4	loop 5
20504100	frig-1.function	1.000000e+00	158.6526	0
20503900	msprtrip	1.000000e+00	0.	1
20503901	635			
20504000	mcptrip	1.000000e+00	1.	1
20504001	-635			
20504101	enrtvar,64,43			
20504201	enrtvar,64,44			
20504300	water power = (flow)*(pressure difference)			
20504301	enrtvar,62,prphd,124			
20504400	water = (water power)/(pump speed)			
20504401	enrtvar,48,enrtvar,43			
20504500	sum of torques divided by pump inertia (rate of speed change)			
20504501	pump inertia = 91.50 kg*m**2			
20504502	sum	1.0929000e-02	-80.9063	0
20504503	0.-1.,enrtvar,41,-1.,enrtvar,42,-1.,enrtvar,44			
20504600	do not adjust speed unless pumps have been tripped			
20504601	adj-1 mult	1.000000e+00	0.	0
20504701	enrtvar,45,enrtvar,39			
20504702	adjustment to pump speed			
20504703	adjus-1 integral	1.000000e+00	0.	0
20504800	accspd sum	1.000000e+00	175.1312	0

* table 956 - scram rod reactivity as function of time after trip

time	reactivity
0.	0.
0.000000	0.3581209
0.000000	0.3769885
0.000000	0.3968502
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
0.000000	0.4775544
0.000000	0.4177584
0.000000	0.4397618
0.000000	0.4629373
0.000000	0.5130022
0.000000	0.4873273
0.000000	0.6331501
0.000000	0.6529865
0.000000	0.5984520
0.000000	0.5684815
0.000000	0.5400299
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20504801 0.1,.cntrivar,83 1.,cntrivar,47
 * velocity head
 20504900 mpvsg1 mult 0.5 27883.9 1
 20504901 rhof1240100000 vefj1240100000
 * saturation pressure for volume 122.02
 20505000 impdge sum 1.000000d+00 45.3833 1
 20505001 -273.15 1.,tempf122030000
 20505100 satpsi function 1.000000d+00 8964.54 1
 20505101 cntrivar,50.35
 * available npsh for loop 1 1.000000d+00 1441890. 1
 20505201 0.1,p,122030000 -1.,cntrivar,51 1.,cntrivar,49
 * calculate NPSH required based on lose letter dated 4/16/93
 * NPSH = $n^2 \cdot (1.65 + 1.68^*n/(1500^*n + v))$
 * where NPSH is required suction head in Pa
 * w is normalized pump speed
 * w is pump flow rate in kg/s
 * divisor of second term for npsh required
 20505500 divisor sum 1. 742.244 1
 20505501 0.0 1500.,cntrivar,64 -1.,mfiflow,124010000
 * second term for npsh required
 20505600 term2 div 1.68 125172.1 1
 20505601 cntrivar,55 cntrivar,64
 * term in parenthesis for npsh required
 20505700 parenthesis sum 1.0 225172. 1
 20505701 1.65 1.,cntrivar,56
 * normalized speed squared
 20505800 velsqnd mult 1.0 .863194 1
 20505801 cntrivar,64 cntrivar,64
 * NPSH required
 20505900 npsheq mult 1.0 194367.2 1
 20505901 cntrivar,56 cntrivar,57
 * ratio of available upst to required npsh
 20506000 npsht1 div 1.000000d+00 7.41838 1
 20506001 cntrivar,59 cntrivar,52
 * head degradation factor
 20506100 degfac function 1.000000d+00 1. 1
 20506101 cntrivar,60.39
 * volumetric flow rate
 20506200 flow1 div 1.0 ,592974 1
 20506201 rhof124010000 mflow1124010000
 * determine nondimensional homologous variables
 20506300 v-1 mult 1.5521 ,9222 1
 20506301 cntrivar,62
 20506400 alpha-1 mult 5.305040d-03 .929082 1
 20506401 cntrivar,48
 20506500 velp1- div 1.000000d+00 ,992593 1
 20506501 cntrivar,64 cntrivar,63
 20506600 alpV-1 div 1.000000d+00 1.007462 1
 20506601 cntrivar,63 cntrivar,64
 20506700 hvmp1 function 1.000000d+00 1. 1
 20506701 cntrivar,66.41
 20506800 vA-VUL tripunit 1.000000d+00 0. 1
 20506801 536
 20506900 A-VUL tripunit 1.000000d+00 1. 1
 20506901 -536
 20507000 hvmp1 mult 1.000000d+00 0. 1
 20507001 cntrivar,67 cntrivar,68 cntrivar,61
 20507100 alpSg1 mult 1.000000d+00 30671.2 1
 20507101 cntrivar,61 cntrivar,48 cntrivar,48 cntrivar,69
 20507200 spdg1-1 power 1.000000d+00 175.132 1
 20507201 cntrivar,71.0.5
 20507300 A-VUL function 1.000000d+00 425 1
 20507301 cntrivar,70.42
 20507400 spdg2-1 mult 188.5 0. 1
 20507401 cntrivar,73 cntrivar,63 cntrivar,68

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* degraded pump speed for pump 1
 20507500 speed-1 sum 1.000000d+00 175.132 1
 * pump 1 speed after lag
 20507600 speedg1 lag 1.000000d+00 175.1338 1
 * control nps speed to reach new steady-state
 *
 20507700 tr-lu tripunit 1.000000d+00 1. 1
 20507701 -528
 20507800 pfiflow constant 2.50000d+01 2.50000d+01 0
 20507900 tfflflow sum 1.00000d+00 -0.01846932 1
 20507901 0. 1.,cntrivar,78 1.,velf1537010200
 20508000 fler mult 1.000000d+00 -0.01846932 0
 20508001 cntrivar,77 cntrivar,79
 20508100 flc-p1 prop-lin 1.000000d+00 175.1318 0
 20508101 0.202.0 cntrivar,80
 20508200 flc-d diffrend 1.000000d+06 1.92897-9 0
 20508201 cntrivar,80
 20508300 mcp1-vel sum 1.000000d+00 175.1318 1
 20508301 0. 1.,cntrivar,81 1.,cntrivar,82
 20508400 mult1 mult 1.000000d+00 175.1318 1
 20508401 cntrivar,83 cntrivar,40
 20508500 mult2 mult 1.000000d+00 0. 1
 20508501 cntrivar,76 cntrivar,39
 20508600 mcp1-vel sum 1.000000d+00 175.1318 1
 20508601 0. 1.,cntrivar,84 1.,cntrivar,85
 *
 ===== loop 2 =====
 20509100 ffrtg-2.function 1.000000d+00 158.6526 0
 20509101 cntrivar,14.43
 20509200 mottq-2.function 1.000000d+00 0. 0
 20509201 cntrivar,14.44
 * water power = (flow)*(pressure difference)
 20509300 wattpw-2.mult 1.0 1.294024. 0
 20509301 cntrivar,112 pmphead,224
 * water torque = (water power)/(pump speed)
 20509400 watrtq-2.div 1.000000000 7388.86 0
 20509401 cntrivar,98 cntrivar,99
 * sum of torques divided by pump inertia (rate of speed change)
 * scaling factor = inertia
 * Pump inertia = 91.50 kg-m**2
 20509500 ltorq-2.sum 1.0929004.02 -82.4867 0
 20509501 0.-1.,cntrivar,91 1.,cntrivar,92 -1.,cntrivar,94
 * do not adjust speed unless pumps have been tripped
 20509600 adjs2-2.mult 1.000000d+00 0. 0
 20509601 cntrivar,95 cntrivar,39
 * adjustment to pump speed
 20509700 adjs2-2.integral 1.000000d+00 0.
 20509701 cntrivar,96
 * actual p1-1 pump speed after pump trip
 20509800 actsp2d.sum 1.000000d+00 175.1318 0
 20509801 0. 1.,cntrivar,83 1.,cntrivar,97
 * velocity head
 20509900 incps2d.mult 0.5 29806.4 1
 20509901 rhof1224010000 refj224010000 refj224010000
 * saturation pressure for volume 222.03
 20510000 tmpf1c sum 1.000000d+00 45.6292 1
 20510001 -273.15 1.,tempf1222030000
 20510100 satpsi function 1.000000d+00 9122.66 1
 20510101 cntrivar,100.35
 * available nps for loop 2
 20510200 npsk-pa.sum 1.000000d+00 1435457. 1
 20510201 0.1,p,222030000 -1.,cntrivar,101 1.,cntrivar,99
 * calculate NPSH required based on Jose letter dated 4/16/93

- NPSH = $n^2 \cdot (1.5 + 1.87/n)(1500^n - n^2)$
 • where NPSH is required suction head in Pa
 • n is normalized pump speed
 • w is pump flow rate in kg/s

 - divisor of second term for nps required
 - 20510500 divisor sum 1. 720.233 1
 - 20510501 0.0 1500.entrivar.114-1.mflow3.224010000
 - second term for nps required
 - 20510600 term2 div 1.8 12897.3 1
 - 20510601 entrivar.105 entrivar.114
 - term in parenthesis for nps required
 - 20510700 parent sum 1.0 22897.3 1
 - 20510701 1.5 1.entrivar.106
 - normalized speed squared
 - 20510800 velsqd mult 1.0 .363193 1
 - 20510801 entrivar.114 entrivar.114
 - NPSH required
 - 20510900 npshead, npsq, mult 1.0 197669. 1
 - 20510901 entrivar.108 entrivar.107
 - ratio of available nps to required nps
 - 20511000 npshead, npsq, mult 1.0 1.00000d+00 7.26193 1
 - 20511001 entrivar.109 entrivar.102
 - head degradation factor
 - 20511100 defac2 function 1.00000d+00 1. 1
 - 20511101 entrivar.110.39
 - volumetric flow rate
 - 20511200 flow2 div 1.0 .613097 1
 - 20511201 rhofj22.4010000 mflow1.224010000
 - determine non-dimensional homologous variables
 - 20511300 v-2 mult 1.55521 .953494 1
 - 20511301 entrivar.112
 - 20511400 alpha2 mult 5.305404.03 .929081 1
 - 20511401 entrivar.98
 - 20511500 v'alp2 div 1.00000d+00 1.026276 1
 - 20511501 entrivar.114 entrivar.113
 - 20511600 alp2 div 1.00000d+00 .974396 1
 - 20511601 entrivar.113 entrivar.114
 - 20511700 hvn2 function 1.00000d+00 .939234 1
 - 20511701 entrivar.116.41
 - 20511800 v'el2 tripunkt 1.00000d+00 1. 1
 - 20511801 .537
 - 20511900 av-vel2 tripunkt 1.00000d+00 0. 1
 - 20511901 -.537
 - 20512000 hvn-pz2 mult 1.00000d+00 .939234 1
 - 20512001 entrivar.117 entrivar.118 entrivar.111
 - 20512100 alpq2.2 mult 1.00000d+00 0. 1
 - 20512101 entrivar.111 entrivar.98 entrivar.119
 - 20512200 spd2 power 1.00000d+00 0. 1
 - 20512201 entrivar.121.5
 - 20512300 v'el2 mult 1.00000d+00 .974396 1
 - 20512301 entrivar.120.42
 - 20512400 spd2.2 mult 188.5 175.1318 1
 - 20512401 entrivar.123 entrivar.113 entrivar.118
 - degraded pump speed for pump 2
 - 20512500 speed2 sum 1.00000d+00 175.1318 1
 - 20512501 0. 1.entrivar.122 1.entrivar.124
 - pump 2 speed after lag
 - 20512600 speed2 lag 1.00000d+00 175.1317 1
 - 20512601 0.050 entrivar.125
 - control mcp speed to reach new steady-state
 - loop 3 ==
 - 20514100 fmrg-3 function 1.00000d+00 158.5526 0
 - 20514101 entrivar.164.43
 - 20514200 mofrg-3 function 1.00000d+00 0. 0
 - 20514201 entrivar.164.44
 - water power = (flow)/(pressure difference)
 - 20514300 wapnw-3 mult 1.0 1291735. 0
 - 20514301 entrivar.162 pmphead.324
 - water torque = (water power)/(pump speed)
 - 20514400 wapng-3 div 1.00000d+00 7315.78 0
 - 20514401 entrivar.148 entrivar.143
 - sum of torques divided by pump inertia (rate of speed change)
 - scaling factor = inertia
 - Pump inertia = $91.50 \text{ kg-m}^{\star 2}$
 - 20514500 fmrg-3 sum 1.05290004-02 .82 2.3438 0
 - 20514501 0. 1.entrivar.141 1.entrivar.142-1.entrivar.144
 - do not adjust speed unless pumps have been tripped
 - 20514600 adj3 mult 1.00000d+00 0. 0
 - 20514601 entrivar.145 entrivar.39
 - adjustment to pump speed
 - 20514700 adj3 integral 1.0000000d+00 0. 0
 - 20514701 entrivar.146
 - actual pre-1 pump speed after pump trip
 - 20514800 acpt43 sum 1.00000d+00 175.1318 0
 - 20514801 0. 1.entrivar.83 1.entrivar.147
 - velocity head
 - 20514900 mprg33 mult 0.5 30045.9 1
 - 20514901 rhofj3.24010000 ref5.324010000 vell5.324010000
 - saturation pressure for volume 322.03
 - 20515000 tmkgc sum 1.00000d+00 45.6568 1
 - 20515001 -273.15 1.entrav.32203000
 - 20515100 satpr function 1.00000d+00 9137.12 1
 - 20515101 entrivar.150.35
 - available nps for loop 3
 - 20515200 rphs:pa sum 1.00000d+00 1453142. 1
 - 20515201 0. 1.p322030000 1.entrivar.151 1.entrivar.149
 - calculate NPSH required based on Jose letter dated 4/16/93
 - $NPSH = n^{\star 2} \cdot ((1.5 + 1.87/n)(1500^n - n^2) - w)$
 - where NPSH is required suction head in Pa
 - n is normalized pump speed
 - w is pump flow rate in kg/s
 - divisor of second term for nps required
 - 20515500 divisor sum 1. 717.535 1
 - 20515501 0.1500.entrivar.164 -1.mflow1.324010000
 - second term for nps required
 - 20515600 entr2 div 1.68 129482.4 1
 - 20515601 entravar.155 entrivar.164
 - term in parenthesis for nps required
 - 20515700 parent sum 1.0 229482.4 1
 - 20515701 1.5 1.entrivar.156
 - normalized speed squared
 - 20515800 velsgd mult 1.0 .863193 1
 - 20515801 entrivar.164 entrivar.164
 - NPSH required
 - 20515900 rphsq mult 1.0 198087.5 1
 - 20515901 entrivar.158 entrivar.157
 - ratio of available nps to required nps
 - 20516000 npdns3 div 1.00000d+00 7.33536 1
 - 20516001 entrivar.159 entrivar.152
 - head degradation factor
 - 20516100 depf3 function 1.00000d+00 1.
 - 20516101 entrivar.160.39
 - volumetric flow rate

20516200 flow-3 div 1.0 .613097 1
 20516201 rh5j,224010000 mflowj,224010000
 * determine nondimensional homologous variables
 20516300 v-3 mult 1.55321 .953494 1
 20516301 cntrivar,162 5.3050404-03 .929281 1
 20516400 alpha-3 mult 1.000000d+00 1.026276 1
 20516401 cntrivar,148 1.000000d+00 1.000000d+00 1
 20516500 v/dp-3 div 1.000000d+00 1.000000d+00 1
 20516501 cntrivar,164 cntrivar,163 1.000000d+00 1.000000d+00 1
 20516600 alpha-3 div 1.000000d+00 .974396 1
 20516601 cntrivar,163 cntrivar,164 1.000000d+00 .974396 1
 20516700 hvr-2 function 1.000000d+00 .939234 1
 20516701 cntrivar,166,41 1.000000d+00 1.
 20516800 v/t-3 tripunit 1.000000d+00 1.
 20516801 538 1.000000d+00 1.
 20516900 av/t-3 tripunit 1.000000d+00 0.
 20516901 -538 1.000000d+00 0.
 20517000 hvr-pu3 mult 1.000000d+00 .939234 1
 20517001 cntrivar,167 cntrivar,168 cntrivar,161 1.000000d+00 0.
 20517100 alpha-3 mult 1.000000d+00 0.
 20517101 cntrivar,161 cntrivar,168 cntrivar,168 cntrivar,169 1.000000d+00 0.
 20517200 cntrivar,171,0,5 1.000000d+00 .974396 1
 20517300 v/dg-3 function 1.000000d+00 .974396 1
 20517301 cntrivar,170,42 1.000000d+00 0.
 20517400 sped-2,3 mult 183.5 175.1318 1
 20517401 cntrivar,173 cntrivar,163 cntrivar,168 1.000000d+00 0.
 * degraded pump speed for pump 3
 20517500 sped-3 sum 1.000000d+00 175.1318 1
 * pump 3 speed after lag 1.000000d+00 175.1337 1
 20517600 sped-3 lag 1.000000d+00 175.1337 1
 20517601 0.050 cntrivar,175 1.000000d+00 0.
 * control mp speed to reach new steady-state
 20518400 multi mult 1.000000d+00 175.1318 1
 20518401 cntrivar,83 cntrivar,40 1.000000d+00 0.
 20518500 multi2 mult 1.000000d+00 0.
 20518501 cntrivar,176 cntrivar,39 1.000000d+00 0.
 20518600 mp3-rel sum 1.000000d+00 175.1318 1
 20518601 0.1,cntrivar,184 1,cntrivar,185 1.000000d+00 0.
 * specified speed cooldown for MCPs
 20519300 mp1sp function 182.5778 182.5778 0.3 .00 182.5778
 20519301 time 0.135
 \$-----\$
 * These control variables are for purely cosmetic purposes (i.e. the solution is not dependent upon) to monitor the limits in the fuel.
 * cost flow excursion predictions (W/m^2)
 * lower fuel hot channel - 95% uncertainty
 20520000 sqrfwl power 1.000000d+00 5.03789 0
 20520001 vel515010000 0.5
 20520100 sattemp sum 1.0 500.447 1
 20520101 0.1,sattemp,515010000 0.5,sattemp,515020000
 20520200 subcoolf sum 1.000000d+00 166.9222 0
 20520201 Q_1,cntrivar,201 1,temp,515010000
 20520300 cost mult 7.812500d+04 63639.132. 0
 20520301 cntrivar,200 cntrivar,202 1.0 505.627 0
 20520400 sqrfwl power 1.000000d+00 5.03627 0
 20520401 vel515020000 0.5
 20520500 sattemp sum 1.0 494.721 1
 \$-----\$
 20520501 0.5,sattemp,515020000 0.5,sattemp,515030000
 20520600 subcoolf sum 1.000000d+00 147.572 0
 20520700 cost mult 7.812500d+04 5829.038. 0
 20520701 cntrivar,204 cntrivar,206 1.000000d+00 5.07606 0
 20520800 sqrfwl power 1.000000d+00 488.389 1
 20520801 vel515030000 0.5
 20520900 sattemp sum 1.0 488.389 1
 20520901 0.1,sattemp,515030000 0.5,sattemp,515040000
 20521000 subcoolf sum 1.000000d+00 128.8313 0
 20521001 0.1,cntrivar,209 1,temp,515030000
 20521100 cost mult 7.812500d+04 51090288. 0
 20521101 cntrivar,208 cntrivar,210 1.000000d+00 5.09637 0
 20521200 sqrfwl power 1.000000d+00 5.09637 0
 20521201 vel515040000 0.5
 20521300 sattemp sum 1.0 481.294 1
 20521301 0.5,sattemp,515040000 0.5,sattemp,515050000
 20521400 subcoolf sum 1.000000d+00 110.5089 0
 20521401 0.1,cntrivar,213 1,temp,515040000
 20521500 subcoolf sum 1.000000d+00 53.4404 0
 20521501 cost mult 7.812500d+04 439.9572. 0
 20521600 sqrfwl power 1.000000d+00 5.11601 0
 20521601 vel515050000 0.5
 20521700 sattemp sum 1.0 473.77 1
 20521701 0.1,sattemp,515050000 0.5,sattemp,515040000
 20521800 subcoolf sum 1.000000d+00 93.4404 0
 20521801 0.1,cntrivar,217 1,temp,515050000
 20521900 cost mult 7.812500d+04 3.724747 0
 20521901 cntrivar,216 cntrivar,218
 * lower fuel hot channel - 99.9% uncertainty
 20522000 sqrfwl power 1.000000d+00 5.03955 0
 20522001 vel516010000 0.5
 20522100 sattemp sum 1.0 500.45 1
 20522101 0.1,sattemp,516010000 0.5,sattemp,516020000
 20522200 subcoolf sum 1.000000d+00 166.325 0
 20522201 0.1,cntrivar,221 1,temp,516010000
 20522300 subcoolf sum 1.000000d+00 65.848508. 0
 20522301 cntrivar,220 cntrivar,222 1.000000d+00 65.848508.
 20522400 sqrfwl power 1.000000d+00 5.0588 0
 20522401 vel516020000 0.5
 20522500 sattemp sum 1.0 494.727 1
 20522501 0.1,sattemp,516020000 0.5,sattemp,516030000
 20522600 subcoolf sum 1.000000d+00 146.4247 0
 20522601 0.1,cntrivar,225 1,temp,516020000
 20522700 cost mult 7.812500d+04 57869.836. 0
 20522701 cntrivar,224 cntrivar,226 1.000000d+00 5.07963 0
 20522800 sattemp sum 1.0 488.395 1
 20522900 subcoolf sum 1.000000d+00 127.7168 0
 20523000 cost mult 7.812500d+04 5829.038. 0
 20523100 sattemp sum 1.0 488.395 1
 20523101 cntrivar,228 cntrivar,230 1.000000d+00 5.10107 0
 20523200 sqrfwl power 1.000000d+00 5.12184 0
 20523201 vel516040000 0.5
 20523300 subcoolf sum 1.000000d+00 127.7168 0
 20523400 cost mult 7.812500d+04 108.3906 0
 20523401 0.1,cntrivar,233 1,temp,516040000
 20523500 cost mult 7.812500d+04 4.3196e+7 0
 20523501 cntrivar,232 cntrivar,234 1.000000d+00 5.12184 0
 20523600 sqrfwl power 1.000000d+00 5.12184 0
 20523601 vel516050000 0.5
 20523700 sattemp sum 1.0 473.762 1
 20523701 0.1,sattemp,516050000 0.5,sattemp,516040000
 20523800 subcoolf sum 1.000000d+00 90.928 0
 20523801 0.1,cntrivar,237 1,temp,516030000

20523900 costaf mult 7.812500d+04 36384216. 0
 20523901 cntrvar.236 cntrvar.238
 • upper fuel hot channel - 95% uncertainty
 20524000 sqrfwl power 1.000000d+00 5.02122. 0
 20524001 refl546010000 0.5
 20524100 sattemp sum 1.0 499.896 1
 20524101 0. 0.5 sattemp,545010000 0.5 sattemp,545020000
 20524200 subcof sum 1.000000d+00 167.2667 0
 20524201 0. 1. cntrvar,241 -1. temp,545010000
 20524300 costaf mult 7.812500d+04 65615780. 0
 20524301 cntrvar,240 cntrvar,242
 20524400 sqrfwl power 1.000000d+00 5.0395 0
 20524401 refl545020000 0.5
 20524500 sattemp sum 1.0 494.208 1
 20524501 0. 0.5 sattemp,545020000 0.5 sattemp,545030000
 20524600 subcof sum 1.000000d+00 146.793 0
 20524601 0. 1. cntrvar,245 -1. temp,545020000
 20524700 costaf mult 7.812500d+04 57794112. 0
 20524701 cntrvar,244 cntrvar,246
 20524800 sqrfwl power 1.000000d+00 5.0611 0
 20524801 refl545030000 0.5
 20524900 sattemp sum 1.0 487.929 1
 20524901 0. 0.5 sattemp,545030000 0.5 sattemp,545040000
 20525000 subcof sum 1.000000d+00 126.838 0
 20525001 0. 1. cntrvar,249 -1. temp,545030000
 20525100 costaf mult 7.812500d+04 50151540. 0
 20525101 cntrvar,248 cntrvar,250
 20525200 sqrfwl power 1.000000d+00 5.08402 0
 20525201 refl54504000 0.5
 20525300 sattemp sum 1.0 480.893 1
 20525301 0. 0.5 sattemp,545040000 0.5 sattemp,545050000
 20525400 subcof sum 1.000000d+00 107.0479 0
 20525401 0. 1. cntrvar,253 -1. temp,545040000
 20525500 costaf mult 7.812500d+04 42518256. 0
 20525501 cntrvar,252 cntrvar,254
 20525600 sqrfwl power 1.000000d+00 5.10745 0
 20525601 refl545050000 0.5
 20525700 sattemp sum 1.0 473.431 1
 20525701 0. 1.5 sattemp,545050000 -0.5 sattemp,545040000
 20525800 subcof sum 1.000000d+00 88.0411 0
 20525801 0. 1. cntrvar,257 -1. temp,545050000
 20525900 costaf mult 7.812500d+04 35130132. 0
 20525901 cntrvar,256 cntrvar,258
 • upper fuel hot channel - 99.9% uncertainty
 20526000 sqrfwl power 1.000000d+00 5.022274 0
 20526001 refl546010000 0.5
 20526100 sattemp sum 1.0 499.9 1
 20526101 0. 0.5 sattemp,546010000 0.5 sattemp,546020000
 20526200 subcof sum 1.000000d+00 166.7146 0
 20526201 0. 1. cntrvar,261 -1. temp,546010000
 20526300 costaf mult 7.812500d+04 6561947 0
 20526301 cntrvar,260 cntrvar,262
 20526400 sqrfwl power 1.000000d+00 5.04191 0
 20526401 refl546020000 0.5
 20526500 sattemp sum 1.0 494.216 1
 20526501 0. 0.5 sattemp,546020000 0.5 sattemp,546030000
 20526600 subcof sum 1.000000d+00 145.6434 0
 20526601 0. 1. cntrvar,265 -1. temp,546020000
 20526700 costaf mult 7.812500d+04 57368772. 0
 20526701 cntrvar,264 cntrvar,266
 20526800 sqrfwl power 1.000000d+00 5.06464 0
 20526801 refl546030000 0.5
 20526900 sattemp sum 1.0 487.938 1
 20526901 refl546030000 0.5 sattemp,546040000
 20527000 subcof sum 1.000000d+00 125.1292 0
 20527001 0. 1. cntrvar,269 -1. temp,546030000
 20527100 costaf mult 7.812500d+04 49510520. 0
 • Peckel numbers for hot channels
 • Assume hydraulic diameters of 0.002498 for LC and 0.002494 for UC
 • LC 95% probability
 20530000 dh-g-cp mult 0.002498 290388. 1
 20530001 refl515010000 refl515010000 csubf515010000
 20530100 pk95-1 div 1.0 465729. 1
 20530101 thconf515010000 cntrvar,300
 20530200 dh-g-cp mult 0.002498 2891776. 1
 20530201 refl515020000 refl515020000 csubf515020000


```

20547200 visc-cp mult 1.0 1.202777 1
20547201 visc,f,545050000 csup,f,545050000
20547300 prandtl5 div 1.0 1.89121 1
20547301 thcont,f,545050000 cntrivar,472
* UC 99.9%
20547400 visc-cp mult 1.0 2.315973 1
20547401 visc,f,546010000 csup,f,546010000
20547500 prandtl5 div 1.0 3.715524 1
20547501 thcont,f,546010000 cntrivar,474
20547600 visc-cp mult 1.0 1.84586 1
20547601 visc,f,546020000 csup,f,546020000
20547700 prandtl5 div 1.0 2.92734 1
20547701 thcont,f,546020000 cntrivar,476
20547800 visc-cp mult 1.0 1.537932 1
20547801 visc,f,546030000 csup,f,546030000
20547900 prandtl5 div 1.0 2.4236 1
20547901 thcont,f,546030000 cntrivar,478
20548000 visc-cp mult 1.0 1.323142 1
20548001 visc,f,546040000 csup,f,546040000
20548100 prandtl5 div 1.0 2.080034 1
20548101 thcont,f,546040000 cntrivar,480
20548200 visc-cp mult 1.0 1.17138 1
20548201 visc,f,546050000 csup,f,546050000
20548300 prandtl5 div 1.0 1.842497 1
20548301 thcont,f,546050000 cntrivar,482
* control system to control primary coolant system temperature by
* adjusting the secondary flow
*.....$.
*cntrivar name type factor init fc min max
20558000 terror sum 1.000004+00 .03304085 1
20558001 318.75 -1. tempf 590010000
* 20558100 spendl prop-int,-1.00000d+00 1774.07 0
* 20558101 3.0 cntrivar 50
20558100 seflow constant 1774.07
* 20558200 se-off tripunit 1.0000d+00 0. 03 .00 1.0000d+00
20558201 240
* 20558300 dchta sum 1.00000d+00 40. 0 1 0.
20558301 -10. 1. ttrn,0
* 20558400 factor mult 0.1 0. 0 3 0.0 0.9677
20558401 cntrivar,582 cntrivar,583
* 20558500 se-dec sum 1.0 1. 0
20558501 1. -1. cntrivar,584
* 20558600 sefl1 mult 1.00000d+00 1774.07 0
20558601 cntrivar,581 cntrivar,585
* control pr speed to reach new steady-state (587-591)
* these control variables should only be active when
* a new steady pressurizing flow rate is being sought
*.....$.

20559700 pwrcl constant 1.6299713.465 0
20559800 ferror sum 1.00000d+00 -00117527 1
20559801 0.1. cntrivar,587 -1..,refj,825000000
20559900 0-pi prop-int 1.0 229.039 0
2055991 0.80. cntrivar,588
20559900 flo-d diffnd 1.00000d-06 -1.61498-10 0
20559901 cntrivar,588
20559100 parvel sum 1.0 229.039 1

```

\$ multiplied by a level factor and divided by 3.5e8 watts.
\$ tiles addxx refer to aluminum beta and gamma decay, the factor
\$ is the sum of those sources on level xx in the 2x1hf composite
\$ multiplied by a level factor and divided by 3.5e8 watts.
\$ radial distribution is applied via the heat structure cards.
\$ summation and by the last saved power before screen. the local
\$ decay powers are thus scaled by the power at screen and weighted
\$ by the screen flag (before screen = no value, after screen = value)
\$ as above, these 15 cards multiply the appropriate scalars by the
\$ corresponding tables, in this case for the d2o in the
\$ central rod hole.

\$ the sums are multiplied the th saved power at screen and the screen
\$ flag, as above there is no value before screen.

*civar name type factor init fc min max
20561100 "d1ss" mult 4.9028e-04 168656.8 1 0

*civar variable name parameter no. variable name parameter no.
20561101 cntrivar 601 cntrivar 605

*civar name type factor init fc min max
20561200 "t1ss" mult 2.3105e-03 794814.1 0

*civar variable name parameter no. variable name parameter no.
20561201 cntrivar 601 cntrivar 605

*civar name type factor init fc min max
20561300 "d2o1ss" mult 2.1391e-04 73585.2 1 0

*civar variable name parameter no. variable name parameter no.
20561301 cntrivar 601 cntrivar 605

*civar name type factor init fc min max
20561400 "acomp" mult 2.1689e-4 74610.4 1 0

*civar variable name parameter no. variable name parameter no.
20561401 cntrivar 601 cntrivar 605

*civar name type factor init fc min max
20561500 "hcomp" mult 6.6004e-4 227054.4 1 0

*civar variable name parameter no. variable name parameter no.
20561501 cntrivar 601 cntrivar 605

*civar name type factor init fc min max
20561600 "ahfs" sum 1.0 301665. 1 0

*civar a0 coeff variable name parameter no.
20561601 0.0 1.0 cntrivar 614
20561602 1.0 cntrivar 615

*civar name type factor init fc min max
20561700 "ahfp" function 4.8823e-4 4.8823e-4 1 0

*civar srch arg. name srch arg. no. table no.
20562101 time 0 606

*civar name type factor init fc min max
20562200 "alid" function 3.4990e-5 3.4990e-5 1 0

*civar srch arg. name srch arg. no. table no.
20562201 time 0 607

*civar name type factor init fc min max
20562500 "alid2" mult 1.0 0. 1 0

*civar variable name parameter no. variable name parameter no.
20562501 cntrivar 600 cntrivar 605

*civar name type factor init fc min max
20562502 cntrivar 624 cntrivar 625

*civar name type factor init fc min max
20562600 "tfisp" function 1.8708e-3 .0018708 1 0

*civar srch arg. name srch arg. no. table no.
20562601 time 0 606

*civar name type factor init fc min max
20562700 "tfisf" function 3.9623e-4 3.9623e-4 1 0

*civar srch arg. name srch arg. no. table no.
20562701 time 0 607

*civar name type factor init fc min max
20562800 "tfifai" function 4.3444e-5 4.3444e-5 1 0

*civar srch arg. name srch arg. no. table no.
20562801 time 0 608

*civar name type factor init fc min max
20562900 "htot1" sum 1.0 .002310474 1 0

*civar a0 coeff variable name parameter no.
20562901 0.0 1.0 cntrivar 626
20562902 1.0 cntrivar 627
20562903 1.0 cntrivar 628

*civar name type factor init fc min max
20563000 "rf02" mult -1.0 -1.0 0. 1 0

*civar variable name parameter no. variable name parameter no.
20563001 cntrivar 600 cntrivar 629

*civar srch arg. name srch arg. no. table no.
20563101 time 0 606

*civar srch arg. name srch arg. no. table no.
20563201 time 0 607

*civar name type factor init fc min max
20563300 "sumsf" function 1.2868e-4 1.2868e-4 1 0

*civar srch arg. name srch arg. no. table no.
20563301 time 0 608

*civar name type factor init fc min max
20563400 "sumal" function 1.7159e-5 1.7159e-5 1 0

*civar srch arg. name srch arg. no. table no.

```

20563400 "sumdot1" sum 1.0 8.962494-10
*   *ctivar a0 coeff variable name parameter no.
20563401 0.0 1.0 ctivar 631
20563402 1.0 ctivar 632
20563403 1.0 ctivar 633
$   *ctivar name type factor init fc min max
20563500 "sumdot2" mult 1.0 0. 1. 0
*   *ctivar variable name parameter no. variable name parameter no.
20563501 ctivar 600 ctivar 605
$   *ctivar name type factor init fc min max
20563502 ctivar 634
$   *ctivar name type factor init fc min max
20563500 "d2ofsp" function 2.1238c-4 2.1238-4 1.0
*   *ctivar name type factor init fc min max
20563501 "d2ofsa" function 7.6092c-6 7.6092-6 1.0
*   *ctivar name type factor init fc min max
20563501 "d2oal" function 1.5251c-6 1.5251-6 1.0
*   *ctivar name type factor init fc min max
20563501 "d2ot" 0. 606
$   *ctivar name type factor init fc min max
20563501 "d2ot1" sum 1.0 2.215143-4 1.0
*   *ctivar a0 coeff variable name parameter no.
20563501 0.0 1.0 ctivar 636
20563502 1.0 ctivar 637
20563503 1.0 ctivar 638
$   *ctivar name type factor init fc min max
20564000 "d2ot2" mult 1.0 0. 1. 0
*   *ctivar variable name parameter no. variable name parameter no.
20564001 ctivar 600 ctivar 605
$   *ctivar name type factor init fc min max
20564002 ctivar 639
$   *ctivar name type factor init fc min max
20564100 "dlhs" sum 1. 168556.8 0.0
*   *ctivar a0 coeff variable name parameter no.
20564101 0. 1. ctivar 625
20564102 1. ctivar 611
$   *ctivar name type factor init fc min max
20564200 "dlhs" sum 1. 301665. 0.0
*   *ctivar a0 coeff variable name parameter no.
20564201 0. 1. ctivar 635
20564202 1. ctivar 616
$   *ctivar name type factor init fc min max
20564300 "dlhs" sum 1. 794814. 0.0
*   *ctivar a0 coeff variable name parameter no.
20564301 0. 1. ctivar 630
20564302 1. ctivar 612
* these are the outer d2o cards, they parallel the above cards
*ctivar name type factor init fc min max

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```

20568201 time 0 606
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20568300 "fsakwo3" function 2.7003e-4 2.7032e-4
  *
  *civar search arg. name search arg. no. table no.
  20568301 time 0 607
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20568400 "fsakwo3" function 1.8319e-5 1.8319e-5 1 0
  *
  *civar search arg. name search arg. no. table no.
  20568401 time 0 608
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20568500 "fspwo4" function 9.5081e-4 9.5081e-4 1 0
  *
  *civar search arg. name search arg. no. table no.
  20568501 time 0 606
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20568600 "fsakwo4" function 2.6235e-4 2.6235e-4 1 0
  *
  *civar search arg. name search arg. no. table no.
  20568601 time 0 607
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20568700 "fsakwo4" function 1.7798e-5 1.7798e-5 1 0
  *
  *civar search arg. name search arg. no. table no.
  20568701 time 0 608
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20568800 "fspwo4" function 7.6993e-4 7.6993e-4 1 0
  *
  *civar search arg. name search arg. no. table no.
  20568801 time 0 606
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20568900 "fsakwo5" function 2.1244e-4 2.1244e-4 1 0
  *
  *civar search arg. name search arg. no. table no.
  20568901 time 0 607
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20569100 "westum01" sum 1.0 .001249821 0
  *
  *civar a0 coeff variable name parameter no.
  20569101 0.0 1.0 cntrivar 676
  20569102 1.0 1.0 cntrivar 677
  20569103 1.0 1.0 cntrivar 678
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20569200 "westum02" sum 1.0 .001260921 0
  *
  *civar a0 coeff variable name parameter no.
  20569201 0.0 1.0 cntrivar 679
  20569202 1.0 1.0 cntrivar 680
  20569203 1.0 1.0 cntrivar 681
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20569300 "westum03" sum 1.0 .00126701 1 0
  *
  *civar a0 coeff variable name parameter no.
  20569400 "westum04" sum 1.0 .001230958 1 0
  *
  *civar a0 coeff variable name parameter no.
  20569401 0.0 1.0 cntrivar 682
  20569402 1.0 1.0 cntrivar 683
  20569403 1.0 1.0 cntrivar 684
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20569500 "westum05" sum 1.0 9.96782e-4 1 0
  *
  *civar a0 coeff variable name parameter no.
  20569501 0.0 1.0 cntrivar 685
  20569502 1.0 1.0 cntrivar 686
  20569503 1.0 1.0 cntrivar 687
$ *civar a0 coeff variable name parameter no.
  *civar name type factor init fc min max
  20569600 "pwwo1" mult 1.0 0. 1 0
  *
  *civar variable name parameter no. variable name parameter no.
  20569601 cntrivar 600 cntrivar 605
  20569602 cntrivar 691
$ *civar a0 coeff variable name parameter no. variable name parameter no.
  20569700 "pwwo2" mult 1.0 0. 1 0
  *
  *civar variable name parameter no. variable name parameter no.
  20569701 cntrivar 600 cntrivar 692
  20569702 cntrivar 691
$ *civar a0 coeff variable name parameter no. variable name parameter no.
  20569800 "pwwo3" mult 1.0 0. 1 0
  *
  *civar variable name parameter no. variable name parameter no.
  20569801 cntrivar 600 cntrivar 605
  20569802 cntrivar 693
$ *civar a0 coeff variable name parameter no. variable name parameter no.
  20569900 "pwwo4" mult 1.0 0. 1 0
  *
  *civar variable name parameter no. variable name parameter no.
  20569901 cntrivar 600 cntrivar 694
  20569902 cntrivar 694
$ *civar a0 coeff variable name parameter no. variable name parameter no.
  20570000 "pwwo5" mult 1.0 0. 1 0
  *
  *civar variable name parameter no. variable name parameter no.
  20570001 cntrivar 600 cntrivar 605
  20570002 cntrivar 695
$ *civar a0 coeff variable name parameter no. variable name parameter no.
  20570100 "spbl" mult 5.39567e-4 185647. 1 0
  *
  *civar variable name parameter no. variable name parameter no.
  20570101 cntrivar 601 cntrivar 605
$ *civar a0 coeff variable name parameter no. variable name parameter no.
  20570200 "spb2" mult 5.4486e-4 1874923.1 0
  *
  *civar variable name parameter no. variable name parameter no.
  20570201 cntrivar 601 cntrivar 605
$ *civar a0 coeff variable name parameter no. variable name parameter no.
  20570300 "spb3" mult 5.4486e-4 1874923.1 0
  *
  *civar a0 coeff variable name parameter no. variable name parameter no.
  20570301 cntrivar 601 cntrivar 605

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20570300 "cpb13" mult 5.4745e-4 188322.3 1.0
*ctivar variable name parameter no. variable name parameter no.
20570301 ctivar 601 ctivar
$=====
*ctivar name type factor init fc min max
20570400 "cpb4" mult 5.3189e-4 182970.7 1.0
*ctivar variable name parameter no. variable name parameter no.
20570401 ctivar 601 ctivar
$=====
*ctivar name type factor init fc min max
20570500 "cpb5" mult 4.3070e-4 148161.2 1.0
*ctivar variable name parameter no. variable name parameter no.
20570501 ctivar 601 ctivar
$=====
*ctivar name type factor init fc min max
20570600 "ispwp1" function 3.1372e-4 3.1372e-4 1.0
*ctivar search arg. name search arg. no. table no.
20570601 time 0 606
$=====
*ctivar name type factor init fc min max
20570700 "fdkp1" function 7.5233e-5 7.5233e-5 1.0
*ctivar search arg. name search arg. no. table no.
20570701 time 0 607
$=====
*ctivar name type factor init fc min max
20570800 "adkp1" function 7.5233e-5 7.5233e-5 1.0
*ctivar search arg. name search arg. no. table no.
20570801 time 0 608
$=====
*ctivar name type factor init fc min max
20570900 "ispwp2" function 3.1676e-4 3.1676e-4 1.0
*ctivar search arg. name search arg. no. table no.
20570901 time 0 606
$=====
*ctivar name type factor init fc min max
20571000 "fdkp2" function 1.5219e-4 1.5219e-4 1.0
*ctivar search arg. name search arg. no. table no.
20571001 time 0 607
$=====
*ctivar name type factor init fc min max
20571100 "adkp2" function 7.5956e-5 7.5956e-5 1.0
*ctivar search arg. name search arg. no. table no.
20571101 time 0 608
$=====
*ctivar name type factor init fc min max
20571200 "ispwp3" function 3.1826e-4 3.1826e-4 1.0
*ctivar search arg. name search arg. no. table no.
20571201 time 0 606
$=====
*ctivar name type factor init fc min max
20571300 "fdkp3" function 1.5291e-4 1.5291e-4 1.0
*ctivar search arg. name search arg. no. table no.
20571301 time 0 607
$=====
*ctivar name type factor init fc min max
20571400 "adkp3" function 7.6318e-5 7.6318e-5 1.0
*ctivar search arg. name search arg. no. table no.
20571401 time 0 608
$=====

*ctivar name type factor init fc min max
20571500 "ispwp4" function 3.0921e-4 3.0921e-4 1.0
*ctivar search arg. name search arg. no. table no.
20571501 time 0 606
$=====
*ctivar name type factor init fc min max
20571600 "fdkp4" function 1.4856e-4 1.4856e-4 1.0
*ctivar search arg. name search arg. no. table no.
20571601 time 0 607
$=====
*ctivar name type factor init fc min max
20571700 "adkp4" function 7.4148e-5 7.4148e-5 1.0
*ctivar search arg. name search arg. no. table no.
20571701 time 0 608
$=====
*ctivar name type factor init fc min max
20571800 "ispwp5" function 2.5038e-4 2.5038e-4 1.0
*ctivar search arg. name search arg. no. table no.
20571801 time 0 606
$=====
*ctivar name type factor init fc min max
20571900 "fdkp5" function 1.203e-4 1.203e-4 1.0
*ctivar search arg. name search arg. no. table no.
20571901 time 0 607
$=====
*ctivar name type factor init fc min max
20572000 "adkp5" function 6.0042e-5 6.0042e-5 1.0
*ctivar search arg. name search arg. no. table no.
20572001 time 0 608
$=====
*ctivar name type factor init fc min max
20572100 "pisum1" sum 1.0 4.6418e-4 1.0
*ctivar a0 coeff variable name parameter no.
20572101 0.0 1.0 ctivar 706
*ctivar 1.0 ctivar 707
*ctivar 1.0 ctivar 708
$=====
*ctivar name type factor init fc min max
20572200 "pisum2" sum 1.0 5.4490e-4 1.0
*ctivar a0 coeff variable name parameter no.
20572201 0.0 1.0 ctivar 709
*ctivar 1.0 ctivar 710
*ctivar 1.0 ctivar 711
$=====
*ctivar name type factor init fc min max
20572300 "pisum3" sum 1.0 5.4748e-4 1.0
*ctivar a0 coeff variable name parameter no.
20572301 0.0 1.0 ctivar 712
*ctivar 1.0 ctivar 713
*ctivar 1.0 ctivar 714
$=====
*ctivar name type factor init fc min max
20572400 "pisum4" sum 1.0 5.31918e-4 1.0
*ctivar a0 coeff variable name parameter no.
20572401 0.0 1.0 ctivar 715
*ctivar 1.0 ctivar 716
*ctivar 1.0 ctivar 717
$=====
```

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$ *civar name type factor init fc min max
$   20572500 "psum5" sum 1.0 4.307224 1.0
$ *civar a0 coeff variable name parameter no.
$   20572501 0.0 1.0 cntrivar 718
$   20572502 1.0 cntrivar 719
$   20572503 1.0 cntrivar 720
$ *civar name type factor init fc min max
$   20572600 "pipow1" mult 1.0 0. 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20572601 cntrivar 600 cntrivar 605
$   20572602 cntrivar 721
$ *civar name type factor init fc min max
$   20572700 "pipow2" mult 1.0 0. 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20572701 cntrivar 600 cntrivar 605
$   20572702 cntrivar 722
$ *civar name type factor init fc min max
$   20572800 "pipow3" mult 1.0 0. 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20572801 cntrivar 600 cntrivar 605
$   20572802 cntrivar 723
$ *civar name type factor init fc min max
$   20572900 "pipow4" mult 1.0 0. 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20572901 cntrivar 600 cntrivar 605
$   20572902 cntrivar 724
$ *civar name type factor init fc min max
$   20573000 "pipow5" mult 1.0 0. 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20573001 cntrivar 600 cntrivar 605
$   20573002 cntrivar 725
$ *civar name type factor init fc min max
$   20573100 "pt1" sum 1.0 185647. 1.0
$ *civar a0 coeff variable name parameter no.
$   20573101 0.0 1.0 cntrivar 701
$   20573102 1.0 cntrivar 726
$ *civar name type factor init fc min max
$   20573200 "pt2"
$ *civar a0 coeff variable name parameter no.
$   20573201 0.0 1.0 cntrivar 702
$   20573202 1.0 cntrivar 727
$ *civar name type factor init fc min max
$   20573300 "pt3" sum 1.0 188323.3 1.0
$ *civar a0 coeff variable name parameter no.
$   20573301 0.0 1.0 cntrivar 703
$   20573302 1.0 cntrivar 728
$ *civar name type factor init fc min max
$   20574100 "epb6" mult 5.3373e-4 183603.6 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20574101 cntrivar 601 cntrivar 605
$ *civar name type factor init fc min max
$   20574100 "epb7" mult 5.3248e-4 186613.6 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20574201 cntrivar 601 cntrivar 605
$ *civar name type factor init fc min max
$   20574300 "epb8" mult 5.164e-4 19644.7 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20574301 cntrivar 601 cntrivar 605
$ *civar name type factor init fc min max
$   20574400 "epb9" mult 6.12123e-4 213703.7 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20574401 cntrivar 601 cntrivar 605
$ *civar name type factor init fc min max
$   20574500 "cpip0" mult 6.4748e-4 222733.7 1.0
$ *civar variable name parameter no. variable name parameter no.
$   20574501 cntrivar 601 cntrivar 605
$ *civar name type factor init fc min max
$   20574600 "tsprpt5" function 2.9139e-4 2.9139 1.0
$ *civar srcharg name srch arg. no. table no.
$   20574601 time 0 606
$ *civar name type factor init fc min max
$   20574700 "rsdp16" function 1.1863e-4 1.1863 4.1 0
$ *civar srcharg name srch arg. no. table no.
$   20574701 time 0 607
$ *civar name type factor init fc min max
$   20574800 "adtp16" function 1.2370e-4 1.237 4.1 0
$ *civar srcharg name srch arg. no. table no.
$   20574801 time 0 608
$ *civar name type factor init fc min max
$   20574900 "rsprpt7" function 2.9617e-4 2.9617 4.1 0
$ *civar srcharg name srch arg. no. table no.
$   20574901 time 0 609
$ *civar name type factor init fc min max
$   20575000 "tsdp17" function 1.2058e-4 1.2058 4.1 0
$ *civar srcharg name srch arg. no. table no.
$   20575001 time 0 607

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$ *civar name type factor init fc min max
  20575100 "idkpi8" function 1.2573e-4 1.2573e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575101 time 0 608
$ =====
  *civar name type factor init fc min max
  20575200 "fspwpi8" function 3.1210e-4 3.1210e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575201 time 0 606
$ =====
  *civar name type factor init fc min max
  20575300 "fekpi8" function 1.2706e-4 1.2706e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575301 time 0 607
$ =====
  *civar name type factor init fc min max
  20575400 "adkpi8" function 1.3249e-4 1.3249e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575401 time 0 608
$ =====
  *civar name type factor init fc min max
  20575500 "fspwp8" function 3.3917e-4 3.3917e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575501 time 0 606
$ =====
  *civar name type factor init fc min max
  20575600 "fekwp8" function 1.3808e-4 1.3808e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575601 time 0 607
$ =====
  *civar name type factor init fc min max
  20575700 "adkwp8" function 1.4398e-4 1.4398e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575701 time 0 608
$ =====
  *civar name type factor init fc min max
  20575800 "fspw0" function 3.5350e-4 3.5350e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575801 time 0 606
$ =====
  *civar name type factor init fc min max
  20575900 "fekw0" function 1.4392e-4 1.4392e-4 1.0
  *
  *civar search name search arg. no. table no.
  20575901 time 0 607
$ =====
  *civar name type factor init fc min max
  20576000 "idkw0" function 1.5008e-4 1.5008e-4 1.0
  *
  *civar search name search arg. no. table no.
  20576001 time 0 608
$ =====
  *civar name type factor init fc min max
  20576100 "psum6" sum 1.0 5.3372e-4 1.0
  *
  *civar a0 coeff variable name parameter no.
  20576101 0.0 1.0 cntrivar 746
  20576102 1.0 cntrivar 747
  20576103 1.0 cntrivar 748
$ =====
  *civar name type factor init fc min max
  20576200 "psum7" sum 1.0 5.4248e-4 1.0
  *
  *civar a0 coeff variable name parameter no.
  20576201 0.0 1.0 cntrivar 749
  20576202 1.0 cntrivar 750
  20576203 1.0 cntrivar 751
$ =====
  *civar name type factor init fc min max
  20576300 "psum8" sum 1.0 5.7165e-4 1.0
  *
  *civar a0 coeff variable name parameter no.
  20576301 0.0 1.0 cntrivar 752
  20576302 1.0 cntrivar 753
  20576303 1.0 cntrivar 754
$ =====
  *civar name type factor init fc min max
  20576400 "psum9" sum 1.0 6.2123e-4 1.0
  *
  *civar a0 coeff variable name parameter no.
  20576401 0.0 1.0 cntrivar 755
  20576402 1.0 cntrivar 756
  20576403 1.0 cntrivar 757
$ =====
  *civar name type factor init fc min max
  20576500 "psum0" sum 1.0 6.4748e-4 1.0
  *
  *civar a0 coeff variable name parameter no.
  20576501 0.0 1.0 cntrivar 758
  20576502 1.0 cntrivar 759
  20576503 1.0 cntrivar 760
$ =====
  *civar name type factor init fc min max
  20576600 "pipow6" mult 1.0 0. 1.0
  *
  *civar variable name parameter no. variable name parameter no.
  20576601 cntrivar 600 cntrivar 605
  20576602 cntrivar 761
$ =====
  *civar name type factor init fc min max
  20576700 "pipow7" mult 1.0 0. 1.0
  *
  *civar variable name parameter no. variable name parameter no.
  20576701 cntrivar 600 cntrivar 605
  20576702 cntrivar 762
$ =====
  *civar name type factor init fc min max
  20576800 "pipow8" mult 1.0 0. 1.0
  *
  *civar variable name parameter no. variable name parameter no.
  20576801 cntrivar 600 cntrivar 605
  20576802 cntrivar 763
$ =====
  *civar name type factor init fc min max
  20576900 "pipow9" mult 1.0 0. 1.0
  *
  *civar variable name parameter no. variable name parameter no.
  20576901 cntrivar 600 cntrivar 605
  20576902 cntrivar 764
$ =====
  *civar name type factor init fc min max
  20577000 "pipow0" mult 1.0 0. 1.0
  *
  *civar variable name parameter no. variable name parameter no.
  20577001 cntrivar 600 cntrivar 605
  20577002 cntrivar 765
$ =====
  *civar name type factor init fc min max
  20577100 "p16" sum 1.0 18360.6 1.0

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*ctivar a0 coeff variable name parameter no.
20577101 0.0 1.0 cntrivar 741
$                                              cntrivar 766
*ctivar name type factor init fc min max
20577102 1.0 1.0 cntrivar 741
*ctivar name type factor init fc min max
20577200 "p17" sum 1.0 186613.6 1.0
*ctivar a0 coeff variable name parameter no.
20577201 0.0 1.0 cntrivar 742
20577202 1.0 1.0 cntrivar 767
$                                              cntrivar 768
*ctivar name type factor init fc min max
20577300 "p18" sum 1.0 196544.7 1.0
*ctivar a0 coeff variable name parameter no.
20577301 0.0 1.0 cntrivar 743
20577302 1.0 1.0 cntrivar 807
$                                              cntrivar 808
*ctivar name type factor init fc min max
20577400 "p19" sum 1.0 213703.7 1.0
*ctivar a0 coeff variable name parameter no.
20577401 0.0 1.0 cntrivar 744
20577402 1.0 1.0 cntrivar 769
$                                              cntrivar 770
*ctivar name type factor init fc min max
20577500 "p10" sum 1.0 222733.7 1.0
*ctivar a0 coeff variable name parameter no.
20577501 0.0 1.0 cntrivar 745
20577502 1.0 1.0 cntrivar 820
$                                              cntrivar 821
*ctivar name type factor init fc min max
20580100 binary tripunit 1.0000d+00 0. 0.3 .00 1.0000d+00
*ctivar trip no.
20580101 550
$                                             
*ctivar name type factor init fc min max
20580200 flow sum 1.0000d+00 14.6141 0
*ctivar a0 coeff variable name parameter no.
20580201 0. 1. milflow 83010000
*ctivar name type factor init fc min max
20580300 flow mult 1.0000d+00 0. 0
*ctivar variable name parameter no. variable name parameter no.
20580301 cntrivar 801
*ctivar name type factor init fc min max
20580400 inflow integral 1.0000d+00 0. 0
*ctivar integrand name integrand no.
20580401 cntrivar 803
*ctivar name type factor init fc min max
20580500 binary tripunit 1.0000d+00 0. 0.3 .00 1.0000d+00
*ctivar trip no.
20580501 551
$                                             
*ctivar var_name parameter no. var_name parameter no.
20580601 cntrivar 943
*ctivar name type factor init fc min max
20580700 nprpm sum 1.0000d+00 1. 0.3 .00 1.0000d+00
*ctivar a0 coeff variable name parameter no.
20580701 0. 1. cntrivar 807
20580702 1. 1. cntrivar 806
$                                             
*ctivar name type factor init fc min max
20581500 mpersp sum 239.4547 239.4547 0.3 .00 239.4547
*ctivar a0 coeff variable name parameter no.
20581501 0. 1. cntrivar 807
$                                             
*ctivar name type factor init fc min max
20582000 stoprs function 1.0000d+00 0. 0.3 .00 239.4547
*ctivar strch arg_name search arg_no. table no.
20582001 time 0 820
$                                             
*ctivar name type factor init fc min max
20583000 stoprs mult 1.0000d+00 0. 0.3 .00 239.4547
*ctivar variable name parameter no. variable name parameter no.
20583001 cntrivar 820
*ctivar name type factor init fc min max
20583100 dp-505 mult 0.381903 24945.97 1
*ctivar variable name parameter no. variable name parameter no.
20583101 fwall 503010000 velj 507010200
*ctivar name type factor init fc min max
20583200 dp-520 mult 0.0123387 159.7177 1
*ctivar variable name parameter no. variable name parameter no.
20583201 fwall 520010000 velj 522010100
*ctivar name type factor init fc min max
20583300 dp-535 mult 0.010047 121.5195 1
*ctivar variable name parameter no. variable name parameter no.
20583301 fwall 535010000 velj 537010200
*ctivar name type factor init fc min max
20583400 dp-555 mult 0.191472 2837.923 1
*ctivar variable name parameter no. variable name parameter no.
20583401 fwall 555010000 velj 556010100
$                                             
*Delta P in average fuel channels including entrance and exit losses
*ctivar name type factor init fc min max
20580600 durnpm mult -1.0000d+00 0. 0.3 -1.00 1.0000d+00
$                                             

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*ctvar name type factor init fc min max
20583500 kcdtip sum 1.0 1708/09.0 0
*ctvar a0 coeff variable name parameter no.
20583501 0.0 1.0 p cntrivar 52/0010000
20583502 1.0 cntrivar 832
*ctvar name type factor init fc min max
20583600 kcdtip sum 1.0 1514/19.0
*ctvar a0 coeff variable name parameter no.
20583601 0.0 1.0 p cntrivar 50/5010000
20583602 -1.0 cntrivar 831
20583603 -1.0 cntrivar 835
*ctvar name type factor init fc min max
20583700 uccxip sum 1.0 1690/09.0
*ctvar a0 coeff variable name parameter no.
20583701 0.0 1.0 p cntrivar 55/5010000
20583702 1.0 cntrivar 834
*ctvar name type factor init fc min max
20583800 uedclap sum 1.0 1512/62.0
*ctvar a0 coeff variable name parameter no.
20583801 0.0 1.0 p cntrivar 53/5010000
20583802 -1.0 cntrivar 833
20583803 -1.0 cntrivar 837
* control variables to develop total reactivity for kinetics model
* (cntrivar 572 is total reactivity driving the kinetics model)
* first order lag applied to sensor location pressure
*ctvar name type factor init fc min max
20583900 lagpres lag 1.00000d+00 1585/146. 0
*ctvar tau=1 variable name parameter no.
20583901 0.03 p
* control system to control primary coolant system pressure by
* adjusting the kldown flow area using:
* d=K*(P-Ps)
* dx/dt=(d-x)/tau
* where:
* K = proportional constant = 5/NPa
* tau = time constant = 1 s
* P = measured sensor pressure
* Ps = setpoint pressure = 3.2 MPa
* d = demand (CV 840)
* x = valve position
* =-1 for fully closed,
* =1 for fully open,
* =0 at normal position
* NOTE: kldown valve orifice area = 0.00028355 m^2
* (calibrated for half-open valve at x=0)
* 2058400 pctrl sum 5.002246796 1.0
* 20584001 -1.690000 1.e-6 cntrivar 837
* SF = A0, multiplier on CV860 = 1/A0
* 20584200 dach sum .5 3/9108.4 10
* 20584201 1.0 -2. cntrivar 860

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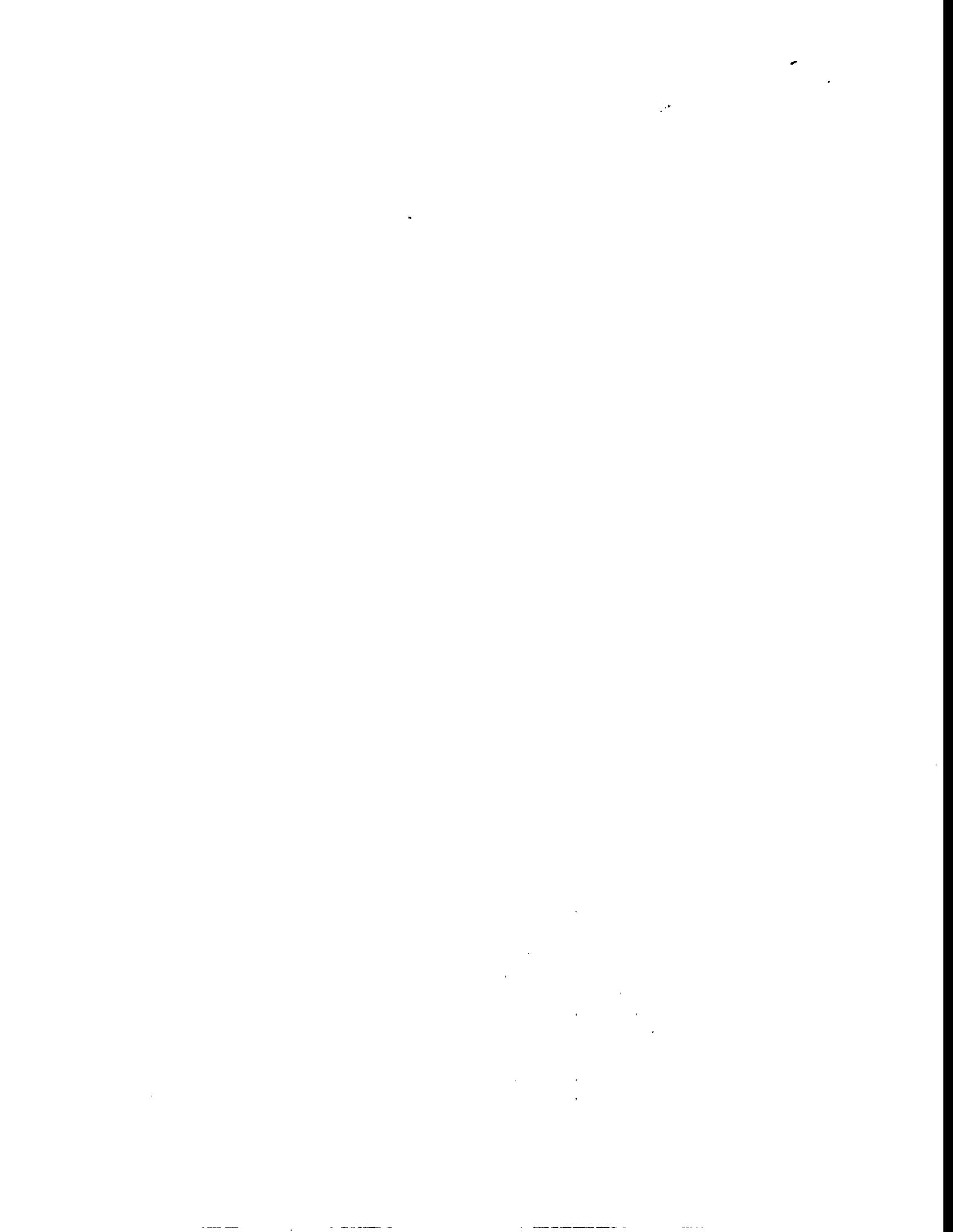
*ctvar a0 coeff variable name parameter no.
20590301 0. 1. rho 545010000
20590302 1. rho 545020000
20590303 1. rho 545030000
20590304 1. rho 545040000
20590305 1. rho 545050000
*ctvar name type factor init fc min max
20590400 rho sum 1.00000d+00 1.754422 -1
*ctvar a0 coeff variable name parameter no.
20590401 -467.766 0.7600 ctivar 900
20590402 0.7600 ctivar 901
20590403 0.2267 ctivar 902
20590404 0.2267 ctivar 903
*ctvar name type factor init fc min max
20590500 ctivar sum 7.50000d-02 0121447 -1
*ctvar a0 coeff variable name parameter no.
20590501 0. 0.0922978 ctivar 904
*ctvar name type factor init fc min max
20590800 c510dm sum 7.69000d-02 13.9115 -1
*ctvar a0 coeff variable name parameter no.
20590801 0. 1. hvat 5101001
20590802 -.5 hvat 5102001
20590803 -.5 hvat 5103001
20590804 1. hvat 5101002
20590805 -.5 hvat 5102002
20590806 -.5 hvat 5103002
20590807 1. hvat 5101003
20590808 -.5 hvat 5102003
20590809 -.5 hvat 5101004
20590810 1. hvat 5102004
20590811 -.5 hvat 5103004
20590812 1. hvat 5101005
20590813 1. hvat 5102005
20590814 -.5 hvat 5103005
20590815 -.5 hvat 5103005
*ctvar name type factor init fc min max
20590900 c515dm sum 3.22000d-04 11.64084 -1
*ctvar a0 coeff variable name parameter no.
20590901 0. 1. hvat 5151001
20590902 -.5 hvat 5152001
20590903 -.5 hvat 5153001
20590904 1. hvat 5151002
20590905 -.5 hvat 5152002
20590906 -.5 hvat 5153002
20590907 1. hvat 5151003
20590908 -.5 hvat 5152003
20590909 -.5 hvat 5153003
20590910 1. hvat 5151004
20590911 -.5 hvat 5152004
20590912 -.5 hvat 5153004
20590913 1. hvat 5151005
20590914 -.5 hvat 5152005
20590915 -.5 hvat 5153005
*ctvar name type factor init fc min max
20591000 c510dm sum 1.22000d-01 249.3547 -1
*ctvar a0 coeff variable name parameter no.
20591001 0. 1. hvat 5401001
20591002 -.1 hvat 5402001
20591004 1. hvat 5401002
*ctvar name type factor init fc min max
20591100 c545dm sum 2.90000d-04 544613 -1
*ctvar a0 coeff variable name parameter no.
20591101 0. 1. hvat 5451001
20591102 -.1 hvat 5452001
20591104 1. hvat 5451002
20591105 -.1 hvat 5452002
20591107 1. hvat 5451003
20591108 -.1 hvat 5452003
20591110 1. hvat 5451004
20591111 -.1 hvat 5452004
20591113 1. hvat 5451005
20591114 -.1 hvat 5452005
*ctvar name type factor init fc min max
20591200 ctifsp sum 1.00000d+00 22.4217 -1
*ctvar a0 coeff variable name parameter no.
20591201 -89.1343 0.7600 ctivar 908
20591202 0.7600 ctivar 909
20591203 0.2267 ctivar 910
20591204 0.2267 ctivar 911
*ctvar name type factor init fc min max
20591300 capaux sum -6.90000d-04 0.138794 -1
*ctvar a0 coeff variable name parameter no.
20591301 0. 1. ctivar 912
*ctvar name type factor init fc min max
20591700 rho sum 1.00000d+00 .058618 -1
*ctvar a0 coeff variable name parameter no.
20591701 -1085.52 0.14536 rho 55310653
20591702 0.07207 rho 505010000
20591703 0.12983 rho 53010000
20591704 0.01712 rho 53020000
20591705 0.01712 rho 53030000
20591706 0.01453 rho 53040000
20591707 0.01453 rho 53050000
20591708 0.01453 rho 53060000
20591709 0.18451 rho 553010000
20591710 0.01550 rho 553010000
20591711 0.12177 rho 52520000
20591712 0.35263 rho 553010000
*ctvar name type factor init fc min max
20591800 axmordr sum 3.33000d-02 -1.806175-4 -1
*ctvar a0 coeff variable name parameter no.
20591801 0. 0.0921472 ctivar 917
*ctvar name type factor init fc min max
20592200 rho sum 1.00000d+00 4.508318 -1

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* 20592300 midptr sum 3.33000d-02 .01378562 1
* civar a0 coeff variable name parameter no.
20592301 0. 0.0918291 cntrvar 922
$ *civar name type factor init fc min max
20592700 "prelim" sum 1. 500.52710
* civar a0 coeff variable name parameter no.
20592701 0. 0.24883 rho 560010000
20592702 0. 0.00659 rho 561010000
20592703 0. 0.00669 rho 561020000
20592704 0. 0.00659 rho 561030000
20592705 0. 0.02418 rho 562010000
20592706 0. 0.02418 rho 562020000
20592707 0. 0.02418 rho 562030000
20592708 0. 0.001936 rho 563010000
20592709 0. 0.001936 rho 563020000
20592710 0. 0.001936 rho 563030000
20592711 0. 0.00888 rho 561040000
20592712 0. 0.00888 rho 561050000
20592713 0. 0.00438 rho 561060000
20592714 0. 0.03206 rho 562040000
20592715 0. 0.03206 rho 562050000
20592716 0. 0.01581 rho 562060000
20592717 0. 0.00257 rho 563040000
20592718 0. 0.00257 rho 563050000
20592719 0. 0.00127 rho 563060000
$ *civar name type factor init fc min max
20592800 rho sum 1.00000d+00 .9188 1 0
* civar a0 coeff variable name parameter no.
20592801 -1095.32 1.0 cntrvar 927
20592802 0.008274 rho 561070000
20592803 0.008274 rho 561080000
20592804 0.02266 rho 562070000
20592805 0.02266 rho 562080000
20592806 0.001815 rho 563070000
20592807 0.001815 rho 563080000
20592808 0.005497 rho 561090000
20592809 0.003407 rho 561100000
20592810 0.005407 rho 561110000
20592811 0.01953 rho 562090000
20592812 0.01953 rho 562100000
20592813 0.01953 rho 562110000
20592814 0.001564 rho 563090000
20592815 0.001564 rho 563100000
20592816 0.001564 rho 563110000
20592817 0.403272 rho 564010000
* civar name type factor init fc min max
20592900 cntr var sum 9.10000d-02 .00763345 1
* civar a0 coeff variable name parameter no.
20592901 0. 0.0912975 cntrvar 928
* civar name type factor init fc min max
20593400 tankrx sum -1.74000d-02 .02925516 1
* nominal power = 350,000,000 W and nominal flow = 2000 kg/s
20594000 powerflow div 6.06061d-06 1.041574 0
* civar divisor name divisor no. dividend name dividend no.
20594001 mflowj 650010000 rtkpow 0

```



APPENDIX B: FORTRAN USED TO LOAD RELAP5 INPUT FILE WITH FUEL SOURCE TERMS (power.f)

```

c This program modifies the ans RELAPS input
c fuel heat structure source terms
c implicit double precision (a-h,p-z)
c character*80 arec
c
c Variable Definition
c avpdh - average power density in upper core average fuel ht str
c avpdh - average power density in lower core average fuel ht str
c avpdh - average power density in upper core hot fuel ht str
c avpdh - average power density in lower core hot fuel ht str
c avpdh - avg pwr density in upper core hot stripe ht str (CHF, FE)
c avpdh - avg pwr density in lower core hot stripe ht str (CHF, FE)
c pduchs - power density, upper core, average channel
c pduchs - power density, upper core, hot stripe (CHF, FE)
c pduchs - power density, lower core, average channel
c pduchs - power density, lower core, hot channel (CHF, FE)
c pduchs - power density, lower core, hot stripe (CHF, FE)
c pd95hc - peaking factor, 95% uncertainty, hot channel
c pd95hc - peaking factor, 95% uncertainty, hot stripe (CHF, FE)
c pd95hc - peaking factor, 99.9% uncertainty, hot channel
c pd95hc - peaking factor, 99.9% uncertainty, hot stripe (CHF, FE)
c
c real mavg1, mavg2, m195, m199, mu99, mu95
c dimension avpdhs(2), avpdls(2)
c dimension pduchs(5), pduchs(5,1)
c dimension pduchs(5), pduchs(5,2)
c dimension pduchs(5), pduchs(5,3)
c dimension pd95hc(5), pd95hc(5,1)
c dimension pd95hc(5), pd95hc(5,2)
c dimension pd95hc(5), pd95hc(5,3)
c open(unit=1,file='IND1',status='old', form='formatted')
c open(unit=23,file='pd.dat',status='old', form='formatted')
c open(unit=24,file='pd.dat',status='old', form='formatted')
c open(unit=22,file='IND2',status='unknown', form='formatted')
c
c read in power densities and peaking factors
c
c power densities
c
c read(23,9998)arec
c read(23,9998)arec
c read(23,9998)arec
c read(23,9998)arec
c read(23,9998)arec
c do 5 i=1,5
c   read(23,9992)iz, pducac(iz), pduchs(iz,1), pduchs(iz,2)
c   do 6 i=1,5
c     read(23,9998)arec
c   do 9 iz=1,5
c     read(24,9992)iz, pf69hs(iz), pf69hs(iz,1),
c     pf69hs(iz,2)
c     read(24,9998)arec
c     read(24,9998)arec
c     read(24,9998)arec
c     read(24,9998)arec
c     read(24,9998)arec
c     do 16 j=1,5
c       read(24,9992)iz, pf69hs(iz), pf69hs(iz,1),
c       pf69hs(iz,2)
c
c calculate average power densities
c
c avpdus = (pduacs(1)+pducac(2)+pducac(3)+pducac(4)
c           + pducac(5))/5
c
c avpdla = (pduchs(1)+pduchs(2)+pduchs(3)+pduchs(4)
c           + pduchs(5))/5.
c
c calculate the power fractions
c
c hot channels
c
c   m199 = avpdh*avpdla*pf69hc(1)/252.
c   m195 = avpdh*avpdla*pf69hc(11)/22.
c   mu99 = avpdh*avpdla*pf69hc(11)/422.
c   mu95 = avpdh*avpdla*pf69hc(11)/432.
c
c average channels
c
c   mavg1 = 1. - m199 - mu99 - mu95
c   mavg2 = 1. - mu99 - mu95
c
c zero summations
c
c   sumf = 0.
c   sumof = 0.
c   sumch1 = 0.
c   sumch2 = 0.
c   sumc1l = 0.
c   sumc2l = 0.
c   sumc1o = 0.
c   sumc2o = 0.
c   sumosp = 0.
c   sumopc = 0.
c
c Read input data to modify heat structure sources
c
c 10 read(21,9998,end=999)arec
c
c IF THIS IS A HEAT STRUCTURE CARD
c   if(arec(1:1).eq.'1', and,arec(8:8).ne.' ') and,
c     arec(6:6).eq.'7') then
c     ipbr = 9
c     ipbr = iread(iptr,arec)
c     if(iv1.ne.0) then
c       w2 = dread(iptr,arec)
c       v3 = dread(iptr,arec)
c       w4 = dread(iptr,arec)
c       w5 = iread(iptr,arec)
c     endif
c
c IF THE SOURCE TERM IS 1000 (POINT KINETICS)
c   if(iv1.eq.1000) then
c     read(arec(8:8),'(1)')n
c
c LOWER FUEL LOWER FUEL LOWER FUEL LOWER FUEL
c
c LOWER FUEL LOWER FUEL LOWER FUEL LOWER FUEL
c
c IF THIS HEAT STRUCTURE IS IN THE LOWER FUEL
c   if(arec(3:3).eq.'1') then
c     c average fuel heat structure
c     if(arec(2:5).eq.'5101') then
c       w2 = 0.05118*mu99*pdlcac(n)/avpdla
c       w3 = 2.56d-4*mu99*pdlcac(n)/avpdla
c       w4 = 0.0
c       sumif = sumif+w2
c       sumcl = sumcl+w3
c       sumch = sumch+w4
c     else if(arec(2:5).eq.'5102') then
c       w2 = 4.38d-4*mu99*pdlcac(n)/avpdla
c       w3 = 1.174d-3*mu99*pdlcac(n)/avpdla
c       w4 = 0.0
c       sumif = sumif+w2
c       sumcl = sumcl+w3
c       sumch = sumch+w4
c
c outer side place heat structure
c

```

```

else if(arec(2:5).eq.'5103') then
  w2 = 3.92d-4*navg1*pdlchc(n)/avpdih
  w3 = 0.0
  w4 = 7.28d-4*ml99*pdlchc(n)/avpdih
  sumisp = sumisp+w2
  sumcll = sumcll+w4
  c 95% 95% 95% 95% 95% 95% 95% 95% 95% 95%
  c hot channel fuel plate
  c sumcll = sumcll+w3+w4
  c sumif = sumif+w2
  sumcll = sumcll+w3+w4
  c hot channel inner side Plate heat structure
  else if(arec(2:5).eq.'5151') then
    w2 = 0.05118*ml99*pdlchc(n)/avpdih
    w3 = 2.56d-4*ml99*pdlchc(n)/avpdih
    w4 = 0.0
    sumisp = sumisp+w2
    sumif = sumif+w4
    sumcll = sumcll+w3+w4
    c hot channel outer side Plate heat structure
    else if(arec(2:5).eq.'5152') then
      w2 = 4.38d-4*ml99*pdlchc(n)/avpdih
      w3 = 1.17d-3*ml95*pdlchc(n)/avpdih
      w4 = 0.0
      sumisp = sumisp+w2
      sumif = sumif+w4
      sumcll = sumcll+w3+w4
      c hot channel inner side Plate heat structure
      else if(arec(2:5).eq.'5153') then
        w2 = 3.92d-4*ml95*pdlchc(n)/avpdih
        w3 = 0.0
        w4 = 7.28d-4*ml95*pdlchc(n)/avpdih
        sumisp = sumisp+w2
        sumif = sumif+w4
        sumcll = sumcll+w3+w4
        c hot channel outer side Plate heat structure
        else if(arec(2:5).eq.'5154') then
          w2 = ml95/5.*0.2559/100.
          a1 = ml95/5.*0.2559/100.
          a2 = (pdlchc(1,1)*p995hs(1,1)+pdlchc(2,1)*p995hs(2,1)+pdlchc(3,1)*p995hs(3,1)+pdlchc(4,1)*p995hs(4,1)+pdlchc(5,1)*p995hs(5,1))/5.
          a3 = (pdlchc(1)*p99hc(1,1)+pdlchc(2)*p99hc(2,1)+pdlchc(3)*p99hc(3,1)+pdlchc(4)*p99hc(4,1)+pdlchc(5)*p99hc(5,1))/5.
          w2 = pdcns(n,1)/avpdis(1)*a1+a2/a3
          w3 = 0.
          w4 = 0.
        sumif = sumif+w2
        sumcll = sumcll+w3+w4
        c CHP hot stripe heat structure
        else if(arec(2:5).eq.'5164') then
          a1 = ml99/5.*0.2555/100.
          a2 = (pdlchc(1,2)*p99hs(1,2)+pdlchc(2,2)*p99hs(2,2)+pdlchc(3,2)*p99hs(3,2)+pdlchc(4,2)*p99hs(4,2)+pdlchc(5,2)*p99hs(5,2))/5.
          a3 = (pdlchc(1)*p99hc(1,1)+pdlchc(2)*p99hc(2,1)+pdlchc(3)*p99hc(3,1)+pdlchc(4)*p99hc(4,1)+pdlchc(5)*p99hc(5,1))/5.
          w2 = pdcns(n,2)/avpdis(2)*a1+a2/a3
          w3 = 0.
          w4 = 0.
        sumif = sumif+w2
        sumcll = sumcll+w3+w4
        endif
        c
        write(arec(9:20),9988)w1,w2,w3,w4,iw5
        do 12 i1=80
        iflarec(i1:i1).eq.'D') arec(i1:i1)=d'
        iflarec(i1:i1).eq.'E') arec(i1:i1)=e'
        12
        c upper fuel heat structures
        c upper fuel upper fuel upper fuel upper fuel
        * c IF THIS HEAT STRUCTURE IS IN THE UPPER FUEL
        * c average fuel heat structure
        * c upper fuel upper fuel upper fuel upper fuel
        * c upper fuel upper fuel upper fuel upper fuel
        * c inner side plate heat structure
        else iflarec(3:3).eq.'4') then
          w2 = 2.71d-4*mavgupdudac(n)/avpdua
          w3 = 6.080d-4*mavgupdudac(n)/avpdua
          w4 = 0.0
          sumof = sumof+w2
          sumcll = sumcll+w1+w4
        c outer side plate heat structure
        else iflarec(2:5).eq.'5403') then
          w2 = 3.25d-4*mavgupdudac(n)/avpdua
          w3 = 0.0
          w4 = 6.00d-4*mavgupdudac(n)/avpdua
          sumof = sumof+w2
          sumcll = sumcll+w1+w4
        c 95% 95% 95% 95% 95% 95% 95% 95% 95% 95%
        c hot channel fuel plate
        c sumcll = sumcll+w3+w4
        c hot channel inner side Plate heat structure
        else iflarec(2:5).eq.'5162') then
          w2 = 0.05118*ml99*pdlchc(n)/avpdih
          w3 = 2.56d-4*ml99*pdlchc(n)/avpdih
          w4 = 0.0
        sumif = sumif+w2
        sumcll = sumcll+w3+w4
        c hot channel outer side Plate heat structure
        else iflarec(2:5).eq.'5163') then
          w2 = 0.117d-3*ml95*pdlchc(n)/avpdih
          w3 = 0.0
          sumif = sumif+w2
          sumcll = sumcll+w3+w4
        c hot channel inner side Plate heat structure
        else iflarec(2:5).eq.'5451') then
          w2 = 0.1306*ml95*pdlchc(n)/avpdih
        c
      end
    end
  end
end

```



```

sumpc = sumpc + (w3 + w4)*794812./3.44d8
else if(iwl.eq.10613) then
  sum613 = sum613 + w2*7585./3.44d8
  sumpc = sumpc + (w3 + w4)/7385./3.44d8
else if(iwl.eq.10671) then
  sum671 = sum671 + w2*42622./3.44d8
  sumpc = sumpc + (w3 + w4)*425622./3.44d8
else if(iwl.eq.10672) then
  sum672 = sum672 + w2*433784./3.44d8
  sumpc = sumpc + (w3 + w4)*433784./3.44d8
else if(iwl.eq.10673) then
  sum673 = sum673 + w2*435848./3.44d8
  sumpc = sumpc + (w3 + w4)*435848./3.44d8
else if(iwl.eq.10674) then
  sum674 = sum674 + w2*423464./3.44d8
  sumpc = sumpc + (w3 + w4)*423464./3.44d8
else if(iwl.eq.10675) then
  sum675 = sum675 + w2*342903./3.44d8
  sumpc = sumpc + (w3 + w4)*342903./3.44d8
else if(iwl.ne.0) then
  write(6,9934) iwl
endif
endif
write(22,9998) arec
go to 10
999 continue
sum734 = sum774+sum773+sum773+sum771+sum73+
totlk = sumlf+sumfp+sumoch
write(6,9999) sumlf,sumfp,sumoch,totlk,sumcl,
.sumclu,sumclu,
write(6,9995) sumpb,sum642,sum643,sum613,sum671,
.sum672,sum673,sum674,sum675,sumpc
+sumclu+sumclu+sumoch+sumpc
9999 format(''Lower Fuel Heating      ''/E10.7,'/
           'Upper Side-Plate Heating   ''/E10.7,'/
           'Upper Fuel Heating        ''/E10.7,'/
           'Upper Side-Plate Heating  ''/E10.7,'/
           'Other Heating (1000)     ''/E10.7,'/
           'Total Heating for 1000    ''/E10.7.''/,
           'Lower Side-Plate Heating   ''/E10.7,'/
           'Upper Fuel Heating        ''/E10.7,'/
           'Upper Side-Plate Heating  ''/E10.7,'/
           'CBT Coolant               ''/E10.7,'/
           'Structures for Gamma Heating in CR Region ''/,
           'CV613                   ''/E10.7,'/
           'CV672                   ''/E10.7,'/
           'CV673                   ''/E10.7,'/
           'CV674                   ''/E10.7,'/
           'CV675                   ''/E10.7,'/
           'Control Rod Coolant     ''/E10.7,'/
           'GRAND TOTAL             ''/E10.7)
9995 format(''//, GRAND TOTAL ''/E10.7)
9994 format(''*** WARNING *** SOURCE ''/E16, ASSURED TO BE ZERO AT S
9993 format(''READY STATE'')
9992 format(''4f10.7)
9999 format(''Input factor by which to multiply hot channel fuel heat s
.structures'')
9998 format(''1x,16.3(1x,15,1pd14.7)1x,16.8x)
9987 format(''lx,84,1x,15,3lx,di2.6,1x,13)
end
c Function to read a real number
c Function dread(lptr,arec)
c Finds the first real number on the record after the lptr character
character=80 arec
character=80 arec
format = '(          )'
do 10 i=lptr+1,80
  if(arec(i:i).ne. ' ') then
    character=10 aread
    character=80 arec
    character=5 format
    format = '(          )'
    do 10 i=lptr+1,80
      if(arec(i:i).ne. ' ') then
        go to 15
      endif
    10 continue
    return
  15 do 20 i=lptr+1,80

```

```
if(arec(i:i);eq.' ') then
    length = i-i1
    iptr = i
    go to 25
endif
20 continue
25 continue
    if(length.lt.10) then
        write(format(3:4),'(a1,i1)') 'a',length
    else
        write(format(2:4),'(a1,i2)') 'a',length
    endif
    read(arec(i1:i1+length-1),format) area1d
return
end
```



APPENDIX C: RELAP5 INPUT FOR MAIN HEAT EXCHANGER COMPARISON WITH DATA

```

*advanced neutron source relap5 system model
 0000001 8 10 22
 00000100 new transit
 00000101 run
 00000102 s1 s1
 00000105 30. 40. 1800.
 00000110 nitrogen
 00000120 106010000 0. d20 primary
 00000232 100.0 1.e-7 0.01 03 100 100000 100000
* minor edit requests
 00000301 mflowj 11.3 010000
 00000308 entrivar 45 106010000
 00000312 p 112010000
 00000313 p
 10400000 source tndpvol
 10400101 0.0832 1.0 0.0 vol. 0. 0. 0. 0.0000457 0.3255 0
 1040200 3 0
 1040201 0. 1.527020e6 354.15
*
* component name component type
*      'pricdij'      'amcpjun'
 1210000
* hydro from to area
 1210101 113010000 122000000 0.08322
* hydro val/flw trip no.
 1210200 1 0 alpha vrc numeric vrc
* hydro time f flow g flow j flow
 1210201 0. 705. 705. 705.
 1220000 sink tndpvol
 1220101 0.0832 1.0 0.0 vol. 0. 0. 0.0000457 0.3255 0
 1220200 3 0
 1220201 0. 1.5e6 357.068
*
* component name component type
*      'hxolin'      'branch'
 1060000
* hydro no. juns val/flw
 1060001 2 0
* hydro area length volume
 1060101 0.08322 1.0 0.
* hydro horz angle vert angle delta z
 1060102 0. 0. 0.
* hydro roughness hyd diam fe
 1060103 0.0000457 0.3555 0
* hydro cbt pressure temp
 1060200 155898. 325442. 2411284. 0.
*
* hydro from to area f loss r loss vchis
 1060101 10600000 10600000 0. 0. 0. 0.1000
 1060201 10400000 10600000 0. 0. 0. 0.1000
* hydro hyd diam
 1061100 0.3255 0. 0. 1.0
 1062110 0.3255 0. 0. 1.0
* hydro f velocity g velocity j velocity
 1061201 7.85898 7.85898 0. * 705.
 1062201 7.85898 7.85898 0. * 705.
*
* component name component type
*      'hydro'      'pipe'
 1080000 *mix-prim*
 1080001 11
* hydro vol area
 1080101 0.8258
 1080102 0.8258
 1080103 0.8258
* hydro length
 1080301 1.11
 1080302 2.03
 1080303 1.11
* hydro volume
 1080401 0.
* hydro vert angle
 1080501 0.
* hydro delta z
 1080701 0.0
* hydro roughness hyd diam
 1080801 0.000057 0.536
 1080802 0.000057 0.594
 1080803 0.000057 0.636
* hydro fe
 1080001 00
* hydro vchis
 1081101 01000
* hydro ebt pressure temp
 1081201 0 1552339. 294260. 2411199. 0. 0.1
 1081202 0 1552334. 267031. 2411199. 0. 0.2
 1081203 0 1552328. 24136.4 2411199. 0. 0.3
 1081204 0 1552322. 22074. 2411199. 0. 0.4
 1081205 0 1552316. 204427.8 2411199. 0. 0.5
 1081206 0 1552320. 204427.8 2411199. 0. 0.6
 1081207 0 1552329. 188400. 15523200. 193865.8 2411199. 0. 0.7
 1081208 0 1552292. 108400. 1552292. 189772. 2411199. 0. 0.8
 1081209 0 1552285. 108400. 1552285. 189772.7 2411199. 0. 0.9
 1081210 0 1552277. 108400. 1552277. 189772.4 2411199. 0. 0.10
 1081211 0 1552270. 108400. 1552270. 189772.4 2411199. 0. 0.11
* hydro f velocity g velocity j velocity
 1081300 0
* hydro component name component type
 1081301 'hydro' 'expolt1'
 1081302 'hydro' 'expolt1'
 1081303 'hydro' 'expolt1'
 1081304 'hydro' 'expolt1'
 1081305 'hydro' 'expolt1'
 1081306 'hydro' 'expolt1'
 1081307 'hydro' 'expolt1'
 1081308 'hydro' 'expolt1'
 1081309 'hydro' 'expolt1'
 1081310 'hydro' 'expolt1'
* hydro no. juns val/flw
 1120000 2 0
* hydro area
 1120001 0.08322
* hydro no. juns val/flw
 1120101 2 0
* hydro length
 1120102 1.0
* hydro horz angle vert angle
 1120103 0. 0.
* hydro roughness hyd diam
 1120103 0.3255
* hydro ebt pressure temp
 1120200 1554344. 182767.6 2410712. 0. 0.
* hydro component name component type
 1120301 'hydro' 'expolt1'
* hydro volume
 1120302 0.
* hydro delta z
 1120303 0.
* hydro fe
 1120304 0.

```

```

* hydro from to area f loss r loss vcahs
1121101 108010000 112000000 0.08322 0.15 0.15 0.1000
1122101 112010000 113000000 0.08322 0. 0. 0.1000
* hydro hyd diam
112110 0.355 0.1 0 1.0
112210 0.3255 0.0 1.0 1.0
* hydro f velocity g velocity j velocity
1121201 7.71669 0. * 705. *
1122201 7.71681 0. * 705. *
* hydro component name component type
1130000 "Joinhx" Pipe
* hydro vol area
1130101 0.08322
* hydro length
1130301 1.981
1130302 1.23
1130303 0.6036
* hydro volume
1130401 0.
* hydro vert angle
1130601 -22.6
1130602 -29.7
1130603 -30.
* hydro elev. change
1130701 -0.762
1130702 -0.6093
1130703 -0.6096
* hydro roughness hyd diam
1130801 0.000457 0.3255
* hydro f loss r loss
1130901 0.182 0.182
* hydro f0
1131001 0.0
* hydro vcahs
1131101 0.0000
* hydro obt pressure tempe
1131201 0 1516478. 187730. 2410740. 0. 0. 1
1131202 0 1515786. 187731.5 2410730. 0. 0. 2
1131203 0 1515177. 182731.8 2410723. 0. 0. 3
* hydro vel/flw
1131300 0
* hydro f flowrate g flowrate j flowrate
1131301 7.71681 7.71681 0. 1 * 705.
1131302 7.71681 7.71681 0. 1 * 705.
$ main heat exchanger secondary flow system (tube side)
* hydro component name component type
"secrel" timdpvol
* hydro area length volume
1300101 1.0e6 .0 1.0e+06
* hydro horz angle vert angle delta z
1300102 .0 .0 .0
* hydro roughness hyd diam fe
1300103 .0 .0 10
* hydro ebt trip no. alpha vrc numeric vrc
1300200 003 * hydro time 5.0000e5 tempe 302.15
* hydro component name component type
"secdj" timdpjun
* hydro from to area
1320101 130000000 0.7122
* hydro vel/flw trip no. alpha vrc numeric vrc
1320200 1 * 134000000 0.7122
* hydro time f flow g flow j flow
1320202 10. 1490. 1490. 0
* hydro component name component type
"mbx-sec" Pipe
1340000 10
* hydro vol area
1340101 0.776
* hydro length
1340301 1.314
* hydro volume
1340401 0.
* hydro vert angle
1340601 0.
* hydro delta z
1340701 0.0
* hydro roughness hyd diam
1340801 0.0000457 0.01588
* hydro fe
1341001 00
* hydro vcahs
1341101 01000
* hydro obt pressure tempe
1341201 484599. 130261.4 2556934. 0. 0. 1
1341202 0 480112. 140233. 0. 0. 2
1341203 0 475815. 2556362. 0. 0. 3
1341204 0 471478. 164434.7 258074. 0. 0. 4
1341205 0 467162. 171915.7 2557786. 0. 0. 5
1341206 0 462826.5 180783. 2557494. 0. 0. 6
1341207 0 458169. 182518. 2557159. 0. 0. 7
1341208 0 454114. 184472.4 2556902. 0. 0. 8
1341209 0 449762. 186629.4 2556602. 0. 0. 9
1341210 0 445413. 189015. 2556300. 0. 0. 10
* hydro jun hyd diam f velocity g velocity
1341300 0 0.01588 0.0 1.0 1.0
* hydro component name component type
"tubeout" snglpjun
* hydro from to area f loss g loss vcahs
1350000 1350000 1.938347 1.938347 0.9 * 1490. jun 9

```



```

20100109    1000.          25.3
20100110    1200.          28.1
20100111    1400.          30.9
20100112    20000.         30.9
+
*compn      temperature      vol ht cap
20100151    273.2          10.0
20100152    20000.          10.0
*20100151    250.           2.97e6
*20100152    478.           3.00e6
*20100153    700.           3.19e6
*20100154    811.           3.28e6
*20100155    866.           3.38e6
*20100156    922.           3.48e6
*20100157    1033.          3.58e6
*20100158    1200.          3.78e6
*20100159    1311.          3.88e6
*20100160    1400.          3.88e6
*20100161    20000.         3.88e6
+
20504500  heater sum   108300100  385.342
20504501  0. 1..htnr 108300100 -100632184.  0
20504502  1..htnr 108300200
20504503  1..htnr 108300300
20504504  1..htnr 108300400
20504505  1..htnr 108300500
20504507  1..htnr 108300600
20504508  1..htnr 108300700
20504509  1..htnr 108300800
20504510  1..htnr 108300900
20504511  1..htnr 108301000
.
end of case

```

APPENDIX D: RELAP5 INPUT FOR EMERGENCY HEAT EXCHANGER COMPARISON WITH DATA

* hydro f velocity g velocity j velocity
 1141201 7.72324 7.72324 0. * 706.
 1142201 7.72335 8.32625 0. * 706.

* hydro component name component type
 1160000 * elix-prm Pipe

1160001 4

* hydro vol area
 1160101 0.894

* hydro length
 1160301 1.6

* hydro volume
 1160401 0.

* hydro vert angle
 1160601 0.

* hydro delta z
 1160701 0.0

* hydro roughness hyd diam
 1160801 0.000457 0.0346
 1160801 0.000457 0.00170

* hydro f loss r loss
 1160901 0.0 0.0

* hydro fe
 1161001 00

* hydro vcahs
 1161101 01000

* hydro ebt pressure tempe
 1161201 0 1551824. 176543. 2411193. 0. 0.1
 1161202 0 1522812. 176332. 4 2411078. 0. 0.2
 1161203 0 1533778. 175510. 7 2410962. 0. 0.3
 1161204 0 1534708. 174581. 2410846. 0. 0.4

* hydro f velocity g velocity j velocity
 1161300 0 .71892 .71892 0. 1 * 706.
 1161301 .718895 .718895 0. 1 * 706.
 1161302 .718895 .718895 0. 3 * 706.
 1161303 .718895 .718895 0. 3 * 706.

* hydro jun hyd diam
 1161401 0.00170 0.0 1.0 1.0

* hydro component name component type
 1200000 * hpxclut1 branch

* hydro no. juns
 1200001 2

* hydro area length volume
 1200101 0.08322 1.0 0.

* hydro horz angle vert angle
 1200102 0. 0.

* hydro roughness hyd diam
 1200103 0.000457 0.3255 0.

* hydro ebt pressure tempe
 1200200 0 1462113. 174582.3 2410243. 0.

* hydro from to area f loss r loss vcahs
 1201101 116010000 120000000 0. 0.15 0.15 01000
 1201101 120010000 122000000 0. 0.08322 0. 0. 01000

* hydro f velocity g velocity j velocity
 1201201 7.72175 7.72175 0. * 706.
 1202201 7.7219 7.7219 0. * 706.

\$ component name component type
 hydro "coldleg" Pipe

1220000 3

* hydro vol area
 1220101 0.08322

* hydro length
 1220301 2.31
 1220302 2.13
 1220303 0.782

* hydro volume
 1220401 0.

* hydro volume
 1220501 0.

* hydro vert angle
 1220601 -7.6
 1220602 0.
 1220603 90.

* hydro delta z
 1220701 -0.305
 1220702 0.
 1220703 0.762

* hydro roughness hyd diam
 1220801 0.000457 0.3255

* hydro f loss r loss
 1220901 0.182 0.182

* hydro fe
 1221001 00

* hydro vcahs
 1221101 01000

* hydro ebt pressure tempe
 1221201 0 1581556. 17585. 2410234. 0. 0. 1
 1221202 0 1474903. 17587. 2401159. 0. 0. 2
 1221203 0 1462316. 174588. 2409927. 0. 0. 3

* hydro vel/ElW 0

* hydro f flowrate g flowrate j flowrate
 1221301 7.7219 7.7219 0. 1 * 706.
 1221302 7.72193 7.72193 0. 2 * 706.

* emergency heat exchanger secondary flow system (tube side) \$

* hydro component name component type
 1380000 * secscr1 bndpvol

* hydro area length volume
 1380101 1.1e6 0. 1.0e+06

* hydro horz angle vert angle delta z
 1380102 .0 .0 .0

* hydro roughness hyd diam fe
 1380103 .0 .0 10

* hydro ebt trip no. alpha vrc numeric vrc
 1380200 003

* hydro time pressure tempe
 1380205 0. 1.800e5 306.
 1380201 0. 1.800e5 308.15

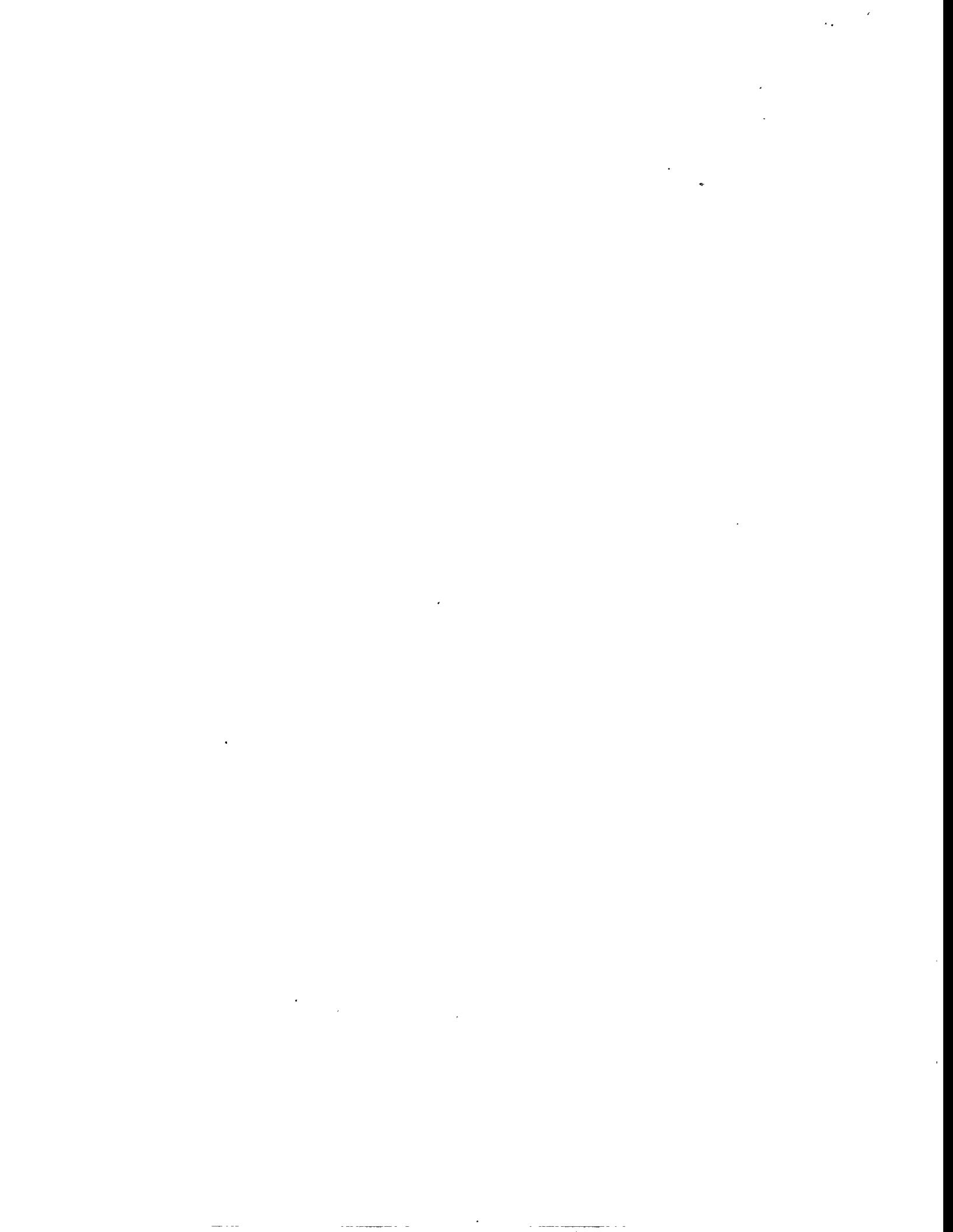
* 1460401 0.
 * hydro component name "tubein" component type singjyun
 * hydro from to area f loss r loss vcahs
 * 1400101 138000000 142000000 0.0 0. 0. 01100
 * hydro hyd diam 0.4573 0.0 1.0 1.0
 * hydro vel/flw f velocity .104126 g velocity j velocity 0. * 44.14
 * hydro component name "elhx-sec" component type pipe
 * 1420000 1420001 2
 * hydro vol area 0.4264 vol 2
 * hydro length 0.7222 vol 2
 * hydro volume 0. vol 2
 * hydro vert angle 0. vol 2
 * hydro delta z 0.0 vol 2
 * hydro roughness 0.000457 vol 2
 * hydro fe 0.0 vol 2
 * hydro vcahs 01000 vol 2
 * hydro ebt pressure 161535.6 tempc 161535.6 2525551. 0. 0. 1
 * hydro 161201 0 179916. 171612. 2525549. 0. 0. 2
 * hydro 161202 0 179912. 173313. 2525546. 0. 0. 3
 * hydro 161203 0 17990.5 182741.5 2525542. 0. 0. 4
 * hydro f velocity jun hyd diam 1461101 0.01905 0.0 1.0 1.0
 * hydro component name "tubeout" component type singjyun
 * hydro from to area f loss r loss vcahs
 * 1480101 14601000 0.0 0. 0. 01100
 * hydro hyd diam 1480110 0.01905 0.0 1.0 1.0
 * hydro vel/flw 1480201 0 .219444 0. * 44.14
 * hydro component name "chimney" component type pipe
 * hydro vol area 1500001 4
 * hydro 1500101 0.203
 * hydro 1500301 0.75
 * hydro 1500401 0.
 * hydro vert angle 1500601 90.
 * hydro elev. change 1500701 0.75
 * hydro roughness 1500801 0.000457 0.508
 * hydro f loss 1500901 0. 0.
 * hydro fe 0. vol 4
 * hydro vol area 0.476 vol 4
 * hydro length 1.6 vol 4
 * hydro volume 0. vol 4
 * hydro component name "elhx-sec" component type pipe
 * 1460000 1460001 4
 * hydro vol area 0.476 vol 4
 * hydro length 1.6 vol 4
 * hydro volume 0. vol 4

```

*calibrate1161901 0. 10. 10. 0. 0. 0. 1. 4
*calibrate*
*calibrate*
$-----+
*ht str no. 1163 hx tube
*htstr ht str m pts geom init 1.coord refl b.vol axl. incr
*11633000 4 2 1 8.65e-3 0 0
*htstr mesh locn mesh fmt 1
*htstr intervals rt. coord 9.525e-3
*htstr 11163101 3
*htstr compen no. interval 3
*htstr source interval 0.
*htstr 11163301
*htstr 11163400 temp flag 0
*htstr 11163401 temp mesh pt. 4
*htstr left vol 10000 1 1
*htstr right vol 146640000 -10000 1 1
*htstr s. type s. mult left heat right heat ht str no. 4
*htstr 11163701 chf flag 0. 10. 10. 0. 0. 1. 4
*htstr 11163801 chf flag 0. 10. 10. 0. 0. 1. 4
*htstr 11163901 chf flag 0. 10. 10. 0. 0. 1. 4
$-----+
*ht str no. 1501 hx tube
*htstr ht str m pts geom init 1.coord refl b.vol axl. incr
*11501000 4 2 1 0.2287 0 0
*htstr mesh locn mesh fmt 1
*htstr intervals rt. coord 0.2341
*htstr compen no. interval 1
*htstr 11501201
*htstr 11501301 source 0.
*htstr 11501400 temp flag 0
*htstr 11501401 temp mesh pt. 4
*htstr left vol 10000 1 1
*htstr right vol 0 0.4581 1 0.75
*htstr s. type s. mult left heat right heat ht str no. 4
*htstr 11501501 chf flag 0. 10. 10. 0. 0. 1. 4
*htstr 11501601 chf flag 0. 10. 10. 0. 0. 1. 4
*htstr 11501701 chf flag 0. 10. 10. 0. 0. 1. 4
*htstr 11501801 chf flag 0. 10. 10. 0. 0. 1. 4
*htstr 11501901 chf flag 0. 10. 10. 0. 0. 1. 4

```

thermal properties of composition 1 - ss3041					
*	composition	th.con	ht.cap	ht.cap	\$
*	tbl/fctn	fctn	fctn	fctn	material
*	*compnx	temperature		th. cond.	\$ss3041
20100100	20100101	273.2		14.7	
20100102	300.			15.2	
20100103	400.			17.0	
20100104	500.			18.4	
20100105	600.			19.8	
20100106	700.			21.2	
20100107	800.			22.5	
20100108	900.			23.9	
20100109	1000.			25.3	
20100110	1200.			28.1	
20100111	1400.			30.9	
20100112	20000.			30.9	
*	*compnx	temperature	vol	ht	cap
20100151	273.2		10.0		
20100152	20000.		10.0		
*20100151	250.		2.97e6		
*20100152	476.		3.08e6		
*20100153	700.		3.13e6		
*20100154	811.		3.23e6		
*20100155	866.		3.33e6		
*20100156	922.		3.43e6		
*20100157	1033.		3.59e6		
*20100158	1200.		3.76e6		
*20100159	1311.		3.82e6		
*20100160	1401.		3.82e6		
*20100161	20000.		3.82e6		
*	*20504500	heater sum	385.342	-100632184.	0
*	*20504501	0. 1..htmrz	108300100		
*	*20504502	1..htmrz	108300200		
*	*20504503	1..htmrz	108300300		
*	*20504504	1..htmrz	108300400		
*	*20504505	1..htmrz	108300500		
*	*20504507	1..htmrz	108300600		
*	*20504508	1..htmrz	108300700		
*	*20504509	1..htmrz	108300800		
*	*20504510	1..htmrz	108300900		
*	*20504511	1..htmrz	108301000		
***** table for water pool temperature - used as boundary condition for					
***** outside surfaces of hot and cold leg piping within the pool					
***** table no. 501 - pool temp					
*	table	type	trip no.	factor 1	constant
20250100	temp			temp	
*	table		time		
20250101		0.		311.15	
***** table no. 581 - htc from vertical piping - independent of length					
***** assumes pool temperature of 311.55 K, McAdams 0.13 Ra**1/3					
20250100	htc-temp	613.	330.	855.	1042.
20250101	320.	1197.	360.	1327.	1467.
20250102	350.	1339.	390.	1733.	1929.
20250103	380.	1439.	420.	2153.	430.
20250104	410.	2049.	450.	2562.	2295.
20250105	440.	2435.	490.	466.	2677.
***** end of case					



APPENDIX E: RELAP5/TECPLLOT TRANSLATOR AND POST-PROCESSOR (rlptec5.f)

```

c scan the date, change some names, define pointers
c
n1 = n1+5
contine
21 if(medi>100).eq.0)write(6,984)
20 continue
30 list=1-1
write(6,994)list

c scan the date, change some names, define pointers
c
do 40 n=1,nt
conv1 = conv1+1
conv2 = conv2+0.
if(names(n).eq.'p') then
technam(n) = 'p'
technam(n)(3:5) = num(n)(2:4)
conv1 = cpres
else ifnames(n).eq.'high'
technam(n) = 'hi'
technam(n)(3:5) = num(n)(2:4)
conv1 = 1.0
conv2 = 0.
else ifnames(n).eq.'toreg ') then
if(num(n)(2:6).eq.515500501) itempf = n-1
technam(n) = 'tf'
technam(n)(3:5) = num(n)(2:4)
conv1 = ctemp1
conv2 = ctemp2
else ifnames(n).eq.'htemp ')
if(num(n)(2:10).eq.550100204) lhtstr=n-1
technam(n) = 'lt'
technam(n)(12:5) = num(n)(2:5)
conv1 = ctemp1
conv2 = ctemp2
else ifnames(n).eq.'hthtc ')
technam(n) = 'h'
technam(n)(3:5) = num(n)(2:5)
conv1 = 1.0
conv2 = 0.0
else ifnames(n).eq.'htmode ')
technam(n) = 'hm'
technam(n)(3:5) = num(n)(2:5)
conv1 = 1.0
conv2 = 0.0
else ifnames(n).eq.'htvat ')
technam(n) = 'ha'
technam(n)(3:5) = num(n)(3:5)
conv1 = ctemp1
conv2 = ctemp2
else ifnames(n).eq.'tempg ')
technam(n) = 'tg'
technam(n)(3:5) = num(n)(2:4)
conv1 = ctemp1
conv2 = ctemp2
if(num(n)(2:6).eq.'51501') lstr = n-1
else ifnames(n).eq.'sattemp ')
technam(n) = 'st'
technam(n)(3:5) = num(n)(2:4)
conv1 = cmass
conv2 = ctemp2
if(num(n)(2:6).eq.'51501') lstr = n-1
else ifnames(n).eq.'mflow ')
technam(n) = 'mf'
technam(n)(3:5) = num(n)(2:4)
conv1 = cmass
conv2 = ctemp2
if(num(n)(2:6).eq.'51501') lstr = n-1
else ifnames(n).eq.'gammaaw ')
technam(n) = 'ga'
technam(n)(3:5) = num(n)(2:4)
conv1 = cdens
else ifnames(n).eq.'hf ')
technam(n) = 'hf'
technam(n)(3:5) = num(n)(2:4)
conv1 = chbf
cmass

```

```

technam(n) = 'rkfis'
else if(names(n).eq.'hig') then
  tecnam(n) = 'hg'
  tecnam(n)(3:5) = num(n)(2:4)
convl = chi
else if(names(n).eq.'pmphead') then
  tecnam(n) = 'ph'
  tecnam(n)(3:5) = num(n)(8:10)
convl = opres
else if(names(n).eq.'rmpvel') then
  tecnam(n) = 'pv'
  tecnam(n)(3:5) = num(n)(8:10)
convl = opqav
else if(names(n).eq.'uf') then
  tecnam(n) = 'uf'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cu
else if(names(n).eq.'ug') then
  tecnam(n) = 'ug'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cu
else if(names(n).eq.'ufj') then
  tecnam(n) = 'uj'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cu
else if(names(n).eq.'ugj') then
  tecnam(n) = 'uj'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cu
else if(names(n).eq.'q') then
  tecnam(n) = 'q'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cpover
else if(names(n).eq.'qwg') then
  tecnam(n) = 'qw'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cpover
else if(names(n).eq.'velfj') then
  tecnam(n) = 'vj'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cova
else if(names(n).eq.'velgj') then
  tecnam(n) = 'vf'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cova
else if(names(n).eq.'velg') then
  tecnam(n) = 'vg'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cova
else if(names(n).eq.'void') then
  tecnam(n) = 'vi'
  tecnam(n)(3:5) = num(n)(2:4)
if(num(n)(2:10).eq.'515010000') lvel = n-1
convl = cova
else if(names(n).eq.'sounde') then
  tecnam(n) = 'so'
  tecnam(n)(3:5) = num(n)(2:4)
convl = cova
else if(names(n).eq.'voidg') then
  tecnam(n) = 'vd'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'voidf') then
  tecnam(n) = 'vf'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'void1') then
  if(num(n)(2:6).eq.'15601') lp = n-1
  tecnam(n) = 'vi'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'voidg') then
  tecnam(n) = 'vg'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'qual1') then
  tecnam(n) = 'q1'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'qualme') then
  tecnam(n) = 'qe'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'quala') then
  tecnam(n) = 'qa'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'cpu') then
  tecnam(n) = 'cpu'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'acv1iq') then
  tecnam(n) = 'ac'
  tecnam(n)(3:5) = num(n)(2:4)
else if(names(n).eq.'rkfpow') then
  tecnam(n) = 'rkfis'
else if(names(n).eq.'rkfpow') then
  tecnam(n) = 'rkfis'

```



```

145 continue
do 146 ih=20,30
  qmhxp(i) = qmhxp(i) + calc1(lp00l+ih,i)
146 continue
do 147 ih=31,38
  qehxp(i) = qehxp(i) + calc1(lp00l+ih,i)
147 continue
do 148 ih=39,49
  qmhxp(i) = qmhxp(i) + calc1(lp00l+ih,i)
148 continue
do 149 ih=50,57
  qehxp(i) = qehxp(i) + calc1(lp00l+ih,i)
149 continue
do 150 ih=58,63
  qhl(i) = qhl(i) + calc1(lp00l+ih,i)
150 continue
do 151 ih=64,78
  qcl(i) = qcl(i) + calc1(lp00l+ih,i)
151 continue
do 152 ih=79,84
  qhl(i) = qhl(i) + calc1(lp00l+ih,i)
152 continue
do 153 ih=85,97
  qcl(i) = qcl(i) + calc1(lp00l+ih,i)
153 continue
do 154 ih=98,101
  qhl(i) = qhl(i) + calc1(lp00l+ih,i)
154 continue
do 155 ih=102,114
  qcl(i) = qcl(i) + calc1(lp00l+ih,i)
155 continue
do 156 ih=115,126
  qcl(i) = qcl(i) + calc1(lp00l+ih,i)
156 continue
do 157 ih=127,138
  qhl(i) = qhl(i) + calc1(lp00l+ih,i)
157 continue
143 continue
c   i4 = 0
      write(22,995)
      do 45 i=1,int
        i1 = i+1
        i2 = i+2
        comin = 1.d6
        szmin = 1.d6
        shmax = 900.
        shmin = 1.d6
        chmin = 1.d6
        icomin = 0
        iszmin = 0
        ishmax = 0
        ishmin = 0
        do 39 m=1,20
          vel(m) = calc1(lvel+m,i)
39      continue
c   translate time variable backwards by 10 s (start transient at time=0)
c   calculate initial values
  calc1(i,1) = calc1(i,1)-10.
  if(calc1(i,1).lt.0.d0) go to 45
  if(calc1(i,1).gt.0.d0) calc1(i,1)=1.d6
  all = calc1(i1-1,i)*calc1(i1+2,i)+calc1(i1+3,i)+calc1(i1+4,i)+calc1(i1+5,i)
  c11 = 1p+6
  al2 = calc1(i1+1,i)*4.09*(calc1(i1+2,i)+calc1(i1+3,i)+calc1(i1+4,i)+calc1(i1+5,i))+0.12-4.88*(i1.-calc1(i1+6,i))
  al3 = calc1(i1+1,i)*4.09*(calc1(i1+2,i)+calc1(i1+3,i)+calc1(i1+4,i)+calc1(i1+5,i))+0.12-4.88*(i1.-calc1(i1+6,i))
c   acf1 = calc1(2,i)*4.09*(calc1(i1+2,i)+calc1(i1+3,i)+calc1(i1+4,i))
  qpool = 0.
  qmhx = qmhx+calc1(lmhx+ih,i)
43      continue
do 43 ih= 1,30
  qmhx = qmhx+calc1(lmhx+ih,i)
43      continue
if(0.0001d0>comin) then
  costar(m) = max(0.0001d0,comf95*calc1(lco+m,i)/
    calc1(lflxht+m,i))
  comin = costar(m)
endif
if(costar(m).lt.1.0) icown = icown+1
46      continue
do 47 m = 6,10
  costar(m) = max(0.0001d0,comf99*calc1(lco+m,i)/
    calc1(lflxht+m,i))
  comin = costar(m)
endif
if(costar(m).lt.comin) then
  comin = costar(m)
  icomin = 10+m
endif
if(costar(m).lt.1.0) icown = icown+1
47      continue
do 48 m = 11,15
  costar(m) = max(0.0001d0,comf95*calc1(lco+m,i)/
    calc1(lflxht+m,i))
  comin = costar(m)
  icomin = -5+m
endif
if(costar(m).lt.1.0) icown = icown+1
48      continue
do 49 m = 16,20
  costar(m) = max(0.0001d0,comf99*calc1(lco+m,i)/
    calc1(lflxht+m,i))
  comin = costar(m)
  icomin = m
endif
if(costar(m).lt.1.0) icown = icown+1
49      continue
if(costar(m).lt.comin) then
  comin = costar(m)
  icomin = m
endif
abc001 = calc1(lsc+m,i)
dh = 0.02498
if(m.gt.10) dh = 0.00294
fact = 0.55 + 1.21/sbcc001
c   Determine peaked heat flux
c   if(pe.ge.70000.) then
  qlim = 0.0065*re*pr*ctb/dh*sbccool*fact
  if((vel(m).gt.8.) .or. (m.ge.11.and.m.le.15.) ) then
    if(m.le.5.or.(m.ge.11.and.m.le.15.) ) then
      pr = pfsz95(1)
      hflx = pfrcalc1(lflxht+m,i)/pfco95
      else
        pr = pfsz95(2)
        hflx = pfrcalc1(lflxht+m,i)/pfco95
      endif
    else
      pr = pfsz99(2)
      hflx = pfrcalc1(lflxht+m,i)/pfco95
    endif
  else
    qlim = 455.*ctb/dh*sbccool*fact
    if(m.le.5.or.(m.ge.11.and.m.le.15.) ) then

```

```

pf = pfar95(3)
hf1x = pf*calc1(lfixht+m,i)/pfc095
else
hf1x = pf*calc1(lfixht+m,i)/pfc099
pf = pfar99(3)
endif

c
szmodr(m) = max(0.00001d0,qdim/hf1x)
szr(m) = max(0.00001d0,qdim/hf1x/fact)
if(szmodr(m).lt.smin.and.szmodr(m).gt.0.0001d0) then
  ismin = m
endif
if(ismodr(m).lt.1.0) iszwn = iszwn+1
56  continue
c.....1.....2.....3.....4.....5.....6.....7..
c CHP ratios
c Average Fuel
c do 70 m = 1,10
chfavr(m) = max(0.00001d0,calc1(lchfavr+m,i)/calc1(lfixht+m,i))
if(chfavr(m).lt.chfmin.and.chfavr(m).gt.0.00001d0) then
  chfmin = chfavr(m)
endif
ichmin = m+20
if(chfavr(m).gt.100.) ichwzn = ichwzn+1
70  continue
do 75 m = 1,20
fp = 1.
c divide out the peaking factor from CHF hot stipe flux if requested
if(tittle(111).eq.'-') then
  if(m.le.5.or.(m.ge.11.and.m.le.15)) then
    if(m.eq.5.or.m.eq.10.or.m.eq.11.or.m.eq.15) then
      fp = 1./pfc095a
    else
      fp = 1./pfc095b
    endif
  else
    if(m.eq.5.or.m.eq.10.or.m.eq.11.or.m.eq.15) then
      fp = 1./pfc099a
    else
      fp = 1./pfc099b
    endif
  endif
c.....1.....2.....3.....4.....5.....6.....7..
chfz(m) = max(0.00001d0,calc1(lchfz+m,i)/
  (calc1(lchfht+m,i)*fp))
if(chfz(m).lt.chfmin.and.chfz(m).gt.0.00001d0) then
  chfmin = chfz(m)
endif
if(chfz(m).gt.100.) ichwzn = ichwzn+1
75  continue
c calculate Petukhov heat flux based on rbulk and tsat
c at hot channel exit locations only
do 76 m=1,20
  dh = 0.002498
  pr = abs(calc1(lpr+m,i))
  pr = calc1(lpr+m,i)
  re = pe/pr
  tsat = calc1(lsatm,i)
  sbcool = calc1(lsbtm,i)
  const = 1.0875 - 0.1125*(1.143/87.35)
  visat = dvisat(tsat)
  visrat = calc1(lvism,i)/visat
  if(m.gt.2) then
    const = 1.0875 - 0.1125*(1.143/87.35)
    dh = 0.002494
  endif
  fd = const/(1.82*1010*(re)-1.64)**2
  hturb = fd*(calc1(lk,m,i)/dh)*pe*visrat**0.11/
    ((k3*(fd)+11.7+1.8/dt)**0.3333)*(fd/6.1)**0.5*
    (pr*0.6667*-1.)
  hlam = 7.63*calc1(lk*m,i)/dh
cmwg 8-3-95 ECR01 SHOURD BR m.gt.10
  if(m.gt.2) then
    const = 1.0875 - 0.1125*(1.143/87.35)
    dh = 0.002494
  endif
  fd = const/(1.82*1010*(re)-1.64)**2
  hturb = fd*(calc1(lk,m,i)/dh)*pe*visrat**0.11/
    ((k3*(fd)+11.7+1.8/dt)**0.3333)*(fd/6.1)**0.5*
    (pr*0.6667*-1.)
  hlam = 7.63*calc1(lk*m,i)/dh
endif

if(hlam.gt.hturb) then
  write(6,962)calc1(l1,i),m,re
  hlam = hlam
else
  hlam = hturb
endif
qlam = hlam*sbcool
c Determine peaked heat flux
c
if(pe.ge.70000.) then
  if(m.le.5.or.(m.ge.11.and.m.le.15)) then
    pf = pfar95(2)
    hf1x = pf*calc1(lfixht+m,i)/pfc095
  else
    pf = pfar99(1)
    hf1x = pf*calc1(lfixht+m,i)/pfc099
  endif
  pf = pfc099(1)
  hf1x = pf*calc1(lfixht+m,i)/pfc099
else
  if(m.le.5.or.(m.ge.11.and.m.le.15)) then
    pf = pfar95(3)
    hf1x = pf*calc1(lfixht+m,i)/pfc095
  else
    pf = pfar99(3)
    hf1x = pf*calc1(lfixht+m,i)/pfc099
  endif
endif
if(m.le.5.or.(m.ge.11.and.m.le.15)) then
  supthr(m) = max(0.0001d0,qdim/hf1x,sbcool,hlim)
  if(supthr(m).gt.0.0001d0) then
    smin = supthr(m)
    if(supthr(m).gt.0.0001d0) then
      smin = m
    endif
  endif
  if(m.eq.10) write(28,9102) calc1(l1,i),qdim,hf1x,sbcool,hlim
endif
76  continue
c
c Calculate Bergles-Rohsenow heat flux at hot channel exit locations only
do 77 m=1,20
  pe = abs(calc1(lpe+m,i))
  pr = calc1(lpr+m,i)
  ckb = calc1(lk+m,i)
  tsat = calc1(lsatm,i)
  sbcool = calc1(lscbm,i)
  visbk = calc1(lvism,i)
  re = pe/pr
  if(m.gt.10) then
    const = 1.0875 - 0.1125*(1.143/70.29)
    dh = 0.002494
  endif
  call incptat-sbcool,tstat,pexit,re,pr,dh,visblk,const,
  const = 1.0875 - 0.1125*(1.143/87.35)
  dh = 0.002498
  pexit = calc1(lpeux+i,i)
endif
if(ierr.eq.1) write(6,970)twlib,qib,calc1(l1,i),m,re
if(ilam.eq.1) write(6,963)calc1(l1,i),m,re
ibr(m) = max(0.0001d0,qdim/hf1x)

if(m.le.5.or.(m.ge.11.and.m.le.15)) then
  pf = pfar95(1)
  hf1x = pf*calc1(lfixht+m,i)/pfc095
else
  pf = pfar99(1)
  hf1x = pf*calc1(lfixht+m,i)/pfc099
endif
c Determine peaked heat flux
c

```



```

c Heat flux removed by convection
c qleft = hfc*(tw-chbulk)
c IB Heat Flux constraint
c Bergles Rohsenow in units of W/m^2
c.....1.....2.....3.....4.....5.....6.....7...
c.....right = 0.9*1.7978e-3*p**1.156*
.....(1.8/(tw-tstat))**(2.8285/p**0.0234)
c
if(hbs(thi-tw).le.eps)then
qib = qleft
twalib = tw
return
else if(qleft.gt.qright) then
twlow = tw
else
thi = tw
endif
10 continue
ierr = 1
return
end

```



APPENDIX F: RELAPS STRIP INPUT FILE (strip5in)

```

* strip file for ans model
100 strip fmcout
103 0
104 noaction
*-----*
1001 mfloop 157000000 * Accumulator 1
1002 mfloop 257000000 * Accumulator 2
1003 mfloop 357000000 * Accumulator 3
1004 mfloop 148000000 * ERK Chimney Flow
1005 mfloop 169000000 * Break Flow - Core Inlet (TD only)
1007 mfloop 124000000 * pump mass flow - loop 1
1008 mfloop 220000000 * pump mass flow - loop 2
1009 mfloop 320000000 * pump mass flow - loop 3
1010 mfloop 567004000 * Total Core Flow
1011 mfloop 865000000 * Letdown Flow Rate
1012 mfloop 850000000 * Pressurizing Flow Rate
1013 mfloop 132000000 * Secondary
1014 rkpow 0
1015 rktrap 0
1016 rkgapow 0
1017 rkrec 0
*-----*
1019 cntrivar 835 * lower core exit pressure
1020 cntrivar 836 * lower core pressure drop
1021 cntrivar 837 * upper core exit pressure
1022 cntrivar 838 * upper core pressure drop
1023 P 490010000
1024 P 500010000
1025 P 505010000
1026 P 520010000
1027 P 535010000
1028 P 555010000
1029 P 545010000
1030 P 545020000
1031 P 545030000
1032 P 545040000
1033 P 545050000
1034 P 122260000 * pump suction pressure
1035 P 126010000 * Pump suction Pressure
1036 P 156010000
1037 P 104010000
1038 P 106010000
1039 P 650030000
1040 battemp 650030000
1041 pmovel 124
1042 pmovel 224
1043 pmovel 324
1044 pmovel 834
1045 pmovel 830
1046 cntrivar 48
1047 cntrivar 98
1048 cntrivar 148
1049 cntrivar 52
1050 cntrivar 102
1051 cntrivar 152
1052 cntrivar 60
1053 cntrivar 110
1054 cntrivar 160
1055 temp 490010000
1056 temp 555010000
1057 temp 645150000
1058 temp 106010000
1059 temp 650030000
1060 temp 546050000
1061 temp 546050000
1062 cntrivar 238 * UC 95% hot channel exit subcooling
1063 welf 572010300 * upper core 95% inlet velocity
1065 welf 556010200 * upper core 95% exit velocity
1067 welf 557010200 * upper average inlet velocity
1068 welf 515040000
1069 welf 515040000
1070 welf 516040000
1071 welf 515040000
1072 welf 540040000
1073 welf 515040000
1074 welf 516040000
1075 voidg 515040000
1076 voidg 515040000
1077 voidg 515040000
1078 voidg 515040000
1079 voidg 515050000
1080
1081 voidg 516010000
1082 voidg 516013000
1083 voidg 516014000
1084 voidg 516015000
1085 voidg 545010000
1086 voidg 545012000
1087 voidg 545013000
1088 voidg 545014000
1089 voidg 545015000
1090 voidg 546010000
1091 voidg 546012000
1092 voidg 546013000
1093 voidg 546014000
1094 voidg 546015000
1095 voidg 550110000
1096 quala 105010000
1097 quala 125010000
1098 quala 490010000
1099 quala 545050000
1100 quala 645115000
1101 hitemp 5501100204 * Max CRBT Temp
1102 hitemp 5521100305 * Max CR- Al Temp
1103 hitemp 5521100307 * Max CR- HF Temp
1104 hitemp 5501100201 * Sur CRBT Temp
1105 hitemp 5521100301 * Sur CR- Al Temp
1106 hitemp 5521100310 * Sur CR- HF Temp
1107 temperatures
1108 tempf 515010000
1109 tempf 515020000
1110 tempf 515030000
1111 tempf 515040000
1112 tempf 516010000
1113 tempf 516020000
1114 tempf 516030000
1115 tempf 516040000
1116 tempf 516050000
1117 tempf 516060000
1118 tempf 516070000
1119 tempf 545030000
1120 tempf 545040000
1121 tempf 545050000
1122 tempf 546010000
1123 tempf 546020000
1124 tempf 546030000
1125 tempf 546040000
1126 tempf 546050000
1127 cpertime 0
1128 voidf
1129 voidf
1130 voidf
1131 voidf
1132 voidf
1133 voidf
1134 voidf
1135 voidf
1136 voidf
1137 voidf
1138 voidf
1139 voidf
1140 voidf
1141 voidf
1142 voidf
1143 voidf
1144 voidf
1145 voidf
1146 heatfluxes at average and hot channels
1147 htrnr 510100100 * LC average channel fuel
1148 htrnr 510100300
1149 htrnr 510100400
1150 htrnr 510100500
1151 htrnr 540100200 * UC average channel fuel
1152 htrnr 540100300
1153 htrnr 540100400
1154 htrnr 540100500
1155 htrnr 545001000
1156 htrnr 515500100 * LC FE 95% hot stripe
1157 htrnr 515500200
1158 htrnr 515500300

```

* strip file for ans model

```

100 strip fintout
103 0
104 noaction
1001 mflow 157000000 * Accumulator 1
1002 mflow 57000000 * Accumulator 2
1003 mflow 57000000 * Accumulator 3
1004 mflow 148000000 * EHX Chimney Flow
1005 mflow 169000000 * Break Flow - Core Inlet (RD only)
1007 mflow 124010000 * pump mass flow - loop 1
1008 mflow 224010000 * pump mass flow - loop 2
1009 mflow 32010000 * pump mass flow - loop 3
1010 mflow 567010400 * Total Core Flow
1011 mflow 865010000 * Letdown Flow Rate
1012 mflow 850010000 * Pressurizing Flow Rate
1013 mflow 132000000 * Secondary
1014 rkbow 0
1015 rkfpow 0
1016 rkgapow 0
1017 rkteac 0
* Pressures
1019 cntrivar 835 * lower core exit pressure
1020 cntrivar 836 * lower core pressure drop
1021 cntrivar 837 * upper core exit pressure
1022 cntrivar 838 * upper core exit pressure drop
1023 P 4901000
1024 P 50010000
1025 P 50501000
1026 P 52001000
1027 P 53501000
1028 P 55010000
1029 P 54501000
1030 P 55001000
1031 P 54503000
1032 P 54504000
1033 P 54505000
1034 P 122260000 * pump suction pressure
1035 P 122610000 * pump suction pressure
1036 P 156010000
1037 P 104010000
1038 P 106010000
1039 P 650030000
1040 sattemp 650030000
1041 propvel 124
1042 propvel 224
1043 propvel 324
1044 propvel 815
1045 propvel 830
1046 cntrivar 48
1047 cntrivar 98
1048 cntrivar 148
1049 cntrivar 52
1050 cntrivar 102
1051 cntrivar 152
1052 cntrivar 60
1053 cntrivar 110
1054 cntrivar 160
1055 tempf 490010000
1056 tempf 555010000
1057 tempf 645150000
1058 tempf 105010000
1059 tempf 650030000
1060 tempf 546505000
1061 tempf 546050000 * UC 95% hot channel exit subcooling
1062 cntrivar 238 * UC 95% hot channel exit subcooling
1063 cntrivar 517010300 * upper core 95% inlet velocity
1064 vel1f 556010200 * upper core 95% exit velocity
1065 vel1f 556010300 * upper average inlet velocity
1066 vel1f 556010200 * upper average exit velocity
1067 vel1f 510040000
1068 vel1f 510040000 * UC average channel fuel
1069 vel1f 515040000
1070 vel1f 515040000
1071 vel1f 516040000
1072 vel1f 515040000
1073 vel1f 515040000
1074 vel1f 516040000
1075 voidg 515010000
1076 voidg 515020000
1077 voidg 515030000
1078 voidg 515040000
1079 voidg 515050000
1080 voidg 516010000
1081 voidg 516020000
1082 voidg 516030000
1083 voidg 516040000
1084 voidg 516050000
1085 voidg 515010000
1086 voidg 515020000
1087 voidg 515030000
1088 voidg 515040000
1089 voidg 516010000
1090 voidg 546010000
1091 voidg 546020000
1092 voidg 546030000
1093 voidg 546040000
1094 voidg 546050000
1095 voidg 650030000
1096 qualia 106010000
1097 qualia 126010000
1098 qualia 490010000
1099 qualia 545050000
1100 qualia 545150000
1101 htemp 55010204 * Max CRPT Temp
1102 htemp 56210306 * Max CR- Al Temp
1103 htemp 56210307 * Max CR- HF Temp
1104 htemp 55010201 * Sur CRPT Temp
1105 htemp 56210301 * Sur CR- Al Temp
1106 htemp 56210310 * Sur CR- HF Temp
* Bulk Temperatures
1107 tempf 515010000
1108 tempf 515020000
1109 tempf 515030000
1110 tempf 515040000
1111 tempf 515050000
1112 tempf 516010000
1113 tempf 516020000
1114 tempf 516030000
1115 tempf 516040000
1116 tempf 516050000
1117 tempf 545010000
1118 tempf 545020000
1119 tempf 545030000
1120 tempf 545040000
1121 tempf 545050000
1122 tempf 44601000
1123 tempf 546020000
1124 tempf 546030000
1125 tempf 546040000
1126 tempf 546050000
1127 cptitime 0
1128 voidf 156010000
1129 voidf 156020000
1130 voidf 156030000
1131 voidf 156040000
1132 voidf 156050000
1133 voidf 156060000
1134 voidf 256010000
1135 voidf 256020000
1136 voidf 256030000
1137 voidf 256040000
1138 voidf 256050000
1139 voidf 356010000
1140 voidf 356020000
1141 voidf 356030000
1142 voidf 356040000
1143 voidf 356050000
1144 voidf 356060000
1145 voidf 51010100 * LC average channel fuel
1146 htrn 51010100
1147 htrn 51010200
1148 htrn 51010300
1149 htrn 51010400
1150 htrn 51010500
1151 htrn 54010100
1152 htrn 54010200
1153 htrn 54010300
1154 htrn 54010400
1155 htrn 54550100 * LC FE 95% hot stripe
1156 htrn 54550200
1157 htrn 54550300
1158 htrn 54550400

```

1159 htrnr 515500400
 1160 htrnr 515500500 * UC FE 99.9% hot stripe
 1161 htrnr 516500100 * UC FE 99.9% hot stripe
 1162 htrnr 516500200
 1163 htrnr 516500300
 1164 htrnr 516500400
 1165 htrnr 516500500 * UC FE 99.9% hot stripe
 1166 htrnr 545500100 * UC FE 99.9% hot stripe
 1167 htrnr 545500200
 1168 htrnr 545500300
 1169 htrnr 545500400 * UC FE 99.9% hot stripe
 1170 htrnr 545500500 * UC FE 99.9% hot stripe
 1171 htrnr 545600100 * UC FE 99.9% hot stripe
 1172 htrnr 545600200
 1173 htrnr 545600300
 1174 htrnr 545600400
 1175 htrnr 545600500 * UC CHP 99.9% hot stripe
 1176 htrnr 515600100 * LC CHP 95% hot stripe
 1177 htrnr 515600200
 1178 htrnr 515600300
 1179 htrnr 515600400
 1180 htrnr 515600500 * UC CHP 99.9% hot stripe
 1181 htrnr 516600100 * LC CHP 99.9% hot stripe
 1182 htrnr 516600200
 1183 htrnr 516600300
 1184 htrnr 516600400
 1185 htrnr 516600500 * UC CHP 99.9% hot stripe
 1186 htrnr 545400100 * UC CHP 99.9% hot stripe
 1187 htrnr 545400200
 1188 htrnr 545400300
 1189 htrnr 545400400
 1190 htrnr 545400500 * UC CHP 99.9% hot stripe
 1191 htrnr 546600100 * UC CHP 99.9% hot stripe
 1192 htrnr 546600200
 1193 htrnr 546600300
 1194 htrnr 546600400
 1195 htrnr 546600500
 1196 cptitime 0
 * CHP indicated by RELAPS
 1197 htchf 510100100 * LC average channel fuel
 1198 htchf 510100200
 1199 htchf 510100300
 1200 htchf 510100400
 1201 htchf 510100500 * UC average channel fuel
 1202 htchf 540100100 * UC average channel fuel
 1203 htchf 540100200
 1204 htchf 540100300
 1205 htchf 540100400
 1206 htchf 540100500 * UC CHP 99.9% hot stripe
 1207 htchf 515400100 * UC CHP 99.9% hot stripe
 1208 htchf 515400200
 1209 htchf 515400300
 1210 htchf 515400400
 1211 htchf 515400500 * UC CHP 99.9% hot stripe
 1212 htchf 516600100 * UC CHP 99.9% hot stripe
 1213 htchf 516600200
 1214 htchf 516600300
 1215 htchf 516600400
 1216 htchf 516600500
 1217 htchf 545400100 * UC CHP 99.9% hot stripe
 1218 htchf 545400200
 1219 htchf 545400300
 1220 htchf 545400400
 1221 htchf 545400500 * UC CHP 99.9% hot stripe
 1222 htchf 546600100
 1223 htchf 546600200
 * Costa heat flux limits
 1230 cntrivar 203 * LC 95% hot stripe
 1231 cntrivar 207
 1232 cntrivar 211
 1233 cntrivar 215
 1234 cntrivar 219
 1235 cntrivar 223 * LC 99.9% hot stripe
 1236 cntrivar 227
 1237 cntrivar 231
 1238 cntrivar 235
 1239 cntrivar 239 * UC 95% hot stripe
 1240 cntrivar 243 * UC 95% hot stripe
 1241 cntrivar 247
 1242 cntrivar 251
 1243 cntrivar 255
 1244 cntrivar 259
 1245 cntrivar 263 * UC 99.9% hot stripe
 1246 cntrivar 267
 1247 cntrivar 271
 1248 cntrivar 275
 1249 cntrivar 279
 1250 cptitime 0
 * Wall superheat at hot spots and average fuel
 1251 cntrivar 280 * UC 95% hot stripe
 1252 cntrivar 281
 1253 cntrivar 282
 1254 cntrivar 283
 1255 cntrivar 284 * UC 99.9% hot stripe
 1256 cntrivar 285
 1257 cntrivar 286
 1258 cntrivar 287
 1259 cntrivar 288
 1260 cntrivar 289 * UC 95% hot stripe
 1261 cntrivar 290 * UC 95% hot stripe
 1262 cntrivar 291
 1263 cntrivar 292
 1264 cntrivar 293
 1265 cntrivar 294 * UC 99.9% hot stripe
 1266 cntrivar 295 * UC 99.9% hot stripe
 1267 cntrivar 296
 1268 cntrivar 297
 1269 cntrivar 298
 1270 cntrivar 299
 * Viscosities in hot channels
 1271 viscf 515010000
 1272 viscf 515020000
 1273 viscf 515030000
 1274 viscf 515040000
 1275 viscf 515050000
 1276 viscf 516010000
 1277 viscf 516020000
 1278 viscf 516030000
 1279 viscf 516040000
 1280 viscf 516050000
 1281 viscf 546010000
 1282 viscf 546020000
 1283 viscf 546030000
 1284 viscf 546040000
 1285 viscf 546050000
 1286 viscf 546100000
 1287 viscf 546200000
 1288 viscf 546300000
 1289 viscf 546400000
 1290 viscf 546500000
 1291 thermal conductivities in hot channels
 1292 theorf 515010000
 1293 theorf 515020000
 1294 theorf 515030000
 1295 theorf 515040000
 1296 theorf 515050000
 1297 theorf 516010000
 1298 theorf 516020000
 1299 theorf 516030000
 1300 theorf 516040000
 1301 theorf 516050000
 1302 theorf 516060000
 1303 theorf 516070000
 1304 theorf 516080000
 1305 theorf 516090000
 1306 theorf 516100000
 1307 theorf 516120000
 1308 theorf 546130000
 1309 theorf 546140000
 1310 theorf 546150000
 * Velocities in hot channels
 1311 velf 515010000
 1312 velf 515020000
 1313 velf 515030000
 1314 velf 515040000

1315 welf 515050000
 1316 welf 516010000
 1317 welf 516020000
 1318 welf 516030000
 1319 welf 516040000
 1320 welf 516050000
 1321 welf 545010000
 1322 welf 545020000
 1323 welf 545030000
 1324 welf 545040000
 1325 welf 545050000
 1326 welf 546010000
 1327 welf 546020000
 1328 welf 546030000
 1329 welf 546040000
 1330 welf 546050000
 * Subcooling
 1331 cntrivar 202
 1332 cntrivar 206
 1333 cntrivar 210
 1334 cntrivar 214
 1335 cntrivar 218
 1336 cntrivar 222
 1337 cntrivar 226
 1338 cntrivar 230
 1339 cntrivar 234
 1340 cntrivar 238
 1341 cntrivar 242
 1342 cntrivar 246
 1343 cntrivar 250
 1344 cntrivar 254
 1345 cntrivar 258
 1346 cntrivar 262
 1347 cntrivar 266
 1348 cntrivar 270
 1349 cntrivar 274
 1350 cntrivar 278
 * Prandtl numbers
 1356 cntrivar 445 * lower core 95% hot channel
 1357 cntrivar 447
 1358 cntrivar 449
 1359 cntrivar 451
 1360 cntrivar 453 * lower core 99.9% hot channel
 1361 cntrivar 455 * lower core 99.9% hot channel
 1362 cntrivar 457
 1363 cntrivar 459
 1364 cntrivar 461
 1365 cntrivar 463 * lower core 95% hot channel
 1366 cntrivar 465 * lower core 95% hot channel
 1367 cntrivar 467
 1368 cntrivar 469
 1369 cntrivar 471
 1370 cntrivar 473
 1371 cntrivar 475 * lower core 99.9% hot channel
 1372 cntrivar 477
 1373 cntrivar 479
 1374 cntrivar 481
 1375 cntrivar 483
 * Pecllet numbers
 1376 cntrivar 301 * lower core 95% hot channel
 1377 cntrivar 303
 1378 cntrivar 305
 1379 cntrivar 307
 1380 cntrivar 309
 1381 cntrivar 311 * lower core 99.9% hot channel
 1382 cntrivar 313
 1383 cntrivar 315
 1384 cntrivar 317
 1385 cntrivar 319
 1386 cntrivar 321 * upper core 95% hot channel
 1387 cntrivar 323
 1388 cntrivar 325
 1389 cntrivar 327
 1390 cntrivar 329
 1391 cntrivar 331 * upper core 99.9% hot channel
 1392 cntrivar 333
 1393 cntrivar 335
 1394 cntrivar 337
 1395 cntrivar 339
 * saturation temperatures in hot channels
 1401 sattemp 545040000

* Fuel surface temperatures

* end of case

APPENDIX G: TABLE OF ALL CONTROL VOLUMES

<u>VOLUME</u>	<u>AREA</u>	<u>LENGTH</u>	<u>dZ</u>	<u>Dh</u>	<u>S</u>	
101-01	0.08322	1.07	0.	0.3255	45.7	*lp1 hot leg
101-02	0.08322	3.66	0.	0.3255	45.7	*lp1 hot leg
101-03	0.08322	2.21	0.	0.3255	45.7	*lp1 hot leg
104-01	0.08322	0.69	0.	0.3255	45.7	*lp1 hot leg
104-02	0.08322	12.95	0.	0.3255	45.7	*lp1 hot leg
104-03	0.08322	2.51	2.44	0.3255	45.7	*lp1 hot leg
106-01	0.08322	1.0	0.	0.3255	45.7	*lp1 MHX primary inlet plenum
108-01	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-02	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-03	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-04	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-05	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-06	0.841	2.03	0.	0.894	45.7	*lp1 MHX primary (shell)
108-07	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-08	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-09	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-10	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
108-11	0.8258	1.11	0.	0.636	45.7	*lp1 MHX primary (shell)
112-01	0.08322	1.0	0.	0.3255	45.7	*lp1 MHX primary exit plenum
113-01	0.08322	1.981	-0.762	0.3255	45.7	*lp1 pipe joining HXs
113-02	0.08322	1.23	-0.6093	0.3255	45.7	*lp1 pipe joining HXs
113-03	0.08322	0.6096	-0.6096	0.3255	45.7	*lp1 pipe joining HXs
114-01	0.08322	1.0	0.	0.3255	45.7	*lp1 EHX primary inlet plenum
116-01	0.894	1.6	0.	0.00170	45.7	*lp1 EHX primary (shell)
116-02	0.894	1.6	0.	0.00170	45.7	*lp1 EHX primary (shell)
116-03	0.894	1.6	0.	0.00170	45.7	*lp1 EHX primary (shell)
116-04	0.894	1.6	0.	0.00170	45.7	*lp1 EHX primary (shell)
120-01	0.08322	1.0	0.	0.3255	45.7	*lp1 EHX primary exit plenum
122-01	0.08322	2.31	-0.305	0.3255	45.7	*lp1 col leg
122-02	0.08322	2.13	0.	0.3255	45.7	*lp1 cold leg
122-03	0.08322	0.762	0.762	0.3255	45.7	*lp1 cold leg
124-01	1.5478	0.5	0.000	-	-	*lp1 primary coolant pump
128-01	0.08322	0.9146	0.0	0.3255	45.7	*lp1 pc pump discharge
129-01	0.08322	6.25	0.0	0.3255	45.7	*lp1 cold leg
130-01	1.66	1.	0.	0.	0.	*lp1 MHX sec src 302.55 K
134-01	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-02	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-03	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-04	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-05	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-06	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-07	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-08	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-09	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
134-10	0.776	1.314	0.	0.01588	45.7	*lp1 MHX secondary (tube)
138-01	1.66	1.	0.	0.	0.	*lp1 MHX sec sink 0.449 MPa
138-01	1.66	1.	0.	0.	0.	*lp1 EHX sec source 311.15 K
142-01	0.4264	0.7622	0.	0.4573	45.7	*lp1 EHX secondary inlet pipe
142-02	0.4264	0.7622	0.	0.4573	45.7	*lp1 EHX secondary inlet pipe
146-01	0.476	1.6	0.	0.01905	45.7	*lp1 EHX secondary (tube)
146-02	0.476	1.6	0.	0.01905	45.7	*lp1 EHX secondary (tube)
146-03	0.476	1.6	0.	0.01905	45.7	*lp1 EHX secondary (tube)
146-04	0.476	1.6	0.	0.01905	45.7	*lp1 EHX secondary (tube)
150-01	0.203	0.75	0.75	0.508	45.7	*lp1 EHX secondary chimney
150-02	0.203	0.75	0.75	0.508	45.7	*lp1 EHX secondary chimney
150-03	0.203	0.75	0.75	0.508	45.7	*lp1 EHX secondary chimney
150-04	0.203	0.75	0.75	0.508	45.7	*lp1 EHX secondary chimney
154-01	1.66	1.	0.	0.	0.	*lp1 EHX sec sink 0.15077366 MPa
156-01	1.65	4.09	-4.09	1.449	45.7	*lp1 ACCUM tank top volume
156-02	1.65	0.12	-0.12	1.449	45.7	*lp1 ACCUM tank top
156-03	1.65	0.12	-0.12	1.449	45.7	*lp1 ACCUM tank top
156-04	1.65	0.12	-0.12	1.449	45.7	*lp1 ACCUM tank top
156-05	1.65	0.12	-0.12	1.449	45.7	*lp1 ACCUM tank top
156-06	0.08322	4.88	-4.88	0.3255	45.7	*lp1 ACCUM standpipe
158-01	0.08322	4.50	0.	0.3255	45.7	*lp1 cold-leg horizontal
158-02	0.08322	4.50	0.	0.3255	45.7	*lp1 cold-leg horizontal
162-01	0.08322	1.83	-1.83	0.3255	45.7	*lp1 cold-leg downcomer pipe
162-02	0.08322	1.57	0.	0.3255	45.7	*lp1 cold-leg downcomer pipe
162-03	0.08322	1.45	0.	0.3255	45.7	*lp1 cold-leg downcomer pipe
162-04	0.08322	12.10439	-12.10439	0.3255	45.7	*lp1 cold-leg downcomer pipe
171-01	0.03095	0.30	-0.3	0.1985	45.7	*lp1 IFD throat
171-02	0.03095	2.00	0.0	0.1985	45.7	*lp1 IFD throat
171-03	0.03095	2.28	0.0	0.1985	45.7	*lp1 IFD throat
174-01	0.08322	0.50	0.50	0.3255	45.7	*lp1 PSVAW join pipe
LOOP2-LOOP2-LOOP2-LOOP2-LOOP2-LOOP2-LOOP2-LOOP2-LOOP2-						
201-01	0.08322	1.07	0.	0.3255	45.7	*lp2 hot leg
201-02	0.08322	3.66	0.	0.3255	45.7	*lp2 hot leg
201-03	0.08322	2.21	0.	0.3255	45.7	*lp2 hot leg
204-01	0.08322	0.69	0.	0.3255	45.7	*lp2 hot leg
204-02	0.08322	12.95	0.	0.3255	45.7	*lp2 hot leg
204-03	0.08322	2.51	2.44	0.3255	45.7	*lp2 hot leg

208-01	0.08322	1.0	0.	0.3255	45.7	* lp2 MHX primary inlet plenum
208-01	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-02	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-03	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-04	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-05	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-06	0.841	2.03	0.	0.894	45.7	* lp2 MHX primary (shell)
208-07	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-08	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-09	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-10	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
208-11	0.8258	1.11	0.	0.636	45.7	* lp2 MHX primary (shell)
212-01	0.08322	1.0	0.	0.3255	45.7	* lp2 MHX primary exit plenum
213-01	0.08322	1.981	-0.762	0.3255	45.7	* lp2 pipe joining HXs
213-02	0.08322	1.23	-0.6093	0.3255	45.7	* lp2 pipe joining HXs
213-03	0.08322	0.6096	-0.6096	0.3255	45.7	* lp2 pipe joining HXs
214-01	0.08322	1.0	0.	0.3255	45.7	* lp2 EHX primary inlet plenum
216-01	0.894	1.6	0.	0.00170	45.7	* lp2 EHX primary (shell)
216-02	0.894	1.6	0.	0.00170	45.7	* lp2 EHX primary (shell)
216-03	0.894	1.6	0.	0.00170	45.7	* lp2 EHX primary (shell)
216-04	0.894	1.6	0.	0.00170	45.7	* lp2 EHX primary (shell)
220-01	0.08322	1.0	0.	0.3255	45.7	* lp2 EHX primary exit plenum
222-01	0.08322	2.31	-0.305	0.3255	45.7	* lp2 cold leg
222-02	0.08322	2.13	0.	0.3255	45.7	* lp2 cold leg
222-03	0.08322	0.762	0.762	0.3255	45.7	* lp2 cold leg
224-01	1.5478	0.5	0.000	-	-	* lp2 primary coolant pump
226-01	0.08322	0.9146	0.0	0.3255	45.7	* lp2 pc pump discharge
229-01	0.08322	6.25	0.0	0.3255	45.7	* lp2 cold leg
230-01	1.66	1.	0.	0.	0.	* lp2 MHX sec src 302.55 K
234-01	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-02	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-03	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-04	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-05	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-06	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-07	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-08	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-09	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
234-10	0.776	1.314	0.	0.01588	45.7	* lp2 MHX secondary (tube)
236-01	1.66	1.	0.	0.	0.	* lp2 MHX sec sink 0.449 MPa
238-01	1.66	1.	0.	0.	0.	* lp2 EHX sec source 311.15 K
242-01	0.4264	0.7622	0.	0.4573	45.7	* lp2 EHX secondary inlet pipe
242-02	0.4264	0.7622	0.	0.4573	45.7	* lp2 EHX secondary inlet pipe
246-01	0.476	1.6	0.	0.01905	45.7	* lp2 EHX secondary (tube)
246-02	0.476	1.6	0.	0.01905	45.7	* lp2 EHX secondary (tube)
246-03	0.476	1.6	0.	0.01905	45.7	* lp2 EHX secondary (tube)
246-04	0.476	1.6	0.	0.01905	45.7	* lp2 EHX secondary (tube)
250-01	0.203	0.75	0.75	0.508	45.7	* lp2 EHX secondary chimney
250-02	0.203	0.75	0.75	0.508	45.7	* lp2 EHX secondary chimney
250-03	0.203	0.75	0.75	0.508	45.7	* lp2 EHX secondary chimney
250-04	0.203	0.75	0.75	0.508	45.7	* lp2 EHX secondary chimney
254-01	1.66	1.	0.	0.	0.	* lp2 EHX sec sink 0.15077366 MPa
256-01	1.66	4.09	-4.09	1.449	45.7	* lp2 ACCUM tank top volume
256-02	1.66	0.12	-0.12	1.449	45.7	* lp2 ACCUM tank top
256-03	1.66	0.12	-0.12	1.449	45.7	* lp2 ACCUM tank top
256-04	1.66	0.12	-0.12	1.449	45.7	* lp2 ACCUM tank top
256-05	1.66	0.12	-0.12	1.449	45.7	* lp2 ACCUM tank top
256-06	0.08322	4.88	-4.88	0.3255	45.7	* lp2 ACCUM standpipe
258-01	0.08322	4.50	0.	0.3255	45.7	* lp2 cold-leg horizontal
258-02	0.08322	4.50	0.	0.3255	45.7	* lp2 cold-leg horizontal
262-01	0.08322	0.64538	0.0	0.3255	45.7	* lp2 cold-leg downcomer pipe
262-02	0.08322	13.93439	-13.93439	0.3255	45.7	* lp2 cold-leg downcomer pipe
271-01	0.03095	0.30	-0.3	0.1985	45.7	* lp2 IFD throat
271-02	0.03095	0.29	0.0	0.1985	45.7	* lp2 IFD throat
271-03	0.03095	0.94	0.0	0.1985	45.7	* lp2 IFD throat
274-01	0.08322	0.50	0.50	0.3255	45.7	* lp2 PVAW join pipe

LOOP3-LOOP3-LOOP3-LOOP3-LOOP3-LOOP3-LOOP3-LOOP3-LOOP3-

301-01	0.08322	3.28	0.	0.3255	45.7	* lp3 hot leg
304-01	0.08322	0.69	0.	0.3255	45.7	* lp3 hot leg
304-02	0.08322	12.95	0.	0.3255	45.7	* lp3 hot leg
304-03	0.08322	2.51	2.44	0.3255	45.7	* lp3 hot leg
306-01	0.08322	1.0	0.	0.3255	45.7	* lp3 MHX primary inlet plenum
308-01	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-02	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-03	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-04	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-05	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-06	0.841	2.03	0.	0.894	45.7	* lp3 MHX primary (shell)
308-07	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-08	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-09	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
308-10	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)

308-11	0.8258	1.11	0.	0.636	45.7	* lp3 MHX primary (shell)
312-01	0.08322	1.0	0.	0.3255	45.7	* lp3 MHX primary exit plenum
313-01	0.08322	1.981	-0.762	0.3255	45.7	* lp3 pipe joining HXs
313-02	0.08322	1.23	-0.6093	0.3255	45.7	* lp3 pipe joining HXs
313-03	0.08322	0.6096	-0.6096	0.3255	45.7	* lp3 pipe joining HXs
314-01	0.08322	1.0	0.	0.3255	45.7	* lp3 EHX primary inlet plenum
316-01	0.894	1.6	0.	0.00170	45.7	* lp3 EHX primary (shell)
316-02	0.894	1.6	0.	0.00170	45.7	* lp3 EHX primary (shell)
316-03	0.894	1.6	0.	0.00170	45.7	* lp3 EHX primary (shell)
316-04	0.894	1.6	0.	0.00170	45.7	* lp3 EHX primary (shell)
320-01	0.08322	1.0	0.	0.3255	45.7	* lp3 EHX primary exit plenum
322-01	0.08322	2.31	-0.305	0.3255	45.7	* lp3 cold leg
322-02	0.08322	2.13	0.	0.3255	45.7	* lp3 cold leg
322-03	0.08322	0.762	0.762	0.3255	45.7	* lp3 cold leg
324-01	1.5478	0.5	.0000	-	-	* lp3 primary coolant pump
326-01	0.08322	0.9146	0.0	0.3255	45.7	* lp3 pc pump discharge
329-01	0.08322	6.25	0.0	0.3255	45.7	* lp3 cold leg
330-01	1.66	1.	0.	0.	0.	* lp3 MHX sec src 302.55 K
334-01	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-02	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-03	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-04	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-05	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-06	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-07	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-08	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-09	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
334-10	0.776	1.314	0.	0.01588	45.7	* lp3 MHX secondary (tube)
336-01	1.66	1.	0.	0.	0.	* lp3 MHX sec sink 0.449 MPa
338-01	1.66	1.	0.	0.	0.	* lp3 EHX sec source 311.15 K
342-01	0.4264	0.7622	0.	0.4573	45.7	* lp3 EHX secondary inlet pipe
342-02	0.4264	0.7622	0.	0.4573	45.7	* lp3 EHX secondary inlet pipe
346-01	0.476	1.6	0.	0.01905	45.7	* lp3 EHX secondary (tube)
346-02	0.476	1.6	0.	0.01905	45.7	* lp3 EHX secondary (tube)
346-03	0.476	1.6	0.	0.01905	45.7	* lp3 EHX secondary (tube)
346-04	0.476	1.6	0.	0.01905	45.7	* lp3 EHX secondary (tube)
350-01	0.203	0.75	0.75	0.508	45.7	* lp3 EHX secondary chimney
350-02	0.203	0.75	0.75	0.508	45.7	* lp3 EHX secondary chimney
350-03	0.203	0.75	0.75	0.508	45.7	* lp3 EHX secondary chimney
350-04	0.203	0.75	0.75	0.508	45.7	* lp3 EHX secondary chimney
354-01	1.66	1.	0.	0.	0.	* lp3 EHX sec sink 0.15077365 MPa
356-01	1.65	4.09	-4.09	1.449	45.7	* lp3 ACCUM tank top volume
356-02	1.65	0.12	-0.12	1.449	45.7	* lp3 ACCUM tank top
356-03	1.65	0.12	-0.12	1.449	45.7	* lp3 ACCUM tank top
356-04	1.65	0.12	-0.12	1.449	45.7	* lp3 ACCUM tank top
356-05	1.65	0.12	-0.12	1.449	45.7	* lp3 ACCUM tank top
356-06	0.08322	4.88	-4.88	0.3255	45.7	* lp3 ACCUM standpipe
358-01	0.08322	7.24	0.	0.3255	45.7	* lp3 cold-leg horizontal
358-02	0.08322	7.24	0.	0.3255	45.7	* lp3 cold-leg horizontal
362-01	0.08322	1.2166	0.0	0.3255	45.7	* lp3 cold-leg downcomer pipe
362-02	0.08322	13.93439	-13.93439	0.3255	45.7	* lp3 cold-leg downcomer pipe
371-01	0.03095	0.30	-0.3	0.1985	45.7	* lp4 IFD throat
371-02	0.03095	0.51	0.0	0.1985	45.7	* lp4 IFD throat
371-03	0.03095	0.98	0.0	0.1985	45.7	* lp4 IFD throat
374-01	0.08322	0.50	0.50	0.3255	45.7	* lp3 PSVAW join pipe
LOOP4-LOOP4-LOOP4-LOOP4-LOOP4-LOOP4-LOOP4-LOOP4-LOOP4-						
451-01	0.08322	3.28	0.	0.3255	45.7	* lp4 hot leg
429-01	0.08322	6.25	0.0	0.3255	45.7	* lp4 col leg
458-01	0.08322	7.24	0.	0.3255	45.7	* lp4 cold-leg horizontal
458-02	0.08322	7.24	0.	0.3255	45.7	* lp4 cold-leg horizontal
462-01	0.08322	1.2166	0.0	0.3255	45.7	* lp4 cold-leg downcomer pipe
462-02	0.08322	13.93439	-13.93439	0.3255	45.7	* lp4 cold-leg downcomer pipe
471-01	0.03095	0.30	-0.3	0.1985	45.7	* lp4 IFD throat
471-02	0.03095	0.51	0.0	0.1985	45.7	* lp4 IFD throat
471-03	0.03095	0.98	0.0	0.1985	45.7	* lp4 IFD throat
474-01	0.08322	0.50	0.50	0.3255	45.7	* lp4 PSVAW join pipe



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