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ORNL Report

ØRCENT: A DIGITAL COMPUTER PROGRAM FOR SATURATED AND LOW SUPERHEAT STEAM TURBINE CYCLE ANALYSIS

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ØRCENT: A DIGITAL COMPUTER PROGRAM FOR SATURATED AND LOW
SUPERHEAT STEAM TURBINE CYCLE ANALYSIS

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ØRCENT: A DIGITAL COMPUTER PROGRAM FOR SATURATED AND LOW
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ABSTRACT

The program will perform full-load, design point calculations for steam turbine cycles supplied with throttle steam characteristic of contemporary water reactor power plants and will handle both condensing and back-pressure turbine exhaust arrangements. Turbine performance calculations are based on the General Electric Company method for large steam turbine-generators operating with saturated and low superheat throttle steam. Output includes all information normally shown on a turbine cycle heat balance diagram. The program is written in Fortran IV for the IBM 360/75 computer at Oak Ridge National Laboratory.

Keywords: AEC Sponsored + Coupling + Dual-purpose Plant + Feedwater Heating + Flowsheets + Heat Balance + Nuclear Desalination + Single-purpose Plants + Programs (computers) + Steam Cycle + Turbine-generators

INTRODUCTION

ØRCENT was prepared specifically to provide steam turbine cycle performance data for use in evaluations conducted by the Nuclear Desalination Program at Oak Ridge National Laboratory. Special attention has been given to simplification of input data requirements for both single-problem calculations and parametric studies. The program is written in Fortran IV for the IBM 360/75 digital computer at Oak Ridge National Laboratory. Turbine performance calculations are based on the method presented by the General Electric Company for predicting the performance of large steam turbine-generators operating with saturated and low superheat throttle steam conditions.¹ Reference to this GE paper is essential for applying and understanding the program.

¹F. G. Baily, K. C. Cotton, and R. C. Spencer, "Predicting the Performance of Large Steam Turbine-Generators Operating with Saturated and Low Superheat Steam Conditions," General Electric Company, GER-2454A, American Power Conference, Chicago, Illinois, April 25-27, 1967.

APPLICATION AND LIMITATIONS

The program will perform full-load, design point calculations for a wide range of input parameters. Part load calculations, off-design throttle and exhaust steam conditions, and heater-out-of-service calculations cannot be handled. In most cases input parameters outside the ranges specified can be handled; however, warning messages may be printed out and the results should be viewed with some suspicion. A reasonable turbine and cycle typical of contemporary practices must be specified; otherwise, unreasonable results may be produced. Typical cycles are shown on Figures 1, 2, and 3. Input parameters are discussed below.

1. Throttle steam temperature: 0 to $\sim 200^{\circ}\text{F}$ above saturation temperature.
2. Throttle steam pressure: ~ 200 to ~ 2000 psia.
3. Generator: 100 to 1500 Mva; conductor cooled or conventionally cooled; rated hydrogen pressure or reduced hydrogen pressure.
4. Number of turbine sections in series: 1, 2, or 3 (tandem arrangement only). A 1-section machine consists of a low-pressure section only. A 2-section machine consists of a high-pressure section followed by a cross-over system and a low-pressure section. A 3-section machine consists of a high-pressure section followed by a cross-over system, an intermediate-pressure section, a second cross-over system, and a low-pressure section. In each instance the initial turbine section is made up of a 1-row governing stage and a non-governing stage group. The number of parallel steam flow paths in each turbine section must be specified. Pressure losses for cross-over systems are calculated as described in Table III (2nd revision) GER-2454A.
5. Turbine speed: 1800 or 3600 rpm. Other speeds can be handled, but there probably will be minor errors in condensing group exhaust loss and generator loss calculations. For example, if a 3000-rpm machine is specified, losses for 3600 rpm will be selected by the program; if a 1500-rpm machine is specified, losses for 1800 rpm will be selected.

6. External moisture separator: Optional; must be located immediately following the intermediate-pressure section of a 3-section machine or immediately following the high-pressure section of a 2-section machine. The moisture separator can drain to a feedwater heater fed from the exhaust of the preceding turbine section, to any lower pressure feedwater heater, or to the condenser.
7. Live steam reheat: Optional; 1 or 2 stages located immediately preceding the low-pressure section of a 2-section machine or immediately preceding the intermediate-pressure section of a 3-section machine. A 1-stage reheat or the second stage of a 2-stage reheat is fed with throttle steam and drains to the highest pressure feedwater heater shell. The first stage of a 2-stage reheat is fed from the highest pressure feedwater heater extraction point and drains to the next highest pressure feedwater heater shell. For a 2-stage reheat cycle the highest pressure feedwater heater extraction point must be in the high-pressure section of the machine.
8. Externally-heated reheat: Optional; 1 stage located immediately preceding the low-pressure section of a 2-section machine or immediately preceding the intermediate-pressure section of a 3-section machine.
9. Turbine exhaust: Condensing or back-pressure. If the exhaust pressure is less than 3 psia, condensing turbine calculations will be performed and it is necessary to specify the last stage bucket length and pitch diameter. Combinations of last stage bucket length and pitch diameter normally specified by General Electric are listed on Figures 16 and 17 of GER-2454A. In addition, the program can accept a 52-in. bucket with a 152-in. pitch diameter. Other combinations of bucket length and pitch diameter can also be handled, but there will be errors in exhaust loss calculations. For back-pressure turbines (exhaust pressure \geq 3 psia) exhaust losses are calculated for non-condensing stage groups, and last stage bucket length and pitch diameter are not required. Back-pressure turbines are assumed to be 1% less efficient than condensing turbines.

10. Moisture removal stages: 0 to 5 in the low-pressure section only. Each moisture removal point will drain to the same or to the next lower pressure feedwater heater shell or will drain to the condenser if there are no intervening feedwater heaters.
11. Feedwater heaters: 0 to 12; optional drain cooler section; optional pumped or flashed drains; one heater can be a direct-contact type. An 8% pressure drop is assumed between the extraction stage and the shell of the feedwater heater except that 5% is assumed when the heater is fed from the high-pressure or intermediate-pressure exhaust.
12. Feedwater pump: Can be located at any point in the feedwater cycle; optional motor drive or steam turbine drive. For a 2-section or 3-section machine the feedwater pump turbine is fed from the cross-over just ahead of the low-pressure section or intermediate-pressure section, respectively. For a 1-section machine the feedwater pump turbine is fed from the main throttle steam supply. In all cases the feedwater pump turbine exhausts at the same pressure as the main turbine and the condensate is returned to the main condenser hotwell.
13. Makeup: Optional; supplied to the condenser hotwell.
14. Throttle valve stem and shaft packing leakage calculations: Optional. If these calculations are omitted, the calculated turbine cycle heat rate will be about 0.5% low and the generator output will be about 0.5% high.
15. Governing stage pitch diameter: In the absence of specific information 66 in. should be used for 1800-rpm machines and 41 in. for 3600-rpm machines. Small variations in this diameter will have only a minor effect on overall performance.

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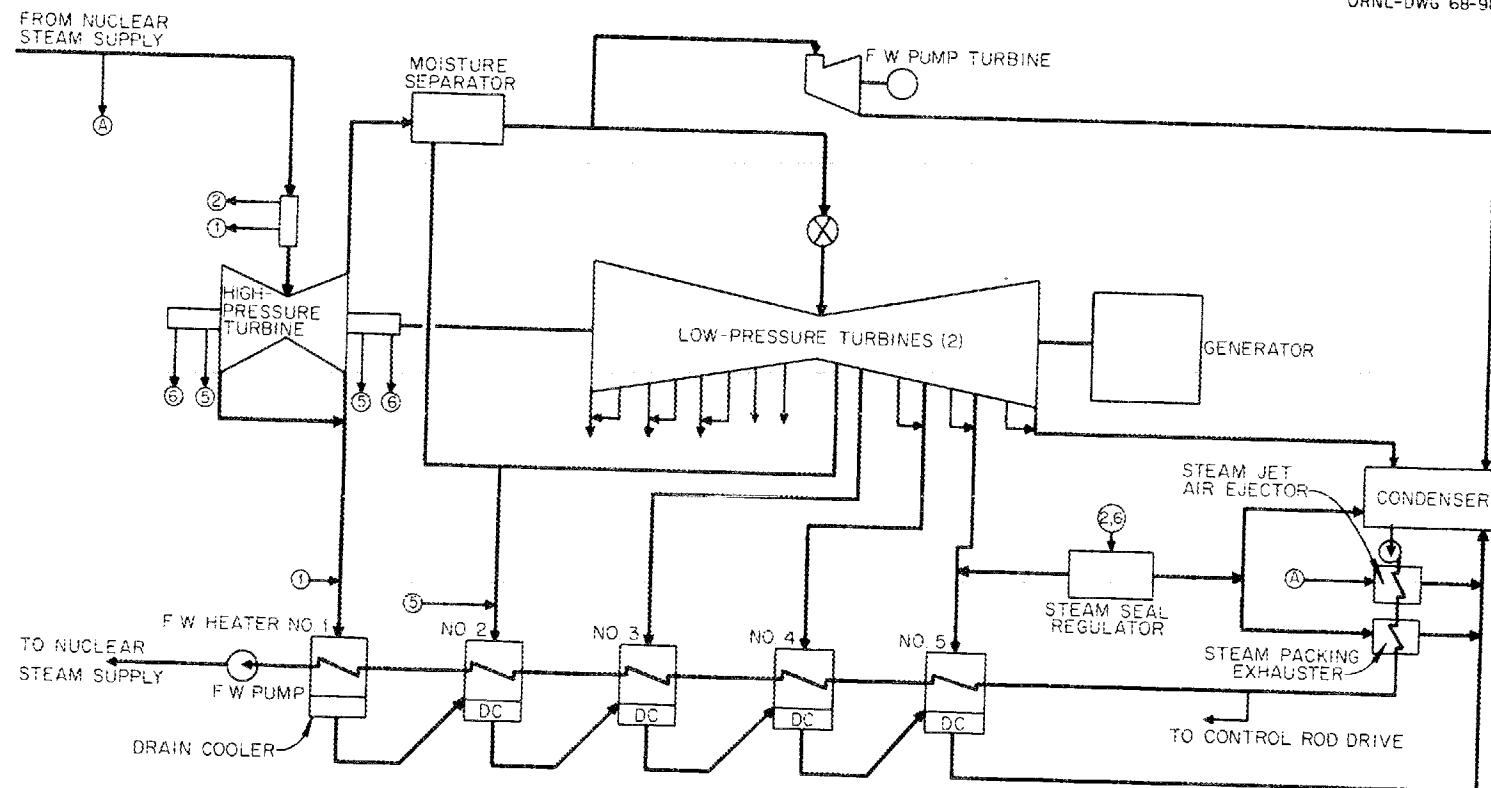


Figure 1. Typical BWR Cycle

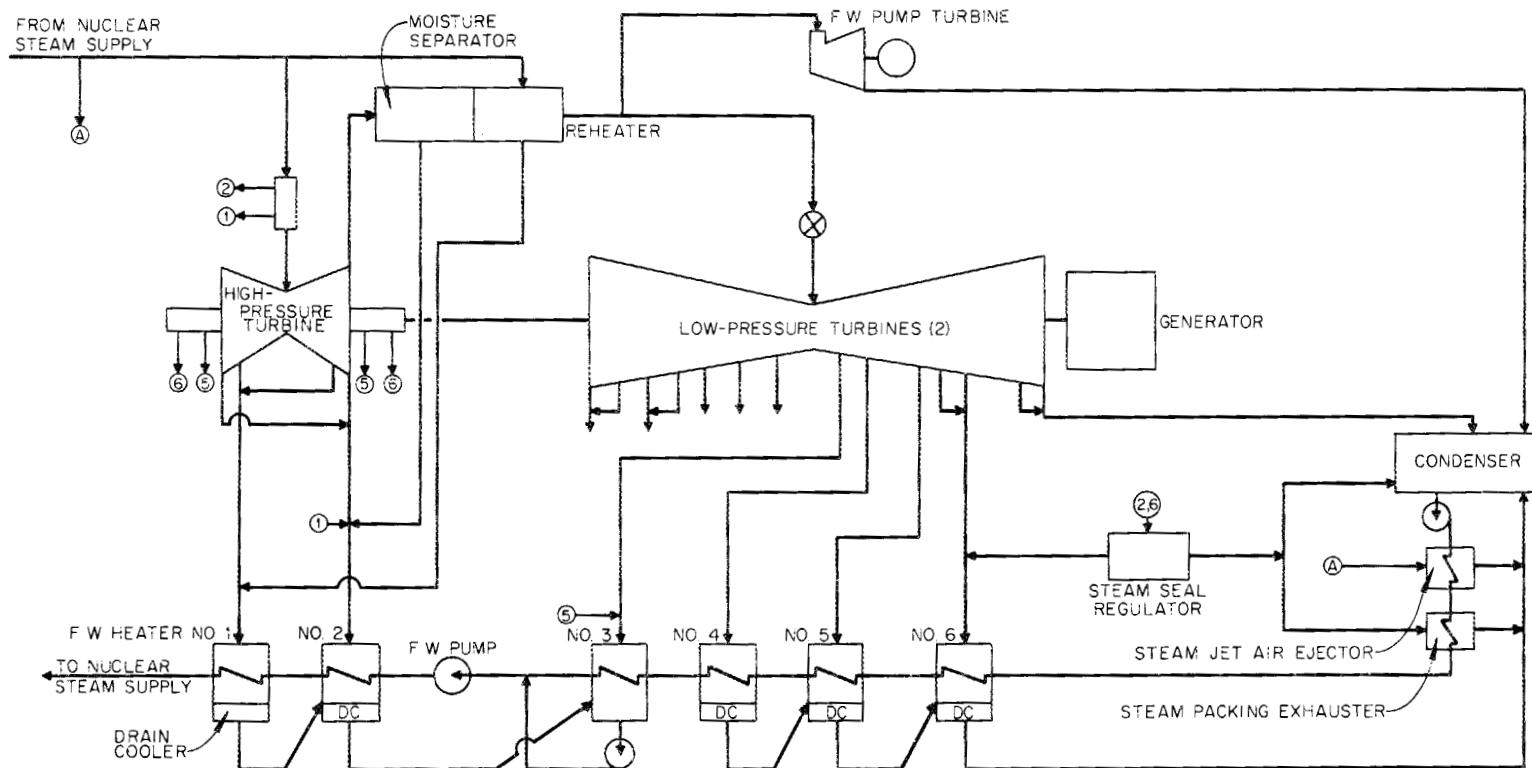


Figure 2. Typical PWR Cycle

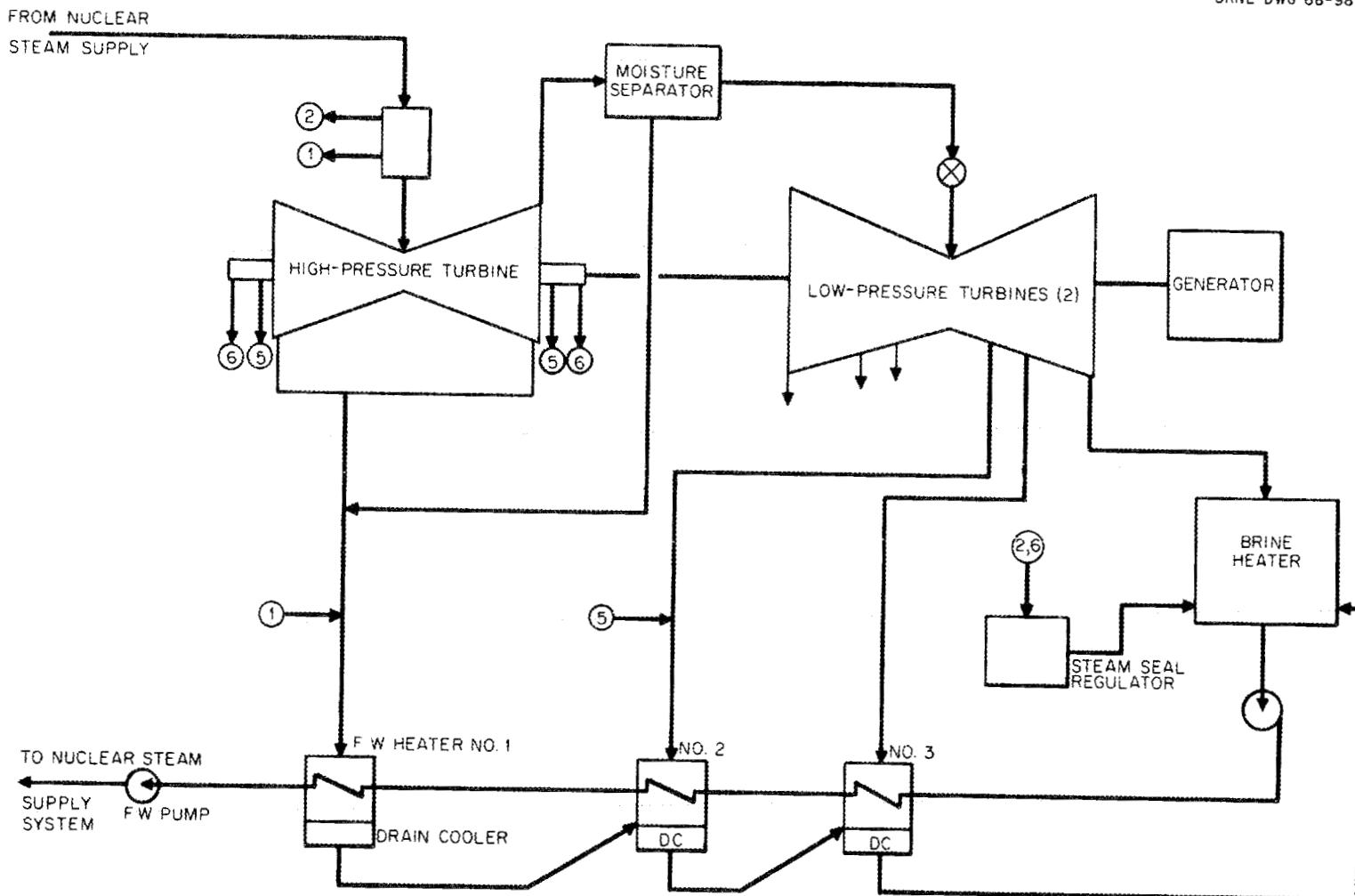


Figure 3. Typical Back-pressure Cycle

INPUT

The input data for a problem are entered on cards as shown on Figure 4 and as described below. The first card of the data deck must be a comment card containing any desired alpha-numeric information in Columns 1-72. The information on this card is used to label the output. Subsequent cards are read with the format statement, (I2, D10.0, 5D12.0, 8X). Columns 1 and 2 are reserved for an integer variable, IFLAG, which is used to identify the data in Columns 3-72. Columns 73-80 may be used for identification by the program user; they are not read by the program. Data card variables are defined below.

1. IFLAG = 1
 - TT = throttle steam temperature, °F
 - PT = throttle steam pressure, psia
 - AMT = throttle steam moisture, %
2. IFLAG = 2
 - QT = estimated throttle steam flow, lb_m/hr
 - PCMU = feedwater makeup rate, %
 - QCR = condensate flow by-passed to steam generator, lb_m/hr
3. IFLAG = 3
 - WRATE = gross electrical output, Mwe
 - GC = generator capability, Mva
 - PF = generator power factor
 - If ICC = 0, generator is conductor cooled
 - If ICC = 1, generator is conventionally cooled
 - If IH2 = 0, generator operates with rated hydrogen pressure
 - If IH2 = 1, generator operates with reduced hydrogen pressure
 - IR = rotational speed of turbine-generator, rpm
4. IFLAG = 4 (This card is not used and should not be included in the data deck.)
5. IFLAG = 5
 - PDGS = pitch diameter of governing stage, in.
6. IFLAG = 6
 - NSHAFT = number of turbine sections in series
7. IFLAG = 7 (This card is not required if NSHAFT = 1.)
 - NHP = number of parallel high-pressure turbine section flow paths

8. IFLAG = 8 (This card is not required if NSHAFT < 3.)
NIP = number of parallel intermediate-pressure turbine section flow paths
PBIP = bowl pressure of intermediate-pressure turbine, psia
9. IFLAG = 9
NLP = number of parallel low-pressure turbine section flow paths
PBLP = bowl pressure of low-pressure turbine, psia (leave blank if NSHAFT = 1)
PXLP1 = exhaust pressure of low-pressure turbine, in. HgA
PXLP = exhaust pressure of low-pressure turbine, psia (must be preceded by a minus sign)
PDLS = pitch diameter of last stage, in. (leave blank if PXLP \geq 3 psia)
BLS = length of last stage buckets, in. (leave blank if PXLP \geq 3 psia)
PCI = condenser pressure, in. HgA
PC = condenser pressure, psia (must be preceded by a minus sign)
10. IFLAG = 10
MR = number of moisture removal stages in low-pressure turbine (MR \leq 5)
PMR(L) = moisture removal stage pressure, psia (L = 1, MR starting from bowl end of low-pressure turbine; leave blank if MR = 0)
11. IFLAG = 11
If MS = 0, there is no external moisture separator
If MS = N, the external moisture separator drains to Feedwater Heater No. N
If MS = NF + 1, the external moisture separator drains to the condenser
EMS = moisture separator effectiveness, % (leave blank if MS = 0)
12. IFLAG = 12
If NRH = 0, there is no reheater
If NRH > 0, there is either a 1-stage or a 2-stage live steam reheater, and
NRH = number of stages of reheat

QERH1 = estimated heating steam flow to the first stage, lb_m/hr
 (leave blank if NRH < 1)

TTDRH1 = terminal temperature difference of the first stage, °F
 (leave blank if NRH = 0)

QERH2 = estimated heating steam flow to the second stage, lb_m/hr
 (leave blank if NRH < 2)

TTDRH2 = terminal temperature difference of the second stage,
 °F (leave blank if NRH < 2)

If NRH = -1, there is a 1-stage externally-heated reheater, and
 TTDRH1 = temperature of steam leaving reheater, °F

13. IFLAG = 13

NF = total number of feedwater heaters (NF \leq 12; NF = NFGS +
 NFH + NFI + NFL)

NFGS = number of feedwater heaters fed from the governing stage
 exhaust (NFGS \leq 1)

NFH = number of feedwater heaters fed from high-pressure turbine
 (leave blank if NSHAFT = 1)

NFI = number of feedwater heaters fed from intermediate-pressure
 turbine (leave blank if NSHAFT < 3)

NFL = number of feedwater heaters fed from low-pressure turbine

14. IFLAG = 14 (one card required for each feedwater heater)

N = feedwater heater number (N = 1, NF starting from high-pressure
 end)

PE(N) = extraction stage pressure, psia (leave blank if feedwater
 heater is fed from governing stage exhaust, high-pressure
 turbine exhaust, or intermediate-pressure turbine exhaust)

TTD(N) = feedwater heater terminal temperature difference, °F
 (a direct contact feedwater heater can be specified by
 letting TTD(N) = 0 and ND(N) = 1)

If ND(N) = 0, the feedwater heater drain is flashed to the next
 lower pressure feedwater heater shell, or to the condenser
 hotwell when N = NF

If ND(N) = 1, the feedwater heater drain is pumped forward to
 the feedwater discharge from Feedwater Heater No. N

If NDC(N) = 0, the feedwater heater is not provided with a
 drain cooler

If NDC(N) = 1, the feedwater heater is provided with a drain cooler

TDCA(N) = drain cooler approach temperature, °F (leave blank if NDC(N) = 0)

15. IFLAG = 15

If IP = 0, the feedwater pump is located at the outlet of Feedwater Heater No. 1

If IP = N, the feedwater pump is located at the inlet of Feedwater Heater No. N

If IFPT = 0, the feedwater pump is motor driven

If IFPT = 1, the feedwater pump is turbine driven and steam flow, bowl steam enthalpy, and exhaust steam enthalpy will be calculated by the program

If IFPT = -1, the feedwater pump is turbine driven and steam flow, bowl steam enthalpy, and exhaust steam enthalpy must be input

QFPT = steam flow to feedwater pump turbine, lb_m/hr (leave blank if IFPT > -1)

HBFPT = bowl steam enthalpy to feedwater pump turbine, Btu/lb_m (leave blank if IFPT > -1)

HXFPT = exhaust steam enthalpy from feedwater pump turbine, Btu/lb_m (leave blank if IFPT > -1)

16. IFLAG = 16

QAE = steam flow to steam jet air ejector, lb_m/hr (leave blank or enter zero if there is no steam jet air ejector)

17. IFLAG = 17

If LK = 0, throttle valve stem and turbine shaft leakages will not be calculated

If LK = 1, throttle valve stem and turbine shaft leakages will be calculated

The last data card for a problem must either be blank or have a zero in Column 2 which will terminate reading of input data. Input data will be printed and control will be returned to the main program where the calculations will be started.

After the calculations are finished and the results printed, the program is ready to read a new set of input data. A new comment card is required. If a parametric study is being made, it is necessary, in addition to the comment card, to read only those data cards on which the parameters being changed are entered.

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COMMENTS (Up to 72 alpha-numeric characters)										72	73	80				
1	3	12	13	24	25	36	37	48	49	60	61	72	73	80		
2	QT	PCMU	QCR													
3	WRATE	GC	PF	ICC	IH2	IR										
4	PDGS															
5	NSHAFT															
6	NHP															
7	NIP	PBIP														
8	NLP	PBLP	PXLPI or -PXLP	PDLS	BLS	PCI or -PC										
9																
10	23	12	13	24	25	36	37	48	49	60	61	72	73	80		
11	MR	PMR(1)	PMR(2)	PMR(3)	PMR(4)	PMR(5)										
12	MS	EMS														
13	NRH	QERH1	TTDRH1	QERH2	TTDRH2											
14	NF	NFGS	NFH	NFI	NFL											
15	N	PE(N)	TTD(N)	ND(N)	NOC(N)	TOCA(N)										
16	IP	IFPT	QFPT	HBFPT	HXFPT											
17	QAE															
18	LK															
19																

Figure 4. Data Cards

OUTPUT

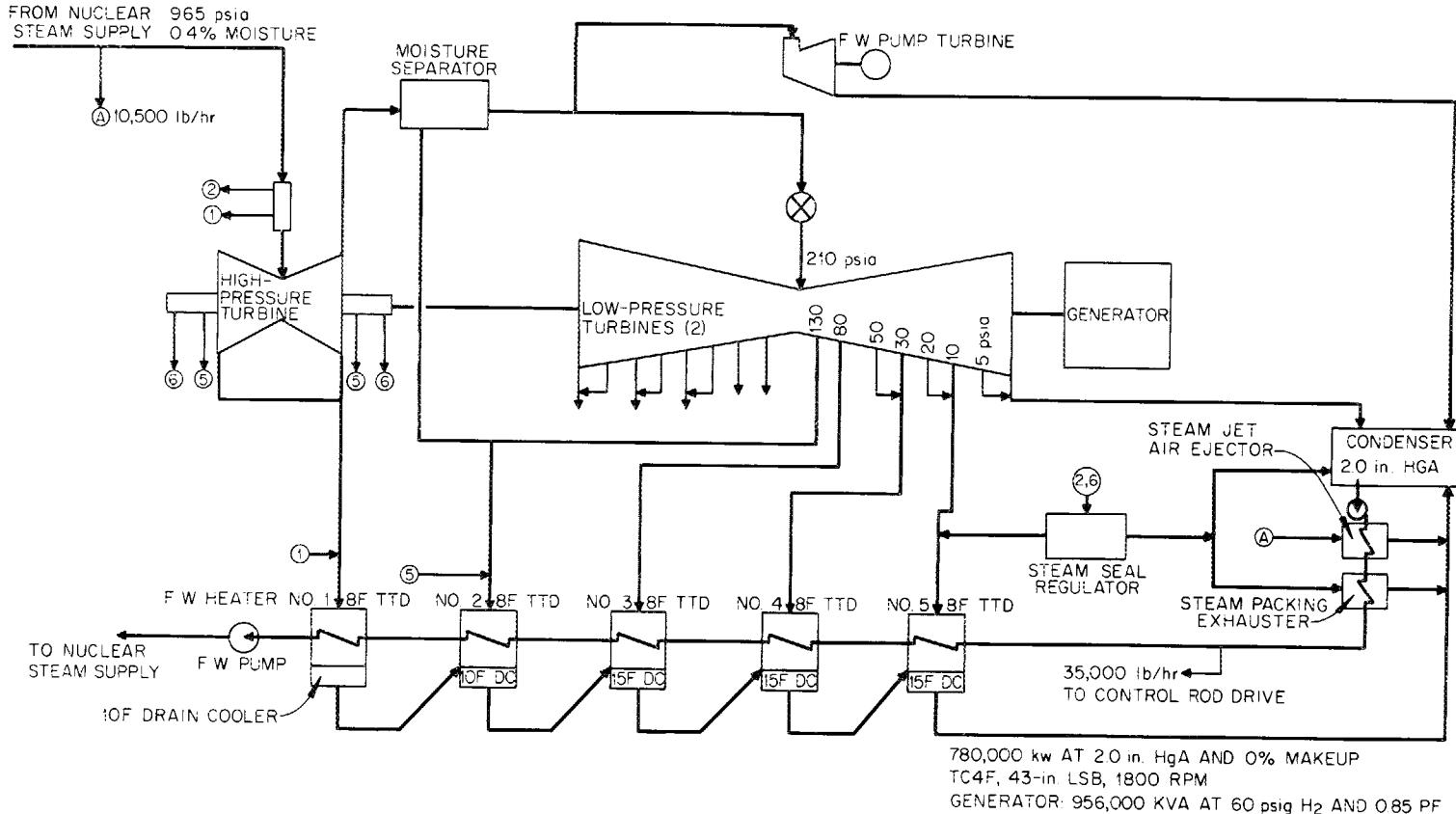
Output from the program includes all information normally shown on a steam turbine cycle heat balance diagram. The input data are printed first by subroutine DATAIN before control is returned to the main program and before the calculations are performed. If iteration limits are exceeded or independent variable limits for the turbine performance functions are exceeded, warning messages will be printed next. Results of the calculations are printed by subroutine RESULT and are summarized in ten tables, each headed by the information read from the comment card.

APPENDIX A

SAMPLE PROBLEM

To illustrate the use of ØRCENT, a sample problem together with a complete input-output listing is included in this appendix. The turbine cycle selected and input data required are shown on Figure 5. The input data, entered on coding forms ready for key-punching, are shown on Figure 6. This problem required about one-half minute of machine time. An exact estimate of throttle steam flow did not reduce machine time significantly.

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Figure 5. Turbine Cycle for Sample Problem

							REFERENCE
12	24	36	48	60	72	60	
SAMPLE PROBLEM							
1 540.3	965.	0.4					
2 7800000.0		35000.					
3 780.	956.	0.85	0.	0.	1800.		
5 66.							
6 9.							
7 2.							
9 4.	210.	2.	132.	43.	2.		
10 5.	50.	30.	20.	10.	5.		
11 2.	100.						
12 0.							
13 5.	0.	1.		9.			
14 1.	0.	6.	0.	1.	10.		
14 2.	130.	8.	0.	1.	10.		
14 3.	80.	8.	0.	1.	15.		
14 4.	30.	8.	0.	1.	15.		
14 5.	10.	8.	0.	1.	15.		
15 0.	1.						
16 10500.							
17 1.							
0							

Figure 6. Input Data for Sample Problem

SAMPLE PROBLEM
 STEAM TURBINE CYCLE HEAT BALANCE
 ORCENT, VERSION 9/23/68

INPUT DATA

THROTTLE STEAM TEMPERATURE	540.3	F			
THROTTLE STEAM PRESSURE	965.0	PSIA			
THROTTLE STEAM MOISTURE	0.40	PER CENT			
ESTIMATED THROTTLE STEAM FLOW	7800000.	LB/HR			
FW MAKE-UP RATE (TO CONDENSER HOTWELL)	0.0	PER CENT			
CONDENSATE BY-PASSED TO STEAM GENERATOR	35000.	LB/HR			
REQUIRED ELECTRICAL OUTPUT	780,000	MWE			
GENERATOR RATED CAPABILITY	956,000	MVA			
GENERATOR POWER FACTOR	0.85				
CONDUCTOR-COOLED GENERATOR, TCC= 0					
GENERATOR OPERATION AT RATED HYDROGEN PRESSURE, TH2= 0					
ROTATIONAL SPEED OF TURBINE-GENERATOR	1800	RPM			
PITCH DIAMETER OF GOVERNING STAGE	66.00	IN.			
NO. OF TURBINE SECTIONS IN SERIES	2				
NUMBER OF PARALLEL HP SECTIONS	2				
NUMBER OF PARALLEL LP SECTIONS	4				
BOWL PRESSURE LP SECTION	210.0	PSIA			
EXHAUST PRESSURE LP SECTION	0.98232	PSIA	=	2.00	IN. HGA
CONDENSER PRESSURE	0.98232	PSIA	=	2.00	IN. HGA
PITCH DIAMETER OF LAST STAGE LP SECTION	132.00	IN.			
LENGTH OF LAST STAGE BUCKETS LP SECTION	43.00	IN.			
NO. OF MOISTURE REMOVAL STAGES LP SECTION	5				
MOISTURE REMOVAL STAGE NO. 1					
MOISTURE REMOVAL STAGE PRESSURE	50.0	PSIA			
MOISTURE REMOVAL STAGE NO. 2					
MOISTURE REMOVAL STAGE PRESSURE	30.0	PSIA			
MOISTURE REMOVAL STAGE NO. 3					
MOISTURE REMOVAL STAGE PRESSURE	20.0	PSIA			
MOISTURE REMOVAL STAGE NO. 4					
MOISTURE REMOVAL STAGE PRESSURE	10.0	PSIA			
MOISTURE REMOVAL STAGE NO. 5					
MOISTURE REMOVAL STAGE PRESSURE	5.0	PSIA			
EXTERNAL MOISTURE SEPARATOR DRAINS TO FW HEATER NO. 2, MS= 2					
MOISTURE SEPARATOR EFFECTIVENESS	100.	PER CENT			
NUMBER OF STAGES OF REHEAT	0				
TOTAL NO. OF FW HEATERS	5				
NO. OF FW HEATERS GS SECTION	0				

NO. OF FW HEATERS HP SECTION	1	
NO. OF FW HEATERS LP SECTION	4	
FW HEATER NO. 1		
EXTRACTION STAGE PRESSURE	0.0	PSTA
TERMINAL TEMPERATURE DIFFERENCE	8.0	F
DRAIN IS FLASHED, NDI 1)= 0		
THERE IS A DRAIN COOLER SECTION, NDC(1)= 1		
DRAIN COOLER APPROACH TEMPERATURE DIFFERENCE	10.0	F
FW HEATER NO. 2		
EXTRACTION STAGE PRESSURE	130.0	PSTA
TERMINAL TEMPERATURE DIFFERENCE	8.0	F
DRAIN IS FLASHED, NDI 2)= 0		
THERE IS A DRAIN COOLER SECTION, NDC(2)= 1		
DRAIN COOLER APPROACH TEMPERATURE DIFFERENCE	10.0	F
FW HEATER NO. 3		
EXTRACTION STAGE PRESSURE	80.0	PSTA
TERMINAL TEMPERATURE DIFFERENCE	8.0	F
DRAIN IS FLASHED, NDI 3)= 0		
THERE IS A DRAIN COOLER SECTION, NDC(3)= 1		
DRAIN COOLER APPROACH TEMPERATURE DIFFERENCE	15.0	F
FW HEATER NO. 4		
EXTRACTION STAGE PRESSURE	30.0	PSTA
TERMINAL TEMPERATURE DIFFERENCE	8.0	F
DRAIN IS FLASHED, NDI 4)= 0		
THERE IS A DRAIN COOLER SECTION, NDC(4)= 1		
DRAIN COOLER APPROACH TEMPERATURE DIFFERENCE	15.0	F
FW HEATER NO. 5		
EXTRACTION STAGE PRESSURE	10.0	PSTA
TERMINAL TEMPERATURE DIFFERENCE	8.0	F
DRAIN IS FLASHED, NDI 5)= 0		
THERE IS A DRAIN COOLER SECTION, NDC(5)= 1		
DRAIN COOLER APPROACH TEMPERATURE DIFFERENCE	15.0	F
FW PUMP IS LOCATED AFTER FW HEATER NO. 1, IP= 0		
FW PUMP IS TURBINE DRIVEN, TRPT= 1		
STEAM FLOW TO FW PUMP TURBINE WILL BE CALCULATED		
STEAM FLOW TO STEAM JET AIR EJECTOR	10500.	LB/HR
VALVE STEM AND PACKING LEAKAGES WILL BE CALCULATED, LK= 1		

SAMPLE PROBLEM
STEAM TURBINE CYCLE HEAT BALANCE
ORCENT, VERSION 9/23/68

CALCULATED RESULTS

TABLE I OVERALL PERFORMANCE

NET TURBINE CYCLE HEAT RATE, BTU/KW-HR	10087.
NET TURBINE CYCLE EFFICIENCY, PER CENT	33.83
GROSS TURBINE CYCLE HEAT RATE, BTU/KW-HR	9949.
GROSS TURBINE CYCLE EFFICIENCY, PER CENT	34.30
GENERATOR OUTPUT, MWE	779.999
POWER REQUIRED BY TURBINE-DRIVEN FW PUMP, MW	10.814
GENERATOR OUTPUT PLUS FW PUMP POWER, MW	790.813
MECHANICAL LOSSES, KW	3678.
GENERATOR LOSSES, KW	9984.

TABLE II TURBINE EXPANSION LINE

	STEAM FLOW LB/HR	PRESSURE PSIA	TEMPERATURE F	MOISTURE PER CENT	ENTHALPY BTU/LB	ENTROPY BTU/LB-F
TURBINE THROTTLE	9416640.	965.0	540.3	0.40	1190.5	
GOVERNING STAGE BOWL	9406753.	918.0	534.3	0.65	1190.5	1.3954
GOVERNING STAGE ELEP AND UEEP	9406753.	678.2	499.6	4.52	1169.4	1.3993
HP SECTION BOWL	9406753.	678.2	499.6	4.52	1169.4	1.3993
HP SECTION ELEP	9406753.	225.4	391.9	12.35	1097.0	1.4143
HP SECTION UEEP		225.4			1098.5	
EXTERNAL MOISTURE SEPARATOR INLET	8808837.	223.8			1098.5	
EXTERNAL MOISTURE SEPARATOR OUTLET	7741763.	221.6	390.5	0.00	1199.7	
LP SECTION BOWL	7605490.	210.0	386.9	0.0	1199.7	1.5420
BEFORE MOISTURE REMOVAL NO. 1		50.0	281.0	8.11	1099.2	1.5573
AFTER MOISTURE REMOVAL NO. 1		50.0	281.0	7.95	1100.6	1.5593
BEFORE MOISTURE REMOVAL NO. 2		30.0	250.3	9.94	1070.2	1.5671
AFTER MOISTURE REMOVAL NO. 2		30.0	250.3	9.67	1072.7	1.5706
BEFORE MOISTURE REMOVAL NO. 3		20.0	228.0	11.07	1049.9	1.5772
AFTER MOISTURE REMOVAL NO. 3		20.0	228.0	10.66	1053.9	1.5829
BEFORE MOISTURE REMOVAL NO. 4		10.0	193.2	12.81	1017.5	1.5951
AFTER MOISTURE REMOVAL NO. 4		10.0	193.2	11.77	1027.7	1.6106
BEFORE MOISTURE REMOVAL NO. 5		5.0	162.2	13.72	993.7	1.6232
AFTER MOISTURE REMOVAL NO. 5		5.0	162.2	10.79	1023.1	1.6705
LP SECTION ELEP	5524744.	0.98232	101.1	15.16	948.6	1.6995
LP SECTION UEEP		0.98232			962.9	

TABLE III STEAM JET AIR EJECTOR

STEAM FLOW, LB/HR	10500.
STEAM ENTHALPY IN, BTU/LB	1190.5
STEAM ENTHALPY OUT, BTU/LB	180.1

TABLE IV EXTERNAL MOISTURE SEPARATOR DRAINS TO FW HEATER NO. 2

DRAIN FLOW, LB/HR	1067774.
DRAIN PRESSURE, PSIA	221.6
DRAIN TEMPERATURE, F	390.5
DRAIN ENTHALPY, BTU/LB	364.7

TABLE V THERE IS NO REHEATER

TABLE VI MOISTURE REMOVAL STAGES

MOISTURE REMOVAL STAGE NO.	1	2	3	4	5
DRAINS TO FW HEATER NO.	4	4	5	5	0
STAGE PRESSURE, PSIA	50.0	30.0	20.0	10.0	5.0
TEMPERATURE, F	281.0	250.3	228.0	193.2	162.2
WATER REMOVED, LB/HR	11918.	19823.	29364.	74253.	189137.
WATER ENTHALPY, BTU/LB	250.1	218.8	196.2	161.2	130.1
STEAM REMOVED, LB/HR	34177.	0.0	31865.	0.0	28739.
STEAM ENTHALPY, BTU/LB	1100.6	0.0	1053.9	0.0	1023.1

TABLE VII FW HEATERS

FW HEATER NO.	1	2	3	4	5
FW FLOW, LB/HR	9392140.	9392140.	9392140.	9392140.	9392140.
FW TEMPERATURE OUT, F	379.6	333.0	298.3	237.6	181.3
FW ENTHALPY OUT, BTU/LB	353.0	303.8	267.8	205.9	149.2
FW TEMPERATURE IN, F	333.0	298.3	237.6	181.3	102.8
FW ENTHALPY IN, BTU/LB	303.8	267.8	215.9	149.2	70.7
EXTRACTION STAGE PRESSURE, PSIA	225.4	130.0	80.0	30.0	10.0
EXTRACTION STEAM FLOW, LB/HR	581096.	249567.	520614.	396437.	495583.
EXTRACTION STEAM ENTHALPY, BTU/LB	1098.5	1163.2	1129.3	1072.7	1027.7
SHELL PRESSURE, PSIA	214.1	119.6	73.6	27.6	9.2
SHELL TEMPERATURE, F	387.6	341.0	306.3	245.6	189.3
SHELL DRAIN FLOW, LB/HR	588673.	1909858.	2430472.	2892826.	3527177.
SHELL DRAIN TEMPERATURE, F	343.0	308.3	252.6	196.3	117.8
SHELL DRAIN ENTHALPY, BTU/LB	314.3	278.2	221.1	164.3	85.7

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TABLE VIII CONDENSER

CONDENSER PRESSURE, PSIA	0.98232	=	2.00	IN _c HGA
CONDENSATE FLOW, LB/HR	9427140.			
CONDENSATE TEMPERATURE, F	101.1			
CONDENSATE ENTHALPY, BTU/LB	69.1			

TABLE IX CONDENSATE AND FEEDWATER

CONDENSATE FLOW BY-PASSED TO STEAM GENERATOR, LB/HR	35000.
CONDENSATE ENTHALPY BY-PASSED TO STEAM GENERATOR, BTU/LB	70.7
FW FLOW TO FW PUMP, LB/HR	9392140.
FW TEMPERATURE TO FW PUMP, F	379.5
FW ENTHALPY TO FW PUMP, BTU/LB	353.0
FW ENTHALPY RISE ACROSS FW PUMP, BTU/LB	3.9
FW PRESSURE INCREASE ACROSS FW PUMP, PSI	1056.
FW FLOW TO STEAM GENERATOR, LP/HR	9392140.
FW TEMPERATURE TO STEAM GENERATOR, F	392.0
FW ENTHALPY TO STEAM GENERATOR, BTU/LB	357.0
MAKE-UP TO CONDENSER HOTWELL, LB/HR	0.0
STEAM FLOW FROM STEAM GENERATOR, LB/HR	9427140.
STEAM ENTHALPY FROM STEAM GENERATOR, BTU/LB	1190.5
THROTTLE STEAM FLOW FW PUMP TURBINE, LB/HR	135572.
THROTTLE PRESSURE FW PUMP TURBINE, PSIA	212.7
THROTTLE ENTHALPY FW PUMP TURBINE, BTU/LB	1190.7
EXHAUST PRESSURE FW PUMP TURBINE, PSIA	0.98232
EXHAUST ENTHALPY FW PUMP TURBINE, BTU/LB	927.5

TABLE X VALVE STEM AND SHAFT LEAKAGES

STEAM SEAL REGULATOR	
FLOW TO SSR, LB/HR	15286.
ENTHALPY AT SSR, BTU/LB	1112.4
FLOW FROM SSR TO MAIN CONDENSER, LB/HR	7200.
FLOW FROM SSR TO STEAM PACKING EXHAUSTER, LB/HR	4800.
FLOW FROM SSR TO FW HEATER NO. 5, LB/HR	3286.
MAKE-UP FROM THROTTLE STEAM, LP/HR	0.0
ENTHALPY OF MAKE-UP STEAM, BTU/LB	0.0
THROTTLE VALVE STEM	
LEAK NO. 1 (DRAINS TO FW HEATER NO. 1), LB/HR	7578.
ENTHALPY LEAK NO. 1, BTU/LB	1190.5
LEAK NO. 2 (DRAINS TO SSR), LB/HR	2310.
ENTHALPY LEAK NO. 2, BTU/LB	1190.5
GOVERNING STAGE SECTION	
LEAK NO. 3 (DRAINS TO FW HEATER NO. 01), LB/HR	0.0
ENTHALPY LEAK NO. 3, BTU/LB	0.0
LEAK NO. 4 (DRAINS TO SSR), LB/HR	0.0
ENTHALPY LEAK NO. 4, BTU/LB	0.0
HP TURBINE SECTION	
TOTAL LEAK NO. 5 (DRAINS TO FW HEATER NO. 2), LB/HR	3843.
ENTHALPY LEAK NO. 5, BTU/LB	1098.5
TOTAL LEAK NO. 6 (DRAINS TO SSR), LB/HR	12977.
ENTHALPY LEAK NO. 6, BTU/LB	1098.5

APPENDIX B

FORTRAN LISTING

This appendix contains a brief description and a complete Fortran listing of the main program and the 60 subprograms. The primary function of the main program is to control the order of calculations and to call the subprograms required by the cycle specified by the input data. (It also performs some calculations.) There are no programmed stops or exits. If a convergence criterion is not satisfied or if the allowable range of an independent variable is exceeded, a warning message will be printed and calculations will continue.

1. DATAIN - reads input data cards and prints input data before returning control to main program.
2. RESULT - prints results of calculations for each problem before proceeding to the next problem.
3. AMOIST - performs internal moisture removal calculations for the low-pressure turbine (Table IV, GER-2454A).
4. FWHEAT - performs heat and mass balance calculations for the feedwater heaters.
5. FWHPAR - calculates the following feedwater heater parameters: shell pressure, shell drain temperature, feedwater inlet temperature, and feedwater outlet temperature.
6. FWPT - calculates steam flow to the feedwater pump turbine.
7. GOVERN and GSTAGE - calculate turbine governing stage performance and shell steam conditions.
8. HXTRAC - calculates feedwater heater extraction steam enthalpy after the turbine expansion line has been determined.
9. INDEX - calculates integer indices for keeping track of steam flows and enthalpies in the low-pressure turbine.
10. PRDROP - calculates cross-over system pressure drops [Table III (2nd revision), GER-2454A].
11. REHEAT - calculates reheater parameters required for reheater heat and mass balance calculations.
12. SGRUP - calculates turbine non-governing stage group performance and shell steam conditions.

- 13. SLEAK1, SLEAK2, and SLEAK3 - calculate throttle valve stem packing and turbine shaft packing leakage flows and enthalpies (Table II, GER-2454A).
- 14. SSRE - calculates steam seal regulator flows and enthalpies (Table II, GER-2454A).
- 15. XLLOSS - calculates exhaust loss and used energy end-point for low-pressure condensing turbine.
- 16. XSEP - performs heat and mass balance calculations for external moisture separator.
- 17. The following 24 subprograms perform the calculations required to determine turbine efficiencies and losses (Appendix IV, GER-2454A).

FIG1	FIG8	FIG19
FIG2	FIG10	FIG20
FIG3	FIG12A	FIG21
FIG4	FIG12B	FIG22
FIG5	FIG14	UNIPOL
FIG6	FIG15	BIVPOL
FIG6A	FIG167	RATFUN
FIG7	FIG18	LAGRAN

- 18. The following 17 subprograms calculate properties of water and steam.

TLIQH	VVAP	TSAT
HC \emptyset M	TVAPH	PSAT
TC \emptyset M	TVAPS	PROPHS
LINT2	HLIQ	PROPPH
HVAP	SLIQ	PROPPS
SVAP	VLIQ	

```

C PROGRAM ORCENT                                ORCE   0
C THIS PROGRAM CALCULATES CYCLE EFFICIENCY FOR NUCLEAR TURBINES AS      ORCE   1
C DESCRIBED IN GER-2454A, 'PREDICTING THE PERFORMANCE OF LARGE STEAM      ORCE   11
C TURBINE-GENERATORS OPERATING WITH SATURATED AND LOW SUPERHEAT STEAM     ORCE   12
C CONDITIONS', BY F G RILEY, K C COTTON, AND R C SPENCER, LARGE STEAM      ORCE   13
C TURBINE-GENERATOR DEPARTMENT, GENERAL ELECTRIC COMPANY, SCHENECTADY,      ORCE   14
C NEW YORK, 1967.                                         ORCE   15
C ORCE   16
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C ORCE 361

C DATA INPUT. INPUT VARIABLES ARE DEFINED IN SUBROUTINE DATAIN.

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100 CONTINUE
    CALL DATAINT CNTS, TT, PT, AMT, QT, WRATE, GC, PCMU, PDGS,
    1 NSHAFT, NHP, IRHP, NIP, IRIP, PRTP, NLP, IRLP, PRLP, PXLP, PDLS,
    2 PLS, MR, PMR, MS, NRH, QERH1, TTORH1, QERH2, TTORH2, NF, NFGS,
    3 NFH, NFI, NFL, PE, TTD, ND, NDC, TDCA, IP, QFPT, IFPT, QAE, LK,
    4 PF, ICC, IH2, VERS, QCR, HBFPT, HXFPT, PG, EMS)
    MATTN=0

C C START CALCULATIONS
C
C THRCITLF STEAM ENTHALPY
    HT=HVAP(TT,PT)
    IF(AMT.LE.0.0)GOTO1210
    AMT1=AMT*0.01
    HT=(1.0-AMT1)*HT+AMT1*HLT0(TT)

C C GOVERNING STAGE PARAMETERS
1210 HRGS=HT
    PRGS=PT*0.9513
    NCGS=0
    IF(NSHAFT.GT.0)GOTO1220
    IRGS=IRLP
    NGS=NLP
    GOT01230
1220 IRGS=IRHP
    NGS=NHP

C C SPEED LEVEL CORRECTION
1230 CSLP=FIG6A(IRLP)
    GOT0(1260,1250,1240),NSHAFT
1240 CSIP=FIG6A(IRIP)
1250 CSHP=FIG6A(IRHP)

C C GENERATOR
1260 IF(ICC.EQ.0)GOTO1263
    IF(IRLP=1800)1261,1261,1262
C ICK= 2, CONVENTIONALLY-COOLED, 1800 RPM
1261 ICK=2
    GOT01266
C ICK= 1, CONVENTIONALLY-COOLED, 3600 RPM
1262 ICK=1
    GOT01266
1263 IF(IRLP=1800)1264,1264,1265
C ICK=-1, CONDUCTOR-COOLED, 1800 RPM
1264 ICK=-1
    GOT01266
C ICK= 0, CONDUCTOR-COOLED, 3600 RPM
1265 ICK=0
1266 GCKVA=GC*1000.
    GCKVA=1000.00*WRATE/PF
    FRKVA=GOKVA/GCKVA
    PCTKVA=FRKVA*100.
C C GENERATOR LOSS (TANDEM COMPOUND)
C RATED HYDROGEN PRESSURE
    GL20=FIG20(GCKVA,ICK,IRLP)
    GL21=FIG21(FRKVA,ICK)
    WGL=GOKVA*GL20*GL21*0.01
C TEST FOR REDUCED HYDROGEN PRESSURE
    IF(IH2.EQ.0)GOTO1267
C REDUCED HYDROGEN PRESSURE
    WGL=WGL-FIG22(GCKVA,ICK)

C C MECHANICAL LOSS
1267 WML=FIG39(GCKVA)

C C INTERMEDIATE SYSTEM PRESSURE DROP AND PXHP
    QMR=0.
    HFSX=0.
    GOT0(1300,1270,1280),NSHAFT

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1270 MS1=MS          ORCE 810
    PR=PRLP          ORCE 820
    GOTO1290         ORCE 830
1280 CALL PRDROP(PXIP,PRLP,MS,0)  ORCE 840
    MS1=0            ORCE 850
    PR=PRLP          ORCE 860
1290 CALL PRDROP(PXHP,PR,MS1,NRH)  ORCE 870
C                                         ORCE 880
C   CONDENSER HOTWELL PARAMETERS      ORCE 881
1300 TC=TSAT(PC)        ORCE 890
    HC=HT10(TC)       ORCE 900
C                                         ORCE 910
C   STEAM JET AIR EJECTOR ENTHALPY  ORCE 911
    HAEI=HT          ORCE 920
    HAEO=180.1        ORCE 930
C                                         ORCE 940
C   SET INDICES FOR FW HEATER HEAT BALANCE CALCULATIONS
    I1GS=1           ORCE 941
    I2GS=NFGS        ORCE 950
    IF(NSHAFT,GT,1)GOTO1310  ORCE 960
    I1LP=I2GS+1      ORCE 970
    GOTO1330         ORCE 980
1310 I1HP=I2GS+1      ORCE1000
    I2HP=I2GS+NFH    ORCE1010
    IF(NSHAFT,GT,2)GOTO1320  ORCE1020
    I1LP=I2HP+1      ORCE1030
    GOTO1330         ORCE1040
1320 I1IP=I2HP+1      ORCE1050
    I2IP=I2HP+NF1    ORCE1060
    I1LP=I2IP+1      ORCE1070
1330 IF(MR,GT,0)GOTO1340  ORCE1080
    T2LP=NF          ORCE1090
    GOTO1360         ORCE1100
1340 I2LP=NF+1        ORCE1110
    CALL INDEX(I1LP,I2LP,NFL,MR)  ORCE1120
C                                         ORCE1130
C   FEEDWATER PUMP ENTHALPY RISE
1360 PLA=PT*1.25      ORCE1131
    IF(PT,GE,200.)GOTO1361  ORCE1140
    PLB=PC          ORCE1150
    GOTO1362         ORCE1160
1361 PLB=150.          ORCE1170
1362 DP=PLA-PLB      ORCE1180
    EFP=0.9          ORCE1190
    DHP=DP*VLTQ(TSAT(PLB))*0.18505/EFP  ORCE1200
C                                         ORCE1210
C   FW HEATER PARAMETERS
    IF(NFGS,EQ,NE)GOTO1400  ORCE1220
    GOTO1390,1380,1370,NSHAFT  ORCE1230
1370 IF(NFI,EQ,0)GOTO1380  ORCE1240
    IF(PE(I2IP),LE,(PXIP+1.0))GOTO1371  ORCE1250
    I2I=T2IP          ORCE1260
    GOTO1380         ORCE1270
1371 PE(I2IP)=PXIP     ORCE1280
    I2I=T2IP-1        ORCE1290
1380 IF(NFH,EQ,0)GOTO1390  ORCE1300
    IF(PE(I2HP),LE,(PXHP+1.0))GOTO1381  ORCE1310
    I2H=T2HP          ORCE1320
    GOTO1390         ORCE1330
1381 PE(I2HP)=PXHP     ORCE1340
    I2H=T2HP-1        ORCE1350
1390 CALL FWHPAR(NFGS+1,NFI)  ORCE1360
C                                         ORCE1370
C   STEAM PACKING EXHAUSTER FLOW
1400 IF(LK,GT,0)GOTO1409  ORCE1380
    GSPE=0.          ORCE1420
    HSSR=0.          ORCE1430
    GOTO1440         ORCE1440
1409 QSSRMU=0.          ORCE1450
    QSSRM1=0.          ORCE1460
    IF(TRLP,EQ,1800)GOTO1410  ORCE1470

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OSPE=650.0*NLP          ORCE1510
QMC=950.0*NLP          ORCE1520
GCT01420                ORCE1530
1410 OSPE=1200.0*NLP    ORCE1540
QMC=1800.0*NLP          ORCE1550
C
C STEAM SEAL REGULATOR PRESSURE
1420 IF(PXLP.LE.18.0)GOTO1430  ORCE1560
PSSR=PXLP
GOTO1440
1430 PSSR=18.0            ORCE1570
C
C REHEATER
1440 QRH1=0ERH1           ORCE1580
QRH2=0ERH2
IF(NRH.NE.1)GOTO1900      ORCE1590
CALL REHEAT(HE(1),PE(1),HT,PT)
C
1900 MAIN=MAIN+1          ORCE1600
ITGS=0                   ORCE1601
ITHP=0                   ORCE1602
ITIP=0                   ORCE1603
NCRH=0                  ORCE1604
ITMS=0                   ORCE1605
ITSSR=0                 ORCE1606
C
C STEAM FLOW FROM STEAM GENERATOR
ORD=OT+OAE               ORCE1607
IF(NRH.LT.1)GOTO1920      ORCE1610
IF(NRH.EQ.1)GOTO1910      ORCE1620
QRD=ORD+QRH2              ORCE1630
GOTO1920
1910 CRC=ORD+ORH1          ORCE1640
C
C MAKE-UP FLOW
1920 QMU=OT*PCMU*0.01      ORCE1650
C
C FEEDWATER FLOW TO STEAM GENERATOR
QR=ORD-QCR+OMU            ORCE1660
C
C TEST FOR 1-SHAFT MACHINE AND FW PUMP TURBINE CALCULATIONS
IF(NSHAFT.GT.1)GOTO1950    ORCE1670
IF(TFPT>1940,1950,1930    ORCE1680
C
C FW PUMP TURBINE STEAM FLOW (1-SHAFT MACHINE)
1930 CALL FWPT(PT,HT, PC,DHP,QR,NSHAFT)  ORCE1690
1940 QRD=ORD+OFTP           ORCE1700
QR=QR+OFTP
C
1950 CONTINUE               ORCE1710
C
C GOVERNING STAGE PERFORMANCE
C
C TEST FOR VALVE STEM LEAKAGE CALCULATIONS
2000 IF(LK.GT.0)GOTO2001    ORCE1720
C
C GOVERNING STAGE FLOW, NO VALVE STEM LEAKAGE
QGS=0T                     ORCE1730
GOTO2003
C
C VALVE STEM LEAKAGE
2001 CALL SLEAK1(NF, PE,OT,PT,HT,LK1,QLK1,HLK1,QLK2,HLK2,NFGS)  ORCE1740
C
C GOVERNING STAGE FLOW WITH VALVE STEM LEAKAGE
2002 QGS=OT-QLK1-QLK2-QSSRMU  ORCE1750
C
C GS BOWL AND SHELL CONDITIONS
2010 CALL GSTAGE(PXLP)       ORCE1760
C
C TEST FOR GOVERNING STAGE SHAFT LEAKAGE
TF(LK.GT.0)GOTO2004        ORCE1770

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C   C FLOW TO NEXT STAGE, NO GS SHAFT LEAKAGE
    QNEXT=QGS
    QXGS=QGS
    GOTO205
C   C GS SHAFT LEAKAGE
    2004 CALL SLEAK2(NF, PE, NGS, IRGS, PXGS, MXGS, HXGS, LK3, QLK3, HLK3, QLK4,
           1HLK4, PSSR, NFGS)
C   C FLOW TO NEXT STAGE WITH GS SHAFT LEAKAGE
    QNEXT=QGS-QLK3-QLK4
    CXGS=QNEXT
C   C TEST FOR FW HEATER AT GS EXHAUST
    2005 IF(NFGS, EQ, 0) GOTO2030
C   C FW HEATER HEAT BALANCE AT GS EXHAUST
    PE(1)=PXGS
    HE(1)=HXGS
    IF(NRH_LT, 2) GOTO2019
    CALL REHEAT(HE(1), PE(1), HT, PT)
    2019 CALL FWHPAR(1,1)
    2020 CALL FMHEAT(1,1,0,0,0,0)
    ITGS=ITGS+1
C   C FLOW TO NEXT STAGE
    QNEXT=QXGS-DE(1)
C   C TEST FOR 2 STAGES OF REHEAT
    IF(NRH_LT, 2) GOTO2030
C   C FLOW TO NEXT STAGE
    QNEXT=QNEXT-QRH1
C   C TEST FOR 1-SECTION MACHINE
    2030 IF(NSHAFT, GT, 1) GOTO2000
C   C LP SECTION BOWL PRESSURE AND ENTHALPY (1-SECTION MACHINE)
    PRLP=PXGS
    HNEXT=HXGS
    GOTO2000
C   C HIGH PRESSURE SECTION PERFORMANCE
C   C BOWL CONDITIONS (HP SECTION)
    3000 QRHP=QNEXT
    PRHP=PXGS
    HRHP=HXGS
    SRHP=SXGS
    VRHP=VXGS
    AMRHP=AMXGS
    MRHP=MXGS
    TRHP=TXGS
C   C SHELL CONDITIONS (HP SECTION)
    CALL SCROUP(PRHP, TBHP, HBHP, SBHP, VRHP, AMRHP, MBHP, QRHP, NHP, CSHP,
               1PXHP, TXHP, HXHP, SXHP, VXHP, AMXHP, MXHP, PTHP, THHP, SHHP, VHHP,
               2AMTHP, MTHP, PXLP)
C   C EXHAUST LOSS AND UEEP (HP SECTION)
    XLHP=FIG8(PXHP)
    UEEPHP=HXHP+XLHP
    CALL PROPHI(AMUEHP, SUUEHP, VUEHP, TUEHP, MUUEHP, PXHP, UEEPHP)
C   C EXHAUST FLOW (HP SECTION)
    CXHP=QRHP
C   C TEST FOR FW HEATERS (HP SECTION)
    3010 IF(NFH, EQ, 0) GOTO3030

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C FW HEATER HEAT BALANCE (HP SECTION)          ORCE2590
  T1=T1HP
  CALL HYTRAC(1,T1HP,T2HP,MRHP,HBHP,SRHP,MXHP,HXHP,SXHP,PTHP,HIHP,
  1STHP,PXHP,UEEPHP)
  IF(NFCS.EQ.1.OR.NPH.EQ.1)GOTO3025
  CALL REHEAT(HE(1),PF(1),HT,PT)
  GOT03025
3025  T1=T
3025  CALL FWHATE(T1,T2HP,0,0,MS,ITGS)
  ITHP=1THP+1
C
C TEST FOR REGRESSIVE FW HEATER HEAT BALANCE CALCULATIONS      ORCE2600
  IF(T1.EQ.0)GOTO2020
C
C TEST FOR ONLY ONE FW HEATER (HP SECTION)                      ORCE2610
C TEST FOR FW HEATER AT EXHAUST (HP SECTION)                   ORCE2611
  IF(NFH.EQ.1.AND.T2H.LT.T2HP)GOTO3031
C
C EXHAUST FLOW, MORE THAN ONE FW HEATER HP SECTION,           ORCE2620
C OR ONLY ONE FW HEATER AND NOT LOCATED AT HP EXHAUST        ORCE2630
  QXHP=0PHP
  DO3030  K=T1HP,T2H
3030  QXHP=QXHP-DE(K)
C
C TEST FOR REHEATER STEAM EXTRACTION (HP SECTION)            ORCE2640
  3031  IF(NPH.EQ.1)GOTO3032
  QXHP=QXHP-ORH1
C
C FLOW TO NEXT SECTION                                     ORCE2650
  3032  QNEXT=QXHP
C
C TEST FOR SHAFT LEAKAGE CALCULATIONS                      ORCE2660
  IF(LK.EQ.0)GOTO3033
C
C SHAFT LEAKAGE FROM EXHAUST END (HP SECTION)             ORCE2670
  CALL SLEAK3(NF,PE,NHP,TRHP,PXHP,VUEHP,UEEPHP,LK5,QLK5,HLK5,QLK6,
  1HLK6,PSSR)
C
C FLOW TO NEXT SECTION                                     ORCE2680
  QNEXT=QNEXT-QLK5-QLK6
C
C TEST FOR FW HEATER AT HP EXHAUST                         ORCE2690
  3033  IF(NFH.EQ.1.OR.T2H.EQ.1)GOTO3040
C
C FLOW TO NEXT SECTION, FW HEATER AT HP EXHAUST           ORCE2700
  QNEXT=QNEXT-DE(T2HP)
C
C TEST FOR EXTERNAL MOISTURE SEPARATOR AND 2-SECTION MACHINE ORCE2710
  3040  IF(MS.GT.0.AND.NSHAFT.EQ.2)GOTO4000
C
C TEST FOR REHEATER                                         ORCE2720
  IF(NRH.EQ.0)GOTO4205
C
C ENTHALPY TO NEXT SECTION (NO MOISTURE SEPARATOR OR REHEATER) ORCE2730
  PNEXT=UEEPHP
  GOT04300
C
C EXTERNAL MOISTURE SEPARATOR PERFORMANCE (2-SECTION MACHINE) ORCE2740
C
C INLET FLOW AND ENTHALPY                                ORCE2750
  4000  QST=QNEXT
        HST=UEEPHP
        ITMS=ITMS+1
C
C HEAT AND MASS BALANCE CALCULATION                      ORCE2760
  QMR1=QMR
  CALL XSEP
C
C TEST FOR MOISTURE FLOW TO FW HEATER AT HP SECTION EXHAUST ORCE2770
  IF(MS.GT.T2HP)GOTO4010
C

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C TEST FOR MOISTURE REMOVAL CONVERGENCE	ORCE3091
ADQMR=DARS((QMR-QMR1)/QMR)	ORCE3100
TF(ADQMR,LE,XSPCON)GOTO4010	ORCE3110
IF(UTMS,GT,.50)GOTO4008	ORCE3120
I1=T2HP	ORCE3130
GOTO3925	ORCE3140
4008 PRINT 4009,ADQMR	ORCE3150
4009 FORMAT("0-MAIN PROGRAM-EXTERNAL MOISTURE SEPARATOR DRAIN CALCULATOR")	ORCE3160
10NS DID NOT CONVERGE, ADQMR =1,1PD14e-6)	ORCE3161
C	ORCE3170
C TEST FOR REHEATER	ORCE3171
4010 IF(NRH,NE,0)GOTO4200	ORCE3180
C	ORCE3190
C FLOW AND ENTHALPY TO NEXT SECTION (NO REHEATER, 2-SECTION MACHINE)	ORCE3191
QNEXT=QSX	ORCE3200
HNEXT=HSX	ORCE3210
GOTO4300	ORCE3220
C	ORCE3230
C REHEATER PERFORMANCE	ORCE3231
C	ORCE3240
C FLOW AND ENTHALPY TO REHEATER (EXTERNAL MOISTURE SEPARATOR)	ORCE3241
4200 ORH=QSX	ORCE3250
HTRH1=HSX	ORCE3260
GOTO4210	ORCE3270
C	ORCE3280
C FLOW AND ENTHALPY TO REHEATER (NO MOISTURE SEPARATOR)	ORCE3281
4205 ORH=QNEXT	ORCE3290
HTRH1=UEEPHP	ORCE3300
C	ORCE3310
C 1ST STAGE HEAT BALANCE	ORCE3311
4210 NCRH=NCRH+1	ORCE3320
C	ORCE3321
C TEST FOR TYPE OF REHEATER	ORCE3322
IF(NRH,GT,0)GOTO4220	ORCE3323
C	ORCE3324
C EXTERNAL REHEATER	ORCE3325
TXRH1=TTDRH1	ORCE3326
HYRH1=HVAP(TXRH1,PXRH1)	ORCE3327
GOTO4250	ORCE3328
C	ORCE3329
C LIVE STEAM REHEATER	ORCE3330
4220 ORH1=ORH*(HYRH1-HTRH1)/(HRH1-HCRH1)	ORCE3331
C	ORCE3340
C TEST FOR 2ND STAGE	ORCE3341
IF(NRH,EQ,2)GOTO4221	ORCE3350
C	ORCE3351
C TEST FOR FW HEATER IN GS OR HP SECTION	ORCE3352
IF((NHF+NEGS),GT,0)GOTO4230	ORCE3353
C	ORCE3354
C RE-CALCULATE REACTOR STEAM AND FW FLOW	ORCE3355
QRD=QT+QAE+QRH1	ORCE3356
QR=QRD-QCR+OMU	ORCE3357
GOTO4250	ORCE3358
C	ORCE3360
C 2ND STAGE HEAT BALANCE	ORCE3361
4221 ORH2=ORH*(HYRH2-HTRH2)/(HRH2-HCRH2)	ORCE3370
C	ORCE3380
C TEST FOR 2ND STAGE CONVERGENCE	ORCE3381
AD02=DARS((ORH2-QRH21)/ORH2)	ORCE3390
IF(AD02,LE,RHCON)GOTO4230	ORCE3400
QRH2=ORH2	ORCE3410
GOTO4240	ORCE3420
C	ORCE3430
C TEST FOR 1ST STAGE CONVERGENCE	ORCE3431
4230 AD01=DARS((ORH1-QRH11)/ORH1)	ORCE3440
IF(AD01,LE,RHCON)GOTO4230	ORCE3450
4240 QRH1=ORH1	ORCE3460
IF(NCRH,LE,.50)GOTO4242	ORCE3470
PRINT 4241,AD01,AD02	ORCE3480

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4241 FORMAT('0-MAIN PROGRAM-REHEATER CALCULATIONS DID NOT CONVERGE, ADQCRCE3490
11 =',1PD14.6,EX,'AD02 =',1PD14.6)
      GOTO4250
C
C  RE-CALCULATE REACTOR STEAM AND FW FLOW
4242 IF(NRH.EQ.1)GOTO4243
      QRD=OT+OAE+ORH2
      GOTO4244
4243 QRD=OT+OAE+ORH1
4244 QR=QRD-OCR+OMU
C
C  RETURN TO GS OR HP SECTION
4245 IF(NEGSEQ.1)GOTO2620
      T1=11HP
      GOTO3025
C
C  FLOW TO NEXT SECTION
4250 QNEXT=ORH
C
C  TEST FOR 2ND STAGE
        IF(NRH.LT.2)GOTO4260
C
C  ENTHALPY TO NEXT TURBINE SECTION (2-STAGE REHEATER)
        HNEXT=HXRH2
        GOTO4300
C
C  ENTHALPY TO NEXT TURBINE SECTION (1-STAGE REHEATER)
4260 HNEXT=HXRH1
C
C  TEST FOR FW PUMP TURBINE CALCULATIONS
4300 IF(TFPT14320,4400,4310
C
C  FW PUMP TURBINE THROTTLE STEAM FLOW
4310 CALL FWPT(PFPT,HNEXT, PC,DHP,QR,NSHAFT)
C
C  FLOW TO NEXT TURBINE SECTION
4320 QNEXT=QNEXT-QPFT
C
C  TEST FOR 2-SECTION OR 3-SECTION MACHINE
4400 GOTO1720,7000,5000),NSHAFT
C
C  INTERMEDIATE PRESSURE SECTION PERFORMANCE
C  (2ND SECTION OF 3-SECTION MACHINE)
C
C  BOWL CONDITIONS (IP SECTION)
5000 QRTP=QNEXT
      HRTP=HNEXT
      CALL PROPPH(AMRTP,S RTP,VRTP,TRTP,M RTP,PRTP,HRTP)
C
C  TEST FOR SHAFT LEAKAGE CALCULATIONS
        IF(LK.EQ.0)GOTO5050
C
C  SHAFT LEAKAGE FROM BOWL END (TP SECTION)
        CALL SLEAK2(INF, PE,NTP,TRTP,PRTP,VRTP,HRTP,LK7,QLK7,HLK7,OLK8,
        1HLK9,PSSR,NEGS)
C
C  BOWL FLOW (TP SECTION)
        QBI=ORTP-QLK7-OLK8
C
C  SHELL CONDITIONS (TP SECTION)
5050 CALL SGROUP(P RTP,TRTP,HRTP,S RTP,VRTP,AM RTP,M RTP,PR RTP,N RTP,C RTP,
        1P RTP,T RTP,H RTP,S RTP,V RTP,AM RTP,M RTP,PR RTP,T RTP,H RTP,S RTP,V RTP,
        2M RTP,M RTP,P XLP)
C
C  EXHAUST LOSS AND UEEP (TP SECTION)
        XLT=FTGR(PXTP)
        UEEP=H RTP+XLT
        CALL PROPPH(AMUETP,SUETP,VUETP,TUETP,MUETP,PXTP,UFEETP)
C
C  EXHAUST FLOW (TP SECTION)
        QYTP=ORTP

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C   TEST FOR FW HEATERS (TP SECTION)          ORCE3910
C   5010 IF(NFI.EQ.0)GOTO5042                ORCE3911
C                                         ORCE3920
C                                         ORCE3930
C                                         ORCE3940
C                                         ORCE3950
C                                         ORCE3960
C   FW HEATER HEAT BALANCE (TP SECTION)      ORCE3970
C   II=I1IP                                  ORCE3971
C   CALL HXTRAC(0,IIIP,I2IP,MBTP,HBTP,SBIP,MXIP,HXTP,SXIP,PTIP,HTIP,
C   I1TP,PXIP,UEEPTP)                      ORCE3980
C   GOT05030                                 ORCE3990
C   5020 II=I                                ORCE4000
C   5030 CALL FWHEAT(II,I2IP,0,0,MS,I1HP)    ORCE4010
C   I1IP=I1IP+1                             ORCE4020
C                                         ORCE4021
C   TEST FOR REGRESSIVE FW HEATER HEAT BALANCE CALCULATIONS
C   IF(I.EQ.12HP.AND.NFH.GT.0)GOTO3020     ORCE4030
C   IF(I.EQ.NEGS)GOTO2020                   ORCE4040
C                                         ORCE4050
C   TEST FOR MORE THAN ONE FW HEATER (TP SECTION) ORCE4051
C   TEST FOR ONLY ONE FW HEATER AND LOCATED AT EXHAUST (TP SECTION) ORCE4052
C   IF(NFI.EQ.1.AND.I2I.LT.I2TP)GOTO5042    ORCE4060
C                                         ORCE4070
C   EXHAUST FLOW, MORE THAN ONE FW HEATER IP SECTION, ORCE4071
C   OR ONLY ONE FW HEATER AND LOCATED AT TP EXHAUST    ORCE4080
C   OXTP=OXIP                                  ORCE4090
C   D05040 K=I1IP,T2I                         ORCE4100
C   5040 OXIP=OXTP-OE(K)                     ORCE4110
C                                         ORCE4120
C   FLOW TO NEXT SECTION                    ORCE4121
C   5042 QNEXT=ONEXT                       ORCE4130
C                                         ORCE4140
C   TEST FOR SHAFT LEAKAGE CALCULATIONS    ORCE4141
C   IF(LK.EQ.0)GOTO5043                   ORCE4150
C                                         ORCE4160
C   SHAFT LEAKAGE FROM EXHAUST END (TP SECTION) ORCE4161
C   CALL SLEAK3(NF,PE,NTP,TRTP,PXIP,VUETP,UEEPTP,LK9,QLK9,HLK9,QLK10,
C   HLK10,PSSR1)                           ORCE4170
C                                         ORCE4171
C                                         ORCE4180
C   FLOW TO NEXT SECTION                  ORCE4181
C   QNEXT=ONEXT-QLK9-QLK10                 ORCE4190
C                                         ORCE4200
C   TEST FOR FW HEATER AT TP EXHAUST       ORCE4201
C   5043 IF(NFI.EQ.0.OR.I2I.EQ.I2TP)GOTO5050 ORCE4210
C                                         ORCE4220
C   FLOW TO NEXT SECTION, FW HEATER AT IP EXHAUST ORCE4221
C   QNEXT=ONEXT-OE(I2TP)                   ORCE4230
C                                         ORCE4240
C   TEST FOR EXTERNAL MOISTURE SEPARATOR FOLLOWING IP SECTION ORCE4241
C   5050 IF(MS.GT.0)GOTO6000               ORCE4250
C                                         ORCE4260
C   ENTHALPY TO LP SECTION                 ORCE4261
C   (NO EXTERNAL MOISTURE SEPARATOR FOLLOWING IP SECTION) ORCE4262
C   HNEXT=UEEPTP                          ORCE4270
C   GOT07000                               ORCE4280
C                                         ORCE4290
C   EXTERNAL MOISTURE SEPARATOR PERFORMANCE (3-SECTION MACHINE) ORCE4291
C                                         ORCE4300
C   TNLET FLOW AND ENTHALPY              ORCE4301
C   6000 CST=QNEXT                      ORCE4310
C   HST=UEEPTP                          ORCE4320
C   ITMS=ITMS+1                          ORCE4330
C                                         ORCE4340
C   HEAT AND MASS BALANCE CALCULATION   ORCE4341
C   QMR1=QMR                            ORCE4350
C   CALL XSEP                            ORCE4360
C                                         ORCE4370
C   TEST FOR MOISTURE FLOW TO FW HEATER AT IP SECTION EXHAUST ORCE4371
C   IF(MS.GT.I2TP)GOTO6010               ORCE4380
C                                         ORCE4390
C   TEST FOR MOISTURE REMOVAL CONVERGENCE ORCE4391
C   ADOMR=DABST(QMR-QMR1)/QMR           ORCE4400

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TF(ADQMR,LE,XSPCON)GOT06010          ORCE4410
IF(TTMS.GT.50)GOT06008          ORCE4420
II=12TP          ORCE4430
GOT05030          ORCE4440
6038 PRINT 4009,ADQMR          ORCE4450
C          ORCE4460
C FLOW AND ENTHALPY TO LP SECTION          ORCE4461
C (EXTERNAL MOISTURE SEPARATOR FOLLOWING IP SECTION)          ORCE4462
6110 CNFEXT=OSX          ORCE4470
    HNEXT=HSX          ORCE4480
C          ORCE4490
C TEST FOR STEAM SEAL REGULATOR          ORCE4491
7000 IF(LK,EQ,0)GOT07008          ORCE4500
C          ORCE4510
C STEAM SEAL REGULATOR ENTHALPY AND MAKEUP          ORCE4511
    CALL SSREC(PSH,HT,PXLP,NSHAFT,NF)          ORCE4520
C          ORCE4530
C TEST FOR SSR MAKE-UP CONVERGENCE          ORCE4531
    TF(OSSRMU, EQ, OSSRM1)GOT07008          ORCE4540
    ADMU=DABSI(OSSRMU-OSSRM1)/OSSRMU          ORCE4550
    IF(ADMU,LE,SSRCON)GOT07008          ORCE4560
    TF(TSSR.GT.50)GOT07006          ORCE4570
    OSSRM1=OSSRMU          ORCE4580
    GOT02102          ORCE4590
7006 PRINT 7007,ADMU          ORCE4600
7007 FORMAT('0-MATN PROGRAM-STEAM SEAL REGULATOR MAKE-UP CALCULATIONS',DORCE4610
    'TO NOT CONVERGE, ADMU = ',1PD14.6)          ORCE4611
C          ORCE4620
C LOW PRESSURE SECTION PERFORMANCE          ORCE4621
C          ORCE4630
C BOWL CONDITIONS (LP SECTION)          ORCE4631
7008 QPLP=QNEXT          ORCE4640
    HALP=HNEXT          ORCE4650
    CALL PROPPH(AMBLP,SRLP,VRLP,TBLP,MRLP,PRLP,HBLP)          ORCE4660
C          ORCE4670
C BASE EXPANSION LINE (LP SECTION)          ORCE4671
7009 TF(PXLP,GE,3)GOT07010          ORCE4680
    PX1=0.73674          ORCE4690
    GOT07020          ORCE4700
7010 PX1=PXLP          ORCE4710
7011 CALL SGROUP(PRLP,TBLP,HBLP,SRLP,VRLP,AMBLP,MRLP,ORLP,NLP,CSLP,PX1,ORCE4720
    TX1,HX1,SX1,VX1,AMX1,MX1,PILP,TLIP,HTLP,STLP,VTLP,AMILP,MILP,PXLP)ORCE4721          ORCE4730
C          ORCE4731
C TEST FOR MOISTURE REMOVAL STAGES (LP SECTION)          ORCE4740
    IF(MR.GT.0)GOT07029          ORCE4750
    HEP=HX1          ORCE4760
    AMEP=AMX1          ORCE4770
    GOT07050          ORCE4780
C          ORCE4781
C MOISTURE REMOVAL CALCULATIONS (LP SECTION)          ORCE4790
7029 IF(MRLP,EQ,3)GOT07030          ORCE4800
    PR=PRLP          ORCE4810
    HR=ORLP          ORCE4820
    SR=SRLP          ORCE4830
    GOT07040          ORCE4840
7030 PR=PILP          ORCE4850
    HR=HTLP          ORCE4860
    SR=STLP          ORCE4870
7041 CALL AMODIST(MR,PMR,PR,HR,SR,PX1,HX1,SX1,HRMR,HAMR,HEP,AMBRMR,AMAMR,ORCE4870
    1AMEP,SRMR,SAMR,PCWD,TMR)          ORCE4871          ORCE4880
C          ORCE4881
C SHELL CONDITIONS (LP SECTION)          ORCE4890
7051 IF(PXLP,GE,3)GOT07160          ORCE4891
    HXL_P=HEP+FTG15(PXLP*2.0361*FIG14(AMEP*100.0))          ORCE4892
    GOT07170          ORCE4910
7056 IF(MR,EQ,3)GOT07080          ORCE4920
    HXL_P=HEP          ORCE4930
7073 CALL PROPPH(AMXLP,SXLP,VXLP,TXLP,MXLP,PXLP,HXLP)          ORCE4940
    GOT07190          ORCE4950
7080 HXL_P=HX1          ORCE4960
    TXLP=TX1          ORCE4970

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SXLP=SX1          ORCE4980
VXLP=VX1          ORCE4990
AMXLP=AMX1        ORCE5000
MXLP=MX1          ORCE5010
C
7390 CONTINUE    ORCE5020
C
C   FW HEATER HEAT BALANCE (LP SECTION)
7390 KL=1          ORCE5030
QFS(KL)=QBLP      ORCE5040
HFS(KL)=HBLP      ORCE5060
IF(NFL.EQ.0)GOTO7110  ORCE5070
IF(MR.EQ.0)GOTO7160  ORCE5080
GOTO7120          ORCE5090
7110 CALL HXTRAC(MR,T1LP,NF,MRLP,HRLP,SBLP,MXLP,HXLP,SXLP,PILP,HLIP,
ISTLP,PXLP,UEEPPLP)  ORCE5100
7120 GOTO(7121,7122,7123),NSHAFT  ORCE5110
7121 IT=ITGS      ORCE5120
GOTO7124          ORCE5121
7122 IT=ITHP      ORCE5130
GOTO7124          ORCE5140
7123 IT=ITIP      ORCE5150
7124 CALL FWHEAT(I1LP,I2LP,MR,KL,MS,IT)  ORCE5160
C
C   TEST FOR REGRESSIVE FW HEATER HEAT BALANCE CALCULATIONS  ORCE5170
GOTO(7150,7140,7130),NSHAFT  ORCE5180
7130 IF(I.EQ.I2IP.AND.NFI.GT.0)GOTO5020  ORCE5190
7140 IF(I.EQ.I2IP.AND.NFH.GT.0)GOTO3020  ORCE5200
7150 IF(I.EQ.NFCS)GOTO2020  ORCE5230
C
C   EXHAUST FLOW (LP SECTION)  ORCE5240
7160 KLT=KL        ORCE5250
OXLP=QFS(IKLT)    ORCE5251
C
C   TEST EXHAUST PRESSURE (LP SECTION)  ORCE5260
IF(PXLP.GE.3)GOTO7170  ORCE5270
C
C   CONDENSING EXHAUST LOSS AND UEEP (LP SECTION)  ORCE5280
CALL XLOSS(PXLP,TXLP,HEP,HXLP,OXLP,AMEP,ANXLP,NLP,RLS,POLs,TRLP,  ORCE5300
UEEPLP,XLLP)        ORCE5301
GOTO7180          ORCE5310
C
C   BACK-PRESSURE EXHAUST LOSS AND UEEP (LP SECTION)  ORCE5311
7170 XLLP=FTGB(PXLP)  ORCE5320
UEEPLP=HXLp+XLLP    ORCE5330
7180 HES(KLT)=UEEPLP  ORCE5331
C
C   GENERATOR OUTPUT  ORCE5340
C
8000 WHP=0.        ORCE5350
WTP=0.            ORCE5360
WLP=0.            ORCE5370
C
C   GS SECTION  ORCE5371
WBTU=1.00/3412.14D0  ORCE5380
WGS=QGS*(HRGS-HXGS)*WBTU  ORCE5390
C
C   TEST FOR NUMBER OF TURBINE SECTIONS IN SERIES  ORCE5400
GOTO(8050,8030,8010),NSHAFT  ORCE5410
C
C   IP SECTION  ORCE5420
8010 WTP=0.1TP*(HRIP-UEEP1P)*WBTU  ORCE5430
C
C   TEST FOR FW HEATERS (IP SECTION)  ORCE5440
IF(NFI.EQ.0)GOTO8030  ORCE5450
C
C   SUBTRACT FW HEATER EXTRACTION STEAM (IP SECTION)  ORCE5460
8030 I=I1IP,T2I      ORCE5470
8020 WTP=WTP-0.1*(HE(I)-UEEPIP)*WBTU  ORCE5480
C
C   HP SECTION  ORCE5490
ORCE5500
ORCE5510
ORCE5511
ORCE5520
ORCE5530
ORCE5531
ORCE5540
ORCE5550
ORCE5560
ORCE5570

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C R330 WHP=ORHP*(HRHP-UEPHP) *WRTU	ORCE5580
C TEST FOR FW HEATERS (HP SECTION)	ORCE5590
TF(NFH,FO,0)GOTOR50	ORCE5591
C TEST FOR REHEATER EXTRACTION STEAM (HP SECTION)	ORCE5600
TF(NRH,LT,2,PR,NGS,FO,1)GOTOR39	ORCE5610
C SUBTRACT REHEATER EXTRACTION STEAM (HP SECTION)	ORCE5611
WHP=WHP-ORH1*(HE(1)-UEPHP1)*WRTU	ORCE5620
C SUBTRACT FW HEATER EXTRACTION STEAM (HP SECTION)	ORCE5630
R339 DDP240 T=11HP, T2H	ORCE5631
R340 WHP=WHP-OF(T1)*(HE(1)-UEPHP1)*WRTU	ORCE5640
C LP SECTION	ORCE5650
R350 DDP260 KL=1,KLT	ORCE5651
R360 MLP=MLP+OFS(KL)*(HFS(KL)-HES(KL))*WRTU	ORCE5660
C NET GENERATOR OUTPUT	ORCE5670
WGEN=(WGS+WHP+WTP+MLP-WML-WGL)*0.001	ORCE5680
C TEST NET ELECTRICAL GENERATION CONVERGENCE	ORCE5690
ADW=DABS((WGEN-WRATE)/HRATE)	ORCE5700
TF(ADW,LE,WGEN)GOTOR200	ORCE5710
C CHECK NUMBER OF ITERATIONS THROUGH MAIN PROGRAM	ORCE5800
TF(MATN,LT,25)GOTOR810	ORCE5810
PRTNT R190,ADW,WGEN	ORCE5820
R300 FORMAT('10-MATN PROGRAM-REQUIRED ELECTRICAL GENERATION DID NOT CONVERGE',ADW =',1PD14.6,EX,'WGEN =',1PD14.6)	ORCE5830
GOTOR200	ORCE5840
C CORRECT THROTTLE FLOW RATE	ORCE5850
R100 QT=BT*WRATE/WGEN	ORCE5860
GOTOR1900	ORCE5870
C STEAM GENERATOR INLET ENTHALPY AND TEMPERATURE	ORCE5880
C TEST FOR FW HEATERS	ORCE5890
R230 TF(NFH,GT,0)GOTOR8210	ORCE5900
C CONDENSER HOTWELL FLOW (INC FW HEATERS)	ORCE5910
QC=OR+OCR	ORCE5920
C NO FW HEATERS	ORCE5930
HCP=HC+OAE*(HAET-HAEO)/QC+QSPE*(HSSR-HAEO)/QC	ORCE5940
HR=HCR	ORCE5950
GOTOR8240	ORCE5960
C TEST DRAIN FROM FW HEATER NO. 1	ORCE5970
R210 TF(ND(1),EG,0)GOTOR8220	ORCE5980
C DRAIN IS PUMPED	ORCE5990
HR=FOR(1)*HD(1)+OF(1)*HO(1)/OR	ORCE6000
GOTOR8230	ORCE6010
C DRAIN IS FLASHED	ORCE6020
R220 HR=HO(1)	ORCE6030
C TEST FOR FW PUMP LOCATION	ORCE6040
R230 TF(IP,GT,0)GOTOR8250	ORCE6050
C FW PUMP IS AFTER FW HEATER NO. 1	ORCE6060
R240 HFP=HR	ORCE6070
CFF=OR	ORCE6080
HR=HR+DHP	ORCE6090
GOTOR8251	ORCE6100
C FW TEMPERATURE TO FW PUMP AND TO STEAM GENERATOR	ORCE6110
R250 CFP=OF(TP)	ORCE6120
	ORCE6130
	ORCE6140
	ORCE6150
	ORCE6160
	ORCE6170
	ORCE6180
	ORCE6190
	ORCE6200

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8251 TEP=TL10H(HFP)
      TR=TCDM(PLA,HR)
C
C   TEST FOR EXTERNAL REHEATER
      TF(NRH.GT.-1)GOTO8255
C
C   HEAT ADDED BY EXTERNAL REHEATER
      RHCORR=ORH*(HXRH1-HIRH)
      GOTO8256
C
C   NO EXTERNAL REHEATER
      8255 RHCORR=0.
C
C   TEST FOR MOTOR-DRIVEN FW PUMP
      8256 TF(TFPT.NE.0)GOTO8260
C
C   KW FOR MOTOR DRIVE
      EFMCG=0.8075
      WFWP=DHP*DFP/(EFMCG*3412.14)
      GOTO8270
C
C   KW FOR TURBINE DRIVE
      8260 WFWP=DFPT*(HREPT-HXEPT)*WBTU
C
C   NET AND GROSS CYCLE HEAT RATES (TURBINE-DRIVEN FW PUMP)
      HTRTN=(QRD*(HT-HR)+QCR*(HR-HCR)+QMU*(HT-HR)+RHCORR)/(WGEN*1000.)
      HTRTG=HTRTN*WGEN/(WGEN-WFWP*0.001)
      GOTO8280
C
C   GROSS AND NET CYCLE HEAT RATES (MOTOR-DRIVEN FW PUMP)
      8270 HTRTG=(QRD*(HT-HR)+QCR*(HR-HCR)+QMU*(HT-HR)+RHCORR)/(WGEN*1000.)
      HTRTN=HTRTG*WGEN/(WGEN-WFWP*0.001)
C
C   NET AND GROSS CYCLE EFFICIENCIES
      8280 CEFFN=341214./HTRTN
      CEFFG=341214./HTRTG
C
C   WRITE RESULTS OF CALCULATIONS
C
C   CALL RESULT(VERS)
C
      GOTO100
      END

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SUBROUTINE DATAINI(CMTS, TT, PT, AMT, QT, WRATE, GC, PCMU, PDGS, DATA  0
1  NSHAFT, NHP, TRHP, NIP, TRTP, PRTP, NLP, TRLP, PRLP, PXLP, PDLS, DATA  1
2  PLS, MR, PMR, MS, NRH, QERH1, TTDRH1, QERH2, TTDRH2, NF, NFGS, DATA  2
3  NFH, NFI, NFI, PE, TTC, ND, NDC, TDCA, TP, DFPT, IFPT, QAE, LK, DATA  3
4  PE, TTC, IH2, VERS, QCR, HREPT, HXEPT, PG, EMSI DATA  4
IMPLICIT REAL*8(A-H,D-Z)
C
C SUBPROGRAM FOR READING AND WRITING INPUT DATA
C
C   DIMENSION CMTS(18),PMR(5),NDC(12),ND(12),PE(12),TTD(12),TDCA(12) DATA 40
C
C   READ ONE COMMENT CARD (COLUMNS 1-72) DATA 50
C
C   READ 110,(CMTS(I),I=1,18) DATA 51
110 FORMAT(18A4) DATA 60
C
C   READ DATA CARDS DATA 70
C
C   200 READ 210,IFLAG,DATA1,DATA2,DATA3,DATA4,DATA5,DATA6 DATA 80
210 FORMAT(12,010.0,5D12.0, 8X) DATA 90
C
C   IF(IFLAG.EQ.0)GOTO300 DATA 91
C
      GOTO(1,2,3,4,5,6,7,8,9,10,11,12,13,14,15,16,17),IFLAG DATA 100

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C
C  IFLAG=1
C  TT=THROTTLE STEAM TEMPERATURE, F
C  PT=THROTTLE STEAM PRESSURE, PSIA
C  AMT=THROTTLE STEAM MOISTURE, PER CENT
   1. TT=DATA1
      PT=DATA2
      AMT=DATA3
      GOTD200

C
C  IFLAG=2
C  OT=ESTIMATED THROTTLE STEAM FLOW, LBM/HR
C  PCMU=FM MAKE-UP RATE, PER CENT
C  QCR=CONDENSATE FLOW BY-PASSED TO STEAM GENERATOR, LB/HR
   2. OT=DATA1
      PCMU=DATA2
      QCR=DATA3
      GOTD200

C
C  IFLAG=3
C  WRATE=ELECTRICAL OUTPUT, MWE
C  GC=GENERATOR CAPABILITY, MVA
C  PF=GENERATOR POWER FACTOR
C  TCC=0, CONDUCTOR-COOLED GENERATOR
C  ICC=1, CONVENTIONALLY-COOLED GENERATOR
C  TH2=0, GENERATOR OPERATION AT RATED HYDROGEN PRESSURE
C  TH2=1, GENERATOR OPERATION AT REDUCED HYDROGEN PRESSURE
C  TR=ROTATIONAL SPEED OF TURBINE-GENERATOR, RPM
   3. WRATE=DATA1
      GC=DATA2
      PF=DATA3
      TCC=DATA4
      TH2=DATA5
      TR=DATA6
      GOTD200

C  ITRHP=ROTATIONAL SPEED OF HP TURBINE, RPM
     ITRP=TR

C  ITRP=ROTATIONAL SPEED OF IP SECTION, RPM
     ITRP=IR

C  IRLP=ROTATIONAL SPEED OF LP SECTION, RPM
     IRLP=TR
     GOTD200

C
C  IFLAG=4
C  IFLAG=4 IS NOT USED
   4. CONTINUE
      GOTD200

C
C  IFLAG=5
C  PGS=PITCH DIAMETER OF GOVERNING STAGE, IN.
   5. PGS=DATA1
      GOTD200

C
C  IFLAG=6
C  NSHAFT=NUMBER OF TURBINE SECTIONS IN SERTES
   6. NSHAFT=DATA1
      GOTD200

C
C  IFLAG=7
C  NHP=NUMBER OF PARALLEL HP SECTIONS
   7. NHP=DATA1
      GOTD200

C
C  IFLAG=8
C  NIP=NUMBER OF PARALLEL IP SECTIONS
C  PRTP=ROWL PRESSURE IP SECTION, PSIA
   8. NIP=DATA1
      PRTP=DATA2
      GOTD200

C
C  IFLAG=9
C  NLP=NUMBER OF PARALLEL LP SECTIONS

```

DATA 195
 DATA 196
 DATA 197
 DATA 198
 DATA 199
 DATA 200
 DATA 210
 DATA 220
 DATA 230
 DATA 240
 DATA 241
 DATA 242
 DATA 243
 DATA 244
 DATA 250
 DATA 260
 DATA 270
 DATA 280
 DATA 290
 DATA 291
 DATA 292
 DATA 293
 DATA 294
 DATA 295
 DATA 296
 DATA 297
 DATA 298
 DATA 299
 DATA 300
 DATA 310
 DATA 320
 DATA 330
 DATA 340
 DATA 350
 DATA 351
 DATA 360
 DATA 361
 DATA 370
 DATA 371
 DATA 380
 DATA 390
 DATA 400
 DATA 401
 DATA 402
 DATA 410
 DATA 420
 DATA 430
 DATA 431
 DATA 432
 DATA 440
 DATA 450
 DATA 460
 DATA 461
 DATA 462
 DATA 470
 DATA 480
 DATA 490
 DATA 491
 DATA 492
 DATA 500
 DATA 510
 DATA 520
 DATA 521
 DATA 522
 DATA 523
 DATA 530
 DATA 540
 DATA 550
 DATA 560
 DATA 561
 DATA 562

```

C PRLP=BOWL PRESSURE LP SECTION, PSTA
C PXLP=EXHAUST PRESSURE LP SECTION, IN. HGA
C PCT=CONDENSER PRESSURE, IN. HGA
C IF DATA3.GT.0, PXLP=DATA3 AND PCT=DATA6
C PXLP=EXHAUST PRESSURE LP SECTION, PSTA
C PC=CONDENSER PRESSURE, PSTA
C IF DATA3.LT.0, PXLP=-DATA3 AND PC=-DATA6
C PDL5=PITCH DIAMETER OF LAST STAGE LP SECTION, IN.
C BLS=LENGTH OF LAST STAGE BUCKETS LP SECTION, IN.
   9 NLP=DATA1
     PBLP=DATA2
     TFL=DATA3.LT.0.0160T091
     PXLP=DATA3*0.49116
     PXLP1=DATA3
     PC=DATA6*0.49116
     PCT=DATA6
     GOTO92
  91 PXLP=-DATA3
     PXLP1=PXLP*2.036
     PC=-DATA6
     PCI=PC*2.036
  92 PDL5=DATA4
     BLS=DATA5
     GOTO200

C
C TFLAG=10
C MR=NUMBER OF MOISTURE REMOVAL STAGES LP SECTION
C PMR(L)=MOISTURE REMOVAL STAGE PRESSURE, PSTA (L=1,MR)
 11 MR=DATA1
     PMR(1)=DATA2
     PMR(2)=DATA3
     PMR(3)=DATA4
     PMR(4)=DATA5
     PMR(5)=DATA6
     GOTO200

C
C TFLAG=11
C MS=0, NO EXTERNAL MOISTURE SEPARATOR
C MS=N, EXTERNAL MOISTURE SEPARATOR DRAINS TO FW HEATER NO. N
C MS=N+1, EXTERNAL MOISTURE SEPARATOR DRAINS TO CONDENSER
C EMS=MOISTURE SEPARATOR EFFECTIVENESS, PER CENT
 11 MS=DATA1
     EMS=DATA2
     GOTO200

C
C TFLAG=12
C ABS(NRH)=NUMBER OF STAGES OF REHEAT
C IF NRH IS POSITIVE, A LIVE STEAM REHEATER IS SPECIFIED, AND
C QERH1=ESTIMATED STEAM FLOW TO 1ST STAGE REHEATER, LBM/HR
C TTDRH1=TERMINAL TEMPERATURE DIFFERENCE 1ST STAGE REHEATER, F
C QERH2=ESTIMATED STEAM FLOW TO 2ND STAGE REHEATER, LBM/HR
C TTDRH2=TERMINAL TEMPERATURE DIFFERENCE 2ND STAGE REHEATER, F
C IF NRH IS NEGATIVE, AN EXTERNAL REHEATER IS SPECIFIED, AND
C TTDRH1=TEMPERATURE OF STEAM LEAVING EXTERNAL REHEATER, F
 12 NRH=DATA1
     QERH1=DATA2
     TTDRH1=DATA3
     QERH2=DATA4
     TTDRH2=DATA5
     GOTO200

C
C TFLAG=13
C NF=TOTAL NUMBER OF FW HEATERS
C NFGS=NUMBER OF FW HEATERS GS SECTION
C NFH=NUMBER OF FW HEATERS HS SECTION
C NFT=NUMBER OF FW HEATERS TP SECTION
C NFL=NUMBER OF FW HEATERS LP SECTION
 13 NF=DATA1
     NFGS=DATA2
     NFH=DATA3
     NFT=DATA4

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NFE=DATA5
GOTO200
C
C IFLAG=14
C N=FW HEATER NUMBER
C PF(N)=EXTRACTION STAGE PRESSURE, PSIA
C TTD(N)=FW HEATER TERMINAL TEMPERATURE DIFFERENCE, F
C ND(N)=0, FW HEATER DRAIN IS FLASHED
C ND(N)=1, FW HEATER DRAIN IS PUMPED
C NDC(N)=0, NO DRAIN COOLER ON FW HEATER
C NDC(N)=1, DRAIN COOLER SECTION ON FW HEATER
C TDCA(N)=DRAIN COOLER APPROXIMATE TEMPERATURE DIFFERENCE, F
14 N=DATA1
    PF(N)=DATA2
    TTD(N)=DATA3
    ND(N)=DATA4
    NDC(N)=DATA5
    TDCA(N)=DATA6
GOTO200

C
C IFLAG=15
C TP=0, FW PUMP IS LOCATED AFTER FW HEATER NO. 1
C TP=N, FW PUMP IS LOCATED BEFORE FW HEATER NO. N
C TEPT=0, FW PUMP IS MOTOR DRIVEN
C TEPT=1, FW PUMP IS TURBINE DRIVEN AND STEAM FLOW, BOWL ENTHALPY,
C     AND EXHAUST ENTHALPY WILL BE CALCULATED
C TEPT=-1, FW PUMP IS TURBINE DRIVEN AND STEAM FLOW, BOWL ENTHALPY,
C     AND EXHAUST ENTHALPY MUST BE SPECIFIED
C QFPT=STEAM FLOW TO FW PUMP TURBINE, LBM/HR
C HRFPt=BOWL ENTHALPY FW PUMP TURBINE, BTU/LB
C 4XFPT=EXHAUST ENTHALPY FW PUMP TURBINE, BTU/LB
15 TP=DATA1
    IFPT=DATA2
    QFPT=DATA3
    HRFPt=DATA4
    4XFPT=DATA5
GOTO200

C
C IFLAG=16
C OAE=STEAM FLOW TO SJAF, LBM/HR
16 OAE=DATA1
GOTO200

C
C IFLAG=17
C LK=0, VALVE STEM AND SHAFT LEAKAGES WILL NOT BE CALCULATED
C LK=1, VALVE STEM AND SHAFT LEAKAGES WILL BE CALCULATED
17 LK=DATA1
GOTO200

C
C WRITE INPUT DATA
C
310 PRINT 310,(CMTS(K),K=1,18),VERS
311 FORMAT('1',T10,18A4/
1' ',T10,'STEAM TURBINE CYCLE HEAT BALANCE'/
2' ',T10,'OPCFNT, VERSION ',A8)
C
    PRINT 320,TT,PT,AMT,OT,PCMU,OCR,WRATE,GC,PF
320 FORMAT('2',T10,'INPUT DATA'/
110',T15,'THROTTLE STEAM TEMPERATURE',T70,4X,F7,1,T87,'F'/
210',T15,'THROTTLE STEAM PRESSURE',T70,4X,F7,1,T87,'PSIA'/
310',T15,'THROTTLE STEAM MOISTURE',T70,4X,F6,2,T87,'PER CENT'/
410',T15,'ESTIMATED THROTTLE STEAM FLOW',T70,F10,0,T87,'LBM/HR'/
510',T15,'FW MAKE-UP RATE (TO CONDENSER HOTWELL)',/
6T70,4X,F5,1,T87,'PER CENT'/
710',T15,'CONDENSATE BY-PASSED TO STEAM GENERATOR',T70,F10,0,T87,/
8'LBM/HR'/
910',T15,'REQUIRED ELECTRICAL OUTPUT',T70,4X,F9,3,T87,'MW'/
A10',T15,'GENERATOR RATED CAPABILITY',T70,4X,F9,3,T87,'MVA'/
B10',T15,'GENERATOR POWER FACTOR',T70,7X,F5,21
C
    IF(TCC.EQ.0)GOTO322

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C      PRINT 321,TCC                                     DATA1320
321 FORMAT('0',T15,'CONVENTIONALLY-COOLED GENERATOR, ICC=1,I2)  DATA1330
C      GOT0324                                         DATA1340
C      PRINT 323,TCC                                     DATA1350
323 FORMAT('0',T15,'CONDUCTOR-COOLED GENERATOR, ICC=1,I2)  DATA1360
C      IF(TH2.EQ.0)GOT0326                           DATA1370
C      PRINT 325,TH2                                     DATA1380
325 FORMAT('0',T15,'GENERATOR OPERATION AT REDUCED HYDROGEN PRESSURE, DATA1390
1TH2=1,I2)                                         DATA1400
C      GOT0328                                         DATA1410
C      PRINT 327,TH2                                     DATA1420
327 FORMAT('0',T15,'GENERATOR OPERATION AT RATED HYDROGEN PRESSURE, THDATA1430
12=1,I2)                                         DATA1440
C      IF(NSHAFT.EQ.1)GOT0350                         DATA1450
C      PRINT 330,NHP                                     DATA1460
330 FORMAT('0',T15,'NUMBER OF PARALLEL HP SECTIONS',T70,7X,I2)  DATA1470
C      IF(NSHAFT.EQ.2)GOT0350                         DATA1480
C      PRINT 340,NTP,POTP                           DATA1490
340 FORMAT('0',T15,'NUMBER OF PARALLEL TP SECTIONS',T70,7X,I2/ DATA1500
1'0',T15,'BOWL PRESSURE TP SECTION',T70,5X,F6.1,T87,'PSIA')  DATA1510
C      IF(NSHAFT.EQ.1)GOT0380                         DATA1520
C      PRINT 370,PBLP                                DATA1530
370 FORMAT('0',T15,'BOWL PRESSURE LP SECTION',T70,5X,F6.1,T87,'PSIA')  DATA1540
C      IF(PXLPL.EQ.3)GOT0399                         DATA1550
C      PRINT 391,PDLS,BLS                            DATA1560
391 FORMAT(1'0',T15,'PITCH DIAMETER OF LAST STAGE LP SECTION',T70,5X,F7.2,T87,DATA1570
2'IN.'/,  DATA1580
3'0',T15,'LENGTH OF LAST STAGE BUCKETS LP SECTION',T70,6X,F6.2,T87,DATA1590
4'IN.')   DATA1600
C      PRINT 400,MR                                  DATA1610
400 FORMAT('0',T15,'NO. OF MOISTURE REMOVAL STAGES LP SECTION',T70,7X,DATA1620
I2)                                         DATA1630
C      IF(MR.EQ.0)GOT0440                         DATA1640
C      DF430 L=1,MR                               DATA1650
C      PRINT 420,L ,PMR(L)                         DATA1660
420 FORMAT('0',T15,'MOISTURE REMOVAL STAGE NO.',I2/ DATA1670

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140,T17,'MOISTURE REMOVAL STAGE PRESSURE',T70,5X,F6.1,T87,'PSIA') DATA1881
C   DATA1890
C   430 CONTINUE
C   DATA1900
C   440 IF(MS.EQ.0)GOTO480
C   DATA1910
C   IF(MS.LE.NF)GOTO460
C   DATA1920
C   PRTNT 450,MS
C   DATA1930
C   450 FORMAT('0',T15,'EXTERNAL MOISTURE SEPARATOR DRAINS TO CONDENSER, MS=',
C   DATA1940
C   '15',T3)
C   DATA1950
C   GOTO500
C   DATA1960
C   460 PRTNT 470,MS,MS
C   DATA1970
C   470 FORMAT('0',T15,'EXTERNAL MOISTURE SEPARATOR DRAINS TO FW HEATER NODATA2020
C   '15',T3,', MS=1,13)
C   DATA2021
C   GOTO500
C   DATA2030
C   480 PRINT 490,MS
C   DATA2040
C   490 FORMAT('0',T15,'THERE IS NO EXTERNAL MOISTURE SEPARATOR, MS=1,12) DATA2050
C   DATA2060
C   GOTO515
C   DATA2070
C   500 PRINT 501,FMS
C   DATA2074
C   501 FORMAT('0',T15,'MOISTURE SEPARATOR EFFECTIVENESS',T70,4X,F6.0,T87,DATA2075
C   '100 PER CENT')
C   DATA2076
C   DATA2080
C   505 INRH=IARS(NRH)
C   DATA2081
C   PRINT 510,INRH
C   DATA2082
C   510 FORMAT('0',T15,'NUMBER OF STAGES OF REHEAT',T70,7X,T2)
C   DATA2090
C   DATA2100
C   DATA2110
C   TF(NRH.EQ.0)GOTO540
C   DATA2120
C   TF(NRH.GT.6)GOTO519
C   DATA2130
C   PRINT 518,TTDRH1
C   DATA2132
C   518 FORMAT('0',T15,'TEMPERATURE OF STEAM LEAVING EXTERNAL REHEATER',
C   '1 T70,4X,F6.0,T87,'F')
C   DATA2134
C   DATA2135
C   GOTO540
C   DATA2136
C   DATA2137
C   DATA2138
C   519 PRINT 520,QERH1,TTDRH1
C   DATA2140
C   520 FORMAT('0',T15,'ESTIMATED STEAM FLOW TO 1ST STAGE REHEATER',T70,
C   '12X,F8.2,T87,'LR/HR')
C   DATA2150
C   210,T15,'TERMINAL TEMPERATURE DIFFERENCE 1ST STAGE REHEATER',T70,
C   '25X,F6.1,T87,'F')
C   DATA2151
C   DATA2152
C   DATA2153
C   DATA2160
C   TF(NRH.EQ.1)GOTO540
C   DATA2170
C   DATA2180
C   PRINT 530,QERH2,TTDRH2
C   DATA2190
C   530 FORMAT('0',T15,'ESTIMATED STEAM FLOW TO 2ND STAGE REHEATER',T70,
C   '12X,F8.2,T87,'LR/HR')
C   DATA2200
C   210,T15,'TERMINAL TEMPERATURE DIFFERENCE 2ND STAGE REHEATER',T70,
C   '25X,F6.1,T87,'F')
C   DATA2202
C   DATA2203
C   DATA2210
C   540 PRINT 550,NF,NEGS
C   DATA2220
C   550 FORMAT('0',T15,'TOTAL NO. OF FW HEATERS',T70,6X,T2/
C   '100',T35,'NO. OF FW HEATERS GS SECTION',T70,7X,T2)
C   DATA2230
C   DATA2231
C   DATA2240
C   IF(NSHAFT.EQ.1)GOTO580
C   DATA2250
C   DATA2260
C   PRINT 560,NFH
C   DATA2270
C   560 FORMAT('0',T15,'NO. OF FW HEATERS HP SECTION',T70,7X,T2)
C   DATA2280
C   DATA2290
C   TF(NSHAFT.EQ.2)GOTO580
C   DATA2300
C   DATA2310
C   PRINT 570,NFI
C   DATA2320
C   570 FORMAT('0',T15,'NO. OF FW HEATERS TP SECTION',T70,7X,T2)
C   DATA2330

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C      580 PRINT 590,NFL          DATA2340
C      590 FORMAT('01',T15,'NO. OF FW HEATERS LP SECTION',T70,TX,12)  DATA2350
C      IF(NF.EQ.0)GOTO731          DATA2360
C      600 DO690 N=1,NF           DATA2370
C      PRINT 610,N,PE(N),TTD(N)   DATA2380
C      610 FORMAT('01',T15,'FW HEATER NO.',I3/
C             '1',T17,'EXTRACTION STAGE PRESSURE',T70,4X,F7.1,T87,'PSIA'/
C             '2',T17,'TERMINAL TEMPERATURE DIFFERENCE',T70,6X,F5.1,T87,'F')  DATA2390
C      IF(ND(N).EQ.0)GOTO630        DATA2400
C      PRINT 620,N,ND(N)          DATA2410
C      620 FORMAT('01',T17,'DRAIN IS PUMPED, ND1',I2,')=',I2)  DATA2420
C      GOT0650                      DATA2430
C      630 PRINT 640,N,ND(N)          DATA2440
C      640 FORMAT('01',T17,'DRAIN IS FLASHED, ND1',I2,')=',I2)  DATA2450
C      IF(ND(N).EQ.1)GOTO670        DATA2460
C      650 PRINT 660,N,ND(N)          DATA2470
C      660 FORMAT('01',T17,'THERE IS NO DRAIN COOLER SECTION, ND1',I2,')=',I2)  DATA2480
C      GOT0690                      DATA2490
C      670 PRINT 680,N,ND(N),TDCA(N)  DATA2500
C      680 FORMAT('01',T17,'THERE IS A DRAIN COOLER SECTION, ND1',I2,')=',I2/DATA2510
C             '2',T17,'DRAIN COOLER APPROACH TEMPERATURE DIFFERENCE',T70,6X,
C             '3F5.1,T87,'F')          DATA2520
C      690 CONTINUE                  DATA2530
C      700 IF(IP.GT.0)GOTO720        DATA2540
C      PRINT 710,IP                DATA2550
C      710 FORMAT('01',T15,'FW PUMP IS LOCATED AFTER FW HEATER NO. 1, IP=',I3)  DATA2560
C      GOT0731                      DATA2570
C      720 PRINT 730,IP,IP          DATA2580
C      730 FORMAT('01',T15,'FW PUMP IS LOCATED BEFORE FW HEATER NO.1,I3,
C             1', IP=1,I3)          DATA2591
C      731 IF(IFPT.EQ.0)GOTO736        DATA2600
C      PRINT 732,IFPT              DATA2610
C      732 FORMAT('01',T15,'FW PUMP IS TURBINE DRIVEN, IFPT=',I3)  DATA2620
C      IF(IFPT.LT.0)GOTO734        DATA2630
C      PRINT 733                  DATA2640
C      733 FORMAT('01',T15,'STEAM FLOW TO FW PUMP TURBINE WILL BE CALCULATED')  DATA2650
C      GOT0740                      DATA2660
C      734 PRINT 735,QFPT,HBPPT,HXPPT  DATA2670
C      735 FORMAT('01',T15,'STEAM FLOW TO FW PUMP TURBINE',T70+2X,F8.0,T87,
C             '1'LB/HR'/          DATA2680
C             '2',T15,'BOWL ENTHALPY FW PUMP TURBINE',T70,F11.1,T87,'BTU/LB'/
C             '3',T15,'EXHAUST ENTHALPY FW PUMP TURBINE',T70,F11.1,T87,'BTU/LB')  DATA2690
C      GOT0740                      DATA2700
C      736 PRINT 737,IFPT          DATA2710
C      737 FORMAT('01',T15,'FW PUMP IS MOTOR DRIVEN, IFPT='I2)  DATA2720

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C   740 IF(QAE.GT.0.)GOTO742          DATA2960
C
C     PRINT 741,QAE                   DATA2970
C   741 FORMAT('1',T15,'THERE IS NO STEAM JET AIR EJECTOR, QAE =',F10.0) DATA2980
C
C     GOT0755                         DATA2990
C
C   742 PRINT 750,QAF                   DATA3000
C   750 FORMAT(                           DATA3010
C     1",T15,'STEAM FLOW TO STEAM JET AIR EJECTOR',T70,3X,F7.0,T87, DATA3020
C     2"LB/HR')                         DATA3030
C
C   755 IF(LK.GT.0.)GOTO760           DATA3040
C
C     PRNT 756,LK                      DATA3050
C   756 FORMAT('1',T15,'VALVE STEM AND PACKING LEAKAGES WILL NOT BE CALCULATED', T15, LK=',T21) DATA3100
C
C     RETURN                            DATA3101
C
C   760 PRINT 770,LK                   DATA3110
C   770 FORMAT('1',T15,'VALVE STEM AND PACKING LEAKAGES WILL BE CALCULATED', T15, LK=',T21) DATA3120
C
C     RETURN                            DATA3130
C
C   771 PRINT 770,LK                   DATA3140
C   771 FORMAT('1',T15,'VALVE STEM AND PACKING LEAKAGES WILL BE CALCULATED', T15, LK=',T21) DATA3150
C
C     RETURN                            DATA3151
C
C     RETURN                            DATA3160
C
C     RETURN                            DATA3170
C
C     END                               DATA3180

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SUBROUTINE RESULT(VERS)	RESU 0
IMPLICIT REAL*8EA-H,D-71	RESU 10
C THIS SUBPROGRAM PRINTS THE CALCULATED RESULTS	RESU 20
	RESU 21
	RESU 22
COMMON /AM/AMRMR(5),AMAMP(51,TMR(6)),MR	RESU 40
COMMON /FPT/QFPT,PFPPT,HRFPT,PXFPT,HXPFT,IFPT	RESU 50
COMMON /FMR/HAFD,HAED,QR,OF(21),HFS(21),HES(21),OMF(5),HMF(5),	PESU 60
1QMC(5),HMG(51,OD(12),OF(12),OE(12),OCR,HCR,QRN,OC,TLLP,T	RESU 61
COMMON /GS/OGS,HRGS,PBGS,AMRGGS,SBGS,VRGS,TRGS,PXGS,AMXGS,SXGS,	RESU 70
1VYGS,TXGS,HXGS,PDGS,MBGS,MXGS,NCGS,TRGS,NGS	RESU 71
COMMON /HP/PRHP,PRHP,TRHP,AMRHP,HRHP,SPHP,OXHP,TXHP,AMXHP,HXHP,	RESU 80
1SXHP,UEFPHD	RESU 81
COMMON /HX1/PE(12),PMR(5)	RESU 90
COMMON /HX2/PE(12),HE(12),HAMR(5),HRMR(5),SAMR(5),SBMR(5),PCMD(5)	RESU 100
COMMON /IN/L1(13),L2(13),J1(13),INR(5)	RESU 110
COMMON /TP/PRTP,PRIP,TRIP,AMRIP,HRTP,SRIP,OXTP,TXTP,AMXTP,HXTP,	RESU 120
1SXTP,UEFPIP	RESU 121
COMMON /LEAK/OLK1,HLK1,QLK2,HLK2,QLK3,HLK3,QLK4,HLK4,QLK5,HLK5,	RESU 130
1OLKA,HLK6,OLK7,HLK7,OLK8,HLK8,QLK9,HLK9,QLK10,HLK10,LK,LK1,LK3,	RESU 131
2LK5,LK7,LK9	RESU 132
COMMON /LP/QLLP,PLLP,TRLP,AMRLP,HRLP,SLRP,OXLP,PXLP,TXLP,AMXLP,	RESU 140
1HYP,SXLP,UEEPLP	RESU 141
COMMON /MIS/CMTS(18), TC,TEP,TR,HR,WRATE,GC,WML,WGL,CMU,QEP,	RESU 150
1CP,WGEN,WFWP,HTRTN,HTRTG,CFFN,CFFG,PC	RESU 151
COMMON /PAR1/HO(12),HI(12),QAF,HC,HFP,DHP,TT(12),TD(12),TOCA(12),	RESU 160
1HD(12),PLA,PLR,ND(12),NDC(12),TP,NE,NSHAFT	RESU 161
COMMON /PAR2/PSH(12),TSH(12),TD(12),TTO(12),PXHP,PXTP	RESU 170
COMMON /RH1/PXRH2,PIRH2,PXRH1,PIRH2,PFPT	RESU 180
COMMON /RH2/QRH1,HCRH1,QRH2,HCRH2,NRH	RESU 190
COMMON /RH3/TDRH1,TTDRH2,HRH1,HPH2,PCRH1,TCH1,PCRH2,TCH2,TXRH1,	RESU 200
1HXRH1,TXRH2,HXRH2,HIRH2,HIRH1,QRH	RESU 201
COMMON /SSR/QSPE,QMC,QSSR,HSSR,PSSR,QFWH,QSSRMU,HS SSMU	RESU 210
COMMON /T/OT,PT,TT,AMT,HT	RESU 220
COMMON /XS1/PSX,PST	RESU 230
COMMON /XS2/HESX,OMR	RESU 240
COMMON /XS3/OSI,HST,TSX,OSX,HSX,AMSX,EMS,MS	RESU 250
C NPAGE=1	RESU 260
PRINT 100,(CHTS(K),K=1,181,VERS,NPAGE	RESU 270
	RESU 280
	RESU 290

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100 FORMAT('1',T10,18A4/
1' ',T10,'STEAM TURBINE CYCLE HEAT BALANCE'/
2' ',T10,'ORCENT, VERSION ',AB/
3' 0',T10,'CALCULATED RESULTS, PAGE',I3///)
C      PRINT 110,HTRTN,CFFN,HTRTG,CFFCG,WGEN
110 FORMAT('0',T10,'TABLE I OVERALL PERFORMANCE'/
1' 0',T10,'NET TURBINE CYCLE HEAT RATE, BTU/KW-HR',T60,F8.0/
2' 1',T10,'NET TURBINE CYCLE EFFICIENCY, PER CENT',T60,F10.2/
3' 0',T10,'GROSS TURBINE CYCLE HEAT RATE, BTU/KW-HR',T60,F8.0/
4' 1',T10,'GROSS TURBINE CYCLE EFFICIENCY, PER CENT',T60,F10.2/
5' 0',T10,'GENERATOR OUTPUT, MWE',T60,F11.3)
C      IF(IFPT.EQ.0)GOTO112
C      WG=WGEN+WFWP*0.001
C      PRINT 111,WFWP,WG
111 FORMAT('0',T10,'POWER REQUIRED BY TURBINE-DRIVEN FW PUMP, MW',
1T60,-3PF11.3/
2' 1',T10,'GENERATOR OUTPUT PLUS FW PUMP POWER, MW',T60,0PF11.3)
C      GOTO114
C      112 WG=WGEN-WFWP*0.001
C      PRINT 113,WFWP,WG
113 FORMAT('0',T10,'POWER REQUIRED BY MOTOR-DRIVEN FW PUMP, MW',
1T60,-3PF11.3/
2' 1',T10,'GENERATOR OUTPUT MINUS FW PUMP POWER, MWE',T60,0PF11.3)
C      114 PRINT 115,WML,WGL
115 FORMAT('0',T10,'MECHANICAL LOSSES, KW',T60,F8.0/
2' 1',T10,'GENERATOR LOSSES, KW',T60,F8.0)
C      NPAGE=NPAGE+1
C      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE
C      PRINT 120
120 FORMAT('0',T10,'TABLE II TURBINE EXPANSION LINE'/
1' 0',T50,'STEAM FLOW          PRESSURE          TEMPERATURE          MOISTURE
2ALPY    ENTROPY'/
3' 1',T50,'  LB/HR          PSIA          F          PER CENT
4/LB     BTU/LB-F')
C      PRINT 130,OT,PT,TT,AMT,HT,
1OCS,PBGS,TRGS,AMBGS,HBGS,SBGS,
2OCS,PXGS,TXGS,AMXGS,HXGS,SXGS
130 FORMAT('0',T10,'TURBINE THROTTLE',
1T50,F10.0,F12.1,F12.1,F14.2,F12.1/
2' 1',T10,'GOVERNING STAGE BOWL',
3T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1,F12.4/
4' 1',T10,'GOVERNING STAGE ELEP AND UEEP',
5T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1,F12.4)
C      IFINSHAFT.EQ.1)GOTO190
C      PRINT 140,QRHP,PRHP,TRHP,AMRHP,HRHP,SRHP,
1QXHP,PXHP,TXHP,AMXHP,HXHP,SXHP,
2PXHP,UEEPHP
140 FORMAT('1',T10,'HP SECTION BOWL',
1T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1,F12.4/
2' 1',T10,'HP SECTION ELEP',
3T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1,F12.4/
4' 1',T10,'HP SECTION UEEP',
5T60,F12.1,T98,F12.1)
C      IFINSHAFT.EQ.2)GOTO160
C      149 IF(MS.EQ.0)GOTO151

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C      PRINT 150,0SI,PST,HST,
10SX,PSX,TSY,AMSX,HSX
150 FORMAT(' ',T10,'EXTERNAL MOISTURE SEPARATOR INLET',
1T50,F10.0,F12.1,T98,F12.1/
2' ',T10,'EXTERNAL MOISTURE SEPARATOR OUTLET',
3T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1)
C      151 IF(NSHAFT.EQ.3)GOTO190
C      160 IF(NRH.EQ.0)GOTO181
C
      PRINT 170,0RH,PRH1,HIRH1,
10RH,PRRH1,TXRH1,HXRH1
170 FORMAT(' ',T10,'1ST STAGE REHEATER INLET',
1T50,F10.0,F12.1,T98,F12.1/
2' ',T10,'1ST STAGE REHEATER OUTLET',
3T50,F10.0,F12.1,F12.1,T98,F12.1)
C      TE(NRH,LT,2)GOTO181
C
      PRINT 180,0RH,PRPH2,HIRH2,
10RH,PRRH2,TXRH2,HXRH2
180 FORMAT(' ',T10,'2ND STAGE REHEATER INLET',
1T50,F10.0,F12.1,T98,F12.1/
2' ',T10,'2ND STAGE REHEATER OUTLET',
3T50,F10.0,F12.1,F12.1,T98,F12.1)
C      181 IF(NSHAFT.EQ.2)GOTO190
C
      PRINT 185,0BIP,PRIP,TRIP,AMBIP,HBIP,SBIP,
10XIP,PXIP,TXIP,AMXIP,HXIP,SXIP,
2PXIP,UEEP1P
185 FORMAT(' ',T10,'IP SECTION BOWL',
1T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1,F12.4/
2' ',T10,'IP SECTION ELEP1',
3T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1,F12.4/
4' ',T10,'IP SECTION HEFP1',
5T60,F12.1,T98,F12.1)
C      GOTO140
C
190 PRINT 200,0RLP,PRLP,TRLP,AMRLP,HBLP,SRLP
200 FORMAT(' ',T10,'LP SECTION BOWL',
1T50,F10.0,F12.1,F12.1,2PF14.2,0PF12.1,F12.4)
C      TE(MR,EQ.0)GOTO230
C
      DO220 L=1,MR
C
      PRINT 210,L,PMR(L),TMR(L),AMMR(L),HRMR(L),SBMR(L),
1L,PMR(L,1),TMR(L,1),AMAMR(L,1),HAMR(L,1),SAMR(L)
210 FORMAT(' ',T10,'BEFORE MOISTURE REMOVAL NO.',T2,
1T60,F12.1,F12.1,2PF14.2,0PF12.1,F12.4/
2' ',T10,'AFTER MOISTURE REMOVAL NO.',T2,
3T60,F12.1,F12.1,2PF14.2,0PF12.1,F12.4)
C      220 CONTINUE
C
230 PRINT 240,0XLP,PXLP,TXLP,AMXLP,HXLP,SXLP,
1PXLP,UEEPLP
240 FORMAT(' ',T10,'LP SECTION ELEP1',
1T50,F10.0,F16.5,FB.1,2PF14.2,0PF12.1,F12.4/
2' ',T10,'LP SECTION HEFP1',
3T60,F16.5,T98,F12.1)
C      NPAGE=NPAGE+1
C
      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE
C      IF(OAE.GT.1.0)GOTO260
C

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PRINT 250
250 FORMAT('0',T10,'TABLE III THERE IS NO STEAM JET ATR EJECTOR')
C
C      GOTO275
C
260 PRINT 270,0AE,HAET,HAEO
270 FORMAT('0',T10,'TABLE III STEAM JET ATR EJECTOR')
 1'0',T10,'STEAM FLOW, LB/HR',T40,F10.0/
 2' ',T10,'STEAM ENTHALPY IN, BTU/LB',T40,F11.1/
 3' ',T10,'STEAM ENTHALPY OUT, BTU/LB',T40,F11.1)
C
275 NPAGE=NPAGE+1
C
      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE
C
      IF(MS.GT.0)GOTO298
C
      PRINT 280
280 FORMAT('0',T10,'TABLE IV THERE IS NO EXTERNAL MOISTURE SEPARATOR')
 1)
C
C      GOTO350
C
290 IF(MS.LE.NF)GOTO310
C
      PRINT 300
300 FORMAT('0',T10,'TABLE IV EXTERNAL MOISTURE SEPARATOR DRAINS TO CORE')
 1'DENSER')
C
C      GOTO330
C
310 PRINT 320,MS
320 FORMAT('0',T10,'TABLE IV EXTERNAL MOISTURE SEPARATOR DRAINS TO FW')
 1' HEATER NO.',T2)
C
330 PRINT 340,QMR,PSX,TSX,HESX
340 FORMAT('0',T10,'DRAIN FLOW, LB/HR',T33,F10.0/
 1' ',T10,'DRAIN PRESSURE, PSIA',T33,F11.1/
 2' ',T10,'DRAIN TEMPERATURE, F',T33,F11.1/
 3' ',T10,'DRAIN ENTHALPY, BTU/LB',T33,F11.1)
C
350 NPAGE=NPAGE+1
C
      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE
C
      IF(NRH.GT.0)GOTO370
C
      IF(NRH.EQ.0)GOTO359
C
      PRINT 358
358 FORMAT('0',T10,'TABLE V EXTERNAL REHEATER, SEE TABLE III')
C
C      GOTO420
C
359 PRINT 360
360 FORMAT('0',T10,'TABLE V THERE IS NO REHEATER')
C
C      GOTO400
C
370 PRINT 380,NRH,OPRH1,HRH1,PCRH1,TCRH1,HCRH1
380 FORMAT('0',T10,'TABLE V LIVE STEAM REHEATER')
 1'0',T10,'1ST STAGE DRAINS TO FW HEATER NO.',T2/
 2' ',T10,'1ST STAGE STEAM FLOW, LB/HR',T43,F10.0/
 3' ',T10,'1ST STAGE STEAM ENTHALPY, BTU/LB',T43,F11.1/
 4' ',T10,'1ST STAGE PRESSURE, PSIA',T43,F11.1/
 5' ',T10,'1ST STAGE DRAIN TEMPERATURE, F',T43,F11.1/
 6' ',T10,'1ST STAGE DRAIN ENTHALPY, BTU/LB',T43,F11.1)
C
      IF(NRH.EQ.1)GOTO460
C
      PRINT 390,OPRH2,HRH2,PCRH2,TCRH2,HCRH2

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393 FORMAT('1',T10,'2ND STAGE DRAINS TO FW HEATER NO. 1'
      '1',T10,'2ND STAGE STEAM FLOW, LB/HR',T43,F10.0)
      '2',T10,'2ND STAGE STEAM ENTHALPY, BTU/LB',T43,F11.1)
      '3',T10,'2ND STAGE PRESSURE, PSTAV',T43,F11.1)
      '4',T10,'2ND STAGE DRAIN TEMPERATURE, F',T43,F11.1)
      '5',T10,'2ND STAGE DRAIN ENTHALPY, BTU/LB',T43,F11.1)
C
400 NPAGE=NPAGE+1
C
      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE
C
      IF(NP.GT.0)GOTO420
C
      PRINT 410
410 FORMAT('1',T10,'TABLE VI THERE ARE NO MOISTURE REMOVAL STAGES')
C
      GOTO440
C
420 PRINT 428
428 FORMAT('1',T10,'TABLE VI MOISTURE REMOVAL STAGES')
C
      PRINT 429,(LMR(L),L=1,MRI)
429 FORMAT('1',T10,'MOISTURE REMOVAL STAGE NO.',T36,5(10X,I2,2X))
C
      PRINT 430,(TMR(L),L=1,MRI)
430 FORMAT('1',T10,'DRAINS TO FW HEATER NO.',T36,5(10X,I2,2X))
C
      PRINT 431,(PMR(L),L=1,MRI)
431 FORMAT('1',T10,'STAGE PRESSURE, PSTAV',T36,5(8X,F6.1))
C
      PRINT 432,(TMF(L),L=1,MRI)
432 FORMAT('1',T10,'TEMPERATURE, F',T36,5(8X,F6.1))
C
      PRINT 433,(OMF(L),L=1,MRI)
433 FORMAT('1',T10,'WATER REMOVED, LB/HR',T36,5(5X,F8.0,1X))
C
      PRINT 434,(HMF(L),L=1,MRI)
434 FORMAT('1',T10,'WATER ENTHALPY, BTU/LB',T36,5(8X,F6.1))
C
      PRINT 435,(OMG(L),L=1,MRI)
435 FORMAT('1',T10,'STEAM REMOVED, LB/HR',T36,5(5X,F8.0,1X))
C
      PRINT 436,(HMG(L),L=1,MRI)
436 FORMAT('1',T10,'STEAM ENTHALPY, BTU/LB',T36,5(7X,F7.1))
C
440 NPAGE=NPAGE+1
C
      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE
C
      IF(NF.GT.0)GOTO460
C
      PRINT 450
450 FORMAT('1',T10,'TABLE VII THERE ARE NO FW HEATERS')
C
      GOTO500
C
460 PRINT 470
470 FORMAT('1',T10,'TABLE VII FW HEATERS')
C
      N1=1
      N2=NF
C
      IF(NF.LE.6)GOTO480
C
      N2=6
C
480 PRINT 481,(I,I=N1,N2)
481 FORMAT('1',T10,'FW HEATER NO.',T44,6I14)
C
      PRINT 482,(OF(I),I=N1,N2)
482 FORMAT('1',T10,'FW FLOW, LB/HR ',T45,6F14.0)

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C      PRINT 483,(TC(I),I=N1,N2)          RESU2290
483 FORMAT(' ',T10,'FW TEMPERATURE OUT, F',T46,6F14.11)  RESU2300
C      PRINT 484,(HD(I),I=N1,N2)          RESU2310
484 FORMAT(' ',T10,'FW ENTHALPY OUT, BTU/LB ',T46,6F14.11)  RESU2320
C      PRINT 485,(TI(I),I=N1,N2)          RESU2330
485 FORMAT(' ',T10,'FW TEMPERATURE IN, F',T46,6F14.11)  RESU2340
C      PRINT 486,(HT(I),I=N1,N2)          RESU2350
486 FORMAT(' ',T10,'FW ENTHALPY IN, BTU/LB ',T46,6F14.11)  RESU2360
C      PRINT 487,(PE(I),I=N1,N2)          RESU2370
487 FORMAT(' ',T10,'EXTRACTION STAGE PRESSURE, PSTA',T46,6F14.11)  RESU2380
C      PRINT 488,(OE(I),I=N1,N2)          RESU2390
488 FORMAT(' ',T10,'EXTRACTION STEAM FLOW, LB/HR ',T45,6F14.01)  RESU2400
C      PRINT 489,(HE(I),I=N1,N2)          RESU2410
489 FORMAT(' ',T10,'EXTRACTION STEAM ENTHALPY, BTU/LB ',T46,6F14.11)  RESU2420
C      PRINT 490,(PSH(I),I=N1,N2)          RESU2430
490 FORMAT(' ',T10,'SHELL PRESSURE, PSTA',T46,6F14.11)  RESU2440
C      PRINT 491,(TSH(I),I=N1,N2)          RESU2450
491 FORMAT(' ',T10,'SHELL TEMPERATURE, F',T46,6F14.11)  RESU2460
C      PRINT 492,(OD(I),I=N1,N2)          RESU2470
492 FORMAT(' ',T10,'SHELL DRAIN FLOW, LB/HR ',T45,6F14.01)  RESU2480
C      PRINT 493,(TD(I),I=N1,N2)          RESU2490
493 FORMAT(' ',T10,'SHELL DRAIN TEMPERATURE, F',T46,6F14.11)  RESU2500
C      PRINT 494,(HD(I),I=N1,N2)          RESU2510
494 FORMAT(' ',T10,'SHELL DRAIN ENTHALPY, BTU/LB ',T46,6F14.11)  RESU2520
C      IF(N2.EQ.NF)GOTO500             RESU2530
C      N1=7                            RESU2540
C      N2=NF                           RESU2550
C      GOTO480                         RESU2560
C      500  NPAGE=NPAGE+1                RESU2570
C      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE  RESU2580
C      PCT=PC*2.036                   RESU2590
      PRINT 510,PC,PCT,QC,TC,HC          RESU2600
510 FORMAT('01',T10,'TABLE VIII CONDENSER'/
1*T1,T10,'CONDENSER PRESSURE, PSTA',T41,9X,F10.5,  RESU2610
2T65,'=',T70,F10.2,T85,'TN, HGA'/
3*1,T10,'CONDENSATE FLOW, LB/HR',T41,F14.0/
4*1,T10,'CONDENSATE TEMPERATURE, F',T41,9X,F6.1/
5*1,T10,'CONDENSATE ENTHALPY, BTU/LB',T41,9X,F6.1)  RESU2620
C      NPAGE=NPAGE+1                  RESU2630
C      PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE  RESU2640
C      PRINT 511                      RESU2650
511 FORMAT('01',T10,'TABLE IX CONDENSATE AND FEEDWATER')  RESU2660
C      IF(OCP.LT.3.)GOTO519            RESU2670
C      PRINT 512,OCP,HCR              RESU2680
512 FORMAT(  RESU2690
1*01,T10,'CONDENSATE FLOW BY-PASSED TO STEAM GENERATOR, LB/HR',  RESU2700
2T70,F10.0/
3*1,T10,'CONDENSATE ENTHALPY BY-PASSED TO STEAM GENERATOR, BTU/LB',RESU2710
RESU2913

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4,T70,5X,F6.1)                                RESU2914
C
519 PRINT 520,QFP,TFP,HFP,EHP,DP,QR,TR,HR,OMU    RESU2920
520 FORMAT(                                           RESU2930
 1E9,T10,'FW FLOW TO FW PUMP, LB/HR',T70,F10.0/   RESU2940
 21 1,T10,'FW TEMPERATURE TO FW PUMP, F',T70,5Y,F6.1/  RESU2941
 31 1,T10,'FW ENTHALPY TO FW PUMP, BTU/LB',T70,5X,F6.1/  RESU2942
 41 1,T10,'FW ENTHALPY RTSE ACROSS FW PUMP, BTU/LB',T70,5X,F6.1/  RESU2943
 51 1,T10,'FW PRESSURE INCREASE ACROSS FW PUMP, PSI',T70,4X,F6.0/  RESU2944
 610 1,T10,'FW FLOW TO STEAM GENERATOR, LB/HR',T70,F10.0/  RESU2945
 71 1,T10,'FW TEMPERATURE TO STEAM GENERATOR, F',T70,5X,F6.1/  RESU2946
 81 1,T10,'FW ENTHALPY TO STEAM GENERATOR, BTU/LB',T70,5X,F6.1/  RESU2947
 910 1,T10,'MAKE-UP TO CONDENSER HOTWELL, LB/HR',T70,F10.0)  RESU2948
C
  PRINT 521,QRN,HT                                RESU2950
521 FORMAT(1E1,T10,'STEAM FLOW FROM STEAM GENERATOR, LB/HR',T70,F10.0/RESU2952
 11 1,T10,'STEAM ENTHALPY FROM STEAM GENERATOR, BTU/LB',T70,4X,F7.1)RESU2951
C
  TF1(FPT,LT6.1)GOT0528                         RESU2952
C
  PRINT 525,QFPT                                RESU2953
525 FORMAT(1E1,T10,'THROTTLE STEAM FLOW FW PUMP TURBINE, LB/HR',T70,
 1E10.0)                                         RESU2954
C
  PXEPTT=PXEPT*2.036                            RESU2955
C
  PRINT 527,PFPPT,HFPPT,PXEPT,PXEPTT,HXPPT      RESU2956
527 FORMAT(1E1,T10,'THROTTLE PRESSURE FW PUMP TURBINE, PSIA',T70,
 1E11.1/   RESU2957
 21 1,T10,'THROTTLE ENTHALPY FW PUMP TURBINE, BTU/LB',T70,F11.1/  RESU2958
 31 1,T10,'EXHAUST PRESSURE FW PUMP TURBINE, PSIA',T70,F15.5,   RESU2959
 4T90,1=F10.2,T105,'IN. HGA')                   RESU2960
 51 1,T10,'EXHAUST ENTHALPY FW PUMP TURBINE, BTU/LB',T70,F11.1)  RESU2961
C
  528 NPAGE=NPAGE+1                               RESU2962
C
  PRINT 100,(CMTS(K),K=1,18),VERS,NPAGE        RESU2963
C
  TF1(LK,GT,3)GOT0550                           RESU2964
C
  PRINT 540                                     RESU2965
540 FORMAT(1E1,T10,'TABLE X VALVE STEM AND SHAFT LEAKAGES WERE NOT CALCULATED')  RESU2966
C
  GOT0560                                     RESU2967
C
  551 PRINT 560,OSSR,HSSR,OMC,OSPF              RESU2968
560 FORMAT(1E1,T10,'TABLE X VALVE STEM AND SHAFT LEAKAGES')/
  1E9,T12,'VALVE SEAL REGULATOR')/             RESU2969
  21 1,T12,'FLOW TO SSR, LB/HR',T65,F8.0/       RESU2970
  21 1,T12,'ENTHALPY AT SSR, BTU/LB',T67,F7.1/  RESU2971
  41 1,T12,'FLOW FROM SSR TO MAIN CONDENSER, LB/HR',T65,F8.0/  RESU2972
  51 1,T12,'FLOW FROM SSR TO STEAM PACKING EXHAUST, LB/HR',T65,
  6F8.0)                                         RESU2973
C
  TF(NF,EO,0)GOT0562                           RESU2974
C
  PRINT 561,NE,CFWH                            RESU2975
561 FORMAT(1E1,T12,'FLOW FROM SSR TO FW HEATER NO.',13.1, LB/HR',T65,
  1E9.0)                                         RESU2976
C
  562 PRINT 563,OSSRMU,HSSRMU                  RESU2977
563 FORMAT(1E1,T12,'MAKE-UP FROM THROTTLE STEAM, LB/HR',T65,F8.0/
  1E1,T12,'ENTHALPY OF MAKE-UP STEAM, BTU/LB',T67,F7.1)  RESU2978
C
  PRINT 573,LK1,QLK1,HLK1,QLK2,HLK2,LK3,QLK3,HLK3,QLK4,HLK4  RESU2979
572 FORMAT(1E1,T10,'THROTTLE VALVE STEM')/
  1E1,T12,'LEAK NO. 1 (DRAINS TO FW HEATER NO.',13.1, LB/HR',T65,
  2F8.0/)                                         RESU2980
  21 1,T12,'ENTHALPY LEAK NO. 1, BTU/LB',T67,F7.1/  RESU2981
  41 1,T12,'LEAK NO. 2 (DRAINTS TO SSR), LB/HR',T65,F8.0/  RESU2982
  RESU2983

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51 1,T12,'ENTHALPY LEAK NO. 2, BTU/LB',T67,F7.1/
5101,T10,'GOVERNING STAGE SECTION'
71 1,T12,'LEAK NO. 3 (DRAINS TO FW HEATER NO.',I3,'), LB/HR',T65,
8F8.0/
91 1,T12,'ENTHALPY LEAK NO. 3, BTU/LB',T67,F7.1/
A1 1,T12,'LEAK NO. 4 (DRAINS TO SSR), LB/HR',T65,F8.0/
B1 1,T12,'ENTHALPY LEAK NO. 4, BTU/LB',T67,F7.1)
C   IF(1NSHAFT.EQ.1)GOTO600
C
C   PRINT 580,LK5,QLK5,HLK5,QLK6,HLK6
580 FORMAT('101,T10,'HP TURBINE SECTION')
11 1,T12,'TOTAL LEAK NO. 5 (DRAINS TO FW HEATER NO.',I3,'), LB/HR',RESU3381
2T65,F8.0/
31 1,T12,'ENTHALPY LEAK NO. 5, BTU/LB',T67,F7.1/
41 1,T12,'TOTAL LEAK NO. 6 (DRAINS TO SSR), LB/HR',T65,F8.0/
51 1,T12,'ENTHALPY LEAK NO. 6, BTU/LB',T67,F7.1)
C   IF(1NSHAFT.EQ.2)GOTO600
C
C   PRINT 590,LK7,QLK7,HLK7,QLK8,HLK8,LK9,QLK9,HLK9,QLK10,HLK10
590 FORMAT('101,T10,'TP TURBINE SECTION')
11 1,T12,'LEAK NO. 7 (DRAINS TO FW HEATER NO.',I3,'), LB/HR',T65,
2F8.0/
31 1,T12,'ENTHALPY LEAK NO. 7, BTU/LB',T67,F7.1/
41 1,T12,'LEAK NO. 8 (DRAINS TO SSR), LB/HR',T65,F8.0/
51 1,T12,'ENTHALPY LEAK NO. 8, BTU/LB',T67,F7.1/
61 1,T12,'TOTAL LEAK NO. 9 (DRAINS TO FW HEATER NO.',I3,'), LB/HR',RESU3436
7T65,F8.0/
81 1,T12,'ENTHALPY LEAK NO. 9, BTU/LB',T67,F7.1/
91 1,T12,'TOTAL LEAK NO. 10 (DRAINS TO SSR), LB/HR',T65,F8.0/
A1 1,T12,'ENTHALPY LEAK NO. 10, BTU/LB',T67,F7.1)
C   600 CONTINUE
C
C   RETURN
END

```

SUBROUTINE AMDIST(K,P,PB,HB,SB,PX,HX,SX,HBMR,HAMR,HEP,AM,	AMDI 0
1AM225,AMEP, SBMR,S225,PCWD,TE)	AMDI 1
IMPLTCIT REAL*8(A-H,O-Z)	AMDI 10
C SUBPROGRAM FOR MOISTURE REMOVAL CALCULATIONS	AMDI 25
C TABLE IV (P. 14, GER-2454A)	AMDI 21
C	AMDI 22
DIMENSION	AMDI 30
3PE(61),TE(61),HF(61),HG(61),H2SI(61),HSL(61),H2BE(61),P(5),	AMDI 40
2AM210(61),UE(51),S210(51),HS313(51),AF(51),BE(51),SBMR(51),	AMDI 41
3RGMLF(51),AMRE(51),AM(5),PCWD(51),PCFR(51),HBMR(51),HAMR(51),S225(51),	AMDI 42
4HS326(51),AEN(51),AM225(51), AMLF(51),CGE(51),UEN(51),HGEP(51),	AMDI 43
5ERM(51)	AMDI 44
C	AMDI 45
COMMON /CDNV/HCON,UERCON,AMCON,RHCON,HCON,PCON,SSRCOM,XSPCON	AMDI 50
C K=NUMBER OF MOISTURE REMOVAL POINTS	AMDI 60
C HBMR=ENTHALPY BEFORE MOISTURE REMOVAL	AMDI 70
C HAMR=ENTHALPY AFTER MOISTURE REMOVAL	AMDI 71
C HEP =ENTHALPY AT END POINT AFTER MOISTURE REMOVAL	AMDI 72
C AM=MOISTURE BEFORE MOISTURE REMOVAL	AMDI 73
C AM225=MOISTURE AFTER MOISTURE REMOVAL	AMDI 74
C AMEP =MOISTURE AT END POINT AFTER MOISTURE REMOVAL	AMDI 75
C SBMR=ENTROPY BEFORE MOISTURE REMOVAL	AMDI 76
C S225=ENTROPY AFTER MOISTURE REMOVAL	AMDI 77
C PCWD=PER CENT WATER DRAINED	AMDI 78
C STEAM PROPERTIES	AMDI 79
L=K+1	AMDI 80
DO100 I=1,K	AMDI 81
PE(I)=P(I)	AMDI 100
	AMDI 110
	AMDI 120

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100 CONTINUE
  PE(I,I)=PX
  DO110 I=1,L
  TE(I)=TSAT(PE(I))
  HF(I)=H2TO(TE(I))
  HG(I)=HVAP(TE(I),PE(I))
  HFG(I)=HG(I)-HF(I)
  SG=SVAP(TE(I),PE(I))
  AM2SI=(SG-1.0)/(SG-SL10(TE(I)))
  H2S1(I)=HG(I)-AM2SI*HFG(I)
  HSL(I)=TE(I)+459.7
110 CONTINUE
C
C  BASE EXPANSION ANALYSIS
  DO121 I=1,K
  CALL FTG12B(PE(I),HR,SB,HX,SX,H2RE(I),S)
121 CONTINUE
  H2RE(I)=HX
  DO122 J=1,L
  AM210(I)=1.0-(H2RE(I)-HF(I))/HFG(I)
122 CONTINUE
  DO130 I=1,K
  UE(I)=H2RE(I)-H2RE(I+1)
  S210(I)=1.0+(H2RE(I)-H2S1(I))/HSL(I)
  HS31(I)=H2S1(I+1)+HSL(I+1)*(S210(I)-1.0)
  AE(I)=H2RE(I)-HS31(I)
  PE(I)=1.0,S*UE(I)/AE(I)
  PGML(I)=1.0-0.435*(AM210(I)+AM210(I+1))
130 CONTINUE
C
C  MOISTURE REMOVAL CALCULATION AND NEW EXPANSION FOLLOWING MOISTURE REMOVAL
  DO150 I=1,K
  AMRE(I)=FTG10(PE(I))
  TE(I,GT,1)GOTO141
  AM(I)=AM210(I)
  GOTO142
141 AM(I)=EPM(I-1)
142 PCWD(I)=AMRE(I)*AM(I)
  PCFR(I)=1.0-0.4*PCWD(I)
  TE(I,GT,1)GOTO143
  HRMR(I)=H2RE(I)
  GOTO144
143 HRMR(I)=HGEPI(I-1)
144 SPMR(I)=1.0+(HRMR(I)-H2S1(I))/HSL(I)
  HAMR(I)=(HRMR(I)*100.0-HF(I)*PCWD(I))/PCFR(I)
  S225(I)=1.0+(HAMR(I)-H2S1(I))/HSL(I)
  HS326(I)=H2S1(I+1)+HSL(I+1)*(S225(I)-1.0)
  AFN(I)=HAMR(I)-HS326(I)
  AM225(I)=1.0-(HAMR(I)-HF(I))/HFG(I)
  EPM=0.1
  DO145 IT=1,100
  AMLF(I)=1.0-0.435*(AM225(I)+EPM)
  CGE(I)=RE(I)*AMLF(I)/BGML(I)
  UEN(I)=AFN(I)*CGE(I)*0.01
  HGEPI(I)=HAMR(I)-UEN(I)
  EPM=0.05-(HGEPI(I)-HF(I+1))/HFG(I+1)
  ADM=DARS(EPM(I))-EPM(I)
  TE(ADM,LE,AMCON1GOTO150
  EPM=EPM(I)
145 CONTINUE
  PRINT 146,ADM,I
146 FORMAT('0-SUBROUTINE AMDIST-END POINT MOISTURE DID NOT CONVERGE, AAMOT',I1,
     1,'DM =',I1D14.6,5X,'I =',I2)
150 CONTINUE
  HEP=HGEPI(K)
  AMEP=EPM(K)
  RETURN
  END

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SUBROUTINE FWHEAT(I1,I2,MR,KL,MS,IT)
  IMPLICIT REAL*8(A-H,D-Z)

C SUBPROGRAM FOR FW HEATER HEAT BALANCE
C
C      DIMENSION IT1(131),OMFE(131)

C
COMMON /CONV/HCON,UERCON,AMCON,RHCON,WCON,PCON,SSRCON,XSPCON
COMMON /FWH/HAET,HAED,OR,QFS(20),HFS(20),HES(20),OME(5),HME(5),
  QMG(5),HMG(5),OD(12),OF(12),OE(12),OCR,HCR,QRD,OC,ILLP,T
COMMON /HX1/PE(12),PMR(5)
COMMON /HX2/HE(12),HF(12),HAMR(5),HBMR(5),SAMR(5),SBMR(5),PCMD(5)
COMMON /IN/L1(131),L2(131),J1(131),TMR(5)
COMMON /LEAK/QLK1,HLK1,QLK2,HLK2,QLK3,HLK3,QLK4,HLK4,QLK5,HLK5,
  1QLK6,HLK6,QLK7,HLK7,QLK8,HLK8,QLK9,HLK9,QLK10,HLK10,LK,LK1,LK3,
  2LK5,LK7,LK9
COMMON /PAR1/HO(12),HI(12),QAE,HC,HFP,DHP,TI(12),TD(12),TDOCA(12),
  1HD(12),PLA,PLB,ND(12),NDC(12),IP,NF,NSHAFT
COMMON /RH2/CRH1,HCRH1,ORH2,HCRH2,NRH
COMMON /SSR/QSPE,QMC,QSSR,HSSR,PSSR,DFWH,OSSRMU,HSSRMU
COMMON /XS2/HFSX,QMR

C
      I=11
      IT2=0
      GOT01930
1900  I=T+1
1910  OMFE(I)=0.
      IT1(I)=0
      IF(MR.EQ.0)GOT02000
      IF(L2(I).LT.L1(I))GOT01995
C FIND DRAIN FROM TURBINE MOISTURE REMOVAL STAGE
      M1=L1(I)
      M2=L2(I)
      DM1990 L=M1,M2
      QMF(L)=PCWD(L)*QFS(KL)*0.01
      HMF(L)=HLTO(TSAT(PMR(L)))
      IF(T.EQ.I2)GOT01980
      IF(PE(I).LT.(PMR(L)-1.0))GOT01980
      QMG(L)=0.0
      HMG(L)=0.0
      OMFE(I)=OME(L)
      GOT02000
1980  QMG(L)=0.005*QFS(KL)
      HMG(L)=HAMR(L)
C FIND FLOW TO FOLLOWING STAGE
      KL=KL+1
      QFS(KL)=QFS(KL-1)-OME(L)-QMG(L)
      HFS(KL)=HAMR(L)
      HES(KL-1)=HBMR(L)
1990  CONTINUE
1995  IF(T.EQ.I2)GOT02400
C FIND DRAIN FROM PREVIOUS FW HEATER
2000  CONTINUE
C FIND DRAINS TO FW HEATER SHELL
      QSUM=0.0
      SUM=0.0
C FIND FW FLOW
      IF(T.GT.1)GOT02020
      QFL=0.0
      IF(NRH.LT.1)GOT02040
C ADD DRAIN FROM 1-STAGE REHEATER
      IF(NRH.EQ.2)GOT02010
      QSUM=QSUM+ORH1
      SUM=SUM+ORH1*(HCRH1-HD(I))
      GOT02040
C ADD DRAIN FROM 2ND STAGE OF 2-STAGE REHEATER
2010  QSUM=QSUM+ORH2
      SUM=SUM+ORH2*(HCRH2-HD(I))
      GOT02040
2020  QFI=QFI-1
C ADD DRAIN FROM PREVIOUS FW HEATER
      FWHE   0
      FWHE   10
      FWHE   20
      FWHE   21
      FWHE   30
      FWHE   40
      FWHE   50
      FWHE   60
      FWHE   70
      FWHE   71
      FWHE   80
      FWHE   90
      FWHE  100
      FWHE  110
      FWHE  111
      FWHE  112
      FWHE  120
      FWHE  121
      FWHE  130
      FWHE  140
      FWHE  150
      FWHE  160
      FWHE  170
      FWHE  180
      FWHE  190
      FWHE  200
      FWHE  210
      FWHE  220
      FWHE  230
      FWHE  240
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      FWHE  250
      FWHE  260
      FWHE  270
      FWHE  280
      FWHE  290
      FWHE  300
      FWHE  310
      FWHE  320
      FWHE  330
      FWHE  340
      FWHE  350
      FWHE  351
      FWHE  360
      FWHE  370
      FWHE  380
      FWHE  390
      FWHE  400
      FWHE  410
      FWHE  411
      FWHE  420
      FWHE  421
      FWHE  430
      FWHE  440
      FWHE  441
      FWHE  450
      FWHE  460
      FWHE  470
      FWHE  471
      FWHE  480
      FWHE  490
      FWHE  500
      FWHE  510
      FWHE  511
      FWHE  520
      FWHE  530
      FWHE  540
      FWHE  550
      FWHE  551

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    IF(ND(T-1),EQ,1)GOTO2030
    QSUM=QSUM+OD(T-1)
    SUM=SUM+OD(T-1)*HD(I-1)-HD(T))
C   ADD DRAIN FROM 1ST STAGE OF 2-STAGE REHEATER
2030  IF(T<GT,2,DR,NRH,LT,2)GOTO2040
    QSUM=QSUM+DRH1
    SUM=SUM+DRH1*(HRH1-HD(I))
C   ADD DRAIN FROM EXTERNAL MOISTURE SEPARATOR
2040  TF(MS,NE,1)GOTO2050
    QSUM=QSUM+OMR
    SUM=SUM+OMR*(HFSX-HD(I))
C   ADD DRAINS FROM VALVE STEM AND SHAFT LEAKAGES
2050  IF(LK,EQ,0)GOTO2070
    TF(L,NE,LK1)GOTO2060
    QSUM=QSUM+QLK1
    SUM=SUM+QLK1*(HLK1-HD(T))
2060  TF(L,NE,LK2)GOTO2061
    QSUM=QSUM+QLK2
    SUM=SUM+QLK2*(HLK2-HD(T))
2061  TF(NSHAFT,Eq,1)GOTO2065
    TF(T,NE,LK5)GOTO2062
    QSUM=QSUM+QLK5
    SUM=SUM+QLK5*(HLK5-HD(T))
2062  TF(NSHAFT,Eq,2)GOTO2065
    TF(T,NE,LK7)GOTO2063
    QSUM=QSUM+QLK7
    SUM=SUM+QLK7*(HLK7-HD(T))
2063  TF(T,NE,LK9)GOTO2065
    QSUM=QSUM+QLK9
    SUM=SUM+QLK9*(HLK9-HD(T))
C   ADD DRAIN FROM STEAM SEAL REGULATOR
2065  IF(T,LT,NE)GOTO2070
    QSUM=QSUM+QFWH
    SUM=SUM+QFWH*(HSSR-HD(I))
C   ADD DRAINS FROM TURBINE MOISTURE REMOVAL STAGES
2070  TF(MR,Eq,0)GOTO2080
    IF(L2(I),LT,L1(I))GOTO2080
C   SUM DRAINS FROM TURBINE MOISTURE REMOVAL STAGES
    M2=L1(I)
    M2=L2(I)
    QD2=QD(L=M1,M2)
    QSUM=QSUM+QMF(L)+QMG(L)
    SUM=SUM+QMF(L)*(HMFL(L)-HD(I))+QMG(L)*(HMG(L)-HD(I))
2080  CONTINUE
2090  IF(ND(T),EQ,1)GOTO2100
C   HEAT BALANCE (FW HEATER DRAIN IS FLASHED)
    QF(T)=QF1
    QF(T)=(QF(I)*(HO(T)-HI(T))-SUM)/(HE(I)-HD(T))
    QD(T)=QF(I)+QSUM
    GOTO2200
C   HEAT BALANCE (FW HEATER DRAIN IS PUMPED)
2100  CONTINUE
    QF(I)=((QF1-QSUM)*(HO(T)-HI(T))-SUM)/(HE(I)-HD(T)+HO(T)-HI(T))
    QD(T)=QF(I)+QSUM
    QF(T)=QF1-QD(T)
    TF(I,Eq,3)GOTO2200
    HI2=(QD(T)*HD(T)+QF(I)*HO(T))/QF1
    TF(TP,NE,(T-1))GOTO2110
C   CORRECT FW PUMP INLET ENTHALPY
    HPI=HT1
    HT1=HT1+DHP
C   TEST FW INLET ENTHALPY
2110  ADH=DCRS(HI1-HI(I-1))
    IT1(T)=IT1(I)+1
    TF(ADH,LF,HCON)GOTO2200
    TF(I,GT,I)GOTO2111
    TF(T,GT,50)GOTO2112
2111  TF(T1(I-1),LE,50)GOTO2114
2112  IX=I-1
    PRINT 2113,TX,ADH
2113  FORMAT('0-SUBROUTINE FMHEAT-FW HEATER INLET ENTHALPY IN IT1 DID NOFWHE1140')

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IT CONVERGE, FW HEATER NO.',13,4X,'ADH= ',1PD14.61          FWHE1141
GOTO2200
C RE-SET INDEX I TO PREVIOUS FW HEATER
2114 I=I-1                                     FWHE1150
C CORRECT FW INLET TEMPERATURE
HT(I)=HI1                                     FWHE1151
IF(I,LE,IP)GOTO2118                           FWHE1160
TI(I)=TLIOH(HI1)                                FWHE1161
GOTO2118                                     FWHE1170
2118 TI(I)=TCOM(PLA,HI1)                         FWHE1180
2119 TF(NDCI(I),EO,0)GOTO2120                  FWHE1190
C CORRECT FW HEATER DRAIN TEMPERATURE
TD(I)=TI(I)+TDCA(I)                            FWHE1200
HD(I)=HLIO(TD(I))                               FWHE1210
2120 IF(I,LE,IILP-1)GOTO2000                  FWHE1220
IF(I,LT,IILP)GOTO2000                           FWHE1221
C RE-SET INDEX KL (FLOW TO FOLLOWING STAGE)
KL=I-IILP+1+L2(I)-J1(I)                        FWHE1230
GOTO2000                                     FWHE1240
2200 CONTINUE                                    FWHE1250
IF(I,LT,IILP)GOTO2210                           FWHE1260
C FIND FLOW TO FOLLOWING STAGE
KL=KL+1                                     FWHE1261
QFS(KL)=QFS(KL-1)-QE(I)-QMFE(I)               FWHE1270
HES(KL-1)=HE(I-1)                             FWHE1280
HES(KL)=HE(I)                                 FWHE1290
2210 IF(I,LT,NE)GOTO2300                         FWHE1300
C FIND ENTHALPY RISE ACROSS SJAЕ AFTER-CONDENSER AND SPE
QC=QE(I)+QCR                                  FWHE1301
DHAЕ=QAE*(HAЕI-HAЕ0)/QC+QSPE*(HSSR-HAЕ0)/QC
HI1=HC+DHAЕ                                     FWHE1310
HCR=HI1                                       FWHE1320
IF(I,IP,NE)GOTO2220                           FWHE1330
C CORRECT FW PUMP INLET ENTHALPY
HFP=HI1                                       FWHE1340
HI1=HI1+DHP                                     FWHE1350
C TEST FW INLET ENTHALPY
2220 ADH=DABS(HI1-HI(I))                      FWHE1351
IT2=IT2+1                                     FWHE1360
IF(I,ADH,LE,HCON)GOTO2300                    FWHE1370
IF(I,IT2,LE,50)GOTO2229                       FWHE1380
PRINT 2221,I,ADH                               FWHE1390
2221 FORMAT('0-SUBROUTINE FWHEAT-FW HEATER INLET ENTHALPY IN IT2 DID NOT')FWHE1400
1T CONVERGE, FW HEATER NO.',13,4X,'ADH= ',1PD14.61          FWHE1401
GOTO2300
2229 TF(I,LT,IILP)GOTO2230                  FWHE1410
C RE-SET INDEX KL (FLOW TO FOLLOWING STAGE)
KL=KL-1                                     FWHE1420
C CORRECT FW INLET TEMPERATURE
2230 HI(I)=HI1                                FWHE1421
IF(I,LE,IP)GOTO2240                           FWHE1430
TI(I)=TLIOH(HI1)                                FWHE1440
GOTO2250                                     FWHE1450
2240 TI(I)=TCOM(PLA,HI1)                         FWHE1460
2250 IF(NDCI(I),EO,0)GOTO2090                  FWHE1470
C CORRECT FW HEATER DRAIN TEMPERATURE
TD(I)=TI(I)+TDCA(I)                            FWHE1480
HD(I)=HLIO(TD(I))                               FWHE1481
GOTO2090                                     FWHE1490
2300 IF(I,LT,I2)GOTO01900                      FWHE1500
2400 RETURN                                     FWHE1501
END                                         FWHE1510
FWHE1511
FWHE1520
FWHE1530
FWHE1540
FWHE1550
FWHE1560
FWHE1570
FWHE1571
FWHE1580
FWHE1590
FWHE1600
FWHE1610
FWHE1620
FWHE1630

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SUBROUTINE FWHPAR(N1,N2)
IMPLICIT REAL*8(A-H,O-Z)

C SUBPROGRAM FOR FW HEATER PARAMETERS
C SHELL PRESSURE, DRAIN TEMPERATURE, AND FW IN AND OUT TEMPERATURES
C
COMMON /HX1/PE(12),PMR(5)
COMMON /PAR1/HO(12),HT(12),OAE,HC,HFP,DHP,TI(12),TO(12),TDCA(12),
1HD(12),PLA,PLR,ND(12),NDC(12),IP,NF,NSHAFT
COMMON /PAR2/PSH(12),TSH(12),TO(12),TTD(12),PXHP,PXIP

C
DO250 I=N1,N2
C SHELL PRESSURE
IF(NSHAFT.EQ.1)GOTO230
IF(PE(I).GT.(PXHP+1.0).OR.PE(I).LT.(PXHP-1.0))GOTO220
210 PSH(I)=0.95*PE(I)
GOTO240
220 IF(NSHAFT.EQ.2)GOTO230
IF(PE(I).GT.(PXIP+1.0).OR.PE(I).LT.(PXIP-1.0))GOTO230
GOTO210
230 PSH(I)=0.92*PE(I)
240 TSH(I)=TSAT(PSH(I))
C FW OUTLET
TO(I)=TSH(I)-TTD(I)
IF(I.LE.IP)GOTO241
HO(I)=HL TO(TO(I))
GOTO250
241 HO(I)=HCOM(PLA,TO(I))
250 CONTINUE
DO310 I=N1,N2
C FW INLET
IF(I.EQ.NF)GOTO260
HI(I)=HO(I+1)
IF(ND(I+1).EQ.0)GOTO270
C CORRECT FW INLET FOR PUMPED DRAIN AT I+1
HI(I)=HI(I)+0
GOTO270
C CORRECT FW INLET FOR SJAЕ ENTHALPY RISE AND SPЕ ENTHALPY RISE
260 HT(I)=HO(I)
270 IF(IP.NE.I)GOTO280
C FW PUMP INLET
HFP=HI(I)
C CORRECT FW INLET FOR FW PUMP ENTHALPY RISE
HI(I)=HT(I)+DHP
280 IF(I.LE.IP)GOTO281
TI(I)=TLTOH(HT(I))
GOTO282
281 TI(I)=TCOM(PLA,HT(I))
282 IF(NDC(I).EQ.0)GOTO290
C DRAIN WITH DRAIN COOLER
TO(I)=TI(I)+TDCA(I)
GOTO290
C DRAIN WITHOUT DRAIN COOLER
290 TD(I)=TSH(I)
295 HO(I)=HL TO(TD(I))
310 CONTINUE
RETURN
END

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FWHP 0
FWHP 10
FWHP 20
FWHP 21
FWHP 22
FWHP 30
FWHP 40
FWHP 50
FWHP 51
FWHP 60
FWHP 70
FWHP 80
FWHP 81
FWHP 90
FWHP 100
FWHP 110
FWHP 120
FWHP 130
FWHP 140
FWHP 150
FWHP 160
FWHP 170
FWHP 180
FWHP 190
FWHP 200
FWHP 210
FWHP 220
FWHP 230
FWHP 240
FWHP 250
FWHP 260
FWHP 270
FWHP 280
FWHP 290
FWHP 291
FWHP 300
FWHP 310
FWHP 311
FWHP 320
FWHP 330
FWHP 340
FWHP 350
FWHP 351
FWHP 360
FWHP 370
FWHP 380
FWHP 390
FWHP 400
FWHP 410
FWHP 411
FWHP 420
FWHP 430
FWHP 431
FWHP 440
FWHP 450
FWHP 460
FWHP 470
FWHP 480

```

SUBROUTINE FWPT(PR,HR,PX,DHP,QR,NSHAFT)
IMPLICIT REAL*8(A-H,O-Z)

C SUBPROGRAM FOR CALCULATING THROTTLE STEAM FLOW TO FW PUMP TURBINE
C
COMMON /FPT/CPPT,PBPPT,HBPPT,PXFPT,HXFPT,TFPT
C FIND BOWL ENTROPY
PRPT=PR*0.96

```

FWPT 0
FWPT 10
FWPT 20
FWPT 21
FWPT 30
FWPT 40
FWPT 50
FWPT 51
FWPT 60

```

HRFPT=HR
CALL PROPPH(AMB,SB,VB,TR,MR,PRFPT,HBFPT)
C   FIND TSENTROPTIC EXHAUST ENTHALPY
    PXFPT=PX
    CALL PROPPS(AMXS,HXS,TXS,VXS,MXS,PXFPT,SB)
C   FIND USED ENERGY
    EFF=0.8
    AE=HRFPT-HXS
    UE=AE*EFF
    HXFPT=HRFPT-UE
C   THROTTLE STEAM FLOW TO FW PUMP TURBINE
    IF(INSHAFT.GT.1)GOTO10
    CFPT=DR*DHP/(UE-DHP)
    RETURN
10  CFPT=DR*DHP/UE
    RETURN
    END

```

```

SUBROUTINE GOVERN(AE,BE,W,WVO,CS,AMB,SB,MR,HB,PB,AMXS,TXS,MXS,PX, GOVE 0
1AMX,SX,VX,TX,MX,HX) GOVE 1
IMPLICIT REAL*8(A-H,O-Z) GOVE 10
C
C SUBPROGRAM FOR CALCULATING GOVERNING STAGE SHELL STEAM CONDITIONS GOVE 20
C
COMMON /CONV/HCON,UERCON,AMCON,RHCON,WCON,PCON,SSRCON,XSPCON GOVE 21
C
C CORRECTIONS TO BASE EFFICIENCY GOVE 30
    CWVO=FIG1(WVO,W)
    CL=FIG2(WVO)
    CE1=CWVO*CL*CS*BE GOVE 40
C
C INITIALIZE GOVE 50
    TX=TXS
    HG=HVAP(TX,PX)
    HF=HLTO(TX)
C
C TEST BOWL STEAM GOVE 60
    IF(MR.GT.2)GOTO121
C
C BOWL STEAM IS WET OR SATURATED GOVE 70
C
C ASSUME EXHAUST MOISTURE GOVE 80
    AMX1=AMXS
C
C MOISTURE CORRECTION GOVE 81
    DD125 IT1=1,50
    120 CM=1.0-0.435*(AMB+AMX1)
    UE=AF*CE1*CM
    HX=HB-UE
C
C EXHAUST MOISTURE GOVE 100
    AMX=(HG-HX)/(HG-HF)
C
C CHECK ASSUMED EXHAUST MOISTURE GOVE 110
    DAMX=DARS(AMX1-AMX)
    IF(DAMX.LE.AMCON)GOTO123
C
C RE-SET EXHAUST MOISTURE GOVE 120
    AMX1=AMX
    125 CONTINUE
    PRINT 122,DAMX
122 FORMAT('D-SUBROUTINE GOVERN-EXHAUST MOISTURE IN IT1 DID NOT CONVERGEGOVE 130
    1GE, DAMX =',IP014.6)
    123 MX=1
    SX=(1.0-AMX)*SVAP(TX,PX)+AMX*SLIQ(TX,PX)
    VX=(1.0-AMX)*VVAP(TX,PX)+AMX*VLIQ(TX,PX)
    RETURN
C
C BOWL STEAM IS SUPERHEATED GOVE 140
C
C TEST EXHAUST STEAM GOVE 150
    121 IF(MXS.GT.1)GOTO140
C

```

C BOWL STEAM IS SUPERHEATED AND SHELL STEAM IS WET
 SG=SVAP(TX,PX)
 SF=SLTO(TX)

C ASSUME EXHAUST MOISTURE AND USED ENERGY RATIO
 AMX1=P1,P
 RUE1=0.0

C MOISTURE CORRECTION
 D0151 IT2=1,100
 150 CM=1.0-0.435*AMX1*RUE1
 UE=AE*CE1*CM
 HX=HR-HE

C TEST EXHAUST STEAM
 IF(HX-HG)124,200,201

C FIND INTERSECTION OF EXPANSION LINE AND SATURATION LINE
 C EXHAUST MOISTURE

124 AMX=(HG-HX)/(HG-HF)
 SX=(1.0-AMX)*SG+AMX*SF
 A=(HR-HX)/(SR-SX)
 P1=PR
 P2=PX
 D0131 IT3=1,100
 P=(P1+P2)/2.
 T=TSAT(P)
 HE=HVAP(T,P)
 SE=SVAP(T,P)
 HT=HR+(S-SR)*A
 ADH=DARS(H-H1)
 IF(ADH,LE,HCON)GOTO134
 IF(H>LT,H1)GOTO133
 P2=P
 GOTO131

133 P1=P
 131 CONTINUE
 PRNT 132,ADH

132 FORMAT('C-SUBROUTINE GOVERN-SATURATION LINE ENTHALPY IN IT3 DID NOT CONVERGE, ADH =',1PD14.6)

C USED ENERGY RATIO

134 UEW=H-HX
 RUE=HEW/UE

C CHECK ASSUMED USED ENERGY RATIO
 ADRUE=DARS(TRUE-RUE1)
 IF(ADRUE,GT,UE)CON1GOTO154

C CHECK ASSUMED EXHAUST MOISTURE
 DAMX=DARS(AMX1-AMX)
 IF(DAMX,LE,AMCON)GOTO152

C RE-SET EXHAUST MOISTURE AND USED ENERGY RATIO

154 AMX1=AMX
 RUE1=RUE

151 CONTINUE
 PRNT 160,DAMX,ADRUE

160 FORMAT('C-SUBROUTINE GOVERN-EXHAUST MOISTURE OR USED ENERGY RATIO DID NOT CONVERGE, DAMX =',1PD14.6,'ADRUE =',1PD14.6)

159 ITM IT2 DID NOT CONVERGE, DAMX =*,1PD14.6,5X,*ADRUE =*,1PD14.6)

152 MX=1
 VX=(1.0-AMX1)*VVAP(TX,PX)+AMX*VLTO(TX,PX)
 RETURN

C SHELL STEAM IS DRY

140 UEF=AE*CE1
 HX=HR-UE
 GOTO201

200 MX=2
 GOTO202

201 MX=3
 TY=TVAPH(PX,HX)

202 AMX=0.0
 SX=SVAP(TX,PX)
 VX=VVAP(TX,PX)
 RETURN

C
 END

GOVE 321
 GOVE 330
 GOVE 340
 GOVE 341
 GOVE 350
 GOVE 360
 GOVE 361
 GOVE 370
 GOVE 380
 GOVE 390
 GOVE 400
 GOVE 401
 GOVE 410
 GOVE 411
 GOVE 412
 GOVE 420
 GOVE 430
 GOVE 440
 GOVE 450
 GOVE 460
 GOVE 470
 GOVE 480
 GOVE 490
 GOVE 500
 GOVE 510
 GOVE 520
 GOVE 530
 GOVE 540
 GOVE 550
 GOVE 560
 GOVE 570
 GOVE 580
 GOVE 590
 GOVE 600
 GOVE 610
 GOVE 611
 GOVE 612
 GOVE 620
 GOVE 630
 GOVE 631
 GOVE 640
 GOVE 650
 GOVE 651
 GOVE 660
 GOVE 670
 GOVE 671
 GOVE 680
 GOVE 690
 GOVE 700
 GOVE 710
 GOVE 720
 GOVE 721
 GOVE 730
 GOVE 740
 GOVE 750
 GOVE 760
 GOVE 761
 GOVE 770
 GOVE 780
 GOVE 790
 GOVE 800
 GOVE 810
 GOVE 820
 GOVE 830
 GOVE 840
 GOVE 850
 GOVE 860
 GOVE 870
 GOVE 880
 GOVE 890

```

SUBROUTINE GSTAGE(PXLP)
IMPLICIT REAL*8(A-H,D-Z)

C SUBPROGRAM FOR GOVERNING STAGE CALCULATIONS
C
COMMON /CONV/HCON,UERCON,AMCON,RHCON,MCON,PCON,SSRCON,XSPCON
COMMON /GS/OGS,HBGS,PBGS,AMBGS,SAGS,VBGS,TBGS,PXGS,AMXGS,SXGS,
1VXGS,TXGS,HXGS,PDGS,MBGS,MXGS,NCGS,IRGS,MGS
GSTA 0
GSTA 10
GSTA 20
GSTA 21
GSTA 30
GSTA 40
GSTA 50
GSTA 51
GSTA 60
GSTA 68
GSTA 70
GSTA 80
GSTA 90
GSTA 100
GSTA 110
GSTA 120
GSTA 130
GSTA 140
GSTA 150
GSTA 160
GSTA 170
GSTA 180
GSTA 190
GSTA 200
GSTA 210
GSTA 220
GSTA 230
GSTA 231
GSTA 240
GSTA 250
GSTA 260
GSTA 261
GSTA 270
GSTA 280
GSTA 290
GSTA 300
GSTA 310
GSTA 320
GSTA 330
GSTA 340
GSTA 350
GSTA 360
GSTA 370
GSTA 371
GSTA 380
GSTA 390
GSTA 400
GSTA 410
GSTA 420
GSTA 430
GSTA 440
GSTA 441
GSTA 450
GSTA 460

C GS VWD BOWL CONDITIONS
NCGS=NCGS+1
OGSD=1.05*OGS
TF(NCGS,GT,1)GOTO120
CSGS=FIG6A(IRGS)
PRGSD=PBGS*1.0091453
CALL PROPPH(AMBGS,SBGSD,VBGSD,TBGSD,MBGSD,PRGSD,HBGS)
C GS VWD ISENTROPIC SHELL CONDITIONS
W=IRGS*0.0043633*PDGS
100 WVD=W/WD
110 VWD=W/WD
AEGSD=(VWD/223.71)**2
HXSGSD=HBGS-AEGSD
CALL PROPHS(PXGSD,TXGSD,VXGSD,AXGSD,MXGSD,HXGSD,SRGSD)
C GS VWD SHELL CONDITIONS
120 OVN=OGSD*VBGSD/MGS
RBGS=0.9195-19.750*O/OVN
C CORRECTION FOR BACK-PRESSURE TURBINE
TF(PXLP,LT,3)GOTO121
BEGS=RBGS*0.99
121 CALL GOVERN(AEGSD,BEGS,W,WVD,CSGS,AMBGS,SBGSD,MBGSD,HBGS,PRGSD,
1AXGSD,TXGSD,MXGSD,PXGSD,AMXGSD,SXGSD,VXGSD,TXGSD,MXGSD,HXGSD)
C GS BOWL CONDITIONS
CALL PROPPH(AMBGS,SAGS,VBGS,TBGS,MBGS,PBGS,HBGS)
C GS ISENTROPIC SHELL CONDITIONS
PXGS=PXGSD*0.95238
D131 LT=1,500
130 CALL PROPHS(AMXGS,HXGS,TXGS,VXGS,MXGS,PXGS,SRGS)
C GS SHELL CONDITIONS
AEGS=HBGS-HXGS
V0=223.7*DSORT(AEGS)
WVG=W/V0
CALL GOVERN(AEGS,BEGS,W,WVD,CSGS,AMBGS,SBGS,MBGS,HBGS,PBGS,AMXGS,
1TXGS,MXGS,PXGS,AMXGS,SXGS,VXGS,TXGS,MXGS,HXGS)
P=0.90703*PXGSD*VXGS/VXGSD
ADP=DARS((P-PXGS)/PXGS)
TF(ADP,LT,PCON)GOTO140
PXGS=P
131 CONTINUE
PRINT 132,ADP
132 FORMAT('0-SUBROUTINE GSTAGE-GOVERNING STAGE EXHAUST PRESSURE DID NOT CONVERGE, ADP =',1PD14.6)
140 RETURN
END

```

```

SUBROUTINE HXTRAC(MR,I1,I2,MRLP,HRLP,SRLP,MXLP,HXLP,SXLP,PTL,HTL,
1STL,PX,UEEP)
IMPLICIT REAL*8(A-H,D-Z)
C SUBPROGRAM FOR FW HEATER EXTRACTION STEAM ENTHALPY
C
COMMON /HX1/PE(12),PMR(5)
COMMON /HX2/PE(12),HE1(12),HAMR(5),HBMR(5),SAMR(5),SBMR(5),PCWD(5)
HXTR 0
HXTR 1
HXTR 10
HXTR 20
HXTR 21
HXTR 30
HXTR 40
HXTR 50
HXTR 60
HXTR 61
HXTR 70
HXTR 80
C TEST FOR PRESENCE OF MOISTURE REMOVAL STAGES
TF(MR,GT,0)GOTO4100
C

```

C NO MOISTURE REMOVAL STAGES PRESENT	HXTR 90
D04060 I=I1,I2	HXTR 100
IF(PE(I).GT.(PX+1.C))GOTO3990	HXTR 110
HE(I)=UEEP	HXTR 120
GOTO4050	HXTR 130
3990 IF(MRLP.EQ.3)GOTO4000	HXTR 140
CALL FTG12B(PE(I),HRLP,SRLP,HXLP,SXLP,HE(I),SE)	HXTR 150
GOTO4050	HXTR 160
4000 IF(MXLP.EQ.1)GOTO4010	HXTR 170
CALL FTG12A(PE(I),HRLP,SRLP,HXLP,SXLP,HE(I),SE)	HXTR 180
GOTO4050	HXTR 190
4010 IF(PE(I).LT.PIL)GOTO4040	HXTR 200
CALL FTG12A(PE(I),HRLP,SRLP,HIL,SIL,HE(I),SE)	HXTR 210
GOTO4050	HXTR 220
4040 CALL FTG12B(PE(I),HIL,SIL,HXLP,SXLP,HE(I),SE)	HXTR 230
4050 HE1(I)=HE(I)	HXTR 240
4060 CONTINUE	HXTR 250
RETURN	HXTR 260
C	HXTR 270
C MOISTURE REMOVAL STAGES PRESENT	HXTR 270
4100 D04200 I=I1,I2	HXTR 280
IF(PE(I).GT.(PX+1.C))GOTO4110	HXTR 290
HE(I)=UEEP	HXTR 300
GOTO4195	HXTR 310
4110 D04190 J=1,MR	HXTR 320
IF(PE(I).GT.(PMR(J)+1.C).OR. PE(I).LT.(PMR(J)-1.0))GOTO4120	HXTR 330
HE(I)=HAMR(J)	HXTR 340
HE1(I)=HRMR(J)	HXTR 350
GOTO4200	HXTR 360
4120 IF(PE(I).GT.PMR(J))GOTO4130	HXTR 370
IF(J.LT.MR)GOTO4190	HXTR 380
HR=HAMR(J)	HXTR 390
SR=SAMR(J)	HXTR 400
HX=HXLP	HXTR 410
SX=SXLP	HXTR 420
GOTO4180	HXTR 430
4130 IF(J.EQ.1)GOTO4140	HXTR 440
HR=HAMR(J-1)	HXTR 450
SR=SAMR(J-1)	HXTR 460
GOTO4170	HXTR 470
4140 IF(MRLP.EQ.3)GOTO4150	HXTR 480
HR=HRLP	HXTR 490
SR=SRLP	HXTR 500
GOTO4170	HXTR 510
4150 IF(PE(I).GT.PIL)GOTO4160	HXTR 520
HR=HIL	HXTR 530
SR=SIL	HXTR 540
GOTO4170	HXTR 550
4160 CALL FTG12A(PE(I),HRLP,SRLP,HIL,SIL,HE(I),SE)	HXTR 560
GOTO4195	HXTR 570
4170 HX=HRMR(J)	HXTR 580
SX=SRMR(J)	HXTR 590
4180 CALL FTG12B(PE(I),HR,SR,HX,SX,HE(I),SE)	HXTR 600
GOTO4195	HXTR 610
4190 CONTINUE	HXTR 620
4195 HE1(I)=HE(I)	HXTR 630
4200 CONTINUE	HXTR 640
RETURN	HXTR 650
END	HXTR 660

```

SUBROUTINE INDEX(I1,I2,NFLP,MR)
IMPLICIT REAL*8(A-H,D-Z)

C SUBPROGRAM FOR CALCULATING INDICES FOR LP TURBINE
C
COMMON /HX1/PE(12),PMR(5)
COMMON /IN/L1(13),L2(13),J1(13),IMR(5)

C
IMR(1)=0
IMR(2)=0
IMR(3)=0
IMR(4)=0
IMR(5)=0
JJ1=0
LL1=0
LL2=0
IF(NFLP.EQ.0)GOTO2750
NN=I2-1
D02740 I=I1,NN
LL1=LL2+1
IF(LL1.GT.MR)GOTO2730
D02710 L=LL1,MR
IF(PMR(L).LT.(PE(I)-1).EQ.0)GOTO2730
IMR(L)=1
LL2=L
IF(PMR(L).LT.(PE(I)+1).EQ.0).AND.(PMR(L).GT.(PE(I)-1).EQ.0))GOTO2720
2710 CONTINUE
GOTO2730
2720 JJ1=JJ1+1
2730 J1(I)=JJ1
L1(I)=LL1
L2(I)=LL2
2740 CONTINUE
2750 J1(I2)=JJ1
L1(I2)=LL2+1
L2(I2)=MR
C
C J1(I)=TOTAL NO. OF FW HEATER EXTRACTION AND MOISTURE REMOVAL
C EXTRACTION POINTS THAT COINCIDE, TO AND INCLUDING FW HEATER
C EXTRACTION POINT 'I'
C L1(I)=FIRST MOISTURE REMOVAL EXTRACTION POINT THAT FEEDS FW HTR 'I'
C L2(I)=LAST MOISTURE REMOVAL EXTRACTION POINT THAT FEEDS FW HEATER 'I'
C
C IF L1(I)=1 AND L2(I)=0, THEN NO MOISTURE REMOVAL EXTRACTION POINTS
C FEED TO FW HEATER 'I'
C
      RETURN
      END

      INDEX          INDE
      0              0
      10             10
      20             20
      21             21
      30             30
      40             40
      50             50
      60             60
      70             70
      80             80
      90             90
      100            100
      110            110
      120            120
      130            130
      140            140
      150            150
      160            160
      170            170
      180            180
      190            190
      200            200
      210            210
      220            220
      230            230
      240            240
      250            250
      260            260
      270            270
      280            280
      290            290
      300            300
      310            310
      320            320
      330            330
      340            340
      350            350
      351            351
      352            352
      353            353
      354            354
      360            360
      361            361
      370            370
      380            380
      381            381
      390            390
      400            400
      410            410

```

```

SUBROUTINE PRDROP(PXHP,PRLP,MS,NRH)
IMPLICIT REAL*8(A-H,D-Z)

C SUBPROGRAM FOR INTERMEDIATE SYSTEM PRESSURE DROP
C (TABLE III, P. 138, GER-2454A)
C
COMMON /RH1/PXRH2,PIRH2,PXRH1,PIRH1,PFPT
COMMON /XS1/PSX,PSI
C
DATA A/1.03093D0/,B/1.03413D0/
DATA A2/1.00705D0/,B2/1.01010D0/,E2/1.02041D0/
DATA A3/1.00705D0/,B3/1.01112D0/,E3/1.01833D0/,E3/1.01112D0/
DATA A4/1.00705D0/,B4/1.01112D0/,C4/1.01317D0/,D4/1.01523D0/,E4/1.01112D0/
C
      IF(MS.GT.0)GOTO30
C
      PRDR          0
      PRDR          10
      PRDR          20
      PRDR          21
      PRDR          22
      PRDR          30
      PRDR          40
      PRDR          50
      PRDR          60
      PRDR          70
      PRDR          71
      PRDR          72
      PRDR          73
      PRDR          74
      PRDR          80
      PRDR          90
      PRDR         100

```

```

C NO MOISTURE SEPARATOR
IF(NRH<NE,0)GOTO10
C NO MOISTURE SEPARATOR, NO REHEATER
PXHP=PPLP*A
PEPT=PXHP
RETURN
10 PTV=PPLP*B
IF(NRH>GT,11)GOTO20
C NO MOISTURE SEPARATOR, 1-STAGE REHEATER
PXRH1=PIV*A3
PEPT=PXRH1
PTRH1=PXRH1*C3
PXHP=PTRH1*A3
RETIJRN
C NO MOISTURE SEPARATOR, 2-STAGE REHEATER
20 PXRH2=PIV*A4
PEPT=PXRH2
PTRH2=PXRH2*D4
PXRH1=PIRH2
PTRH1=PXRH1*C4
PYHP=PIRH1*A4
RETIJRN
C
C MOISTURE SEPARATOR
30 PTV=PPLP*B
IF(NRH<NE,0)GOTO40
C MOISTURE SEPARATOR, NO REHEATER
PSX=PTV*A2
PEPT=PSX
PST=PSX*B2
PXHP=PSI*A2
RETIJRN
40 IF(NRH>GT,11)GOTO50
C MOISTURE SEPARATOR, 1-STAGE REHEATER
PXRH1=PIV*A3
PEPT=PXRH1
PTRH1=PXRH1*C3
PSX=PTRH1
PST=PSX*B3
PYHP=PST*A3
RETIJRN
C MOISTURE SEPARATOR, 2-STAGE REHEATER
50 PXRH2=PIV*A4
PEPT=PXRH2
PTRH2=PXRH2*D4
PXRH1=PTRH2
PTRH1=PXRH1*C4
PSX=PTRH1
PST=PSX*B4
PYHP=PST*A4
RETIJRN
END

```

SUBROUTINE REHEAT(HE,PE,HT,PT)
IMPLICIT REAL*8(A-H,O-Z)

```

C SUBPROGRAM FOR REHEATER PARAMETERS
C
COMMON /RH1/PXRH2,PTRH2,PXRH1,PTRH1,PEPT
COMMON /RH2/QRH1,HCRH1,QRH2,HCRH2,NRH
COMMON /RH3/TTDRH1,TTDRH2,HRH1,HRH2,PCRH1,TCRH1,PCRH2,TCRH2,TXRH1,
1HXRH1,TXRH2,HXRH2,HTRH2,HTRH1,NRH
C 1ST STAGE
IF(NRH<E0,1)GOTO110
HRH1=HE
PCRH1=PE*0.9555
GOTO120

```

REHE	0
REPE	10
REHE	20
REHE	21
REHE	30
REHE	40
REHE	50
REHE	60
REHE	61
REHE	70
REHE	71
REHE	80
REHE	90
REHE	100
REHE	110

```

110 HRRH1=HT
  PCRH1=PT*0.985
120 TCRH1=TSAT(PCRH1)
  HCRH1=HL10(TCRH1)
  TXRH1=TCRH1-TTDRH1
  T1=TSAT(PXRH1)
  IF(TXRH1.GE.T1)GOTO122
  TXRH1=T1
  TTDRH1=TXRH1-TCRH1
  PRINT 121,TTDRH1
121 FORMAT('0',T10,'THERE IS A DATA ERROR IN SUBROUTINE REHEAT.')
1T10,'REHEATER TERMINAL TEMPERATURE DIFFERENCE HAS BEEN CHANGED TO'
2,F10e21
122 HXRH1=HVAP(TXRH1,PXRH1)
  IF(NRH.EQ.1)GOTO130
C 2ND STAGE
  HRRH2=HT
  PCRH2=PT*0.985
  TCRH2=TSAT(PCRH2)
  HCRH2=HL10(TCRH2)
  TXRH2=TCRH2-TTDRH2
  T2=TSAT(PXRH2)
  IF(TXRH2.GE.T2)GOTO124
  TXRH2=T2
  TTDRH2=TXRH2-TCRH2
  PRINT 121,TTDRH2
124 HXRH2=HVAP(TXRH2,PXRH2)
  HTPH2=HXRH1
130 RETURN
  END

```

```

SUBROUTINE SGROUP(PB,TB,HR,SR,VF,AMB,MB,QR,NE,CS,PX,TX,HX,SX,VX,
1AMX,MX,PXI,TXI,HXI,SXI,VXI,AMXT,MXT,PXLPI)
1IMPLICIT REAL*8(A-H,D-Z)
C
C SUBPROGRAM FOR STAGE GROUP STEAM CONDITIONS
C
C COMMON /CONV/HCON,UERCON,AMCON,RHCON,WCON,PCON,SSRCON,XSPCON
C
C INITIALIZE
  TX=TSAT(PX)
  SG=SVAP(TX,PX)
  SF=SL10(TX)
  HG=HVAP(TX,PX)
  HF=HL10(TX)
C  CORRECTION FOR BACK-PRESSURE TURBTNE
  IF(PXLPI.LT.3.0)GOTO10
  CT=0.99
  GOTO100
10 CT=1.0
C  TEST BOWL STEAM
100 IF(MB.GT.2)GOTO200
C
C  BOWL STEAM IS WET, OR DRY AND SATURATED
C  SHELL STEAM IS WET
  AMXS=(SG-SR)/(SG-SF)
  HYS=(1.0-AMXS)*HG+AMXS*HF
  PR=PB/PX
  VF=(2.0D+6)*VVAP(TB,PB)
  QVN=QR*VB/NE
  BE=FIG4(PR,PB,VF)
  CIVF=FIG5(QVN,PR,VF,PB)
  CM=1.0-AMB*FIG7(PR,PB)
  HE=HB-HXS
  UE=AF*BE*CIVF*CS*CM*CT
  HX=HB-UE
  GOTO510
C

```

```

C BOWL STEAM IS SUPERHEATED SGRO 291
C TEST SHELL STEAM SGRO 292
260 IF(SG>GT,SR)GOTO300 SGRO 300
C SHELL STEAM IS SUPERHEATED SGRO 301
  TXS=TVAPS(PX,SB) SGRO 310
  HXS=HVAP(TXS,PX) SGRO 320
  PR=PR/PX SGRO 330
  QVN=QR*VR/NE SGRO 340
  RE=FIG3(QVN,PR) SGRO 350
  AE=HR-HXS SGRO 360
  UE=AE*RE*CS*CT SGRO 370
  HX=HR-UE SGRO 380
  GOTO530 SGRO 390
SGRO 400
C BOWL STEAM IS SUPERHEATED SGRO 401
C SHELL STEAM IS WET SGRO 402
C FIND UE FROM BOWL TO SATURATION LINE SGRO 403
300 P1=PR SGRO 410
  P2=PX SGRO 420
  D0320 IT=1,100 SGRO 430
  PXI=(P1+P2)/2. SGRO 440
  PR=PR/PXI SGRO 450
  QVN=QR*VR/NE SGRO 452
  RE=FIG3(QVN,PR) SGRO 470
  TXSI=TVAPS(PXI,SB) SGRO 480
  HXSI=HVAP(TXSI,PXI) SGRO 490
  AET=HR-HXSI SGRO 500
  UET=AET*RE*CS*CT SGRO 510
  HXT=HR-UET SGRO 520
  TXI=TSAT(PXI) SGRO 530
  HG1=HVAP(TXI,PXI) SGRO 540
SGRO 541
C TEST HXI SGRO 550
  ADH=DABS(HG1-HXT) SGRO 560
  TF(ADH,LE,HCON)GOTO370 SGRO 561
C RE-SET P1 OR P2 SGRO 570
  IF(HG1<LT,HXI)GOTO310 SGRO 570
  P2=PXT SGRO 580
  GOTO320 SGRO 590
310 P1=PXI SGRO 600
320 CONTINUE SGRO 610
  PRINT 321,ADH SGRO 620
321 FORMAT('D-SUBROUTINE SGROUP-SATURATION LINE ENTHALPY DID NOT CONVERGEGRO 630
  IRCE, ADH = ',1PD14.6) SGRO 631
270 IF(PX<LT,(PXT-0.1))GOTO380 SGRO 640
  UE=UET SGRO 650
  HX=HXT SGRO 660
  TF(HX,GT,HG)GOTO530 SGRO 670
  GOTO520 SGRO 680
SGRO 681
C FIND STEAM CONDITIONS AT SATURATION LINE SGRO 690
380 MXT=2 SGRO 700
  AMXT=0.0 SGRO 710
  SXI=SVAP(TXT,PXI) SGRO 720
  VXT=VVAP(TXT,PXI) SGRO 721
SGRO 730
C FIND UE FROM SATURATION LINE TO SHELL SGRO 740
  PR=PXI/PX SGRO 750
  VF=(3.0D+6)*VXT SGRO 760
  QVN=QR*VXT/NE SGRO 770
  RE=FIG4(PR,PXI,VF) SGRO 780
  CIVF=FIG5(QVN,PR,VE,PXI) SGRO 790
  AMXS=(SG-SXI)/(SG-SF) SGRO 800
  HXS=(1.0-AMXS)*HG+AMXS*HF SGRO 810
  AFIX=HXT-HXS SGRO 820
  UFIX=AEIX*RE*CIVF*CS*CT SGRO 830
  HX=HXI-UFIX SGRO 840
  UE=HR-HX SGRO 841
SGRO 842
C FIND SHELL STEAM CONDITIONS SGRO 842
C WET SGRO 850
510 MX=1 SGRO 860
  AMX=(HG-HX)/(HG-HF) SGRO 870
  SX=(1.0-AMX)*SG+AMX*SF

```

```

VX=(1.0-AMX)*VVAP(TX,PX)+AMX*VLTO(TX)           SGRO 880
RETURN                                              SGRO 890
C DRY AND SATURATED                               SGRO 891
520 MX=2                                         SGRO 900
AMX=0.0                                         SGRO 910
SX=50                                           SGRO 920
VX=VVAP(TX,PX)                                    SGRO 930
RETURN                                              SGRO 940
C SUPERHEATED                                     SGRO 941
530 MX=3                                         SGRO 950
AMX=0.0                                         SGRO 960
TX=TVAPH(PX,HX)                                   SGRO 970
SX=SVAP(TX,PX)                                    SGRO 980
VX=VVAP(TX,PX)                                    SGRO 990
RETURN                                              SGRO1000
C                                                 SGRO1010
END                                                SGRO1020

```

```

SUBROUTINE SLEAK1(NF,PSH,DT,PT,HT,LK1,QLK1,HLK1,QLK2,HLK2,NEGS)
IMPLICIT DT REAL*8(A-H,D-Z)
C
C SUBPROGRAM FOR VALVE STEM PACKING LEAKAGES
C TABLE IT, P. 12, GER-2454A
C
DIMENSION PSH(12)
C
100 LK1=0
QLK12=0.00105*DT
IF(PT.GE.300.0)GOTO110
QLK1=0.
HLK1=0.
QLK2=QLK12
HLK2=HT
RETURN
110 TF(NF,EQ,NEGS)GOTO130
T=NEGS+1
00120 TL=I,NF
IF(PSH(TL).GT.0.0)GOTO120
LK1=TL
PLK1=PSH(TL)
GOTO140
120 CONTINUE
130 PLK1=200.
140 QLK2=QLK12*PLK1/PT
QLK1=QLK12-QLK2
HLK1=HT
HLK2=HT
RETURN
END

```

SLEA	0
SLEA	10
SLEA	20
SLEA	21
SLEA	22
SLEA	30
SLEA	40
SLEA	50
SLEA	60
SLEA	70
SLEA	80
SLEA	90
SLEA	100
SLEA	110
SLEA	120
SLEA	130
SLEA	140
SLEA	150
SLEA	160
SLEA	170
SLEA	180
SLEA	190
SLEA	200
SLEA	210
SLEA	220
SLEA	230
SLEA	240
SLEA	250
SLEA	260
SLEA	270
SLEA	280

```

SUBROUTINE SLEAK2(NF,PSH,NGS,TRGS,PXGS,VXGS,HXGS,LK3,QLK3,HLK3,
1QLK4,HLK4,PSSR,NEGS)
IMPLICIT DT REAL*8(A-H,D-Z)
C
C SUBPROGRAM FOR TURBINE SHAFT PACKING LEAKAGES (BOWL END)
C TABLE IT, P. 12, GER-2454A
C
DIMENSION PSH(12)
C
200 LK3=0
IF(PXGS.GT.PSSR)GOTO211
210 QLK3=0.
QLK4=0.
HLK3=0.
HLK4=0.
RETURN

```

SLEA	0
SLEA	1
SLEA	10
SLEA	20
SLEA	21
SLEA	22
SLEA	30
SLEA	40
SLEA	50
SLEA	60
SLEA	70
SLEA	80
SLEA	90
SLEA	100
SLEA	110
SLEA	120

```

211 GOTD(220,210,220,210,220,210,220,210,220,210,220,210,220,210,220, SLEA 130
1210),NGS SLEA 131
220 IF(IRGSe.E0,1800)GOTD230 SLEA 140
C34=600.
C4=900.
GOTD240 SLEA 150
230 C34=800.
C4=1200.
SLEA 160
240 IF(PXGS.GE.150.0)GOTD250 SLEA 170
QLK3=0.
HLK3=0.
CLK4=C4*DSQRT(PXGS/VXGS)
HLK4=HXGS
RETURN SLEA 180
250 IF(NF.E0,NFGS)GOTD270 SLEA 190
I=NFGS+1 SLEA 200
00260 IL=I,NF SLEA 210
IF(PSH(IL).GT.150.0)GOTD260 SLEA 220
LK3=IL
PLK3=PSH(IL)
GOTD280 SLEA 230
260 CONTINUE SLEA 240
270 PLK3=100.
SLEA 250
280 HLK3=HXGS SLEA 260
CALL PROPHCAM,S,VLK3,T,M,PLK3,HLK3) SLEA 270
QLK34=C34*DSQRT(PXGS/VXGS)
CLK4=C4*DSQRT(PLK3/HLK3)
QLK3=QLK34-QLK4 SLEA 280
HLK4=HXGS
RETURN SLEA 290
END SLEA 300
SLEA 310
SLEA 320
SLEA 330
SLEA 340
SLEA 350
SLEA 360
SLEA 370
SLEA 380
SLEA 390
SLEA 400
SLEA 410
SLEA 420

```

```

SUBROUTINE SLEAK?(NF,PSH,NHP,IRHP,PXHP,VXHP,HXHP,LK5,QLK5,HLK5,
1QLK6,HLK6,PSSR)
      TMPLICITY REAL*8(A-H,D-Z)
C
C SUBPROGRAM FOR TURBINE SHAFT LEAKAGES (EXHAUST END)
C TABLE II, Pg. 12, GEP-2454A
C
C      ETMENSION PSH(12)
C
300 LK5=0
      IF(PXHP.GT.PSSR)GOTD305 SLEA 1
QLK5=0.
SLEA 2
QLK6=0.
SLEA 3
HLK5=0.
SLEA 4
HLK6=0.
SLEA 5
RETURN SLEA 6
305 GOTD(310,320,310,320,310,320,310,320,310,320,310,320,310,320,310, SLEA 7
1320),NHP SLEA 8
310 NE1=1 SLEA 9
NE2=NHP-1 SLEA 10
GOTD330 SLEA 11
320 NE1=0 SLEA 12
NE2=NHP SLEA 13
330 IF(IRHP.E0,1800)GOTD340 SLEA 14
C56=NE1*400.0+NE2*550.0 SLEA 15
C6=NE1*600.0+NE2*750.0 SLEA 16
GOTD360 SLEA 17
340 C56=NE1*500.0+NE2*750.0 SLEA 18
C6=NE1*700.0+NE2*1000.0 SLEA 19
350 IF(PXHP.GE.150.0)GOTD360 SLEA 20
QLK5=0.
SLEA 21
HLK5=0.
SLEA 22
QLK4=C6*DSQRT(PXHP/VXHP)
SLEA 23
HLK6=HXHP
SLEA 24
RETURN SLEA 25
SLEA 26
SLEA 27
SLEA 28
SLEA 29
SLEA 30

```

360	TF(NF,FO,0)GOTO380	SLEA 310
	DO370 IL=1,NF	SLEA 320
	IF(PSH(IL).GT.150.0)GOTO370	SLEA 330
	LK5=IL	SLEA 340
	PLK5=PSH(IL)	SLEA 350
	GOTO390	SLEA 360
370	CONTINUE	SLEA 370
380	PLK5=100.	SLEA 380
390	HLK5=HXHP	SLEA 390
	CALL PROPPH(AM,S,VLK5,T,M,PLK5,HLK5)	SLEA 400
	QLK56=C56*DSORT(PXHP/VXHP)	SLEA 410
	QLK6=C6*DSORT(PLK5/VLK5)	SLEA 420
	QLK5=QLK56-QLK6	SLEA 430
	HLK6=HXHP	SLEA 440
	RETURN	SLEA 450
	END	SLEA 460

	SUBROUTINE SSRE(PSH,HT,PXLP,NSHAFT,NF)	SSRE 0
	IMPLICIT REAL*8(A-H,D-Z)	SSRE 10
C	C SUBPROGRAM FOR STEAM SEAL REGULATOR ENTHALPY	SSRE 20
C	DIMENSION PSH(12)	SSRE 30
C	COMMON /LEAK/QLK1,HLK1,QLK2,HLK2,QLK3,HLK3,QLK4,HLK4,QLK5,HLK5,	SSRE 40
	1QLK6,HLK6,QLK7,HLK7,QLK8,HLK8,QLK9,HLK9,QLK10,HLK10,LK,LK1,LK2,	SSRE 50
	2LK5,LK7,LK9	SSRE 60
	COMMON /SSR/CSPE,QMC,QSSR,HSSR,PSSR,QFWH,QSSRMU,HSSRMU	SSRE 61
C	QSSR=QLK2+QLK4	SSRE 62
	HSUM=QLK2*HLK2+QLK4*HLK4	SSRE 70
	IF(NSHAFT.EQ.1)GOTO100	SSRE 80
	QSSR=QSSR+QLK6	SSRE 90
	HSUM=HSUM+QLK6*HLK6	SSRE 100
	IF(NSHAFT.EQ.2)GOTO100	SSRE 110
	QSSR=QSSR+QLK8+QLK10	SSRE 120
	HSUM=HSUM+QLK8*HLK8+QLK10*HLK10	SSRE 130
100	HSUM=HSUM/QSSR	SSRE 140
	Q=QMC+OSPE	SSRE 150
	IF(QSSR.GT.0)GOTO110	SSRE 160
	QFWH=0.	SSRE 170
	QSSRMU=0-QSSR	SSRE 180
	QSSR=Q	SSRE 190
	HSSRMU=HT	SSRE 200
	HSUM=HSUM+QSSRMU*HSSRMU	SSRE 210
	HSSR=HSUM/QSSR	SSRE 220
	GOTO100	SSRE 230
110	QSSRMU=0.	SSRE 240
	HSSRMU=0.	SSRE 250
	IF(NF.GT.0)GOTO130	SSRE 260
120	QFWH=0.	SSRE 270
	QMC=QSSR-OSPE	SSRE 280
	GOTO140	SSRE 290
130	IF(PSSR.LE.PSH(NF))GOTO120	SSRE 300
	QFWH=QSSR-Q	SSRE 310
140	IF(PXLP.LE.14.696)GOTO150	SSRE 320
	QMC=QSSR	SSRE 330
	QFWH=0.	SSRE 340
	OSPE=0.	SSRE 350
150	RETURN	SSRE 360
	END	SSRE 370
		SSRE 380
		SSRE 390
		SSRE 400

```

SUBROUTINE XLOSS(PA,TX,HEP,HX,QA,AMEP,AMX,NE,BL,PD,IRL,UEEP,XL2)
IMPLICIT REAL*8(A-H,O-Z)

C SUBPROGRAM FOR LP CONDENSING TURBINE UEEP
C APPENDIX III (P. 59, GER-2454A)

C
PX=PA*2.936
AAN=0.021817*PD*BL
VP=VVAP(TX,PA)
VAN=QA*VP*(1.0-AMX)/(3600.0*AAN*NE)
IF(VAN.GT.1400.0)GOTO10
XL=FIG167(VAN,BL,TRL)
AMF2=FIG14(AMX*100.)
XL2=XL*AMF2
UEEP=HX+XL2
RETURN
10 PD=PX*VAN*0.000768049
AMF1=FIG14(AMEP*100.)
DO21 IT=1,50
21 DEP=FIG15(PD)
HDP=HEP+DEP*AMF1
P=PD*0.49116
TPP=TSAT(P)
VPP=VVAP(TPP,P)
HCPP=HVAP(TPP,P)
AMPP=(HCPP-HPP)/(HCPP-HL10(TPP))
VPAN=QA*VPP*(1.0-AMPP)/(3600.0*AAN*NE)
IF(VPAN.LE.1400.0)GOTO30
PD=PD*VPAN/1302.0
CONTINUE
PRINT 22,VPAN
22 FORMAT(*0-SUBROUTINE XLOSS-VPAN DID NOT CONVERGE, VPAN =*,1PD14.6)XL0S 290
XL=FIG167(VPAN,BL,TRL)
AMFP=FIG14(AMPP*100.0)
XL2=XL*AMFP
UEEP=HPP+XL2
RETURN
END

```

```

SUBROUTINE XSEP
IMPLICIT REAL*8(A-H,O-Z)

C COMMON /XS1/PSX,PSI
C COMMON /XS2/HFSX,OMR
C COMMON /XS3/QSI,HST,TSX,OSX,HSX,AMSX,EMS,MS

C SUBPROGRAM FOR EXTERNAL MOISTURE SEPARATOR CALCULATIONS
C
C STEAM CONDITIONS AT MOISTURE SEPARATOR OUTLET BEFORE SEPARATION
    HSX=HST
    TSX=TSAT(PSX)
    HFSX=HL10(TSX)
    HGSX=HVAP(TSX,PSX)
    AMSXB=(HGSX-HSX)/(HGSX-HFSX)
C MOTSTURE REMOVAL
    FMR=EMS*AMSXB*0.01
    QMR=FMR*QSI
    OSX=QSI-QMR
C STEAM CONDITIONS AT MOISTURE SEPARATOR OUTLET AFTER SEPARATION
    AMSX=(AMSXB-FMR)/(1.0-FMR)
    HSX=(HSXB-FMR*HFSX)/(1.0-FMR)
    RETURN
END

```

```

FUNCTION FIG1(WV0,W)
IMPLICIT REAL*8(A-H,K-Z)
C WV0 IS W/V0
C CHECK TO SEE IF DATA IS WITHIN SPECIFIED LIMITS
C IF(WV0<-0.113,12,12
C IF DATA IS OUTSIDE LIMITS PRINT MESSAGE AND
C CONTINUE EXECUTION
3 PRINT 13,WV0
12 IF(WV0<-0.511,1,4
4 PRINT 13,WV0
1 TPIW-250,015,6,6
5 PRINT 14,W
6 IF(W-800>012,2,7
7 PRINT 14,W
C CALCULATE FIG1 AND RETURN
2 FIG1=4.*((WV0-WV0*WV0)*(1e-0.00391*(0.5-WV0)*(0.5-WV0)
1 *(W-250,011)
RETURN
13 FORMAT(7H0WV0 = ,D23.16,5X,23HIS A DATA ERROR IN FIG1)
14 FORMAT(5H0W = ,D23.16,5X,23HIS A DATA ERROR IN FIG1)
END

```

F1	100
F1	105
F1	110
F1	115
F1	120
F1	125
F1	130
F1	135
F1	140
F1	145
F1	150
F1	155
F1	160
F1	165
F1	170
F1	175
F1	176
F1	180
F1	185
F1	190
F1	195

```

FUNCTION FIG2(WV0)
IMPLICIT REAL*8(A-H,K-Z)
DIMENSION A(6)
C THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS
DATA A/-0.144664D1,0.264778D2,-0.129062D3,0.330252D3,-0.429721D3,
1 -0.224804D3/,1/5/
C TEST FOR WV0 .GE.0.e1 .AND. .LE.0.5
IF (WV0>0.1) 15,10,10
10 IF (WV0>0.5) 20,20,15
C PRINTED FLAG FOR WV0 NOT WITHIN SPECIFIED LIMITS
15 PRINT 16,WV0
16 FORMAT(6H0WV0 =,D25.16,2X,36HTS OUTSIDE SPECIFIED LIMITS FOR FIG2)F2
20 CALL UNIPOL(A,WV0,Z,T)
FIG2 = Z
RETURN
END

```

F2	100
F2	105
F2	110
F2	115
F2	120
F2	121
F2	125
F2	130
F2	135
F2	140
F2	145
F2	150
F2	155
F2	160
F2	165
F2	170

```

FUNCTION FIG3(OVN,PRI)
IMPLICIT REAL*8(A-H,K-Z)
DIMENSION AALPHA(3),ATHETA(3)
C THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS
DATA AALPHA/-0.17387620D1,-0.24241363D0,0.95370576D-2/,ATHETA/
1 -0.23694637D1,-0.99561861D-1,-0.29889354D-2/,1/2/
C TEST FOR OVN .GE. 0.2D6 .AND..LE. 100.06
IF (OVN>0.2D6) 15,10,10
10 IF (OVN>100.06) 20,20,15
C PRINTED FLAG FOR OVN NOT WITHIN SPECIFIED LIMITS
15 PRINT 16,OVN
16 FORMAT(6H0OVN =,D25.16,2X,36HTS OUTSIDE SPECIFIED LIMITS FOR FIG3)F3
C TEST FOR PR .GE. 1.0 .AND..LT. 500.0
20 IF (PR>1.0) 30,25,25
25 IF (PR>500.0) 35,30,30
C PRINTED FLAG FOR PR NOT WITHIN SPECIFIED LIMITS
30 PRINT 31,PR
31 FORMAT(5H0PR =,D25.16,38H IS OUTSIDE SPECIFIED LIMITS FOR FIG3) F3
35 X = DLOG(PRI)
CALL UNIPOL(AALPHA,X,ZALPHA,T)
ALPHA = DEXP(ZALPHA)
CALL UNIPOL(ATHETA,X,ZTHETA,T)
THETA = DEXP(ZTHETA)
FIG3 = 1.0-(ALPHA+((THETA-ALPHA1/OVN)*((OVN-250000,1/0.9751))
RETURN
END

```

F3	100
F3	105
F3	110
F3	115
F3	120
F3	121
F3	125
F3	130
F3	135
F3	140
F3	145
F3	150
F3	155
F3	160
F3	165
F3	170
F3	175
F3	180
F3	185
F3	190
F3	195
F3	200
F3	205
F3	210
F3	215
F3	220

```

FUNCTION FIG4(PR,PB,VE)
IMPLTCIT REAL*8(A-H,K-7)
C PR IS PR/PX
DIMENSTON A(6,7)
DATA A//,.90265965D0,-D.16830190D-1,D.22481349D-2,
1-D.21178836D-3,D.91380561D-5,D.0D0,
2-D.52519228D-4,D.10910256D-4,-D.20090378D-4,
3,D.49191537D-5,-D.35197958D-6,D.0D0,
4,D.27863077D-6,-D.38164297D-6,D.25227588D-6,
5-D.54516150D-7,D.38424326D-8,D.0D0,
6-D.68155332D-9,D.10184591D-8,-D.63504086D-9,
7,D.13690704D-9,-D.97149103D-11,D.0D0,
8,D.69937432D-12,-D.10905089D-11,D.66534494D-12,
9-D.14337663D-12,D.10204672D-13,D.0D0,
A-D.32231499D-15,D.51336378D-15,-D.30982329D-15,
B,D.66775818D-16,-D.47614950D-17,D.0D0,
C,D.54818623D-19,-D.88601007D-19,D.53145257D-19,
D-D.11459126D-19,C.81819448D-21,D.0D0/
ALD=DLNG(2,1DC)
APL=DLNG(PR)
C CALCULATE NU1
NU1=1,D-1D.17573783-D.08227699*((VE-25D000,D0)/
1,(D.975*VE))1
C CHECK TO SEE IF INPUT ARGUMENTS ARE WITHIN SPECIFIED LMTITS
IF(PR>2000,D013,3,2
C IF DATA IS OUTSIDE LMTITS PRINT MESSAGE AND
C CONTINUE EXECUTION
2 PRINT 13,PR
3 IF(PR>1,D0)29,5,9
29 PRINT 14,PR
2 D.15,5,4
4 D.50,D016,6,7
C CALCULATE NU2 BY CALLING A GENERAL SUBROUTINE
C TO COMPUTE THE BIVARIATE POLYNOMIAL
5 CALL RTVPOL(A,PR,ALD,2,4,6)
NU2=D
C CALCULATE FIG4 WHERE PR IS BETWEEN 1,D AND
2,D INCLUSIVE
FIG4=NU1+(NU2-NU1)*(APL/ALD)
RETURN
7 PRINT 14,PR
C CALCULATE FIG4 BY CALLING A GENERAL SUBROUTINE
C TO COMPUTE THE BIVARIATE POLYNOMIAL
6 CALL RTVPOL(A,PR,APL,2,4,6)
FIG4=D
RETURN
13 FORMAT(6H)PR = ,D25.16,5X,23HTS A DATA ERROR IN FIG4)
14 FORMAT(6H)PR = ,D25.16,5X,23HTS A DATA ERROR IN FIG4)
END

```

```

FUNCTION FIG5(QVN,PR,VE,PR1)
IMPLTCIT REAL*8(A-H,K-7)
DIMENSTON A(?,),B(1)
C THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS
DATA A/-D.10239761DD,0.14091448D-1,-D.88660084D-3,+B/D.52514486DD/F5
1,D.1/2/,J/1/
C TEST FOR PR <=CF. 1,D & AND<=LE. 500.
1F (PR>1,D) 15,10,10
10 IF (PR>500,D0) 20,20,15
C PRINTED FLAG FOR PR NOT WITHIN SPECIFIED LIMITS
15 PRINT 16,PR
16 FORMAT(5H)PR =,D25.16,38H TS OUTSIDE SPECIFIED LIMITS FOR FIG5)
C TEST FOR PR <=LE. 2000.
20 IF (PR > 2000,D1) 40,40,30
30 PRINT 31,PR
31 FORMAT(5H)PR =,D25.16,38H TS OUTSIDE SPECIFIED LIMITS FOR FIG5)
40 X = DLNG(PR)
CALL RATFUN(A,B,X,K,I,J)
KCONST = 250000,D*K
FIG5=(KCONST/QVN)+1,D)/(KCONST/VE)+1,D)
RETURN
END

```

```

FUNCTION FIG6(TFR)
IMPLICIT REAL*8(A-H,K-Z)
FIG6=8.5-10e9/(1.e2-TFR)
RETURN
END

          F6    100
          F6    105
          F6    110
          F6    115
          F6    120

          F6A    0
          F6A    10
          F6A    20
          F6A    30
          F6A    40
          F6A    50
          F6A    60
          F6A    70
          F6A    80

FUNCTION FIG6A(TR)
IMPLICIT REAL*8(A-H,K-Z)
SPEED CORRECTION, P 20, GER-2454A
IF(TR-1800)10,10,20
10 FIG6A=1.e01
RETURN
20 FIG6A=1.e
RETURN
END

          F6A    0
          F6A    10
          F6A    20
          F6A    30
          F6A    40
          F6A    50
          F6A    60
          F6A    70
          F6A    80

FUNCTION FIG7(PR,PB)
IMPLICIT REAL*8(A-H,K-Z)
PR IS PR/PX
DIMENSION A(6,7)
DATA A/0.8862096200,-0.579661630-1,-0.705470920-2,
10.532879320-2,-0.108344130-2,0.747995660-4,0.730235130-4,
2-0.908705840-3,0.514973770-3,-0.158707880-3,0.245599730-4,
3-0.146495240-5,-0.932322070-6,0.458633910-5,-0.304145660-5,
40.984980640-6,-0.152880210-6,0.901664920-8,0.268421960-8,
5-0.103846130-7,0.720728940-8,-0.241010820-8,0.376409970-9,
6-0.219289840-10,-0.30566380-11,0.106441490-10,-0.770440700-11,
70.257414440-11,-0.400548150-12,0.233840130-13,0.156751290-14,
8-0.495962330-14,0.365253590-14,-0.122927910-14,0.191545180-15,
9-0.111628440-16,-0.26954610-18,0.855805170-18,-0.637354590-18,
40.215567660-18,-0.336256620-19,0.195753800-20/
AL1=DLG(2.e000)
AP1=DLG(PR)
C CHECK TO SEE IF INPUT ARGUMENTS ARE WITHIN SPECIFIED LIMITS
C IF(PR>2000.0)13,3,2
C IF DATA IS OUTSIDE LIMITS PRINT MESSAGE AND
C CONTINUE EXECUTION
2 PRINT 13,PR
3 IF(PR<-0.0129,5,9
20 PRINT 14,PR
5 IF(PR>2.0)5,6,4
4 IF(PR>500.0)16,6,7
C CALCULATE NUB BY CALLING A GENERAL SUBROUTINE
5 CALL BIVPOL(A,PB,AL1,2,5,6)
NUB=?
C CALCULATE FIG7 WHERE PR IS BETWEEN 1.e1 AND
2.e0 INCLUDING 1.e0 BUT NOT 2.e0
FIG7=0.87*(NUB-0.87)*(AP1/AL1)
RETURN
7 PRINT 14,PR
C CALCULATE FIG7 BY CALLING A GENERAL SUBROUTINE
C TO COMPUTE THE BIVARIATE POLYNOMIAL
6 CALL BIVPOL(A,PB,AP1,2,5,6)
FIG7=?
RETURN
13 FORMAT(6H0PB = ,D25.16,5X,23HIS A DATA ERROR IN FIG7)
14 FORMAT(6H0PR = ,D25.16,5X,23HIS A DATA ERROR IN FIG7)
END

          F7    100
          F7    105
          F7    110
          F7    115
          F7    120
          F7    121
          F7    122
          F7    123
          F7    124
          F7    125
          F7    126
          F7    127
          F7    128
          F7    129
          F7    130
          F7    131
          F7    132
          F7    133
          F7    134
          F7    135
          F7    136
          F7    137
          F7    138
          F7    139
          F7    140
          F7    141
          F7    142
          F7    143
          F7    144
          F7    145
          F7    146
          F7    147
          F7    148
          F7    149
          F7    150
          F7    151
          F7    152
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          F7    165
          F7    166
          F7    167
          F7    168
          F7    169
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          F7    251
          F7    252
          F7    253
          F7    254
          F7    255
          F7    256
          F7    257
          F7    258
          F7    259
          F7    260
          F7    261
          F7    262
          F7    263
          F7    264
          F7    265

```

```

FUNCTION FIG8(PX)
IMPLICIT REAL*8(A-H,K-Z)
DIMENSION A(5)
C THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS
DATA A/0.130401,0.197302,-0.111802,-0.958702,0.314803/,I/4/
C TEST FOR PX .GE. 3.0 .AND. LE. 100.0 .OR. GE.100.0
IF (PX .LT. 3.0) 30,10,10
10 IF (PX .LT. 100.0) 35,15,15
15 IF (PX .LT. 100.0) 35,25,25
25 FIG8 = 1.5
      RETURN
30 PRINT 31,PX
31 FORMAT(1SHDX =,025.16,38H IS OUTSIDE SPECIFIED LIMITS FOR FIG8)
35 X = 1.0/PX
      CALL UNTPNL(A,X,Z,I)
      FIG8 = Z
      RETURN
END

```

```

FUNCTION FIG10(P)
IMPLICIT REAL*8(A-H,K-Z)
DIMENSION A(5)
C THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS
C DATA A/0.1383D1,0.2329D2,0.8501D3,-0.5161D4,0.21358D5/,T/4/
C TEST FOR P .LE. 5.E-7 .OR. .GT. 5.E-7
      IF (P = 5.E-7 - (1.E-5)) 15,15,20
15 FIG10 = 24.0
      RETURN
20 X = 1.E/P
      CALL UNTPOL(A,X,Z,II)
      FIG10 = Z
      RETURN
      END

```

```

      SUBROUTINE FIG12A(P,HR,SR,HA,SA,H,S)
      IMPLICIT REAL*8(A-H,K-7)
C
C      * CALCULATE CONSTANT TERM RD
C      RD=((SA-SB)+(0.0177)-(10.**((HR-(HA+65.0))/371.0)))/(HA-HR)
C      INITIALIZE ENTROPY AT END CONDITION SR
C      AS=SB
C      BEGIN ITERATIVE PROCESS ON CONVERGING ENTROPY
C      DO 5 T=1,50
C      T=TMAPS(P,AS)
C      H1=HMAP(T,P)
C      S=10.**((HR-(H1+65.0)/371.0)+RD*(H1-HR)+SR-(0.0177))
C      DTFF=S-AS
C      TF(DABS(DTFF)-1.0D-5)2,2,1
      1 AS=S
      5 CONTINUE
      *
      IF(ENTROPY DOES NOT CONVERGE
      IN 50 ITERATIONS THEN PRINT MESSAGE AND
      RETURN THE LATEST VALUES OF H AND S TO
      CALLING ROUTINE
      *
      PRINT 3
      3 FORMAT(52H0ENTROPY IN FIG12A DID NOT CONVERGE IN 50 ITERATIONS)
      2 H=H1
      RETURN
      END

```

```

SUBROUTINE FIG12B(P,HB,SB,HX,SX,H,S) F12B 100
  IMPLICIT REAL*8(A-H,K-Z) F12B 105
C   CALCULATE CONSTANT TERMS F12B 110
  K=0.16129D5 F12B 115
  M=50.0*(SB-SX) F12B 120
  N=0.1*(HB-HX) F12B 125
  MN=M/N F12B 130
  L=2500.0*(SB*SB-SX*SX)+0.01*(HB*HB-HX*HX) F12B 135
  LN=L/N F12B 140
  A=0.25*(1.0+MN*MN) F12B 145
  B=50.0*SX+MN*(0.5*LN-0.1*HX) F12B 150
  C=(50.0*SX+1*(150.0*SX)+(0.1*HX)*(0.1*HX)) F12B 155
  I-K+LN*(0.25*LN-0.1*HX) F12B 156
  SC=(0.25/4)*(B+DSORT(B*B-4.*A*C)) F12B 156
  HC=0.5*(LN-2.0*MN*SC) F12B 160
C   INITIALIZE ENTROPY AT END CONDITION SB F12B 165
  AS=SR F12B 170
  T=TSAT(P) F12B 175
C   BEGIN ITERATIVE PROCESS ON CONVERGING ENTROPY F12B 180
  DO 5 I=1,50 F12B 185
  SG=SVAP(T,P) F12B 190
  M=(SG-AS)/(SG-SLT0(T)) F12B 191
  HG=HVAP(T,P) F12B 192
  H1=HG-M*(HG-HLT0(T)) F12B 193
  S=(SC-DSORT(K-(0.1*H1-HC)*(0.1)*H1-HC))/50.0 F12B 200
  DIFF=S-AS F12B 205
  IF(DABS(DIFF)-1.0-512.2,1
1  AS=S F12B 210
5  CONTINUE F12B 215
C   * F12B 220
C   IF ENTROPY DOES NOT CONVERGE F12B 225
C   IN 50 ITERATIONS THEN PRINT MESSAGE AND F12B 230
C   RETURN THE LATEST VALUES OF H AND S TO F12B 235
C   CALLING ROUTINE F12B 240
C   * F12B 245
C   PRINT 3 F12B 250
3  FORMAT(52H0ENTROPY IN FIG12B DID NOT CONVERGE IN 50 ITERATIONS) F12B 255
2  H=H1 F12B 260
  RETURN F12B 265
  END F12B 270
                                         F12B 275

```

```

FUNCTION FIG14(M) F14 100
  IMPLICIT REAL*8(A-H,K-Z) F14 105
  FIG14 = 0.87*(1.0 - 0.01*M)*(1.0 - 0.0065*M) F14 110
  RETURN F14 115
  END F14 120

```

```

FUNCTION FIG15(INHGA) F15 100
  IMPLICIT REAL*8(A-I,K-Z) F15 105
  DIMENSION A(3) F15 110
C   DATA FOLLOWS F15 115
  DATA A(1),A(2),A(3)/-0.23984811D2,0.57862440D2,0.31849404D1/ F15 120
C   CHECK TO SEE IF INPUT ARGUMENTS ARE WITHIN SPECIFIED LIMITS F15 125
  IF(INHGA<-0.2515.2,3 F15 130
C   IF DATA OUTSIDE LIMITS PRINT MESSAGE AND F15 135
C   CONTINUE EXECUTION F15 140
5  PRINT 13,INHGA F15 145
3  IF(INHGA>6.012.1,1 F15 150
1  PRINT 13,INHGA F15 155
C   CALCULATE FIG15 BY CALLING A GENERAL SUBROUTINE F15 160
C   TO COMPUTE THE UNIVARIATE POLYNOMIAL F15 165
2  AINHGA=DLOG(INHGA) F15 170
  CALL UNIPOL(A,AINHGA,Z,2) F15 175
  FIG15=Z F15 180
  RETURN F15 185
13 FORMAT(9H0INHGA = ,D25.16,5X,24HIS A DATA ERROR IN FIG15) F15 190
  END F15 195

```

```

FUNCTION FIG167(VAN,BLS,IR)
IMPLICIT REAL*8(A-H,O-Z)
DIMENSION VANX(21),F20(21),F23(21),F38(21),FS2(21)
C THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS
DATA VANX/128.00,150.00,175.00,200.00,250.00,300.00,350.00,400.00,
      450.00,500.00,550.00,600.00,650.00,700.00,800.00,900.00,1000.00,F167 100
      1100.00,1200.00,1300.00,1400.00,F20/25.6100,20.6400,16.1800, F167 105
      12.7500,8.3300,5.5300,4.2900,3.7300,3.9500,4.9600,6.5700,8.6500 F167 110
      10.9500,13.5600,19.3500,25.6200,32.0000,38.3500,44.3500, F167 115
      49.9500,54.7000,F23/53.6500,46.5000,40.3800,34.3500,24.9500, F167 120
      18.6800,14.2300,10.9000,8.6500,7.4500,7.1200,7.5500,8.7000, F167 121
      7.4500,15.4500,21.0700,26.9500,33.0500,38.7500,44.1500,48.9000 F167 122
      ,F38/51.6300,45.5000,38.3800,32.6500,23.8000,17.4300,12.9100, F167 123
      9.8/00,7.9700,7.0700,7.0200,7.7200,9.6000,11.0000,16.2500, F167 124
      21.9700,27.9200,34.8000,39.9200,45.2500,49.8500, F167 125
      FS2/71.200,63.500,55.800,48.00,35.900,27.800,21.500, F167 126
      16.400,12.500,9.600,8.600,8.400,9.00,10.400,14.400,19.400, F167 127
      25.00,30.900,36.400,41.700,46.500/,NPOINT/5/,NORDER/4/ F167 128
C FINDING A VANX WHICH ROUNDS VAN ABOVE
10 IF (VAN = VANX(4)) 15,15,10 F167 129
10 IF (VAN = VANX(20)) 20,16,16 F167 130
15 I = 1 F167 131
   GO TO 60 F167 132
16 I = 17 F167 133
   GO TO 60 F167 134
20 ILO = 4 F167 135
   IHI = 20 F167 136
   DO 25 J=1,4 F167 137
   IVAN = .5*(ILO + IHI) F167 138
   IF (VAN = VANX(IVAN)) 30,30,35 F167 139
25 IHI = IVAN F167 140
   GO TO 25 F167 141
30 ILO = IVAN F167 142
25 CONTINUE F167 143
   I = IHI - 3 F167 144
60 IF (IR=18) 181,80,61 F167 145
61 IF (BLS=21) 165,65,75 F167 146
65 CALL LAGRAN(VAN,VANX,F20,Z,NPOINT,NORDER,I) F167 147
   FIG167 = 7 F167 148
   RETURN F167 149
75 CALL LAGRAN(VAN,VANX,F23,Z,NPOINT,NORDER,I) F167 150
   FIG167 = 7 F167 151
   RETURN F167 152
85 IF (BLS=52) 181,85,85 F167 153
81 CALL LAGRAN(VAN,VANX,F38,Z,NPOINT,NORDER,I) F167 154
   FIG167 = 7 F167 155
   RETURN F167 156
95 CALL LAGRAN(VAN,VANX,FS2,Z,NPOINT,NORDER,I) F167 157
   FIG167=7 F167 158
   RETURN F167 159
   END F167 160

FUNCTION FIG18(PDT,PDD)
PDT IS PD/PT
PDD IS PD/PD*
IMPLICIT REAL*8(A-H,K-Z)
DIMENSION A(6,7)
DATA A/0.1038786900,0.510164590-1,0.2910290801,
      10.2747181800,-0.2131456301,0.00,
      2-0.198273501,-0.4519037201,-0.3713594502,
      3-0.1356002802,0.3261232202,0.00,
      40.1006329102,0.2003762603,0.6954799902,
      50.9841107102,-0.1716062203,0.00,
      6-0.1853811202,-0.2782900603,-0.2944975203,
      7-0.1825888203,0.3865099103,0.00,
      80.1274903502,0.2007378503,0.3048218603,
      90.4872359902,-0.2902521703,0.00,
      A12*0.00/
C CHECK TO SEE IF INPUT ARGUMENTS ARE WITHIN SPECIFIED LIMITS F18 100
F18 105
F18 110
F18 115
F18 120
F18 121
F18 122
F18 123
F18 124
F18 125
F18 126
F18 127
F18 128
F18 129
F18 130
F18 131
F18 135

```

```

PD=1.0/PDT          F18 140
1 IF(PD-1.217,3,8   F18 145
C   IF DATA OUTSIDE LIMITS PRINT MESSAGE AND      F18 150
C   CONTINUE EXECUTION                                F18 155
7 PRINT 13,PDT          F18 160
8 IF(PD-10,013,3,2   F18 165
2 PRINT 13,PDT          F18 170
3 PDINV=1.0/PDD        F18 175
4 IF(PDINV-0.519,5,10  F18 180
9 PRINT 14,PDD          F18 185
10 IF(PDINV-3.215,5,4  F18 190
4 PRINT 14,PDD          F18 195
C   CALCULATE FIG18 BY CALLING A GENERAL SUBROUTINE    F18 200
C   TO COMPUTE THE BIVARIATE POLYNOMIAL                F18 205
5 APDD=0LOG(PDD)        F18 210
CALL BIVPOL(A,PDT,APDD,Z,5,5)  F18 215
FIG18=Z            F18 220
RETURN             F18 225
13 FORMAT(7HD PDT = ,D25e16.5X,24H TS A DATA ERROR IN FIG18) F18 230
14 FORMAT(7HD PDD = ,D25e16.5X,24H TS A DATA ERROR IN FIG18) F18 235
END                 F18 240

FUNCTION FIG19(KVA)          F19 100
IMPLICIT REAL*8(A-H,K-Z)    F19 105
DIMENSION A(3)              F19 110
C   THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS      F19 115
DATA A/0.298980D3,0.294888D-2,0.612245D-9/,1/2/    F19 120
C   TEST FOR KVA .GE. 1000000 .AND. LE. 1500000       F19 125
1 IF (KVA - 1.05) 15,13,10  F19 130
10 IF (KVA - 15.05) 20,20,15  F19 135
15 PRINT 16,KVA          F19 140
16 FORMAT(6H0KVA =,D25.16,39H IS OUTSIDE SPECIFIED LIMITS FOR FIG19) F19 145
20 CALL UNTPOL(A,KVA,Z,1)  F19 150
FIG19 = Z                F19 155
RETURN                   F19 160
END                     F19 165

FUNCTION FIG20(KVA,ICK,TR)    F20 100
IMPLICIT REAL*8(A-H,K-Z)    F20 105
DIMENSION A(4),AA(4),B(1)    F20 110
DATA A/11,A/21,A/31,A/41/-0.34293488D0,0.89126466D0,  F20 115
1-0.10877851D0,0.36908686D-2/,AA(1),AA(2),AA(3),AA(4)/  F20 116
20.18479050D1,0.56681377D-1,-0.26652558D-1,           F20 117
30.10759713D-2/,B(1)/-0.49564581D-1/                  F20 118
ALD=0LOG(KVA)          F20 120
C   FIND DELTA          F20 121
1 IF(1R-180012,2,1      F20 122
1 DELTA=0.          F20 123
GOTO5                F20 124
2 IF(ICK13,3,4        F20 125
3 DELTA=-0.1         F20 126
GOTO5                F20 127
4 DELTA=-0.095        F20 128
*
C   THE INTEGER VARIABLE ICK WILL BE SET IN THE          F20 129
C   CALLING ROUTINE TO DETERMINE THE METHOD          F20 130
C   USED IN COMPUTING FIG20 AS FOLLOWS          F20 135
C   ICK GREATER THAN ZERO          FIG20 COMPUTED BY UNIVARIATE  F20 140
C                                         POLYNOMIAL FOR CONVENTIONALLY  F20 145
C                                         COOLED
C   ICK LESS THAN OR EQUAL TO ZERO          FIG20 COMPUTED BY RATIONAL  F20 150
C                                         FUNCTION FOR CONDUCTOR  F20 155
C                                         COOLED
C   *
C   DETERMINE PRANCH          F20 160
5 IF(ICK120,20,10        F20 165
10 CALL UNTPOL(A,ALD,Z,3)  F20 170
FIG20=Z+DELTA          F20 175
RETURN                 F20 180
20 CALL RATFUN(A,B,ALD,Z,3,1)  F20 185
FIG20=Z+DELTA          F20 190
RETURN                 F20 195
F20 200
F20 205
F20 210
F20 215
F20 220
F20 225
F20 230
F20 235
F20 240

```

```

FUNCTION FIG21(PCTKVA,TCK) F21 100
  IMPLICIT REAL*8(A-H,K-Z) F21 105
  DIMENSION ACD18(5),BCD18(1),ACD36(2),BCD36(2),ACONV(4),BCONV(1) F21 110
C   THE FOLLOWING IS THE LIST OF PROGRAM CONSTANTS F21 115
  DATA ACD18/-0.2272774400,-0.2493997602,0.34283283D2,-0.35808901D2,F21 120
    1 -0.94544169D1/,BCD18/-0.18638959D2/,J1/1/,ACD36/ F21 121
    2 -0.17535942D2,-0.15515139D2/,BCD36/-0.65338483D2,0.31286714D2/,F21 122
    3 T2/1/,J2/2/,ACONV/-0.20525271D2,-0.35019203D2,0.25514027D2, F21 123
    4 -0.25182400D2/,BCONV/-0.56218495D2/,T3/3/,J3/1/ F21 124
C   TCK .GT. 0 IF CONDITION IS CONVENTIONALLY COOLED, 3600 + 1800 RPM F21 125
C   TCK = 0 IF CONDITION IS CONDUCTOR COOLED, 3600 RPM F21 130
C   TCK .LT. 0 IF CONDITION IS CONDUCTOR COOLED, 1800 RPM F21 135
C   IF (TCK1 .LT. 0,20,30 F21 140
10 CALL RATEFUN(ACD18,BCD18,PCTKVA,Z,T1,J1) F21 145
  FIG21 = 7 F21 150
  RETURN F21 155
20 CALL RATEFUN(ACD36,BCD36,PCTKVA,Z,T2,J2) F21 160
  FIG21 = 7 F21 165
  RETURN F21 170
30 CALL RATEFUN(ACONV,BCONV,PCTKVA,Z,T3,J3) F21 175
  FIG21 = 7 F21 180
  RETURN F21 185
END F21 190

```

```

FUNCTION FIG22(KVA,TCK) F22 100
  IMPLICIT REAL*8(A-H,K-Z) F22 105
  DIMENSION A(4),AA(2),AR(2),AC(2),R(1) F22 110
  DATA A(1),A(2),A(3),A(4)/0.10949623D2,0.12755560D-3,0.71452351D-8,F22 115
    1-0.58323495D-14/,R(1,1)/0.56299996D-5/,AR(1,1),AR(2)/
    21.12D3,C96D-4/,AC(1,1),AC(2)/0.4002,0.96D-4/ F22 116
C   *
C   THE INTEGER VARIABLE TCK WILL BE SET IN THE F22 117
C   CALLING ROUTINE TO DETERMINE THE METHOD F22 120
C   USED IN COMPUTING FIG22 AS FOLLOWS F22 125
C   TCK GREATER THAN ZERO F22 130
C     TCK=1 F22 135
C     FIG22 COMPUTED BY RATIONAL F22 140
C     FUNCTION FOR CONVENTIONALLY F22 145
C     COOLED AT 3600RPM F22 150
C     TCK=2 F22 155
C     FIG22 COMPUTED BY UNIVARIATE F22 160
C     POLYNOMIAL FOR CONVENTIONALLY F22 165
C     COOLED AT 1800RPM F22 170
C     TCK EQUAL ZERO F22 175
C     FIG22 COMPUTED BY UNIVARIATE F22 180
C     POLYNOMIAL FOR CONDUCTOR F22 185
C     COOLED AT 3600RPM F22 190
C     TCK LESS THAN ZERO F22 195
C     FIG22 COMPUTED BY UNIVARIATE F22 200
C     POLYNOMIAL FOR CONDUCTOR F22 205
C     COOLED AT 1800RPM F22 210
C     *
C     DETERMINE BRANCH F22 215
C     IF(TICK140,30,5 F22 220
      5 IF(TICK-2110,20,20 F22 225
10 CALL RATEFUN(A,B,KVA,Z,3,J1) F22 230
  FIG22=7 F22 235
  RETURN F22 240
20 CALL UNIPOL(AA,KVA,Z,1) F22 245
  FIG22=7 F22 250
  RETURN F22 255
30 CALL UNIPOL(AR,KVA,Z,1) F22 260
  FIG22=7 F22 265
  RETURN F22 270
40 CALL UNIPOL(AC,KVA,Z,1) F22 275
  FIG22=7 F22 280
  RETURN F22 285
END F22 285

```

SUBROUTINE UNIPOL(A,X,Z,T)	UNIP 100
IMPLICIT REAL*8(A-H,D-Z)	UNIP 105
DIMENSION A(10)	UNIP 110
Z = 0.0	UNIP 115
II = I + 2	UNIP 120
DO 1 N=1,I	UNIP 125
Z = Z*X	UNIP 130
1 Z = Z + A(II-N)	UNIP 135
Z = Z*X + A(1)	UNIP 140
RETURN	UNIP 145
END	UNIP 150
SUBROUTINE BIVPOL(A,X,Y,Z,I,J)	BIVP 100
IMPLICIT REAL*8(A-H,K-Z)	BIVP 105
DIMENSION A(6,7)	BIVP 110
C INCREASE THE ROW AND COLUMN DIMENSION EACH	BIVP 115
C BY ONE BECAUSE ZERO SUBSCRIPTS ARE ILLEGAL	BIVP 120
C INCREMENT BELOW BASED ON ASSUMPTION DATA	BIVP 125
C IN CALLING ROUTINE IMPLICITLY LISTS A	BIVP 130
C ARRAY AS A(J,I) IN ORDER TO CONFORM	BIVP 135
C TO DEFINITION IN APPENDIX 1	BIVP 140
II=J+1	BIVP 145
JJ=I+1	BIVP 150
C INITIALIZE Z	BIVP 155
Z=0.0	BIVP 160
DO 1 J1=1,JJ	BIVP 165
DO 1 II=1,II	BIVP 170
1 Z=Z+A(J1,II)*(X**(II-1))*(Y**(J1-1))	BIVP 175
RETURN	BIVP 180
END	BIVP 185
SUBROUTINE RATEFUN(A,B,X,Z,T,J)	RATE 100
IMPLICIT REAL*8(A-H,D-Z)	RATE 105
DIMENSION A(10),B(5)	RATE 110
ZNUM = 0.0	RATE 115
ZDENOM = 0.0	RATE 120
II = I + 2	RATE 125
J1=J + 1	RATE 130
DO 1 N=1,I	RATE 135
ZNUM = ZNUM*X	RATE 140
1 ZNUM = ZNUM + A(II-N)	RATE 145
ZNUM = ZNUM**X + A(1)	RATE 150
DO 2 M=2,J	RATE 155
ZDENOM = ZDENOM*X	RATE 160
2 ZDENOM = ZDENOM + B(J1-M)	RATE 165
ZDENOM = ZDENOM**X + 1.	RATE 170
Z = ZNUM/ZDENOM	RATE 175
RETURN	RATE 180
END	RATE 185
SUBROUTINE LAGRANT(X,T,F,Z,NPOINT,NORDER,1)	LAGR 100
IMPLICIT REAL*8(A-H,D-Z)	LAGR 105
DIMENSION T(30),F(30),P(20),PNUM(30),PDENOM(30)	LAGR 110
C ADJUSTING NPOINT AND NORDER FOR USE IN DO LOOPS	LAGR 115
NPTI = NPOINT - 1 + 1	LAGR 120
NORDI = NORDER - 1 + 1	LAGR 125
Z = 0.0	LAGR 130
DO 1 J=1,NPTI	LAGR 135
PNUM(J1) = X - T(J)	LAGR 140
1 P(J)=1.0	LAGR 145
DO 2 K=1,NPTI	LAGR 150
DO 3 N=1,NORDI	LAGR 155
IF (K = N) 20,20,10	LAGR 160
20 P(K) = P(K)*PNUM(N)/(T(K) - T(N))	LAGR 165
GO TO 3	LAGR 170
20 P(K) = P(K)*PNUM(N+1)/(T(K) - T(N+1))	LAGR 175
3 CONTINUE	LAGR 180
2 Z=Z+P(K)*F(K)	LAGR 185
RETURN	LAGR 190
END	LAGR 195

```

FUNCTION TLIQH(H)
  IMPLICIT REAL*8(A-H,D-Z)
C CALCULATES TEMPERATURE (F) OF SATURATED LIQUID
C AS FUNCTION OF ENTHALPY (BTU/LB) OF
C SATURATED LIQUID
C PROCEDURE SUGGESTED IN WESTINGHOUSE,
C TRANS ASME V80, NO4, MAY,1958.
C CHECK TO SEE IF INPUT ARGUMENTS ARE WITHIN SPECIFIED LIMITS
C IF(H>18.07)21,3,25
C IF DATA OUTSIDE LIMITS PRINT MESSAGE AND
C CONTINUE EXECUTION
21 PRINT 13,H
25 IF(H>870.0)12,4,1
  1 PRINT 13,H
  2 IF(H<400.0)13,3,4
  3 TD=H+35.0
    GO TO 21
  4 TDE=(H*H)/1022.49+1.855*H-172.25
C BEGIN PROCESS WHEREBY H IS BOUNDED ABOVE
C BY HD AND BELOW BY HL
20 T1=TD-3.0
  HD=TLIQH(TD)
  HL=TLIQH(T1)
  IF(H>HD)5,6,7
  7 TD=TD+5.0
    GO TO 20
  6 TLQH=TD
    RETURN
  5 TDE=H18.9,10
  9 TLQH=T1
    RETURN
10 T1=TD-1
  GO TO 20
C BEGIN HALVING PROCEDURE TO FIND DESIRED T
  8 DO 31 T=1,50
    TAVG=(T1+T0)/2.0
    HT=TLIQH(TAVG)
    D=H-HT
    DT=DCABS(D)-1.0E-2
    TDE=15.16,17
16 TLQH=TAVG
    RETURN
15 T0=TAVG
    GO TO 18
17 T1=TAVG
18 IF(DT)>19.19,11
19 TLQH=TAVG
    RETURN
11 CONTINUE
  PRTNT 14
  TLQH=TAVG
13 FORMAT(5H0H = ,D20.11,5X,24HIS A DATA ERROR IN TLQH)
14 FORMAT(4DH0HTLQH DID NOT CONVERGE IN 50 ITERATIONS)
    RETURN
  END

```

TLIQ	0
TLIQ	1
TLIQ	2
TLIQ	10
TLIQ	20
TLIQ	30
TLIQ	40
TLIQ	50
TLIQ	60
TLIQ	70
TLIQ	80
TLIQ	90
TLIQ	100
TLIQ	110
TLIQ	120
TLIQ	130
TLIQ	140
TLIQ	150
TLIQ	160
TLIQ	170
TLIQ	180
TLIQ	190
TLIQ	200
TLIQ	210
TLIQ	220
TLIQ	230
TLIQ	240
TLIQ	250
TLIQ	260
TLIQ	270
TLIQ	280
TLIQ	290
TLIQ	300
TLIQ	310
TLIQ	320
TLIQ	330
TLIQ	340
TLIQ	350
TLIQ	360
TLIQ	370
TLIQ	380
TLIQ	390
TLIQ	400
TLIQ	410
TLIQ	420
TLIQ	430
TLIQ	440
TLIQ	450
TLIQ	460
TLIQ	470
TLIQ	480
TLIQ	500
TLIQ	510
TLIQ	511
TLIQ	520

```

FUNCTION HCOM(P,T)
  IMPLICIT REAL*8(A-H,D-Z)
C CALCULATES ENTHALPY (BTU/LB) OF COMPRESSED LIQUID
C AS FUNCTION OF TEMP (F) OF SATURATED
C LIQUID AND PRESSURE (LB/SQ.IN) BY LINEAR
C INTERPOLATION IN TABLE 4, KEENAN + KEYES,
C 1951, PP.74-75.
C PROCEDURE SUGGESTED IN WESTINGHOUSE,
C TRANS ASME V80, NO4, MAY,1958.
C DMENSTON PP(10),TT(14),HH(10,14),DH(51),PS(51)
  DATA PP/200.00,400.00,600.00,800.00,1000.00,1500.00,
        12000.00,2500.00,3000.00,3200.200/, TT/32.00,120.00,
        2200.00,300.00,400.00,500.00,600.00,620.00,640.00,

```

HCOM	0
HCOM	1
HCOM	2
HCOM	17
HCOM	20
HCOM	30
HCOM	40
HCOM	50
HCOM	60
HCOM	70
HCOM	80
HCOM	81
HCOM	82

```

2660.00, 680.00, 690.00, 700.00, 705.400/, HH/0.61D2,
41.2100, 1.8000, 2.3900, 2.9900, 4.4800, 5.9700, 7.4900,
59.0400, 9.6100, 9.5400, 1.0900, 1.6700, 2.1700, 2.7000,
63.9900, 5.3100, 6.5800, 7.8800, 8.4500, 9.4100, 9.8300,
71.3100, 1.7800, 2.2100, 3.3600, 4.5100, 5.6300, 6.7600,
87.2500, 8.2300, 9.6100, 9.9700, 1.3500, 1.7500, 2.7200,
93.6400, 4.5500, 5.4900, 5.9600, 6.6000, 6.1600, 6.3900, 6.6100,
40.8400, 1.4400, 2.2300, 2.6600, 3.3300, 3.6200, 6.0000, 6.0000,
80.0000, -6.0500, -8.1400, -6.2900, -6.3800, -6.4100, -6.4100, -6.4000,
C1.0004, 1.0004, 2.0000, 4.0000, 6.0000, 8.0000, -2.5000, -4.9000,
D-6.9000, -7.6000, 5*1.004, 6.0000, -1.8000, -5.6000, -8.7000, -9.8000,
E5*1.004, 2*6.0000, -5.4000, -10.3000, -12.1000, 6*1.004, 6.0000,
F-3.1000, -11.8000, -14.6000, 6*1.004, 2*6.0000, -12.2000, -17.6000,
G7*1.004, 6.0000, -8.9000, -19.4000, 7*1.004, 2*6.0000, -21.6000, 8*1.004, 6.0000,
H0.0000/, DH/0.600, 6.2300, 6.4100, 6.5400, 6.6100/
C CHECK TO SEE IF PRESSURE IS SUFFICIENT FOR A
C COMPRESSED LIQUID - IF NOT PRINT MESSAGE
C AND RETURN
P1=PSAT(T)
H1=HL10(T)
TFID=P1)3,3,4
3 PRINT 13,P
RETURN
4 IF(P-200.0)10,9,9
C IF PRESSURE IS LESS THAN 200 A LINEAR
C INTERPOLATION IS DONE WITH SATURATED PRESSURES
C AND TABLE ENTRIES TO CALCULATE H-H(SAT)
10 PFRACT=P/200.0
DO 5 I=1,5
IF(T-TT(I))6,7,5
7 YF=DH(6-T)
GO TO 8
6 YF=DH(6-T)+(DH(7-T)-DH(6-T))/(TT(1)-TT(1-1))*(T-TT(1-1))
C OBTAIN Z BY MULTIPLYING THE INTERPOLATED
C H-H(SAT) VALUE BY THE FRACTION P/200
8 Z=YF*PFRACT
HCOM=H1+Z
RETURN
5 CONTINUE
C VARTABLE BLANK SET TO INDICATE UPON RETURN
C FROM LINT2 THAT INTERPOLATION FAILED
9 BLANK=1.0D4
C CALL LINEAR INTERPOLATION ROUTINE TO CALCULATE
C H-H(SAT)
CALL LINT2(Z,P,T,PP,10,10,TT,14,HH,BLANK)
HCOM=H1+Z
13 FORMAT(5HOP = ,D20.11,5X,23HIS A DATA ERROR IN HCOM)
RETURN
END

```

```

FUNCTION TCOM(P,H)
IMPLICIT TT REAL*8(A-H,D-Z)
CALCULATES TEMPERATURE (F) OF COMPRESSED LIQUID
C AS FUNCTION OF THE ENTHALPY (BTU/LB) OF
C A SATURATED LIQUID AND PRESSURE (LB/SQ.IN)
C PROCEDURE SUGGESTED IN WESTINGHOUSE,
C TRANS ASME VRG, NO4, MAY,1958.
C CHECK TO SEE IF PRESSURE IS SUFFICIENT FOR A
C COMPRESSED LIQUID - IF NOT PRINT MESSAGE
C AND RETURN
T0=TL10H(H)
P1=PSAT(T0)
IF(P-P1)1,1,2
1 PRINT 13,P
RETURN
C A POSSIBLE ERROR IN THIS ROUTINE IS THE
C ARBITRARY CHOICE OF T1 AND T2
C BOUND TO BY T1 BELOW AND T2 ABOVE
2 T1=T0-20.0
T2=T0+20.0

```

TCOM	0
TCOM	1
TCOM	2
TCOM	10
TCOM	20
TCOM	30
TCOM	40
TCOM	50
TCOM	60
TCOM	70
TCOM	80
TCOM	90
TCOM	100
TCOM	110
TCOM	120
TCOM	130
TCOM	140
TCOM	150
TCOM	160
TCOM	170

C	CALCULATE COMPRESSED ENTHALPY FOR T1 AND T2	TCOM 180
	H1=HCOM(P,T1)	TCOM 190
	H2=HCOM(P,T2)	TCOM 200
C	CALCULATE DH/DT	TCOM 210
	DHDT=(H2-H1)/(T2-T1)	TCOM 220
C	BEGIN ITERATIVE PROCEDURE ON TEMPERATURE	TCOM 230
	DO 3 I=2,30	TCOM 240
	HP=HCOM(P,T0)	TCOM 250
C	CALCULATE T3 ESTIMATE	TCOM 260
	T3=(H-H0)/DHDT+T0	TCOM 270
C	CHECK CONVERGENCE ON TEMPERATURE	TCOM 280
	IF(DABS(T3-T0)-1.0D-2)>4,4,3	TCOM 290
3	T0=T3	TCOM 300
C	IF CONVERGENCE FAILS PRINT MESSAGE AND	TCOM 310
C	RETURN LATEST T3	TCOM 320
	PRINT 14	TCOM 330
4	TCOM=T3	TCOM 340
13	FORMAT(5HDP = ,0.2G<11.5X,23HITS A DATA ERROR IN TCOM)	TCOM 360
14	FORMAT(37HTEMPERATURE DID NOT CONVERGE IN TCOM)	TCOM 370
	RETURN	TCOM 371
	END	TCOM 380

SUBROUTINE LINT2(I,X,Y,XA,NX,LIMX,YA,NY,ZA,BLANK)		LINT 0
IMPLICIT REAL*8(A-H,O-Z)		LINT 1
C	TWO INDEPENDENT VARIABLE TABLE LOOK UP AND LINEAR INTERPOLATION ROLINT	LINT 10
C	Z=FUNCTION(X,Y) , XA THE ARRAY OF X VALUES IN INCREASING ORDER AND LINT	LINT 20
C	WITH DIMENSION LIMX AND NX NON-BLANK ENTRIES , YA THE ARRAY OF Y LINT	LINT 30
C	WITH NY NON-BLANK ENTRIES . BOTH XA AND YA MUST BE FILLED FROM THLINT	LINT 40
C	LOW SUBSCRIPT END . ZA IS THE ARRAY OF Z SUCH THAT Z(I,J)=F(X(I),LINT	LINT 50
C	AND DIMENSION Z(LIMX,NY) (OR GREATER).	LINT 60
C	BLANK IS A CONSTANT PLACED IN THE ZA TABLE TO INDICATE NO ENTRY LINT	LINT 70
C	IF Z=BLANK UPON RETURN, THE (X,Y) DID NOT FALL WITHIN THE ZA TABLELINT	LINT 80
	DIMENSION XA(10),YA(14),ZA(140)	LINT 90
1	IF(X-XA(1))<9,6,2	LINT 100
2	DO 4 I=2,NX	LINT 110
3	IF(X-XA(I))<7,7,4	LINT 120
4	CONTINUE	LINT 130
5	GO TO 99	LINT 140
6	I=2	LINT 150
7	IFI(Y-YA(1))<9,12,8	LINT 160
8	DO 10 J=2,NY	LINT 170
9	IF(Y-YA(J))<13,13,10	LINT 180
10	CONTINUE	LINT 190
11	GO TO 99	LINT 200
12	J=2	LINT 210
13	K22=(J-1)*LIMX+I	LINT 220
14	K12=K22-1	LINT 230
15	K11=K12-LIMX	LINT 240
16	K21=K11+1	LINT 250
	IF(BLANK-ZA(K11))<18,99,18	LINT 260
18	IF(BLANK-ZA(K12))<0,99,10	LINT 270
19	IF(BLANK-ZA(K22))<0,99,20	LINT 280
20	IF(BLANK-ZA(K21))<0,99,21	LINT 290
21	A=(Y-YA(J-1))/(XA(I)-XA(J-1))	LINT 300
22	R=(Y-YA(J))/((YA(J)-YA(J-1))	LINT 310
23	710=R*ZA(K12)+I1.-R)*ZA(K11)	LINT 320
24	Z20=(I.-R)*ZA(K21)+R*ZA(K22)	LINT 330
25	Z=Z20*A+(I.-A)*710	LINT 340
26	RETURN	LINT 350
99	PRINT 101	LINT 360
	Z=BLANK	LINT 370
101	FORMAT(34HBLANK WAS RETURNED FOR Z IN LINT2)	LINT 390
100	RETURN	LINT 391
	END	LINT 400

```

FUNCTION HVAP(TF,PF)
IMPLICIT REAL*8(A-H,D-Z)
C CALCULATES ENTHALPY OF STEAM REFERRED TO WATER AT 32F AND .08854 PSIA
C KEENAN + KEYES, 1951, PP. 15-16, ED 13-15
C COMMON /H2OGEN/ TOLD,POLD,TAU,TAU2,R0,0.03,012,DB0,F0,F1,G1,F2,G2
1,F3,G3
P=PF/14.6959
T=(TF+45.69)/1.8
IF(T-TOLD)33,32,33
32 IF(P-POLD)34,220,34
33 TOLD=T
34 POLD=P
TAU=1./T
TAU2=TAU*TAU
TAU3=TAU2*TAU
TAU12=TAU3**4
EXTAU=-(10.**(.80870.*TAU2))
R0=EXTAU*TAU*2641.62+1.89
Q=R0*TAU
Q2=Q*0
Q3=Q2*0
Q12=Q3**4
DB0=(372420.11*TAU2+1.1*EXTAU*2641.62
F0=DB0*TAU+R0
G1=-3.2492D5*TAU+82.546
G1=(-1.6246D5*TAU+82.546)*TAU
F1=(G1)*F0*2.+0.*DG1)*0
DG2=-2.5394D5*TAU
G2=-1.2647D5*TAU2+.21828
F2=(G2*F0*4.+0.*DG2)*03
DG3=+1.62432D6.6*TAU12*TAU12*T
G3=+6.768D6.4*TAU12*TAU12-3.635D-4
G3=SIGNS OF G3 + DG3 REVERSED FROM K+K AVOIDS - IN F3
F3=(G3*F0*13.+0.*DG3)*012
220 DHCT=((PF**9*F3/3.25+F21*0.5*P+P+F1)*.5*P+F0)*P*4.3557D-2+.2158633HVAP 255
C DHCT=CHANGE IN H AT CONSTANT T AS PRESSURE GOES FROM ZERO TO PF PLHVAP 260
C CHANGE IN H AT 32F AS P=.08854 GOES TO P=0 HVAP 265
C DHZP=((3.7783D-4*T+1.472)*T*DLOG(T)*47.83651*0.43-300.420108 HVAP 270
C DHZP=CHANGE IN H AT ZERO PRESSURE AS TEMP. GOES FROM 32F TO TF HVAP 275
C INTEGRAL(CP0*DT) EVALUATED AT 32F = 300.420108 HVAP 280
C HVAP=DHZP+DHCT+1075.8 HVAP 285
C H OF EVAPORATION AT 32F = .08854PSIA = 1075.8 RTU/LBM HVAP 290
C RETURN HVAP 295
END HVAP 300

FUNCTION SVAP(TF,PF)
IMPLICIT REAL*8(A-H,D-Z)
C CALCULATES ENTHALPY OF STEAM REFERRED TO WATER AT 32F AND .08854 PSIA
C KEENAN + KEYES, 1951, PP. 15-16, ED 13, 15, 16A
C COMMON /H2OGEN/ TOLD,POLD,TAU,TAU2,R0,0.03,012,DB0,F0,F1,G1,F2,G2
1,F3,G3
P=PF/14.6959
T=(TF+45.69)/1.8
IF(T-TOLD)33,32,33
32 IF(P-POLD)34,220,34
33 TOLD=T
34 POLD=P
TAU=1./T
TAU2=TAU*TAU
TAU3=TAU2*TAU
TAU12=TAU3**4
EXTAU=-(10.**(.80870.*TAU2))
R0=EXTAU*TAU*2641.62+1.89
Q=R0*TAU
Q2=Q*0
Q3=Q2*0
Q12=Q3**4
DB0=(372420.11*TAU2+1.1*EXTAU*2641.62
F0=DB0*TAU+R0
G1=-3.2492D5*TAU+82.546
HVAP 100
HVAP 101
HVAP 102
HVAP 105
HVAP 110
HVAP 113
HVAP 115
HVAP 120
HVAP 125
HVAP 130
HVAP 135
HVAP 140
HVAP 145
HVAP 150
HVAP 155
HVAP 160
HVAP 165
HVAP 170
HVAP 175
HVAP 180
HVAP 185
HVAP 190
HVAP 195
HVAP 200
HVAP 205
HVAP 210
HVAP 215
HVAP 220
HVAP 225
HVAP 230
HVAP 235
HVAP 240
HVAP 245
HVAP 250
HVAP 255
HVAP 260
HVAP 265
HVAP 270
HVAP 275
HVAP 280
HVAP 285
HVAP 290
HVAP 295
HVAP 300

SVAP 100
SVAP 101
SVAP 102
SVAP 105
SVAP 110
SVAP 111
SVAP 115
SVAP 120
SVAP 125
SVAP 130
SVAP 135
SVAP 140
SVAP 145
SVAP 150
SVAP 155
SVAP 160
SVAP 165
SVAP 170
SVAP 175
SVAP 180
SVAP 185
SVAP 190
SVAP 195
SVAP 200
SVAP 205

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G1=(-1.6246D5*TAU+82.546)*TAU          SVAP 210
F1=(G1*F0*2.+0.*DG1)*Q                  SVAP 215
DG2=-2.5394D5*TAU                      SVAP 220
G2=-1.2697D5*TAU2+.21828                SVAP 225
F2=(G2*F0*4.+0.*DG2)*Q                  SVAP 230
DG3=+1.62432D66*TAU12*TAU12*T          SVAP 235
G3=+6.768064*TAU12*TAU12-3.635D-4      SVAP 240
C SIGNS OF G3 + DG3 REVERSED FROM K+K    AVOIDS - IN F3
F3=(G3*F0*13.+0.*DG3)*Q12              SVAP 245
220 EMO= DRO*TAU2                      SVAP 250
EM1=(-R0*0.*G3+F1)*TAU*.5             SVAP 255
EM2=(-R0*03*G2+F2)*TAU*.25            SVAP 260
EM3=(-R0*012*G3+F3)*TAU/13.           SVAP 265
DSCT=((((EM3*P**9+EM2)*P*P+EM1)*P+EM0)*P-DLOG(P)*4.55504)*
1 2.419833D-2 -.56307532               SVAP 270
C DSCT=CHANGE IN ENTROPY AT CONSTANT TF FROM ZERO PRESSURE TO PF PLUSVAP 280
C CHANGE IN ENTROPY AT 32F FROM .08854PSIA TO 0.0PSIA          SVAP 285
C DSZP=(DLOGIT)*1.472+7.5566D-4*T-47.8365*TAU1*.23888889-1.98022309  SVAP 290
C DSZP=CHANGE IN ENTROPY AT ZERO PRESSURE AS TEMP. GOES FROM 32F TO SVAP 295
C INTEGRAL(CP0/T*DT) EVALUATED AT 32F = 1.98022309          SVAP 300
C SVAP=DSZP+DSCT+2.1877                  SVAP 305
C S OF EVAPORATION AT 32F + .08854 PSIA = 2.1877          SVAP 310
RETURN                                     SVAP 315
END                                         SVAP 320

FUNCTION VVAP(TF,PF)
IMPLICIT REAL*8(A-H,D-Z)
CALCULATES SPECIFIC VOLUME OF STEAM
C KEENAN + KEYES, 1951, Pg. 15, Eq. 13
P=PF/14.6959                                VVAP 100
T=(TF+459.691/1.8)                          VVAP 101
TAU=1./T                                      VVAP 102
TAU2=TAU*TAU                                    VVAP 105
TAU3=TAU2*TAU                                  VVAP 110
TAU12=TAU3**4                                   VVAP 115
EXTAU=-((10.**((80870.*TAU2)))              VVAP 120
R0=EXTAU*TAU*2641.62+3.89                     VVAP 125
Q=P*TAU                                       VVAP 130
QP=0.*P                                       VVAP 135
G1=(-1.6246D5*TAU+82.546)*TAU              VVAP 140
G2=-1.2697D5*TAU2+.21828                    VVAP 145
G3=+6.768064*TAU12*TAU12-3.635D-4          VVAP 150
C SIGN OF G3 REVERSED FROM K+K
P=((G3*QP**9+G2*QP*QP+G1*QP+1.)*R0*,0160185 VVAP 155
VVAP=.072964908*T/P+B                         VVAP 160
RETURN                                         VVAP 165
END                                         VVAP 170

FUNCTION TVAPH(PI,HI)
IMPLTCIT REAL*8(A-H,D-Z)
CALCULATES TEMPERATURE OF STEAM FROM PRESSURE AND ENTHALPY USING HVAP ANTVAPH102
C LINEAR INTERPOLATION
P=PI                                         TVAPH100
H=HI                                         TVAPH101
C START WITH ABOUT 50 DEGREES SUPERHEAT
DELT=40.                                     TVAPH102
T=8574./(15.424-DLOG(PI))-410.              TVAPH105
H1=HVAP(T,P)                                 TVAPH110
TF(H1-H12,10,1)                             TVAPH115
C 1 USE LESS SUPERHEAT
1 DELT=-DELT                                TVAPH120
2 T=DELT+T                                    TVAPH125
5 HQ=H1                                       TVAPH130
H1=HVAP(T,P)                                 TVAPH135
DELT=(H1-H)*DELT/(HQ-H1)                     TVAPH140
T=DELT+T                                    TVAPH145
IF(DABS(DELT)>.01110,10,5)                 TVAPH150
10 TVAPH=T                                     TVAPH155
RETURN                                         TVAPH160
END                                         TVAPH165
TVAPH170
TVAPH175
TVAPH180
TVAPH185
TVAPH190
TVAPH195

```

```

FUNCTION TVAPS(PT,ST)
IMPLICIT REAL*8(A-H,D-Z)
CALCULATES TEMPERATURE OF STEAM FROM PRESSURE AND ENTROPY USING SVAP AND TVAPS100
C   LINEAR INTERPOLATION
      S=ST
      P=PT
C   START WITH ABOUT 50 DEGREES SUPERHEAT
      DELT=40.
      T=8574. / (15.424-DLOG(P))-410.
      S1=SVAP(T,P)
      IF(S1>S12,10,1
C   1 USE LESS SUPERHEAT
      1 DELT=-DELT
      2 T=DELT+T
      5 S0=S1
      S1=SVAP(T,P)
      DELT=(S1-S)*DELT/(S0-S1)
      T=DELT+T
      IF(DABS(DELT)>0.01)10,10,5
10 TVAPS=T
      RETURN
      END

```

TVAPS100
TVAPS101
TVAPS102
TVAPS105
TVAPS110
TVAPS115
TVAPS120
TVAPS125
TVAPS130
TVAPS135
TVAPS140
TVAPS145
TVAPS150
TVAPS155
TVAPS160
TVAPS165
TVAPS170
TVAPS175
TVAPS180
TVAPS185
TVAPS190
TVAPS195

```

FUNCTION HLIO(TF)
IMPLICIT REAL*8(A-H,D-Z)
CALCULATES ENTHALPY (BTU/LBM) OF SATURATED WATER FROM 50 TO 600 DEG F.
C   WESTINGHOUSE ALGORITHM, TRANS ASME V80, NO4, MAY, 1958, P.959
      T=TF
      IF(T>360,120,20,10
C   10 TEMP ABOVE 360 F
      10 HLIO=((((4.560246D-11*T-1.0315357D-7)*T+9.41244D-5)*T-4.2753836D-2
      1      )*T+10.673802)*T-904.11736
      RETURN
C   20 TEMP BELOW 360 F
      20 HLIO=((((9.6350315D-13*T-7.3618778D-10)*T+4.8553836D-7)*T
      1      -1.1516996D-4)*T+1.0688084)*T-32.179105
      RETURN
      END

```

HLIO 100
HLIO 101
HLIO 102
HLIO 105
HLIO 110
HLIO 115
HLIO 120
HLIO 125
HLIO 126
HLIO 130
HLIO 135
HLIO 140
HLIO 141
HLIO 145
HLIO 150

```

FUNCTION SLIO(T)
IMPLICIT REAL*8(A-H,D-Z)
CALCULATES ENTROPY (BTU/LBM/F) OF SATURATED WATER FROM 50F TO 670F
C   WESTINGHOUSE ALGORITHM, TRANS ASME V80, NO4, MAY, 1958, P.959
COORDINATES SHIFTED FROM ORIGINAL OF TO 360F OR 560F
      IF(T>450,120,20,10
C   10 TEMP ABOVE 450
      10 TB=(T-560.)/110.
      SLIO=(((((3.4265601D-3*TB+3.9726934D-31*TB-2.1403201D-31)*TB
      1      -1.0108801D-31*TB+5.7828937D-31*TB+7.5137762D-31*TB
      2      +e.136908251*TB+e.76209767
      RETURN
C   20 TEMP BELOW 450
      20 TB=(T-360.)/130.
      SLIO=(((((e.01234655*TB+e.012035893)*TB-3.670358D-31)*TB-6.072333D-3
      1      1*TB+e.0342516971)*TB-e.045979941)*TB+e.396796461*TB+e.51575516
      RETURN
      END

```

SLIO 100
SLIO 101
SLIO 102
SLIO 105
SLIO 106
SLIO 110
SLIO 115
SLIO 120
SLIO 125
SLIO 126
SLIO 127
SLIO 130
SLIO 135
SLIO 140
SLIO 145
SLIO 146
SLIO 150
SLIO 155

```

FUNCTION VLIO(TF)
IMPLICIT REAL*8(A-H,O-Z)
CALCULATES SPECIFIC VOLUME (CU.FT./LBM) OF SATURATED WATER FROM 32F TO 6VLIO 100
C KEENAN + KEYES, 1951, P.21, EQ.18 VLIO 101
T=374.11-(TF-32.)/1.8 VLIO 105
CRT=T**.333333333333 VLIO 110
DEN=CRT*.1342489-3.9462630-3*T+1. VLIO 115
VLTO=(T**3*7.48908D-13-1.203374D-3)*T-.3151548*CRT+.19751 VLIO 120
1 * .0160185/DEN VLIO 125
RETURN VLIO 126
END VLIO 130
VLIO 135

```

```

FUNCTION TSAT(P)
IMPLICIT REAL*8(A-H,O-Z)
CALCULATES SATURATION TEMPERATURE (DEG F) OF WATER, .178PSIA TO CRITICALTSAT 100
C KEENAN + KEYES, 1951, P.14, EQ.11 + 12 TSAT 101
T=500. TSAT 105
CORR=.2 TSAT 110
FOP=LOG(3206.37858/P)/2.30258509 TSAT 115
GOTO1 TSAT 120
C 4 TEMP BELOW 140C = 284F TSAT 125
4 CORR=((1.1702379D-8*TK*TK+5.86826D-3)*TK+3.2437814) TSAT 130
1 /(2.1878462D-3*TK+1.) TSAT 135
1 TS=.1165.09/(FOP/CORR+1.) TSAT 136
IF(DABS(TS-T)>.01)10,10,2 TSAT 140
2 T=TS TSAT 145
TK=(1165.09-T)/1.8 TSAT 150
IF(P>52.41814,4,3 TSAT 155
C 3 TEMP ABOVE 140C = 284 F TSAT 160
3 CORR=((6.56444D-11*TK+7.515484D-9)*TK*TK+4.14113D-21*TK TSAT 165
1 +3.346313)/(1.+1.3794481D-2*TK) TSAT 170
GO TO 1 TSAT 171
10 TSAT=TS-.459.69 TSAT 175
RETURN TSAT 180
END TSAT 181
TSAT 185

```

```

FUNCTION PSAT(TF)
IMPLICIT REAL*8(A-H,O-Z)
CALCULATES SATURATION PRESSURE IN PSIA AT TEMPERATURE TF PSAT 100
C DEGREES FAHRENHEIT 50 TO 705.4 PSAT 101
PSAT 102
C KEENAN AND KEYES PAGE 14 PSAT 105
T=(TF+459.69)/1.8 PSAT 110
X=647.27-T PSAT 115
TF(X-234.11)20,10,10 PSAT 120
C 10 TEMP BELOW 140 CENT PSAT 125
10 A=((1.1702379D-8*X*X+5.86826D-3)*X+3.2437814) PSAT 130
1 /(2.1878462D-3*X+1.) PSAT 135
GO TO 20 PSAT 136
C 20 TEMP ABOVE 140 CENT PSAT 140
20 A=((6.56444D-11*X+7.515484D-9)*X*X+4.14113D-21*X+3.346313) PSAT 145
1 /(1.3794481D-2*X+1.) PSAT 150
30 PSAT=DEXP(-2.30258509*A*X/T)*3206.37858 PSAT 151
RETURN PSAT 155
END PSAT 160
PSAT 165

```

```

SUBROUTINE PROPHS(PX,TX,VX,AMX,MX,HX,SX)
IMPLICIT REAL*8(A-H,O-Z)
C SUBPROGRAM FOR STEAM PROPERTIES WHEN H AND S ARE KNOWN PROP 0
C P1=2500. PROP 1
P2=0. PROP 2
D055 IT=1,100 PROP 3
C GUESS PX AND FIND REGION OF MOLLIER CHART PROP 4
PX=(P1+P2)/2. PROP 5
TX=TSAT(PX) PROP 6
SGX=SVAP(TX,PX) PROP 7
TF(SX-SGX)20,30,40 PROP 8
PROP 9
PROP 10

```

```

C WET
20 AMX=(SGX-SX)/(SGX-SLIQ(TX))
MX=1
HXP=(1.0-AMX)*HVAP(TX,PX)+AMX*HLIQ(TX)
GOTO50
C DRY AND SATURATED
30 AMX=0.0
MX=2
HXP=HVAP(TX,PX)
GOTO50
C SUPERHEATED
40 AMX=0.0
MX=3
TX=TVAPS(PX,SX)
HXP=HVAP(TX,PX)
C CHECK HXP AGAINST HX
50 ADH=DABS(HX-HXP)
IF(ADH.LE..01)GOTO60
C RE-SET P1 OR P2
IF(HX.LT.HXP)GOTO54
P2=PX
GOTO55
54 P1=PX
55 CONTINUE
PRINT 56,ADH
56 FORMAT('0-SUBROUTINE PROPHS-ENTHALPY DID NOT CONVERGE, ADH =',
1PD14.6)
C FIND VX
60 VX=VVAP(TX,PX)
IF(MX.GT.1)GOTO70
VX=(1.0-AMX)*VX+AMX*VLIQ(TX)
70 RETURN
END

```

PROP 101
PROP 110
PROP 120
PROP 130
PROP 140
PROP 141
PROP 150
PROP 160
PROP 170
PROP 180
PROP 181
PROP 190
PROP 200
PROP 210
PROP 220
PROP 221
PROP 230
PROP 240
PROP 241
PROP 250
PROP 260
PROP 270
PROP 280
PROP 290
PROP 300
PROP 310
PROP 311
PROP 312
PROP 320
PROP 330
PROP 340
PROP 350
PROP 360

```

SUBROUTINE PROPRH(A,M,S,V,T,M,P,H)
IMPLICIT REAL*8(A-H,D-Z)
C SUBPROGRAM FOR STEAM PROPERTIES WHEN P AND H ARE KNOWN
C
T=TSAT(P)
HG=HVAP(T,P)
IF(H-HG).GT.2.E-3
C WET STEAM
1 M=1
AM=(HG-H)/((HG-HLIQ(T)))
S=(1.0-AM)*SVAP(T,P)+AM*SLIQ(T)
V=(1.0-AM)*VVAP(T,P)+AM*VLIQ(T)
RETURN
C SATURATED STEAM
2 M=2
GOTO4
C SUPERHEATED STEAM
3 M=3
T=TVAPH(P,H)
4 AM=0.0
S=SVAP(T,P)
V=VVAP(T,P)
RETURN
END

```

PROP 0
PROP 10
PROP 20
PROP 21
PROP 30
PROP 40
PROP 50
PROP 60
PROP 61
PROP 70
PROP 80
PROP 90
PROP 100
PROP 110
PROP 111
PROP 120
PROP 130
PROP 131
PROP 140
PROP 150
PROP 160
PROP 170
PROP 180
PROP 190
PROP 200

```

SUBROUTINE PROPPS(M,H,T,V,M,P,S)
IMPLICIT REAL*8(A-H,D-Z)

C SUBPROGRAM FOR STEAM PROPERTIES WHEN P AND S ARE KNOWN
C
T=TSAT(P)
SG=SVAP(T,P)
IF(S-SG)1,2,3
C WET STEAM
1 M=1
AM=(SG-S)/(SG-SLIO(T))
H=(1.0-AM)*HVAP(T,P)+AM*HLIO(T)
V=(1.0-AM)*VVAP(T,P)+AM*VLIO(T)
RETURN
C SATURATED STEAM
2 M=2
GOTO4
C SUPERHEATED STEAM
3 M=3
T=TVAPS(P,S)
4 AM=0.0
H=HVAP(T,P)
V=VVAP(T,P)
RETURN
END
      PROP   0
      PROP   10
      PROP   20
      PROP   21
      PROP   30
      PROP   40
      PROP   50
      PROP   60
      PROP   61
      PROP   70
      PROP   80
      PROP   90
      PROP  100
      PROP  110
      PROP  111
      PROP  120
      PROP  130
      PROP  131
      PROP  140
      PROP  150
      PROP  160
      PROP  170
      PROP  180
      PROP  190
      PROP  200

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