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MERCURY COSTS IN HERMEX PROCESS

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Mr. S. A. Lawroski, of Argonne National Laboratory, raised the question of the cost of mercury holdup and replacement in the Hermex process. He thought a low limiting concentration of <1 wt % uranium in mercury would make the cost of mercury inventory prohibitive. This seemed to be an important consideration, therefore I determined the cost per pound of uranium for mercury inventory and annual mercury process loss. Certain assumptions were made for fuel geometry in order to calculate dissolving surface available. Dissolution to 0.5 wt % U was assumed to take advantage of the fast initial rate (straight line portion of dissolving curve). The ratio of mercury to uranium in the dissolver was calculated from the rate equation to determine whether or not the geometry of the dissolver would be reasonable.

The calculations follow:

Hermex Dissolver Design Information

A. Assumptions Made in the Hermex Process

1. Continuous processing through washing and drying.
2. Dissolution to 0.5 wt % uranium.
3. No mercury holdup on hot filter.
4. Diameter of dekad fuel elements, 0.15 in.
5. Ten percent of the mercury inventory per year will be lost in process.
6. The mercury inventory is three times holdup.
7. Interest charges, 4% per annum.

B. Hermex Dissolver Design

Fuel, dekad uranium rods 0.15 in. dia.

Cross section of rods, $\text{cm}^2 = (0.15 \times 2.54)^2 \left(\frac{\pi}{4}\right) = 0.114 \text{ cm}^2$.

Density of U = 18.7 g/cm^3 .

Weight of rod per cm length = $(0.114)(18.7) = 2.13 \text{ g}$.

Length of rod per pound U = $453.6/2.13 = 213 \text{ cm}$.

Approximate surface of 1 pound of rods (not counting ends) = $(3.1416)(0.381)(213) = 255 \text{ cm}^2/\text{lb U}$.

The optimum time holdup in the dissolver is 30 min. To determine whether or not the dissolver pot would have a reasonable geometry with this holdup, use is made of the dissolution rate equation, $dC/dt = ks/m(C_s - C)$, where C is the molal concentration of U in Hg at time t ; C_s is the molal concentration at saturation (0.047 m); k is the specific rate constant, $\text{g}\cdot\text{Hg}/\text{cm}^2/\text{min}$; s is the U surface, cm^2 ; m is the mass of mercury used in the dissolution, g ; and t is the time, min . Integrated between $C = 0$ at $t = 0$ and C_s , it becomes $\log(1 - \frac{C}{C_s}) = \frac{-ks}{m} t$. At $0.5 \text{ wt } \% \text{ U in Hg}$ C is 0.021 m ; $k = 2.2 \text{ g Hg}/\text{cm}^2 \text{ U}/\text{min}$; $t = 30 \text{ min}$; $C/C_s = 0.448$; $1 - C/C_s = 0.552$. Solving, $s/m = 0.009 \text{ cm}^2 \text{ U}/\text{g Hg}$. For the U shapes assumed the mercury to uranium mass ratio in the dissolver is $255 \text{ cm}^2/\text{lb U}/0.009 = 24,800 \text{ g} = 62.5 \text{ lb Hg}/\text{lb U}$.

this is nonsense

The uranium which will be dissolved by 62.5 lb Hg in 30 min at $0.5 \text{ wt } \% \text{ U}$ is 142 g . The mercury required to dissolve 1 lb U in such a dissolver is 200 lb , and the dissolver uranium heel, $3.2 \text{ lb}/\text{lb U}/\text{hr}$. The mercury feed rate would be $200 \text{ lb}/\text{hr}$.

The flowsheet and mercury holdup analysis is shown in Fig. 1.

C. Calculation of Mercury Holdup Per Pound Uranium

From the flowsheet (Fig. 1)

$200 \text{ lb Hg}/\text{lb U}/\text{hr}$ for $3/4 \text{ hr} = 150 \text{ lb Hg}/\text{hr}$. ✓

$33 \text{ lb Hg}/\text{lb U}/\text{hr}$ for $1 1/4 \text{ hr} = 41 \text{ lb Hg}/\text{hr}$. ✓

Average Hg holdup/ $\text{lb U}/\text{hr} = 191 \text{ lb}$

Mercury inventory ($3 \times$ holdup) = $573 \text{ lb Hg}/\text{lb U}/\text{hr}$.

Mercury investment ($\$3/\text{lb Hg}$) = $\$1720/\text{lb U}/\text{hr}$.

Interest for 1 hr at 4% per annum = $1720 \times .04/6000 \text{ hr}/\text{yr}$
= $1.15\text{¢}/\text{lb U}$.

Mercury losses (10% of inventory)/ $\text{yr} = 573 \times .10 = 57.3 \text{ lb Hg}/\text{lb U}/\text{hr}/\text{yr}$.

[Redacted]

Replacement cost = $57.3 \times 3/6000 = 2.87\text{¢/lb U.}$

Total mercury cost = $2.87 + 1.15 = 4.0\text{¢/lb U.}$

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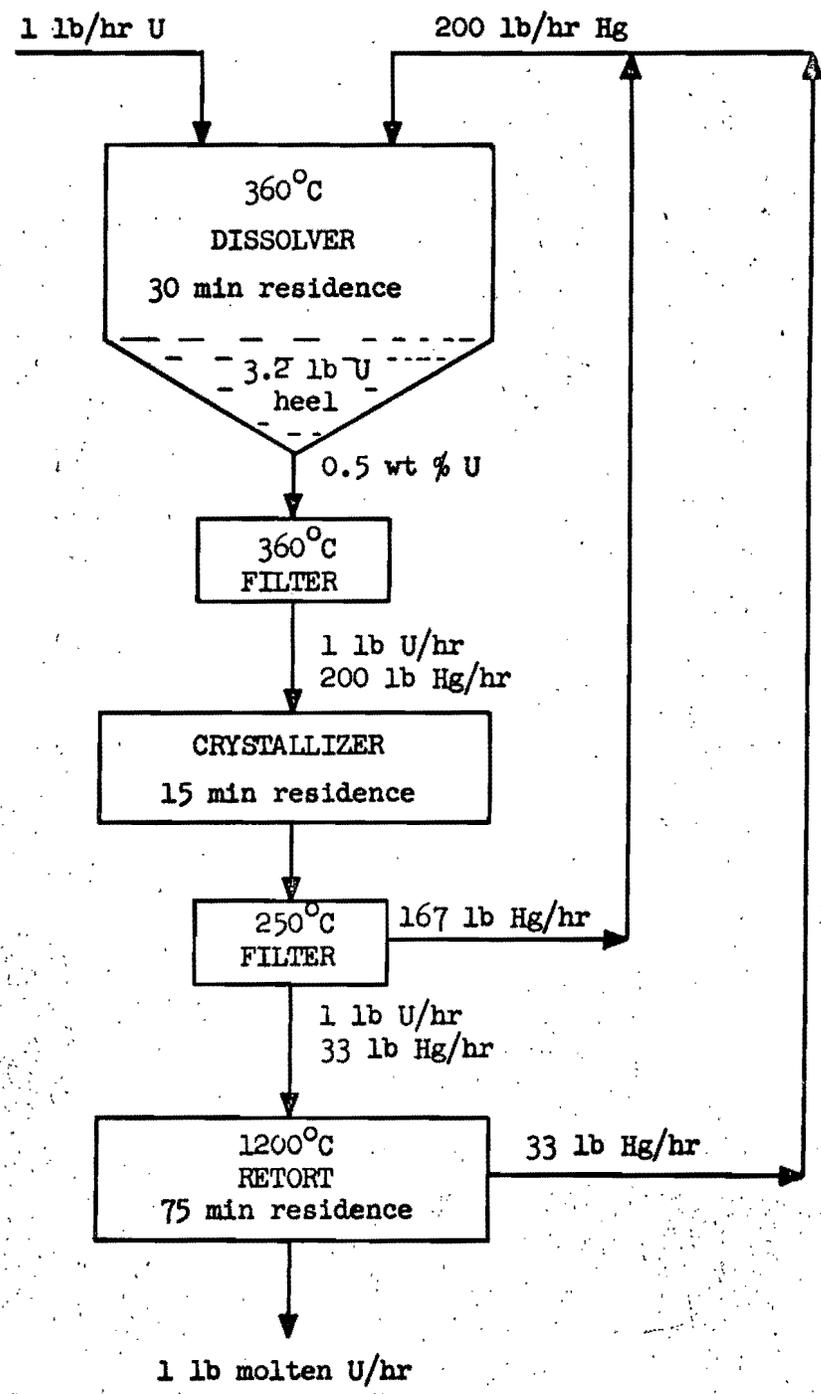


Fig. 1. HERMEX FLOWSHEET AND MERCURY HOLDUP ANALYSIS

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